



Deliverable 15.3: Training materials

Work Package 15 ConCorD

This project has received funding from the European Union's Horizon 2020 research and innovation programme 2014-2018 under grant agreement N°847593.



Document information

Project Acronym	EURAD
Project Title	European Joint Programme on Radioactive Waste Management
Project Type	European Joint Programme (EJP)
EC grant agreement No.	847593
Project starting / end date	1st June 2019 – 30 May 2024
Work Package No.	15
Work Package Title	CONTainer CORrosion under Disposal conditions
Work Package Acronym	ConCorD
Deliverable No.	15.3
Deliverable Title	Training materials
Lead Beneficiary	SCK CEN
Contractual Delivery Date	30/04/2022
Actual Delivery Date	22/03/2023
Type	Document
Dissemination level	Public
Authors	Kristel Mijndonckx (SCK CEN)

To be cited as:

Mijndonckx K. (2023): Training Materials of WP15 ConCorD. Final version as of 22.03.2023 of deliverable D15.3 of the HORIZON 2020 project EURAD. EC Grant agreement no: 847593.

Disclaimer

All information in this document is provided "as is" and no guarantee or warranty is given that the information is fit for any particular purpose. The user, therefore, uses the information at its sole risk and liability. For the avoidance of all doubts, the European Commission or the individual Colleges of EURAD (and their participating members) has no liability in respect of this document, which is merely representing the authors' view.

Acknowledgement

This document is a deliverable of the European Joint Programme on Radioactive Waste Management (EURAD). EURAD has received funding from the European Union's Horizon 2020 research and innovation programme under grant agreement No 847593.

Status of deliverable		
	By	Date
Delivered (Lead Beneficiary)	K. Mijndonckx	17/03/2023
Verified (WP Leader)	N. Diomidis	22/03/2023
Reviewed (Reviewers)	F. King, M. Behazin, B. Kalinowski, C. Stephan-Scherb, C. Lilja, J. Binns, P. Keech, V. Maillot, S. Suzuki, T. Glas	30/01/2023
Approved (PMO)	K. Smith	09/05/2023
Submitted to EC (Coordinator)	Andra	10/05/2023

Executive Summary

This report provides an overview of presentations that can be used as training materials related to the ConCorD WP. The topics and content are based on the SotA document (deliverable 15.1). The first topic gives an overview of the evolution of the environmental conditions focussed on the near-field and their impact on corrosion behaviour. More detailed information about the transient conditions, the impact of irradiation and microbial processes is provided. The second topic gives an overview of novel technological concepts for container materials and the third topic summarizes prediction tools for assessment of long-time barrier integrity and the integration of corrosion phenomena in performance assessments. The outline and learning outcomes for each of the topics is given in this report. In general, the target audience for all lectures are people that have already a basic background in corrosion but want to learn more details about a topic outside their field. For example, beginning PhD students/scientist in the field. This enables people to gain a broad basic background in studying corrosion processes related to nuclear waste disposal. A more detailed technical training or practical sessions that cover different modelling tools can be developed depending on the needs of future Training Event organizers. In principle, the slides can be used on a stand-alone basis to learn the main principles, however, more subtle information will be gained if the slides are taught by a lecturer. At the end of the project, the lectures will be updated with relevant results. The slides are attached as annexes.

Table of content

Executive Summary	4
Table of content	5
1. Introduction	6
1.1 Environmental factors altering the corrosion behaviour	6
1.1.1 Content of the presentation	6
1.1.2 Learning outcomes	7
1.1.3 Further reading	7
1.2 Novel technologies technological concepts for container materials	7
1.2.1 Content	7
1.2.2 Learning outcomes	8
1.2.3 Further reading	8
1.3 Prediction tools for assessment of long-time barrier integrity	8
1.3.1 Content	8
1.3.2 Learning outcomes	8
1.3.3 Further reading	8
Appendix A. Environmental factors altering the corrosion behaviour	10
Appendix B. Novel technologies technological concepts for container materials	Error! Bookmark not defined.
Appendix C. Prediction tools for assessment of long-time barrier integrity	10
References	11

1. Introduction

Even though the feasibility and safety of established container solutions has been demonstrated, recent progress in understanding of materials and processes has shown that optimisation of container manufacturing and performance is possible. Widespread interest in repository optimisation exists and relevant projects are ongoing, e.g., WP HITEC and the HotBENT experiment in Grimsel. The systematic exploration of novel materials, while placing existing solutions in a broader context, will provide a solid state-of-the-art for the pursuit of container optimisation according to available geology, disposal concept and regulatory requirements. The testing of alternative container materials, their mechanical structural response and corrosion resistance will also bring new insights into novel technical solutions for container design.

To further increase the knowledge base and reduce remaining uncertainties, WP ConCorD aims to:

- Explore the potential of novel/advanced container materials and processes for optimisation of container performance within the engineered barrier system.
- Increase/extend the understanding of complex/coupled interfacial processes influencing container performance under repository relevant conditions, with a focus on irradiation-accelerated corrosion, microbial activity and degradation during nearfield transients, at varying scales.
- Mechanistic process understanding and development of predictive models, which will incorporate system variability and will lead to improved performance assessments addressing identified safety needs

During and after the end of ConCorD various national programs will be able to evaluate cooperatively the long-term behaviour of container materials to such an extent as to be able to ensure confidence in the performance of engineered barriers. Such progress will particularly benefit early-stage programmes and those with a small inventory. An Expert Review Group will review and provide guidance on the scientific work performed. Emphasis will be given to issues relevant to end user needs and repository implementation, while ensuring that the generation of information is implementable and useful for performance assessment.

This document contains the content and learning outcomes of training materials developed based on the SotA (deliverable 15.1). Training materials are in the form of lectures divided over three topics related to the ConCorD project. In general, the target audience for all lectures are people that have already a basic background in corrosion but want to learn more details about a topic outside their field. For example, beginning PhD students/scientist in the field. This enables people to gain a broad basic background in studying corrosion processes related to nuclear waste disposal. A more detailed technical training or practical sessions that cover different modelling tools can be developed depending on the needs of future Training Event organizers. In principle, the slides can be used on a stand-alone basis to learn the main principles, however, more subtle information will be gained if the slides are taught by a lecturer. At the end of the project, the lectures will be updated with relevant results.

1.1 Environmental factors altering the corrosion behaviour

1.1.1 Content of the presentation

The corrosion of container materials has been extensively studied under constant conditions. However, the environment is not constant but the evolution of the chemistry of the repository environment in the period after its closure will depend mainly on two factors: the engineered barriers and the composition of groundwater. After facility closure, the thermal phase of the development of the repository is important, with a typical example being the saturation rate of the bentonite barrier leading to swelling and the development of mechanical stresses on the container. Such transients can be further influenced by attempts at repository footprint optimisation (e.g., increased container heat production). The corrosion of container materials has been usually studied under constant conditions and the translation of the

experimental result to the evolving chemical, mechanical and redox conditions of the early post-closure period needs to be verified and complemented. The different transients and their impact on the corrosion behaviour are discussed in the lectures. Two different transients, studied in the ConCorD project are discussed in more detail, namely possible effect of irradiation and of microbial activity. An example of a large *in situ* experiment studying several transient processes is given at the end of the presentation.

1.1.2 Learning outcomes

Following this presentation, people are able to:

- Understand the function of the waste container in the disposal of HLW/SF
- Sum up the different container concepts & expected exposure conditions
- Identify the different transient process in the near field environment
- Comprehend the effect of transient processes on the corrosion behavior of waste containers

1.1.3 Further reading

- <https://www.ejp-eurad.eu/publications/eurad-d151-concord-initial-sota>
- Allard, T., E. Balan, G. Calas, C. Fourdrin, E. Morichon and S. Sorieul (2012). Radiation-induced defects in clay minerals: A review. *Nuclear Instruments and Methods in Physics Research Section B: Beam Interactions with Materials and Atoms* 277: 112-120
- Dixon, D. (2019). Review of the THMC Properties of MX-80 Bentonite, NWMO-TR-2019-07
- Enning, D. and J. Garrelfs (2014). Corrosion of iron by sulfate-reducing bacteria: new views of an old problem. *Appl Environ Microbiol* 80: 1226-1236
- King, F. (2017). 13 - Nuclear waste canister materials: Corrosion behavior and long-term performance in geological repository systems. *Geological Repository Systems for Safe Disposal of Spent Nuclear Fuels and Radioactive Waste (Second Edition)*. M. J. Apted and J. Ahn, Woodhead Publishing: 365-408
- King, F. and M. Behazin (2021). A Review of the Effect of Irradiation on the Corrosion of Copper-Coated Used Fuel Containers. *Corrosion and Materials Degradation* 2: 678-707
- Fraser King, 2017 - 13 - Nuclear waste canister materials: Corrosion behavior and long-term performance in geological repository systems - doi.org/10.1016/B978-0-08-100642-9.00013-X
- Landolt, D., A. W. Davenport, J. H. Payer and D. W. Shoosmith (2011). A Review of Materials and Corrosion Issues Regarding Canisters for Disposal of Spent Fuel and High-Level Waste in Opalinus Clay. *ChemInform* 42

1.2 Novel material solutions for nuclear waste disposal container concepts

1.2.1 Content of the presentation

The understanding of degradation mechanisms and resulting container durability estimates is mature and has been demonstrated for already existing disposal concepts envisaging the use of copper (e.g. Sweden, Finland, Canada) and carbon steel in a clay environment (e.g. France, Switzerland, Japan, Czech Republic). These materials are called “traditional materials” but are also the ones on which “corrosion allowance” designs are based, i.e. materials that corrode slowly and in a uniform and predictable manner. The second type of materials under consideration are the “novel materials”, which

are typically subject to very low corrosion rates. The lecture provides an overview of different “novel materials” under consideration and corrosion processes are discussed in more detail.

1.2.2 Learning outcomes

Following this presentation, people are able to:

- Understand the advantages & disadvantages of the use of ceramic/metallic materials in nuclear waste disposal
- Identify the current knowledge gaps of the use of ceramic/metallic materials in nuclear waste disposal
- Give an historical overview of the use of ceramic materials in nuclear waste disposal

1.2.3 Further reading

- <https://www.ejp-eurad.eu/publications/eurad-d151-concord-initial-sota>
- Holdsworth, S.R., 2013. Ceramic Material Solutions for Nuclear Waste Disposal Canisters. NAGRA report NAB12-45.
- Holdsworth, S.R. 2018. Alternative coating Materials as Corrosion Barriers for SF and HLW Disposal Canisters. NAGRA report NAB18-19.
- INTERNATIONAL ATOMIC ENERGY AGENCY (2006). Development of Specifications for Radioactive Waste Packages. IAEA-TECDOC-1515. IAEA, Vienna

1.3 Prediction tools for assessment of long-time barrier integrity

1.3.1 Content of the presentation

Development of models to predict container failure times and the development of a thorough mechanistic understanding of the corrosion processes involved have progressed significantly over the past 40 years. An overview is given of several generic corrosion modelling approaches for general corrosion and localized corrosion. For each, the assumptions, advantages and disadvantages are given. Furthermore, detailed examples of modelling processes related to copper and steel containers are provided. In a second part of the lecture, detailed information on integration of corrosion processes in performance assessments are discussed.

1.3.2 Learning outcomes

Following this presentation, people are able to:

- Identify principles of different modelling approaches for several corrosion processes
- Understand advantages & disadvantages of different modelling tools
- Compare processes relevant for copper & steel containers
- Understand how corrosion processes can be integrated in performance assessments (PA)
- Get acquainted with basic modelling tools

1.3.3 Further reading

- <https://www.ejp-eurad.eu/publications/eurad-d151-concord-initial-sota>
- King, F. (2014). "Predicting the Lifetimes of Nuclear Waste Containers." JOM 66(3).

EURAD Deliverable 15.3 – Training Materials

- King, F. and M. Kolář (2018). "Lifetime Predictions for Nuclear Waste Disposal Containers." Corrosion 75(3).
- Nagra. (2002). Demonstration of disposal feasibility for spent fuel, vitrified high-level waste and long-lived intermediate-level waste. Nagra Report NTB 02-05.
- Performance Assessment for the Proposed High-Level Radioactive Waste Repository at Yucca Mountain, Nevada <https://www.sciencedirect.com/journal/reliability-engineering-and-system-safety/vol/122/suppl/C>
- Svensk Kärnbränslehantering, A. (2010). Corrosion calculations report for the safety assessment SR-Site. SKB TR-10-66

Appendix A. Environmental factors altering the corrosion behaviour

Appendix B. Novel material solutions for nuclear waste disposal container concepts

Appendix C. Prediction tools for assessment of long-time barrier integrity

References

- Abdelouas A., Alonso U., Bernier-Latmani R., Bosch C., Cherkouk A., Dobrev D., Fernández A.M., Finck N., Gaggiano R., Havlová V., Hesketh J., Idiart A., Mijnenonckx K., Montoya V., Muñoz A.G., Padovani, C., Pont A., Rajala P., Riba O., Sarrasin L., Sayenko S., Smart N., Texier-Mandoki N., Wersin P. (2022): Initial State-of-the-Art of WP ConCorD. Final version as of 17.08.2022 of deliverable D15.1 of the HORIZON 2020 project EURAD. EC Grant agreement no: 847593. <https://www.ejp- eurad.eu/publications/eurad-d151-concord-initial-sota>
- H12 : Project to establish the scientific and technical basis for HLW disposal in Japan : second progress report on research and development for the geological disposal of HLW in Japan, Japan Nuclear Cycle Development Institute
- Allard, T., E. Balan, G. Calas, C. Fourdrin, E. Morichon and S. Sorieul (2012). Radiation-induced defects in clay minerals: A review. *Nuclear Instruments and Methods in Physics Research Section B: Beam Interactions with Materials and Atoms* 277: 112-120
- Alkhimov, A. P., V. F. Kosarev, S. V. Klinkov, A. A. Sova, G. V. Trubacheev and V. N. Zaikovskiy (2012). Conical separation zone formation at impingement of supersonic jet on obstacle under cold spraying. *Thermophysics and Aeromechanics* 19: 225-232
- Baroux, C. and C. Martin (2016). Summary Report of the preliminary feasibility study for ceramic HLW overpacks. Andra Report CG.RP.ASCM.13.0023
- Bataillon, C., F. Bouchon, C. Chainais-Hillairet, C. Desgranges, E. Hoarau, F. Martin, S. Perrin, M. Tupin and J. Talandier (2010). Corrosion modelling of iron based alloy in nuclear waste repository. *Electrochimica Acta* 55: 4451-4467
- Briggs, S., C. Lilja and F. King (2021). Probabilistic model for pitting of copper canisters. *Materials and Corrosion* 72: 308-316
- Červinka, R., Vašíček, R., a kolektiv 2018. Kompletní charakterizace bentonitu. BCV 2017, SÚRAO TZ 419/2019
- Crusset, D., V. Deydier, S. Necib, J.-M. Gras, P. Combrade, D. Féron and E. Burger (2017). Corrosion of carbon steel components in the French high-level waste programme: evolution of disposal concept and selection of materials. *Corrosion Engineering, Science and Technology* 52: 17-24
- Diler, E., V. Leblanc, H. Gueuné, N. Larché, V. Deydier, Y. Linard, D. Crusset and D. Thierry (2021). Potential influence of microorganisms on the corrosion of carbon steel in the French high- and intermediate-level long-lived radioactive waste disposal context. *Materials and Corrosion* 72: 218-234
- Dixon, D. (2019). Review of the THMC Properties of MX-80 Bentonite, NWMO-TR-2019-07
- Enning, D. and J. Garrelfs (2014). Corrosion of iron by sulfate-reducing bacteria: new views of an old problem. *Appl Environ Microbiol* 80: 1226-1236
- Faraji, G., H. S. Kim and H. T. Kashi (2018). Introduction. Severe Plastic Deformation. G. Faraji, H. S. Kim and H. T. Kashi, Elsevier: 1-17
- Fernández, A.M. (2019). Gas and water sampling from the FEBEX in situ test. NAGRA Report NAB 16-13
- Giroud, N., Y. Tomonaga, P. Wersin, S. Briggs, F. King, T. Vogt and N. Diomidis (2018). On the fate of oxygen in a spent fuel emplacement drift in Opalinus Clay. *Applied Geochemistry* 97: 270-278
- Gómez-Espina, R. and M. V. Villar (2010). Geochemical and mineralogical changes in compacted MX-80 bentonite submitted to heat and water gradients. *Applied Clay Science* 47: 400-408
- Gu, B. X., L. M. Wang, L. D. Minc and R. C. Ewing (2001). Temperature effects on the radiation stability and ion exchange capacity of smectites. *Journal of Nuclear Materials* 297: 345-354

Guo, X., S. Gin, P. Lei, T. Yao, H. Liu, D. K. Schreiber, D. Ngo, G. Viswanathan, T. Li, S. H. Kim, J. D. Vienna, J. V. Ryan, J. Du, J. Lian and G. S. Frankel (2020). Self-accelerated corrosion of nuclear waste forms at material interfaces. *Nature Materials* 19: 310-316

Hadi, J., P. Wersin, V. Serneels and J.-M. Greneche (2019). Eighteen years of steel–bentonite interaction in the FEBEX in situ test at the Grimsel Test Site in Switzerland. *Clays and Clay Minerals* 67: 111-131

Hall, D. S., M. Behazin, W. Jeffrey Binns and P. G. Keech (2021). An evaluation of corrosion processes affecting copper-coated nuclear waste containers in a deep geological repository. *Progress in Materials Science* 118: 100766

Holdsworth, S.R., (2013). Ceramic Material Solutions for Nuclear Waste Disposal containers. NAGRA report NAB12-45.

Holdsworth, S.R., (2014). Feasibility evaluation study of candidate container solutions for the disposal of spent nuclear fuel and high-level waste-A status review. NAGRA report NAB14-90.

Holdsworth, S.R. (2018). Alternative coating Materials as Corrosion Barriers for SF and HLW Disposal containers. NAGRA report NAB18-19.

INTERNATIONAL ATOMIC ENERGY AGENCY (2006). Development of Specifications for Radioactive Waste Packages. IAEA-TECDOC-1515. IAEA, Vienna

Idiart, A., Coene, E. (2019). Modelling diffusion through compacted bentonite in the BHA vault. SKB R-19-10

Itälä, A. and M. Olin (2011). Chemical Evolution of Bentonite Buffer in a Final Repository of Spent Nuclear Fuel During the Thermal Phase. *Nuclear Technology* 174: 342-352

Johnson, L. and F. King (2003). Canister options for the disposal of spent fuel. Switzerland. NTB--02-11

Johnson, L. and F. King (2008). The effect of the evolution of environmental conditions on the corrosion evolutionary path in a repository for spent fuel and high-level waste in Opalinus Clay. *Journal of Nuclear Materials* 379: 9-15

Kerber, A. and J. Knorr (2013). SiC encapsulation of high level waste for long-term immobilization. *Atw Internationale Zeitschrift fuer Kernenergie* 58: 8-13

King, F. (2007). Overview of a carbon steel container corrosion model for a deep geological repository in sedimentary rock. *Nuclear Waste Management Organization NWMO TR-2007-01*

King, F. (2009). Microbiologically Influenced Corrosion of Nuclear Waste Containers. *Corrosion* 65: 233-251

King, F. (2011). TR-1069 Critical review of the literature on the corrosion of copper by water

King, F. (2014). Predicting the Lifetimes of Nuclear Waste Containers. *JOM* 66: 526-537

King, F., Sanderson, D., Watson, S. (2016). Durability of High-Level Waste and Spent Fuel Disposal Containers – an overview of the combined effect of chemical and mechanical degradation mechanisms. AMEC Report 17697/TR/03

King, F. (2017). 13 - Nuclear waste canister materials: Corrosion behavior and long-term performance in geological repository systems. Geological Repository Systems for Safe Disposal of Spent Nuclear Fuels and Radioactive Waste (Second Edition). M. J. Apted and J. Ahn, Woodhead Publishing: 365-408

King, F., L. Ahonen, C. Taxen, U. Vuorinen and L. Werme (2001). Copper corrosion under expected conditions in a deep geologic repository. Sweden: 171

King, F. and M. Behazin (2021). A Review of the Effect of Irradiation on the Corrosion of Copper-Coated Used Fuel Containers. *Corrosion and Materials Degradation* 2: 678-707

- King, F. and M. Kolář (2018). Lifetime Predictions for Nuclear Waste Disposal Containers. *Corrosion* 75: 309-323
- King, F., M. Kolar and P. Maak (2008). Reactive-transport model for the prediction of the uniform corrosion behaviour of copper used fuel containers. *Journal of Nuclear Materials* 379: 133-141
- King, F., M. Kolář, I. Puigdomenech, P. Pitkänen and C. Lilja (2021). Modeling microbial sulfate reduction and the consequences for corrosion of copper canisters. *Materials and Corrosion* 72: 339-347
- Knorr, J., W. Lippmann, A. M. Reinecke, R. Wolf, A. Kerber and A. Wolter (2008). SiC encapsulation of (V)HTR components and waste by laser beam joining of ceramics. *Nuclear Engineering and Design* 238: 3129-3135
- Kursten, B., D. D. Macdonald, N. R. Smart and R. Gaggiano (2017). Corrosion issues of carbon steel radioactive waste packages exposed to cementitious materials with respect to the Belgian supercontainer concept. *Corrosion Engineering, Science and Technology* 52: 11-16
- Landolt, D., A. W. Davenport, J. H. Payer and D. W. Shoesmith (2011). A Review of Materials and Corrosion Issues Regarding Canisters for Disposal of Spent Fuel and High-Level Waste in Opalinus Clay. *ChemInform* 42
- Larker, H. (1980). Method of containing spent nuclear fuel or high-level nuclear fuel waste. United States: Medium: X; Size: Pages: v 2008-2002-2007
- Leupin, O. X., N. R. Smart, Z. Zhang, M. Stefanoni, U. Angst, A. Papafotiou and N. Diomidis (2021). Anaerobic corrosion of carbon steel in bentonite: An evolving interface. *Corrosion Science* 187: 109523
- Lloyd, A. C., R. J. Schuler, J. J. Noël, D. W. Shoesmith and F. King (2004). The Influence of Environmental Conditions and Passive Film Properties on the MIC of Engineered Barriers in the Yucca Mountain Repository. *MRS Online Proceedings Library (OPL)* 824: CC1.9
- Maanoja, S., A.-M. Lakaniemi, L. Lehtinen, L. Salminen, H. Auvinen, M. Kokko, M. Palmroth, E. Muuri and J. Rintala (2020). Compacted bentonite as a source of substrates for sulfate-reducing microorganisms in a simulated excavation-damaged zone of a spent nuclear fuel repository. *Applied Clay Science* 196: 105746
- Nagra. (2002). Demonstration of disposal feasibility for spent fuel, vitrified high-level waste and long-lived intermediate-level waste. Nagra Report NTB 02-05.
- Necib, S., N. Diomidis, P. Keech and M. Nakayama (2017). Corrosion of carbon steel in clay environments relevant to radioactive waste geological disposals, Mont Terri rock laboratory (Switzerland). *Swiss Journal of Geosciences* 110: 329-342
- Padovani, C., S. J. Williams and P. Wood (2012). An introduction to package evolution and criticality research studies relevant to the UK disposal programme. *Mineralogical Magazine* 76: 2881-2890
- Performance Assessment for the Proposed High-Level Radioactive Waste Repository at Yucca Mountain, Nevada <https://www.sciencedirect.com/journal/reliability-engineering-and-system-safety/vol/122/suppl/C>
- Pospiskova, I., D. Dobrev, M. Kouril, J. Stouilil, D. Novikova, P. Kotnour and O. Matal (2017). Czech national programme and disposal canister concept. *Corrosion Engineering, Science and Technology* 52: 6-10
- Rajala, P., L. Carpén, M. Vepsäläinen, M. Raulio, E. Sohlberg and M. Bomberg (2015). Microbially induced corrosion of carbon steel in deep groundwater environment. *Frontiers in Microbiology* 6
- Rebata-Landa, V. and J. C. Santamarina (2006). Mechanical limits to microbial activity in deep sediments. *Geochemistry, Geophysics, Geosystems* 7
- Rockhvarger, A.E., Khizh, A.B. 1998. Large size, thick-walled ceramic containers. NUCON SYSTEMS INC, Patent WO9844834

- Schindelholz, E., B. E. Risteen and R. G. Kelly (2014). Effect of Relative Humidity on Corrosion of Steel under Sea Salt Aerosol Proxies: I. NaCl. *Journal of The Electrochemical Society* 161: C450
- Shi, J., J. Wang and D. D. Macdonald (2015). Prediction of primary water stress corrosion crack growth rates in Alloy 600 using artificial neural networks. *Corrosion Science* 92: 217-227
- Shoesmith, D. W. (2006). Assessing the Corrosion Performance of High-Level Nuclear Waste Containers. *Corrosion* 62: 703-722
- Svemar, C., Johannesson, L-E., Gram, Svensson, D. (2016). Opening and retrieval of outer section of Prototype Repository at Äspö Hard Rock Laboratory. SKB TR-13-22
- Svensk Kärnbränslehantering, A. (2010) - Metodval - utvärdering av strategier och system för att ta hand om använt kärnbränsle. SKB R-10-25
- Svensk Kärnbränslehantering, A. (2010). Corrosion calculations report for the safety assessment SR-Site. SKB TR-10-66
- Villar, M. V., A. M. Fernández, R. Gómez, J. F. Barrenechea, F. J. Luque, P. L. Martín and J. M. Barcala (2007). State of a bentonite barrier after 8 years of heating and hydration in the laboratory. *Materials Research Society Symposium Proceedings*
- Villar, M. V., R. Gómez-Espina and A. Lloret (2010). Experimental investigation into temperature effect on hydro-mechanical behaviours of bentonite. *Journal of Rock Mechanics and Geotechnical Engineering* 2: 71-78
- Villar, M. V. and A. Lloret (2008). Influence of dry density and water content on the swelling of a compacted bentonite. *Applied Clay Science* 39: 38-49
- Vinsot, A., M. Lundy and Y. Linard (2017). O₂ Consumption and CO₂ Production at Callovian-oxfordian Rock Surfaces. *Procedia Earth and Planetary Science* 17: 562-565
- Wang, L., S. Fan, H. Sun, B. Ji, B. Zheng, J. Deng, L. Zhang and L. Cheng (2020). Pressure-less joining of SiCf/SiC composites by Y₂O₃-Al₂O₃-SiO₂ glass: Microstructure and properties. *Ceramics International* 46: 27046-27056
- Weetjens, E., Marivoet, J., Govaerts, J., & Leterme, B. (2012). Preparatory Safety Assessment: Conceptual model description of the reference case. SCK CEN Reports, ER-215
- Wersin, P., P. Alt-Epping, M. Pekala, P. Pitkänen and M. Snellman (2017). Modelling Sulfide Fluxes and Cu Canister Corrosion Rates in the Engineered Barrier System of a Spent Fuel Repository. *Procedia Earth and Planetary Science* 17: 722-725
- Wilson, J., Savage, D., Bond, A., Watson, S., Pusch, R., Bennett, D. (2011). Bentonite. A Review of key properties, processes and issues for consideration in the UK context. Quintesa report QRS-1378ZG-1
- Yamaji, K. (2015). Issues of HLW Disposal in Japan. Nuclear Back-end and Transmutation Technology for Waste Disposal: Beyond the Fukushima Accident. K. Nakajima. Tokyo, Springer Japan: 279-287
- Yoshikawa, H., S. Lee and T. Matsui (2009). A Sampling Method and Data Evaluation of Archaeological Samples to Support Long-Term Corrosion Prediction. *Corrosion* 65: 227-232

ENVIRONMENTAL FACTORS AFFECTING THE CORROSION PROCESS



This project has received funding from the European Union's Horizon 2020 research and innovation programme 2014-2018 under grant agreement N°847593



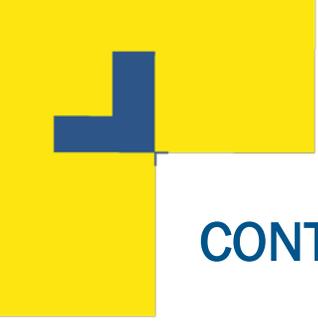
LEARNING OUTCOMES

- Understand the function of the waste container in the disposal of HLW/SF
- Sum up the different container concepts & expected exposure conditions
- Identify the different transient process in the near field environment
- Comprehend the effect of transient processes on the corrosion behavior of waste containers



CONTENT

- Introduction
- Thermal transients
- Pore water transients
- Redox transients
- Saturation transients
- Mechanical transients
- Transitional processes involving gas generation
- Effects of irradiation
- Effects of Microbial processes
- Example of an integrated test
- Summary

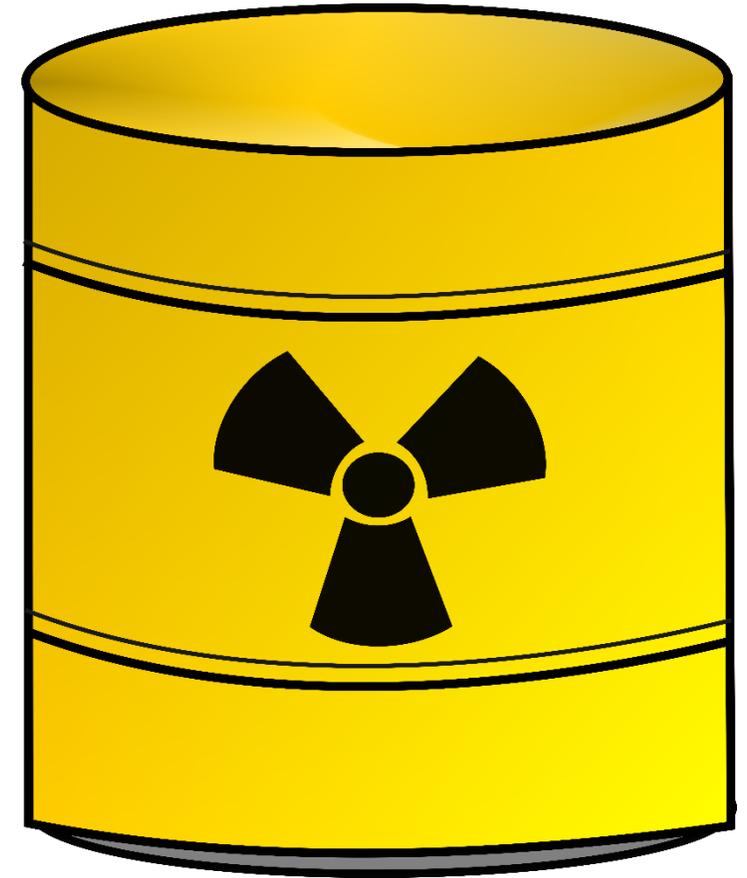


CONTENT

- **Introduction**
- Thermal transients
- Pore water transients
- Redox transients
- Saturation transients
- Mechanical transients
- Transitional processes involving gas generation
- Effects of irradiation
- Effects of Microbial processes
- Example of an integrated test
- Summary

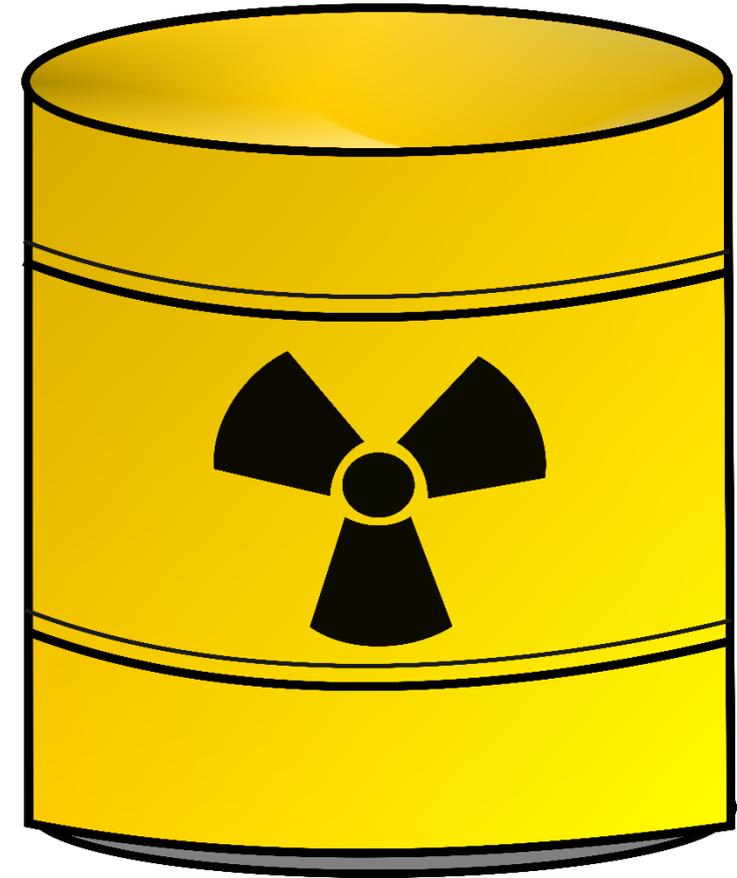
WASTE CONTAINER IS ESSENTIAL IN THE DISPOSAL OF HLW/SF

- Designed to contain, physically protect, and/or radiologically shield the waste form during the various activities involved during the period from conditioning until emplacement and closure of a disposal facility



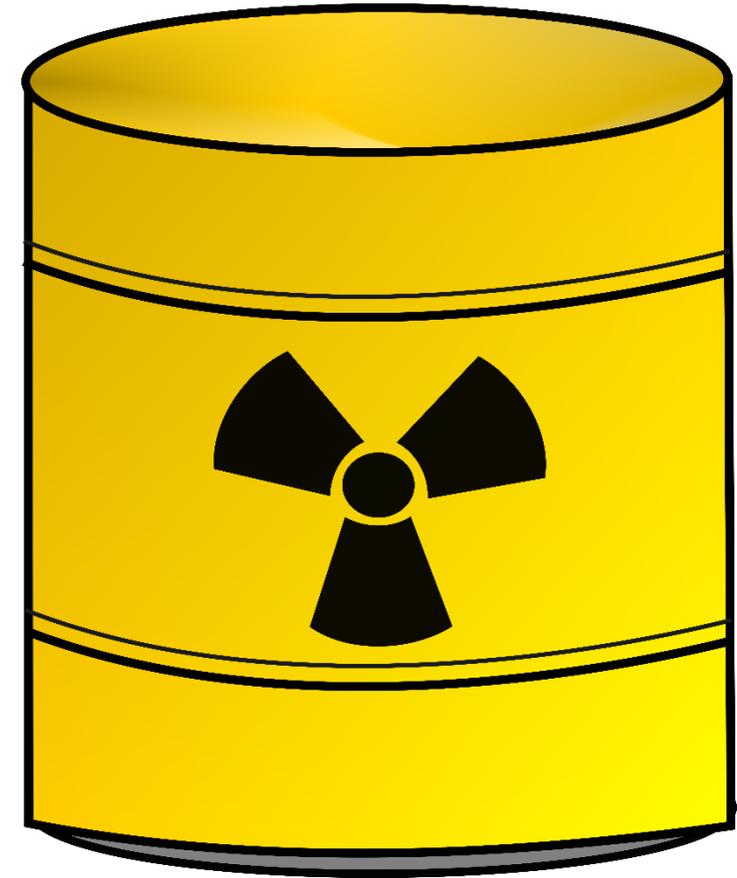
WASTE CONTAINER IS ESSENTIAL IN THE DISPOSAL OF HLW/SF

- Designed to contain, physically protect, and/or radiologically shield the waste form during the various activities involved during the period from conditioning until emplacement and closure of a disposal facility
- In some cases the container also plays a role in the near field containment of the radionuclides for a certain period after closure



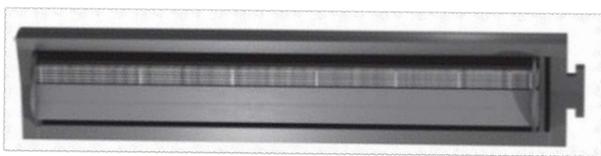
WASTE CONTAINER IS ESSENTIAL IN THE DISPOSAL OF HLW/SF

- Designed to contain, physically protect, and/or radiologically shield the waste form during the various activities involved during the period from conditioning until emplacement and closure of a disposal facility
- In some cases the container also plays a role in the near field containment of the radionuclides for a certain period after closure
- Main parameters & control methods according to IAEA (2006):
 - Material itself
 - Geometric shape & dimensions
 - Design & operation of internal features
 - Lifting arrangements
 - Container internal corrosion
 - Container strength
 - Selection of surface coating & texture
 - Design & operation of closure features
 - Resistance to environmental conditions

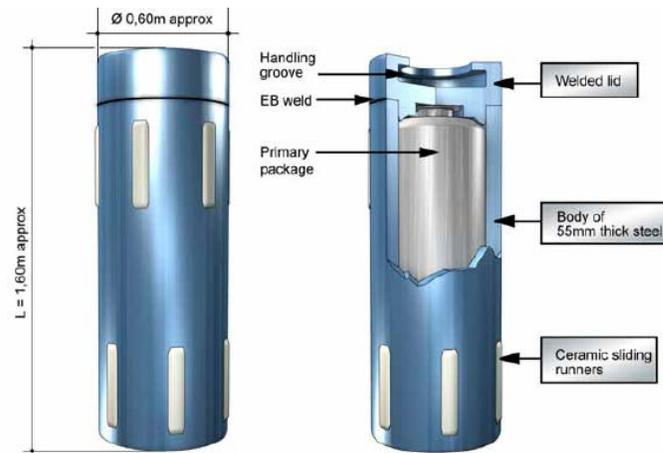


DIFFERENT TYPES OF WASTE CONTAINERS EXIST

- Configuration & life time requirements depend on
 - Type of waste
 - Surrounding geological structure
 - Material used to increase canister integrity



NAGRA



ANDRA



SKB/POSIVA

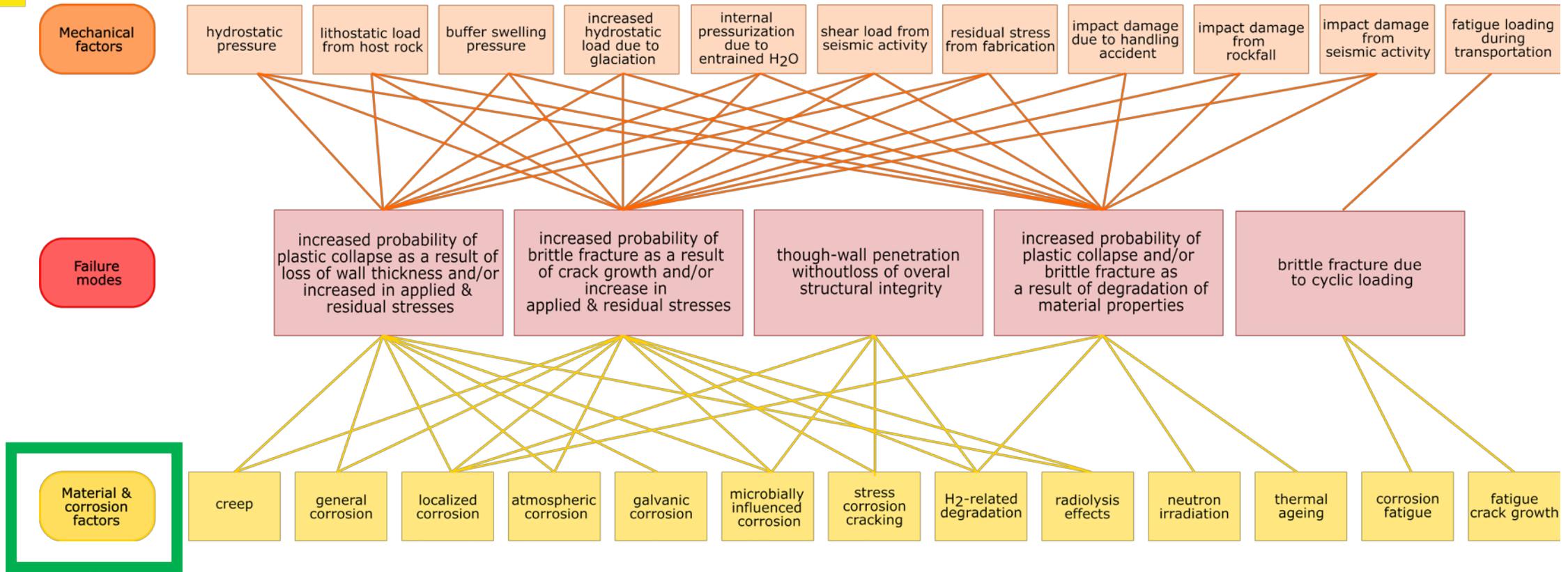


CANADA

DIFFERENT CONTAINER CONCEPTS & EXPECTED EXPOSURE CONDITIONS

WMO	Container concept	Estimated or target lifetime (year)	Nominal buffer dry density (g/cm ³)	Max. canister temp. (°C)	Time to full nearfield saturation (year)	Max. surface absorbed dose (Gy/h)	Expected mechanical loads (MPa)
SKB	Cu-cast Fe	>10 ⁶	1.6	95	Few 10s – few 1000	0.2	15 50 (glacial)
Posiva	Cu-cast Fe	>10 ⁶	1.55	95	Few 10s – few 1000	0.3	14 50 (glacial)
Andra	Carbon steel	>500	Cementitious buffer on the external face of the casing	90		10	10 Mpa (on casing)
Ondraf-Niras	Carbon steel	Several thousand	Cementitious buffer	100	5-10 to few 1000	25	8
Nagra	Carbon steel	10 000	>1.45	±120	Few centuries	0.2	22-29 max
SURAO	Carbon steel	10 000	1.4	95	100	0.3	20
NMWO	Cu-coated steel	>10 ⁶	1.6	85	50-5000 ~ host rock dependent	0.8	15 45 (glacial)
NUMO	Carbon steel	> 1000	1.6	100	<1000 ~ host rock dependent	0.006-0.011	11 (hard rock)

FAILURE MODES OF CONTAINERS



Detailed knowledge of mechanisms under environmental conditions in the near-field of the container is necessary

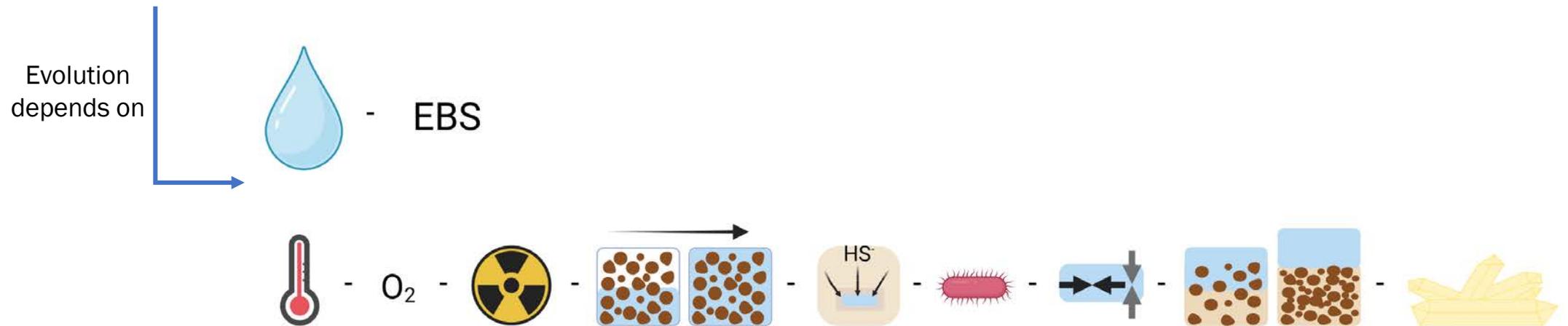


CORROSION UNDER ENVIRONMENTAL TRANSIENTS

- Corrosion behavior depends on:
 - Container material
 - Environmental conditions

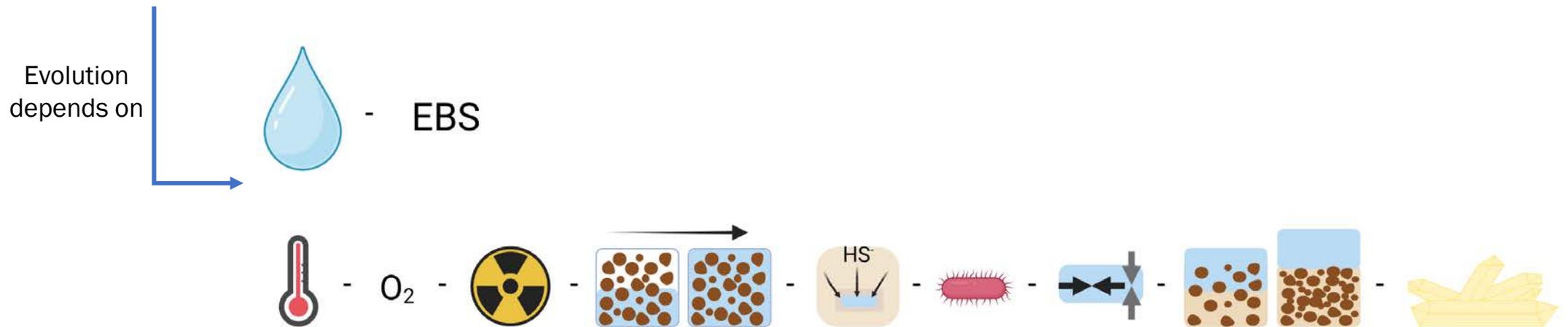
CORROSION UNDER ENVIRONMENTAL TRANSIENTS

- Corrosion behavior depends on:
 - Container material
 - Environmental conditions



CORROSION UNDER ENVIRONMENTAL TRANSIENTS

- Corrosion behavior depends on:
 - Container material
 - Environmental conditions



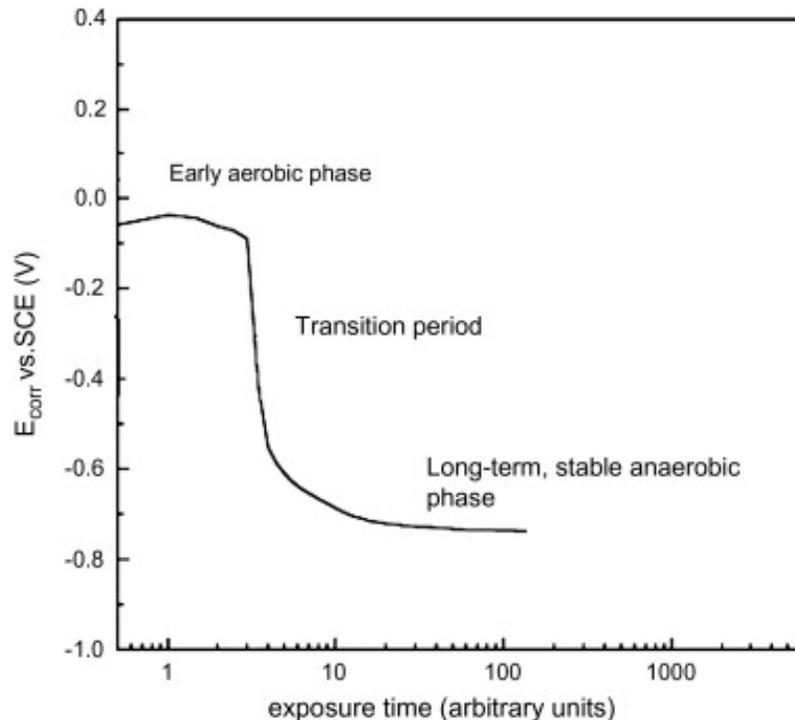
- Constant conditions extensively studied ↔ transient conditions

CORROSION UNDER ENVIRONMENTAL TRANSIENTS

- Corrosion evolutionary path (CEP) → time-dependent corrosion behavior of the container
 - Closely tied to the evolution of environmental conditions
 - Corrosion potential (E_{corr}) is a useful indicator

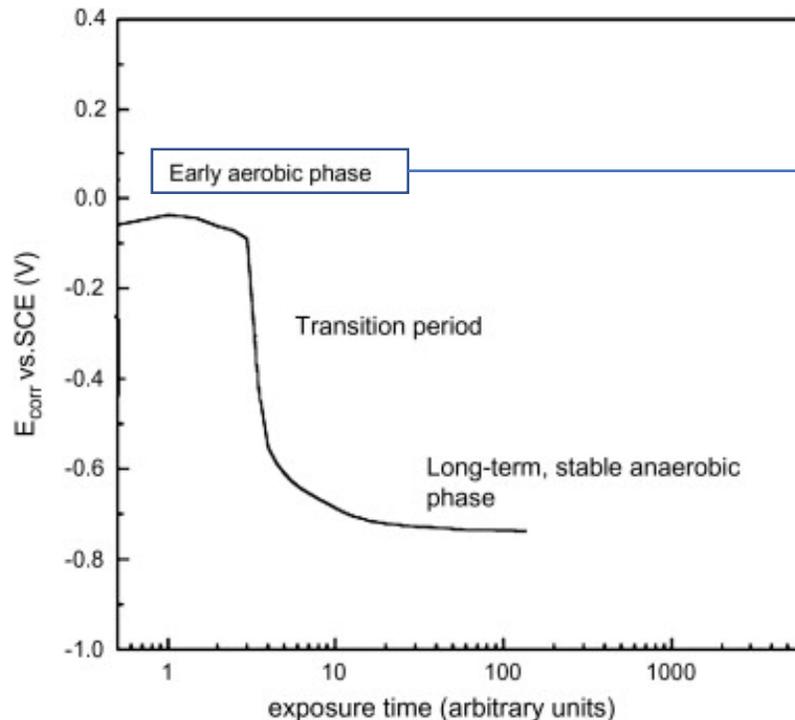
CORROSION UNDER ENVIRONMENTAL TRANSIENTS

- Corrosion evolutionary path (CEP) → time-dependent corrosion behavior of the container
 - Closely tied to the evolution of environmental conditions
 - Corrosion potential (E_{corr}) is a useful indicator
 - Example: Evolution in sealed repository containing a limited amount of entrapped O_2 .



CORROSION UNDER ENVIRONMENTAL TRANSIENTS

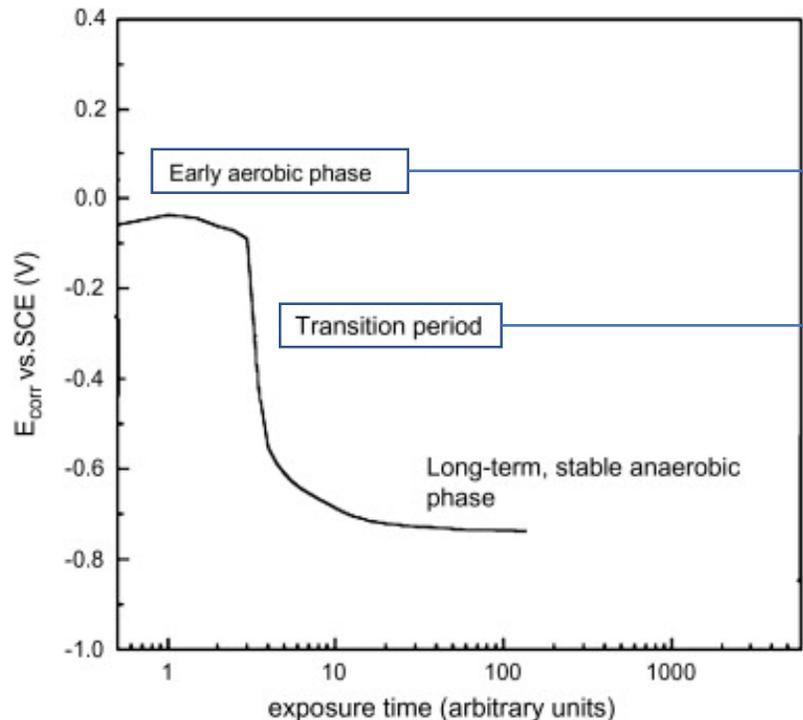
- Corrosion evolutionary path (CEP) → time-dependent corrosion behavior of the container
 - Closely tied to the evolution of environmental conditions
 - Corrosion potential (E_{corr}) is a useful indicator
 - Example: Evolution in sealed repository containing a limited amount of entrapped O_2 .



E_{CORR} is relatively noble (positive) because of the cathodic reduction of O_2 and because of the possible spatial separation of anodic and cathodic processes

CORROSION UNDER ENVIRONMENTAL TRANSIENTS

- Corrosion evolutionary path (CEP) → time-dependent corrosion behavior of the container
 - Closely tied to the evolution of environmental conditions
 - Corrosion potential (E_{corr}) is a useful indicator
 - Example: Evolution in sealed repository containing a limited amount of entrapped O_2 .

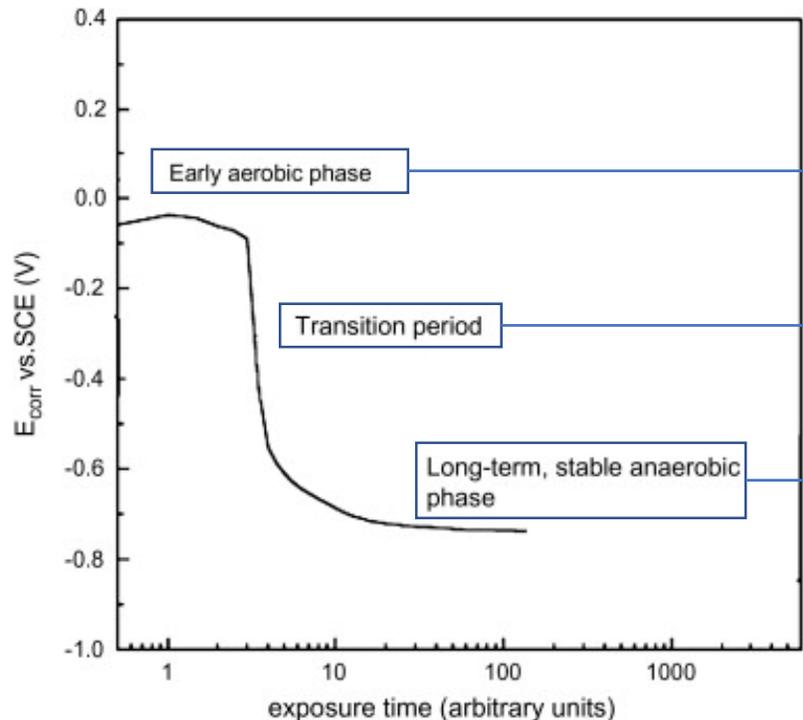


E_{CORR} is relatively noble (positive) because of the cathodic reduction of O_2 and because of the possible spatial separation of anodic and cathodic processes

Fe(III) corrosion products formed during the aerobic phase are reductively dissolved to Fe(II) species

CORROSION UNDER ENVIRONMENTAL TRANSIENTS

- Corrosion evolutionary path (CEP) → time-dependent corrosion behavior of the container
 - Closely tied to the evolution of environmental conditions
 - Corrosion potential (E_{corr}) is a useful indicator
 - Example: Evolution in sealed repository containing a limited amount of entrapped O_2 .



E_{CORR} is relatively noble (positive) because of the cathodic reduction of O_2 and because of the possible spatial separation of anodic and cathodic processes

Fe(III) corrosion products formed during the aerobic phase are reductively dissolved to Fe(II) species

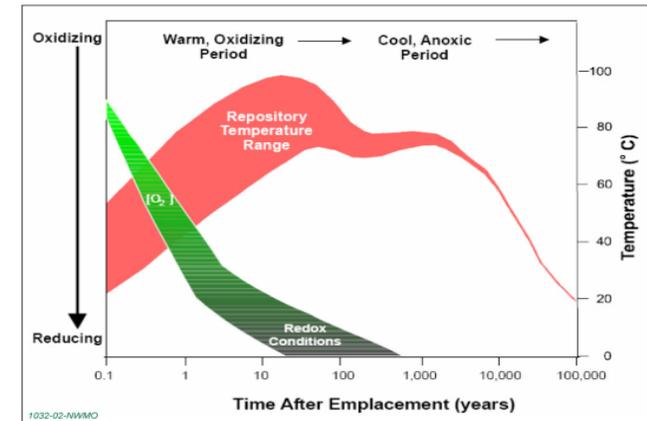
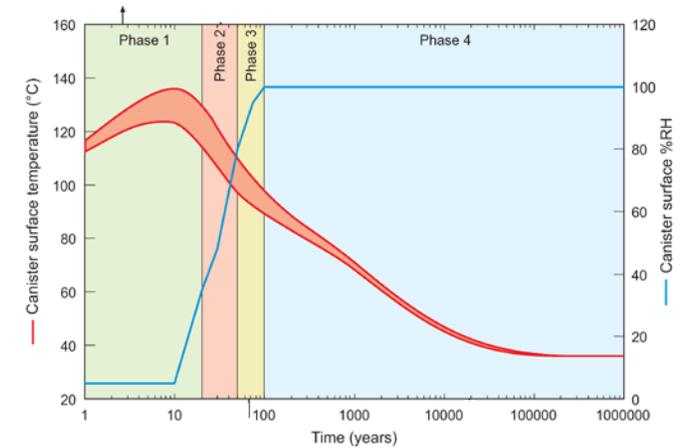
relative rates of Fe dissolution and the reduction of H_2O , resulting in E_{CORR} values close to the $\text{H}_2/\text{H}_2\text{O}$ equilibrium

CONTENT

- Introduction
- **Thermal transients**
- Pore water transients
- Redox transients
- Saturation transients
- Mechanical transients
- Transitional processes involving gas generation
- Effects of irradiation
- Effects of Microbial processes
- Example of an integrated test
- Summary

THERMAL TRANSIENT

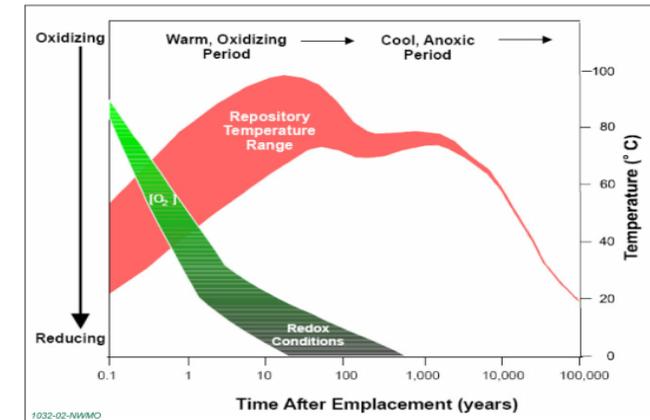
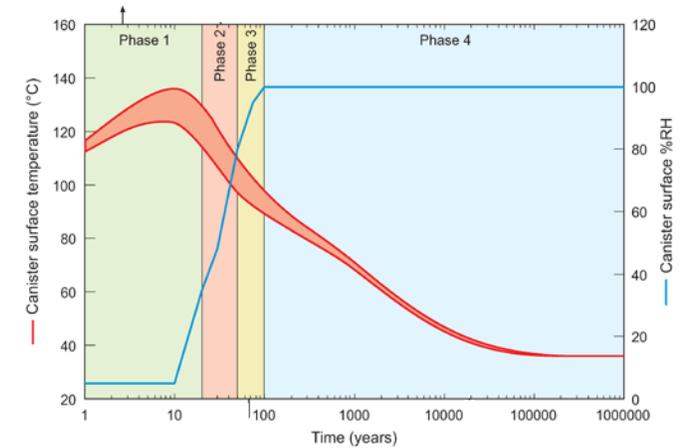
- Sources:
 - Ambient temperature \uparrow with depth
 - Waste
- Longest transient but with slower changes



THERMAL TRANSIENT

- Sources:
 - Ambient temperature \uparrow with depth
 - Waste
- Longest transient but with slower changes

Thermal gradient between container/buffer – buffer/rock boundary

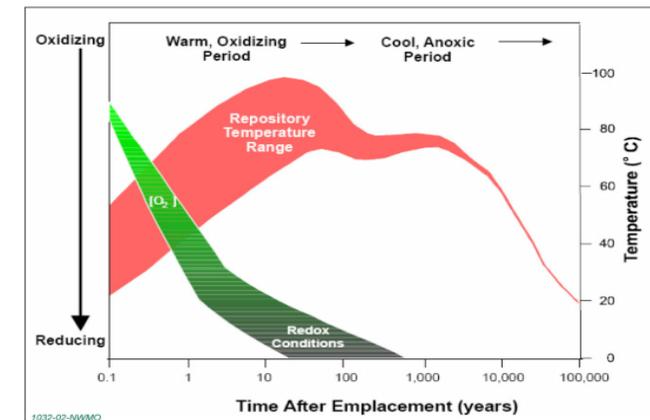
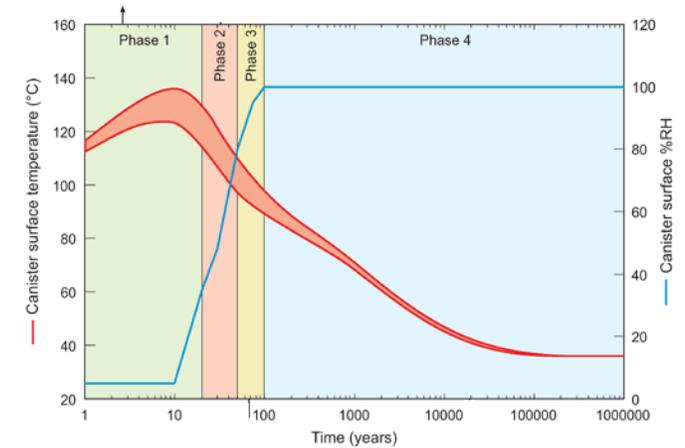


THERMAL TRANSIENT

- Sources:
 - Ambient temperature \uparrow with depth
 - Waste
- Longest transient but with slower changes

Thermal gradient between container/buffer – buffer/rock boundary

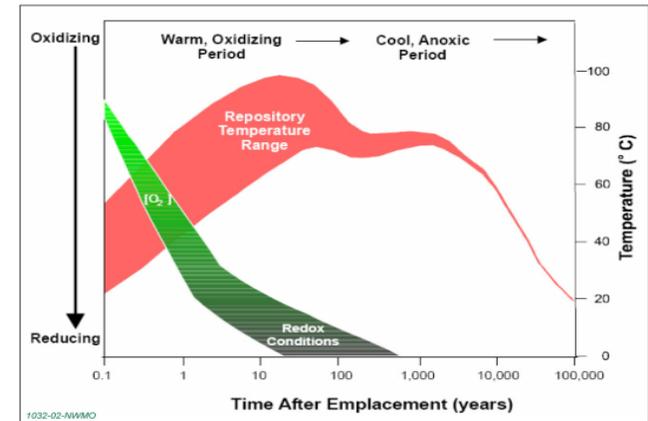
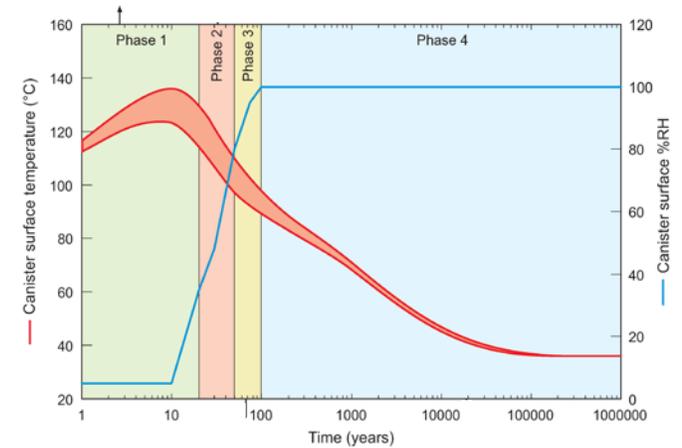
Concentration gradient among aqueous solutes



THERMAL TRANSIENT

- Sources:
 - Ambient temperature \uparrow with depth
 - Waste
- Longest transient but with slower changes

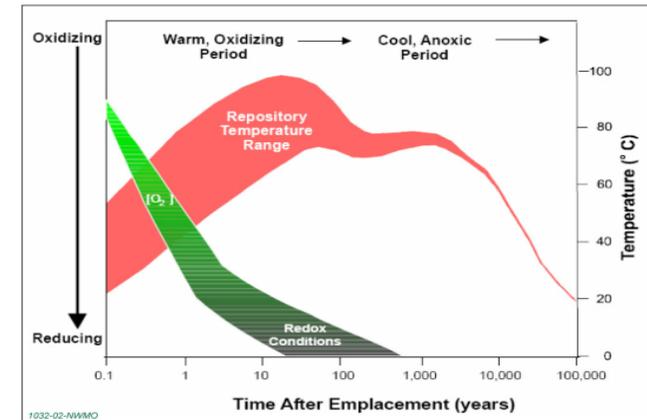
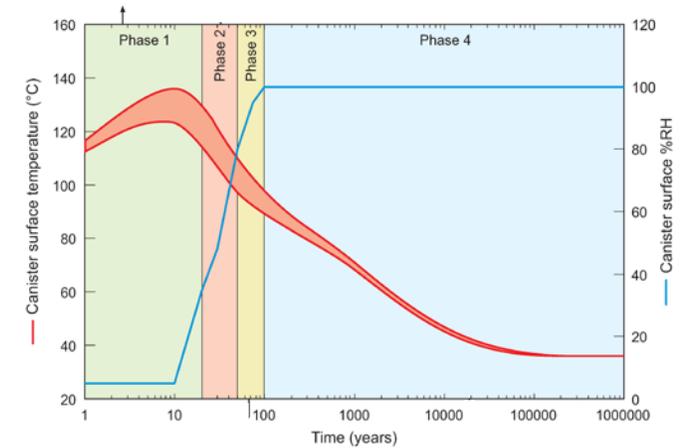
- Thermal gradient between container/buffer – buffer/rock boundary
- Concentration gradient among aqueous solutes
- Secondary minerals can precipitate onto surfaces of primary clay minerals



THERMAL TRANSIENT

- Sources:
 - Ambient temperature \uparrow with depth
 - Waste
- Longest transient but with slower changes

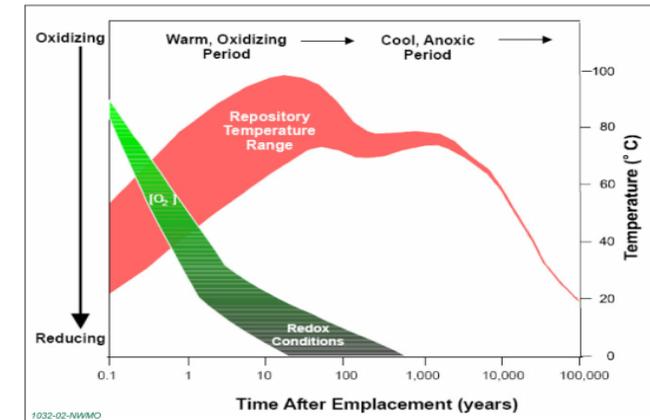
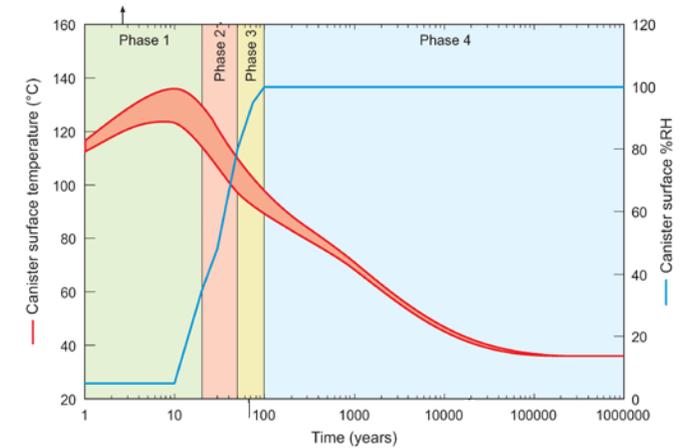
- Thermal gradient between container/buffer – buffer/rock boundary
- Concentration gradient among aqueous solutes
- Secondary minerals can precipitate onto surfaces of primary clay minerals
- If significant changes in mass transfer \rightarrow individual clay particles cemented in secondary solids



THERMAL TRANSIENT

- Sources:
 - Ambient temperature \uparrow with depth
 - Waste
- Longest transient but with slower changes

- Thermal gradient between container/buffer – buffer/rock boundary
- Concentration gradient among aqueous solutes
- Secondary minerals can precipitate onto surfaces of primary clay minerals
- If significant changes in mass transfer \rightarrow individual clay particles cemented in secondary solids
- Could irreversibly alter the swelling pressure & other properties of the buffer





CONTENT

- Introduction
- Thermal transients
- **Pore water transients**
- Redox transients
- Saturation transients
- Mechanical transients
- Transitional processes involving gas generation
- Effects of irradiation
- Effects of Microbial processes
- Example of an integrated test
- Summary



PORE WATER TRANSIENTS

- Corrosion → contact of water with container surface
- Chemistry is modified by backfill/groundwater interactions
 - ↳ Typically highly compacted bentonite or cementitious backfill

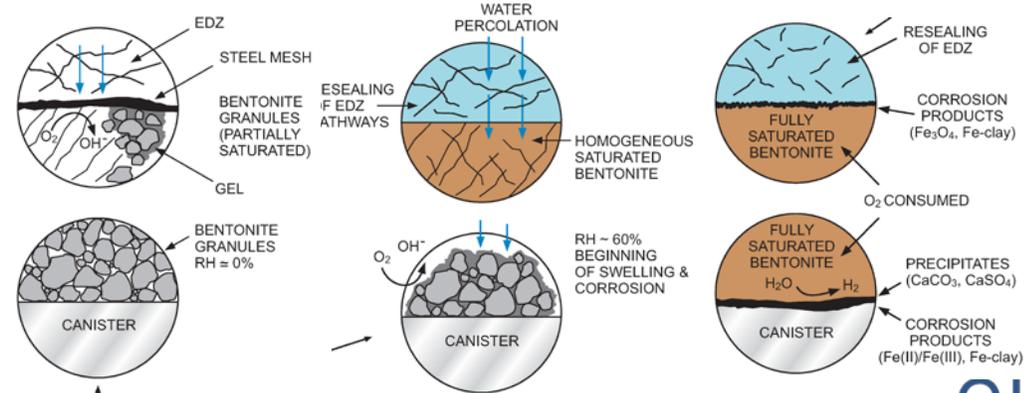


PORE WATER TRANSIENTS

- Corrosion → contact of water with container surface
- Chemistry is modified by backfill/groundwater interactions
 - ↳ Typically highly compacted bentonite or cementitious backfill
- Nature of the pore fluid?
 - Multi-porosity model ↔ Donnan Equilibrium processes?

PORE WATER TRANSIENTS

- Corrosion → contact of water with container surface
- Chemistry is modified by backfill/groundwater interactions
 - ↳ Typically highly compacted bentonite or cementitious backfill
- Nature of the pore fluid?
 - Multi-porosity model ↔ Donnan Equilibrium processes?
- In non-isothermal unsaturated conditions water at container from:
 - Episodic fracture flow
 - Dripping into open drifts
 - Deliquescence of salt contaminants



PORE WATER TRANSIENTS

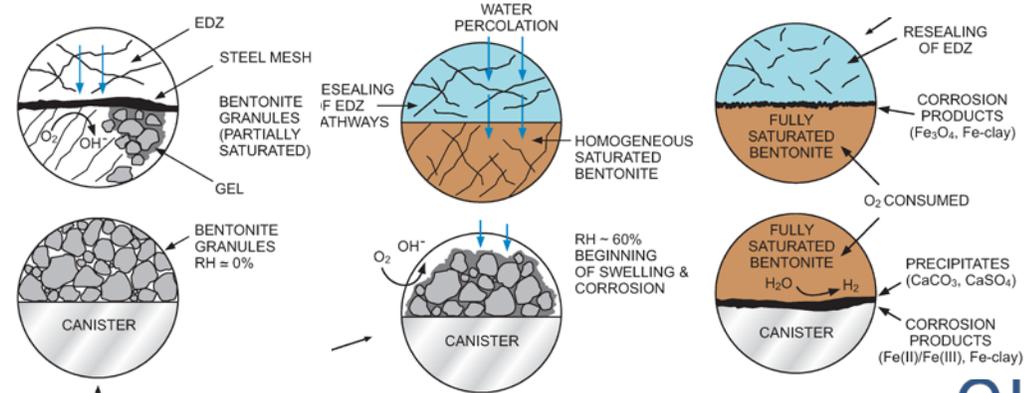
- Corrosion → contact of water with container surface
- Chemistry is modified by backfill/groundwater interactions
 - ↳ Typically highly compacted bentonite or cementitious backfill

- Nature of the pore fluid?

- Multi-porosity model ↔ Donnan Equilibrium processes?

- In non-isothermal unsaturated conditions water at container from:

- Episodic fracture flow
 - Dripping into open drifts
 - Deliquescence of salt contaminants
 - Temp & RH depends on type of salt deposit



PORE WATER TRANSIENTS

- Corrosion → contact of water with container surface
- Chemistry is modified by backfill/groundwater interactions
 - ↳ Typically highly compacted bentonite or cementitious backfill

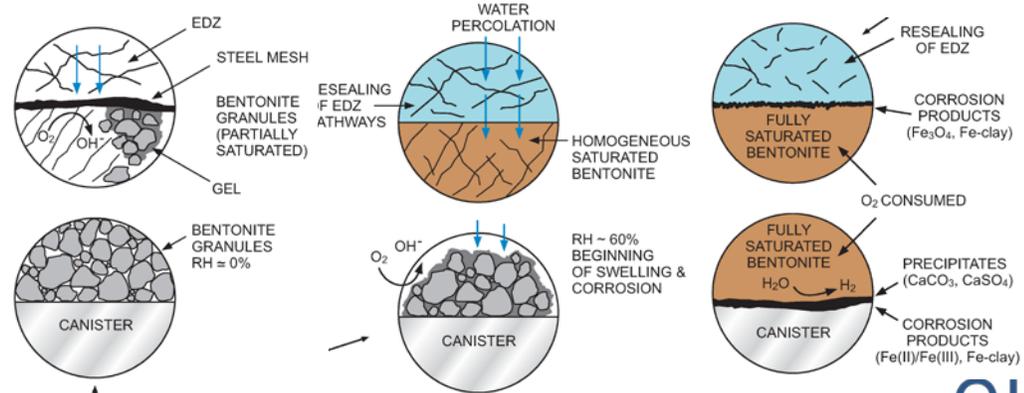
• Nature of the pore fluid?

- Multi-porosity model ↔ Donnan Equilibrium processes?

• In non-isothermal unsaturated conditions water at container from:

- Episodic fracture flow
- Dripping into open drifts
- Deliquescence of salt contaminants
 - Temp & RH depends on type of salt deposit

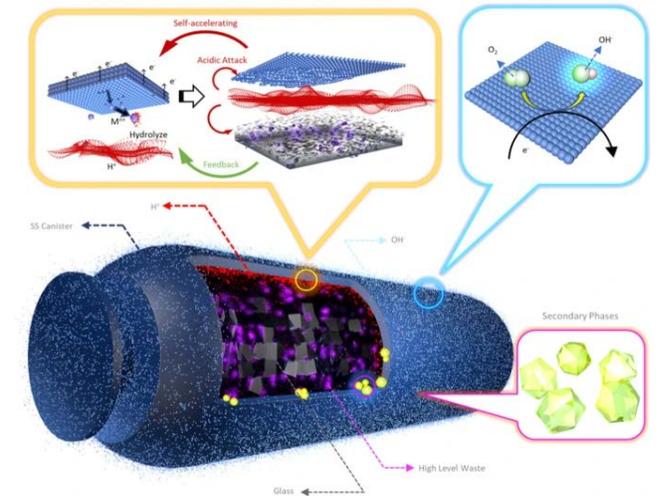
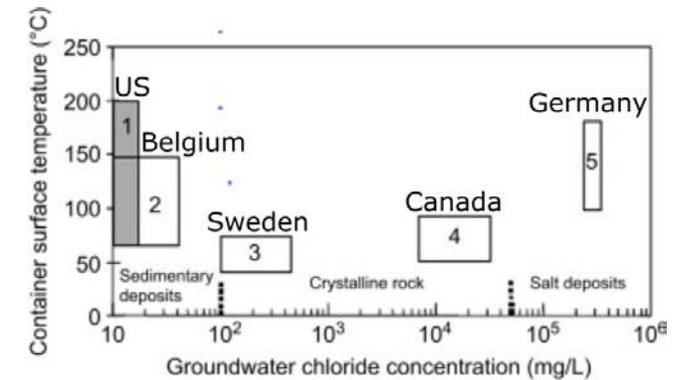
↳ Non-uniform wetting of the surface



PORE WATER TRANSIENTS

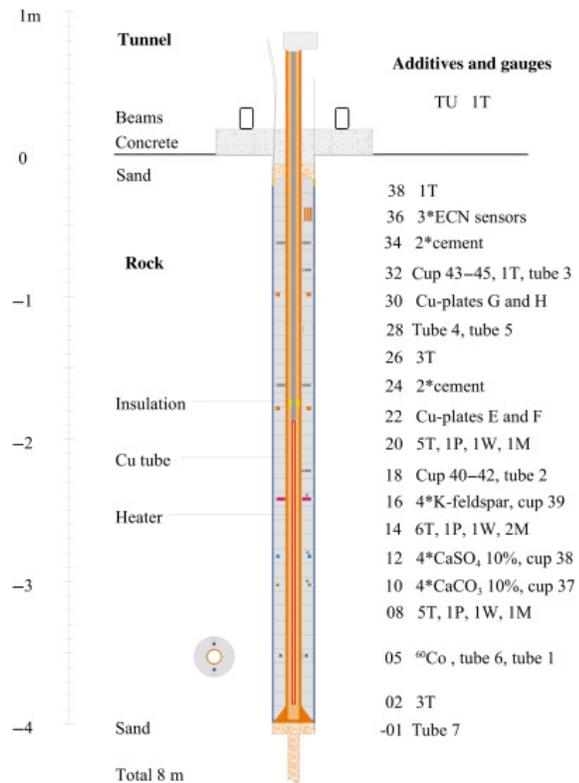
- Species important for corrosion:

- Cl^-
- $\text{SO}_4^{2-} \rightarrow \text{HS}^-$
- $\text{CO}_3^{2-}/\text{HCO}_3^-$
 - pH buffering
 - passivating certain metals (e.g. Cu or C-steel)
- pH \rightarrow alkaline pH \rightarrow passivation of C-steel
- Cations (Ca^{2+} , Mg^{2+})
 - hydrolyze to produce aggressive environments
 - promote formation of protective mineralized surface films
- NH_4^+ stress corrosion cracking of Cu alloys



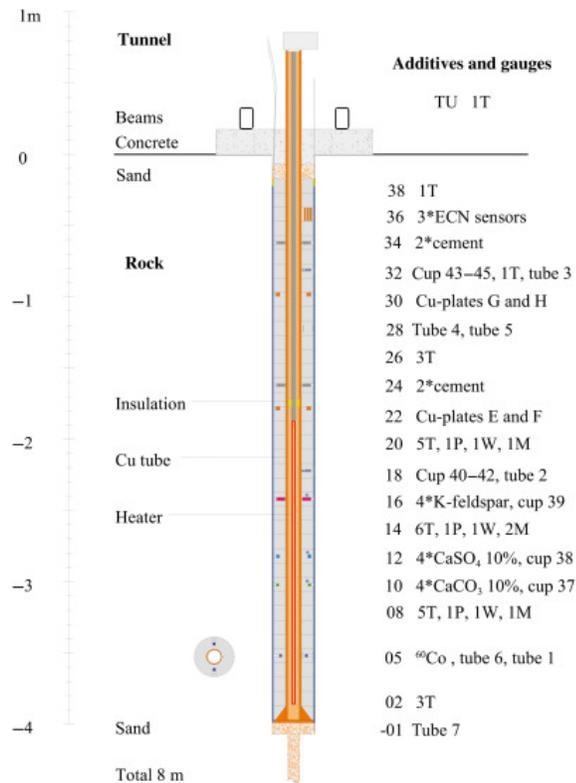
PORE WATER TRANSIENTS: EXPERIMENTAL WORK

- 10 year modelling of chemistry of MX-80 during saturation and heating (up to 130 °C)
 - pH ↓ with saturation



PORE WATER TRANSIENTS: EXPERIMENTAL WORK

- 10 year modelling of chemistry of MX-80 during saturation and heating (up to 130 °C)
 - pH ↓ with saturation

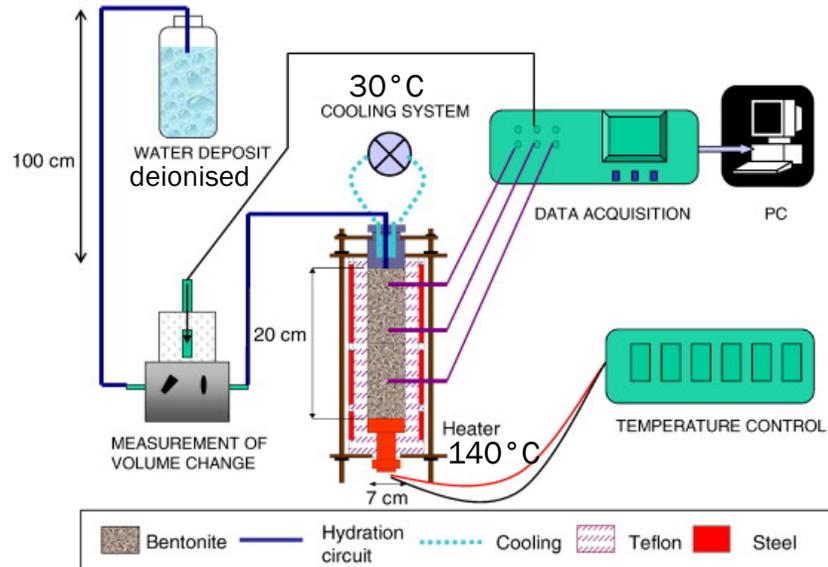


- Influence of Ca-Mg-bentonite chemistry in contact with granitic groundwater after the thermal phase

- [Cl⁻] ↓ → pH ↑ → aggressive behavior ↓

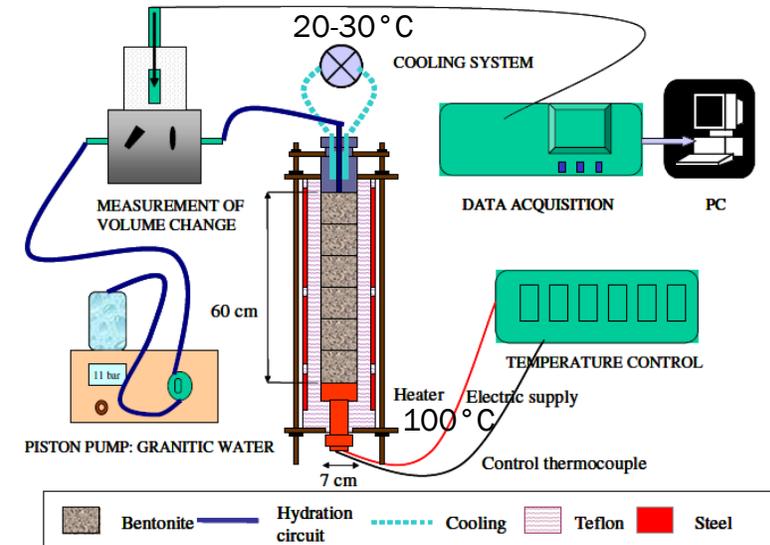
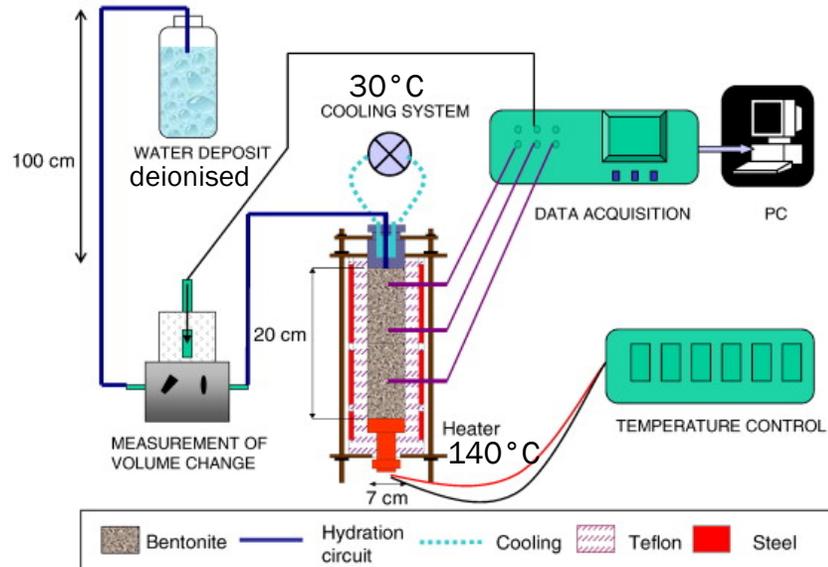


PORE WATER TRANSIENTS: EXPERIMENTAL WORK



- 496 days, 1.72 g/cm³ dry density, initial water content 16%
 - No water penetration into the column beyond the area where > 100 °C
 - Advection, interlayer exchange & dissolution/precipitation processes conditioned the composition of the pore water along the column
 - Na-SO₄²⁻ → Na-Cl type near the heater
 - Changes in cation content could be explained by changes in smectite interlayer & mineral phases equilibrium
 - No significant alteration of smectite or other mineral phases of the bentonite

PORE WATER TRANSIENTS: EXPERIMENTAL WORK

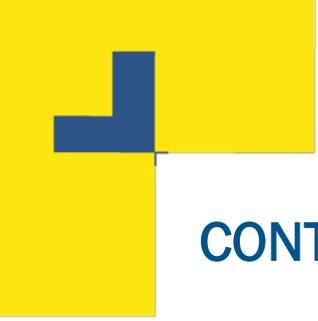


- 496 days, 1.72 g/cm³ dry density, initial water content 16%

- No water penetration into the column beyond the area where > 100°C
- Advection, interlayer exchange & dissolution/precipitation processes conditioned the composition of the pore water along the column
- Na-SO₄²⁻ → Na-Cl type near the heater
- Changes in cation content could be explained by changes in smectite interlayer & mineral phases equilibrium
- No significant alteration of smectite or other mineral phases of the bentonite

- 7.6 years, 1.64 g/cm³ dry density, initial water content 13.8%

- Overall degree of saturation: 92 %
- Gradient of water content & dry density along the column
- Advection, interlayer exchange & dissolution/precipitation processes conditioned the composition of the pore water along the column
- Exchangeable complex of smectite changed
- Na-SO₄²⁻ → Na-Cl type near the heater
- Physical properties not irreversibly affected



CONTENT

- Introduction
- Thermal transients
- Pore water transients
- **Redox transients**
- Saturation transients
- Mechanical transients
- Transitional processes involving gas generation
- Effects of irradiation
- Effects of Microbial processes
- Example of an integrated test
- Summary

REDOX TRANSIENTS

- Most important species undergoing redox reactions contain:
 - C, Fe, S, N species (gases + dissolved components + solids + components associated with solids by ion exchange)

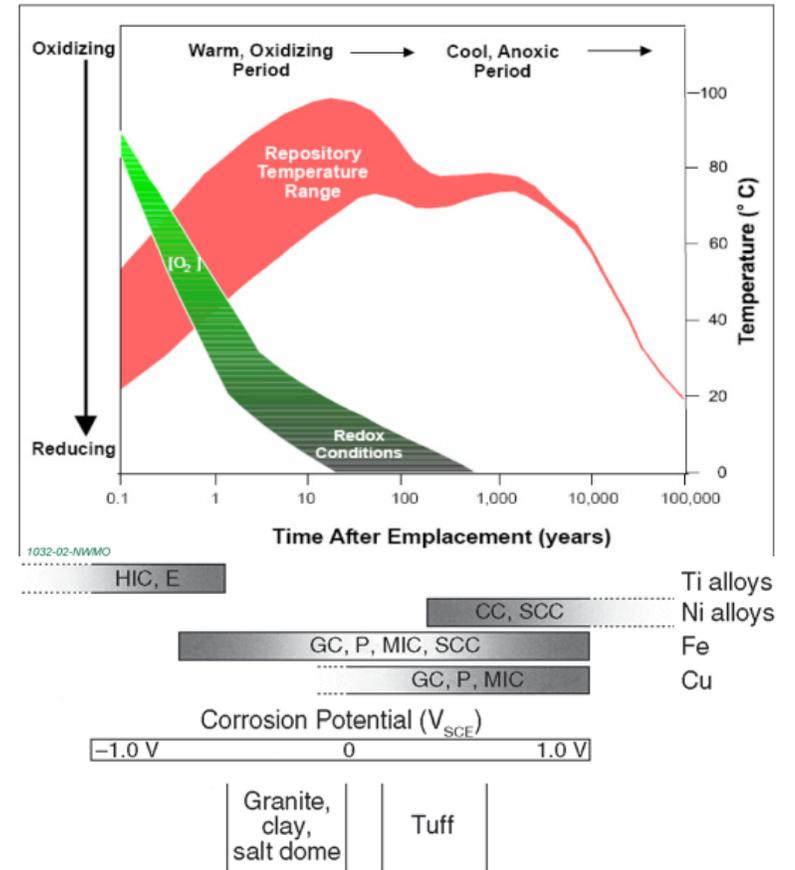


Figure from King, F. (2017). 13 - Nuclear Waste Canister Materials: Corrosion Behavior and Long-Term Performance in Geological Repository Systems. Geological Repository Systems for Safe Disposal of Spent Nuclear Fuels and Radioactive Waste (Second Edition). M. J. Apted and J. Ahn, Woodhead Publishing; Shoosmith, D. W. (2006). "Assessing the Corrosion Performance of High-Level Nuclear Waste Containers." Corrosion 62(8).

Anticipated corrosion behavior of various materials as a function of redox conditions (expressed as a corrosion potential): P—pitting; MIC—microbially-induced corrosion; SCC—stress corrosion cracking; CC—crevice corrosion; HIC—hydrogen-induced cracking; GC—general corrosion; E—embrittlement.

REDOX TRANSIENTS

- Most important species undergoing redox reactions contain:
 - C, Fe, S, N species (gases + dissolved components + solids + components associated with solids by ion exchange)
- Determined by O_2
 - O_2 trapped in pore space
 - Oxidizing species produced by the radiolysis of water (\downarrow in absence of O_2)

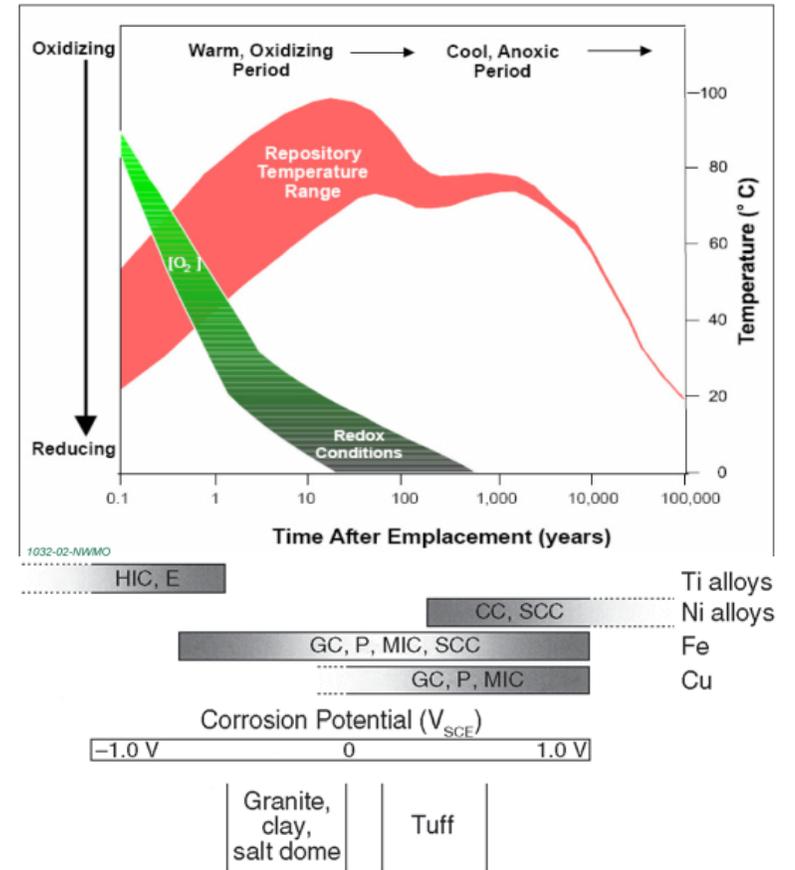


Figure from King, F. (2017). 13 - Nuclear Waste Canister Materials: Corrosion Behavior and Long-Term Performance in Geological Repository Systems. Geological Repository Systems for Safe Disposal of Spent Nuclear Fuels and Radioactive Waste (Second Edition). M. J. Apted and J. Ahn, Woodhead Publishing; Shoosmith, D. W. (2006). "Assessing the Corrosion Performance of High-Level Nuclear Waste Containers." Corrosion 62(8).

Anticipated corrosion behavior of various materials as a function of redox conditions (expressed as a corrosion potential): P—pitting; MIC—microbially-induced corrosion; SCC—stress corrosion cracking; CC—crevice corrosion; HIC—hydrogen-induced cracking; GC—general corrosion; E—embrittlement.

REDOX TRANSIENTS

- Most important species undergoing redox reactions contain:
 - C, Fe, S, N species (gases + dissolved components + solids + components associated with solids by ion exchange)
- Determined by O₂
 - O₂ trapped in pore space
 - Oxidizing species produced by the radiolysis of water (↓ in absence of O₂)
 - Consumed by:
 - Diffusion in the surrounding rock
 - Reaction with mineral phases in buffer & backfill materials
 - Corrosion
 - Microbial activity
- O₂ consumption in time predictions vary from a few year to a few centuries

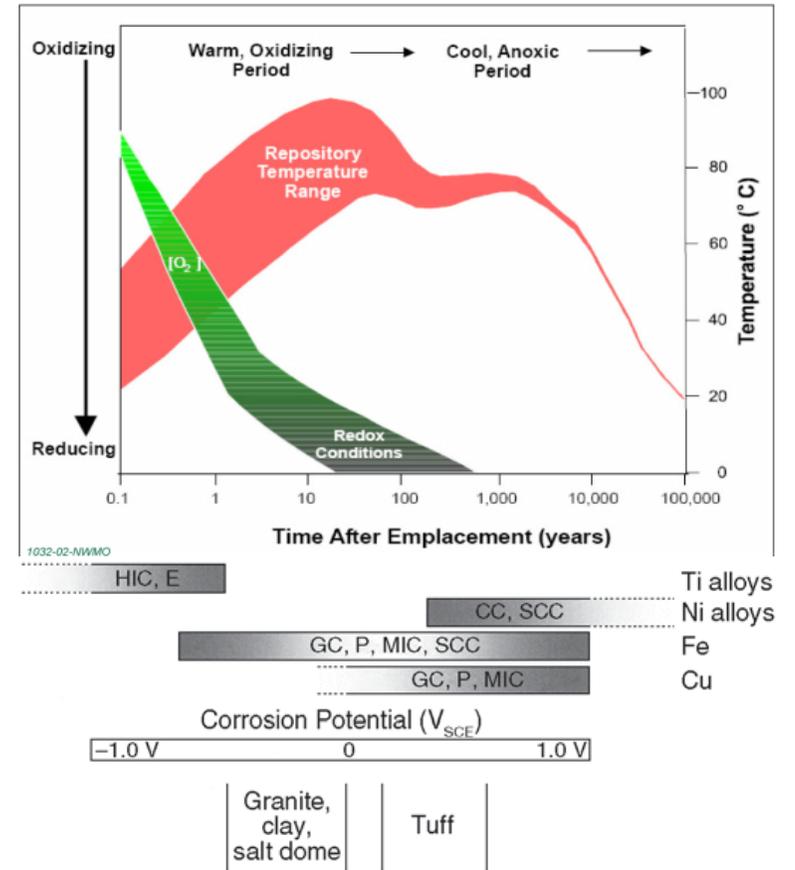
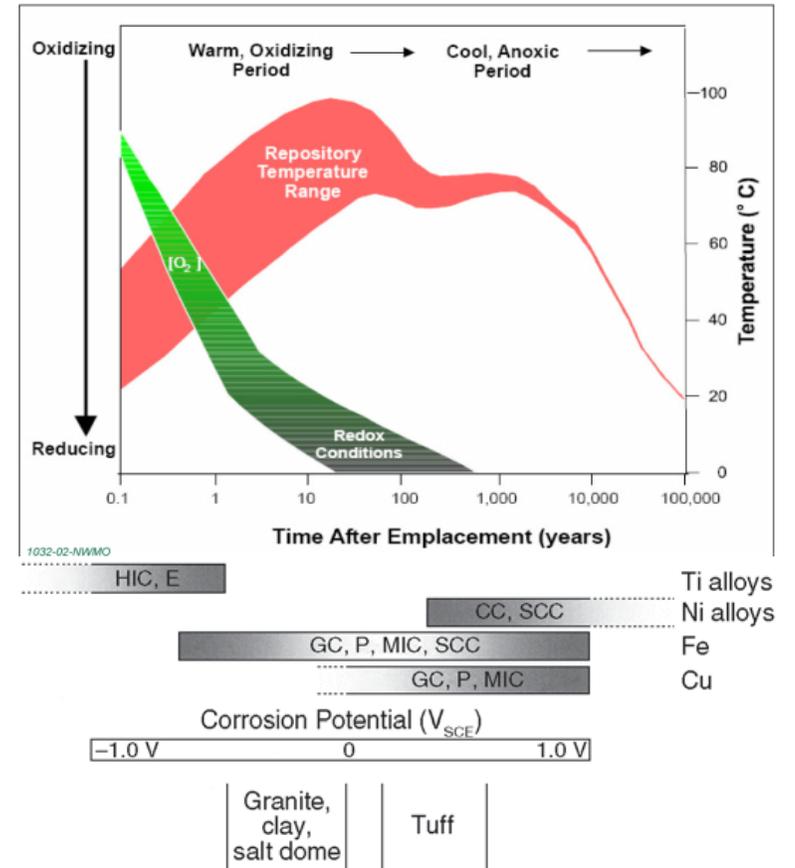


Figure from King, F. (2017). 13 - Nuclear Waste Canister Materials: Corrosion Behavior and Long-Term Performance in Geological Repository Systems. Geological Repository Systems for Safe Disposal of Spent Nuclear Fuels and Radioactive Waste (Second Edition). M. J. Apted and J. Ahn, Woodhead Publishing; Shoesmith, D. W. (2006). "Assessing the Corrosion Performance of High-Level Nuclear Waste Containers." Corrosion 62(8).

Anticipated corrosion behavior of various materials as a function of redox conditions (expressed as a corrosion potential): P—pitting; MIC—microbially-induced corrosion; SCC—stress corrosion cracking; CC—crevice corrosion; HIC—hydrogen-induced cracking; GC—general corrosion; E—embrittlement.

REDOX TRANSIENTS

- Most important species undergoing redox reactions contain:
 - C, Fe, S, N species (gases + dissolved components + solids + components associated with solids by ion exchange)
- Determined by O₂
 - O₂ trapped in pore space
 - Oxidizing species produced by the radiolysis of water (↓ in absence of O₂)
 - Consumed by:
 - Diffusion in the surrounding rock
 - Reaction with mineral phases in buffer & backfill materials
 - Corrosion
 - Microbial activity
- O₂ consumption in time predictions vary from a few year to a few centuries
- If all the O₂ initially present reacts uniformly with the steel containers → max. corroded depth would be < 100 μm

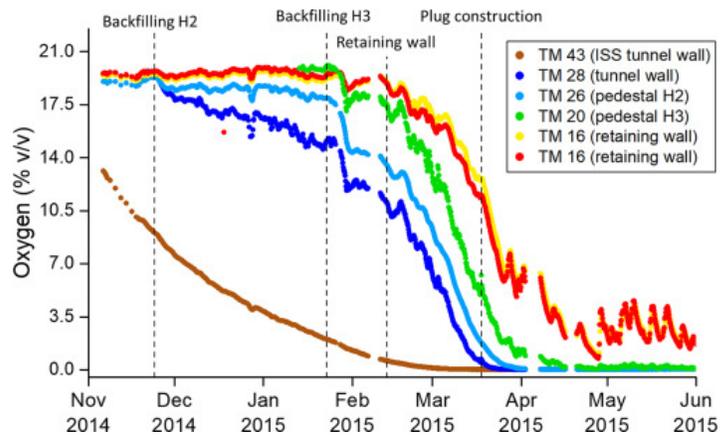
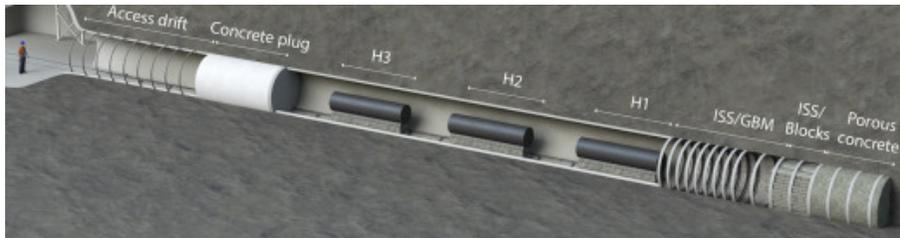


Anticipated corrosion behavior of various materials as a function of redox conditions (expressed as a corrosion potential): P—pitting; MIC—microbially-induced corrosion; SCC—stress corrosion cracking; CC—crevice corrosion; HIC—hydrogen-induced cracking; GC—general corrosion; E—embrittlement.

Figure from King, F. (2017). 13 - Nuclear Waste Canister Materials: Corrosion Behavior and Long-Term Performance in Geological Repository Systems. Geological Repository Systems for Safe Disposal of Spent Nuclear Fuels and Radioactive Waste (Second Edition). M. J. Apted and J. Ahn, Woodhead Publishing; Shoesmith, D. W. (2006). "Assessing the Corrosion Performance of High-Level Nuclear Waste Containers." Corrosion 62(8).

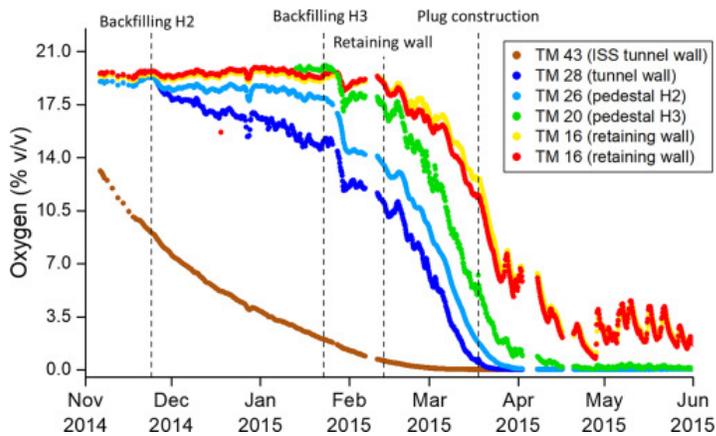
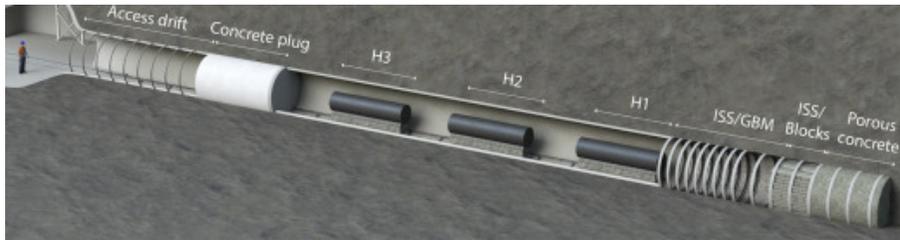
REDOX TRANSIENTS: EXPERIMENTAL WORK

- FE-G experiment @ Mont Terri
 - Very rapid O₂ consumption
 - By the bentonite buffer
 - In the EDZ

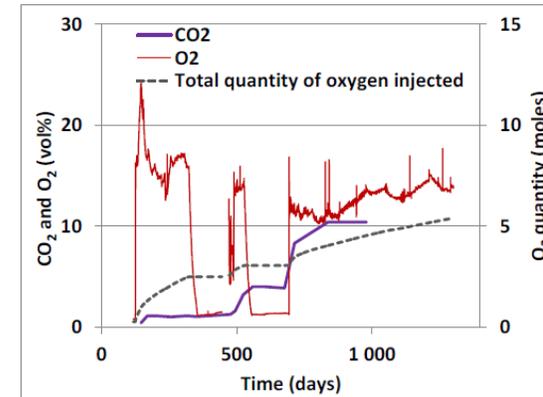
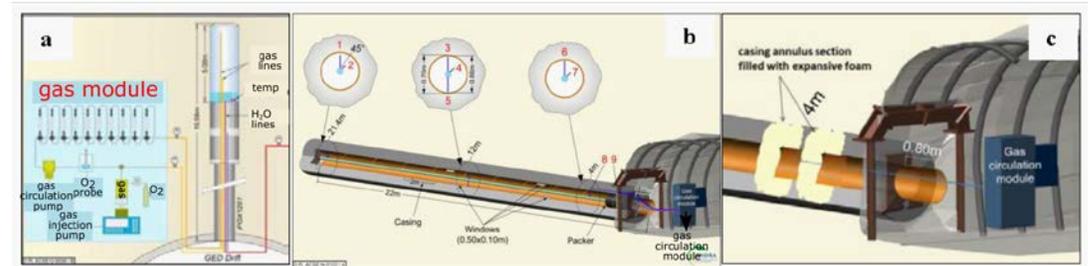


REDOX TRANSIENTS: EXPERIMENTAL WORK

- FE-G experiment @ Mont Terri
 - Very rapid O₂ consumption
 - By the bentonite buffer
 - In the EDZ



- CO_x argillaceous rock @ Meuse/Haute-Marne URL
 - O₂ consumption by
 - Pyrite oxidation
 - Calcite dissolution



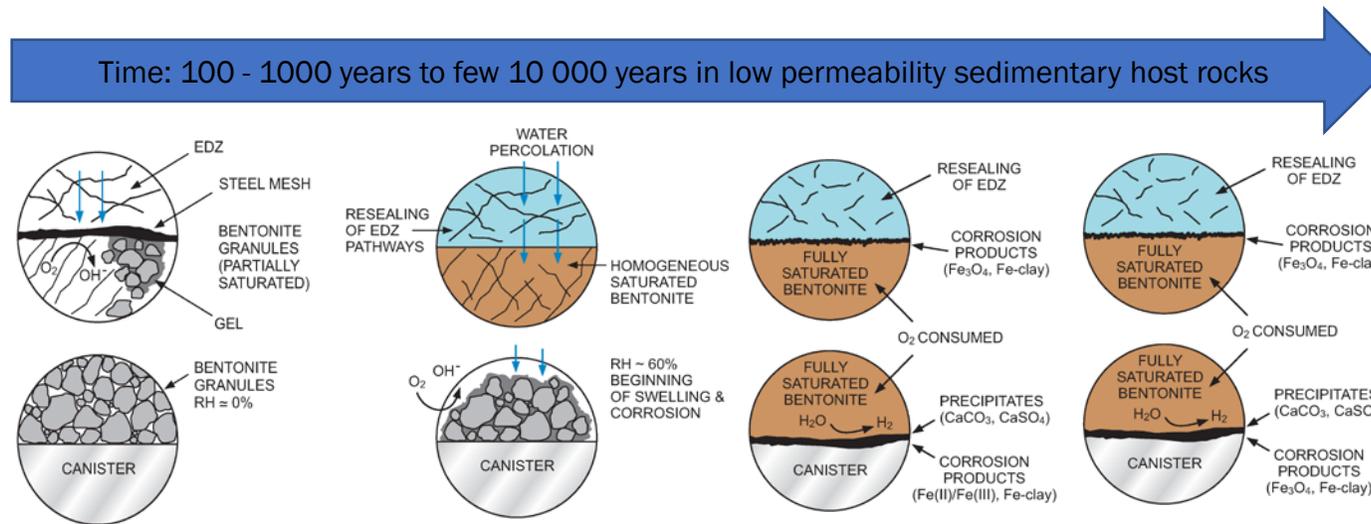


CONTENT

- Introduction
- Thermal transients
- Pore water transients
- Redox transients
- **Saturation transients**
- Mechanical transients
- Transitional processes involving gas generation
- Effects of irradiation
- Effects of Microbial processes
- Example of an integrated test
- Summary

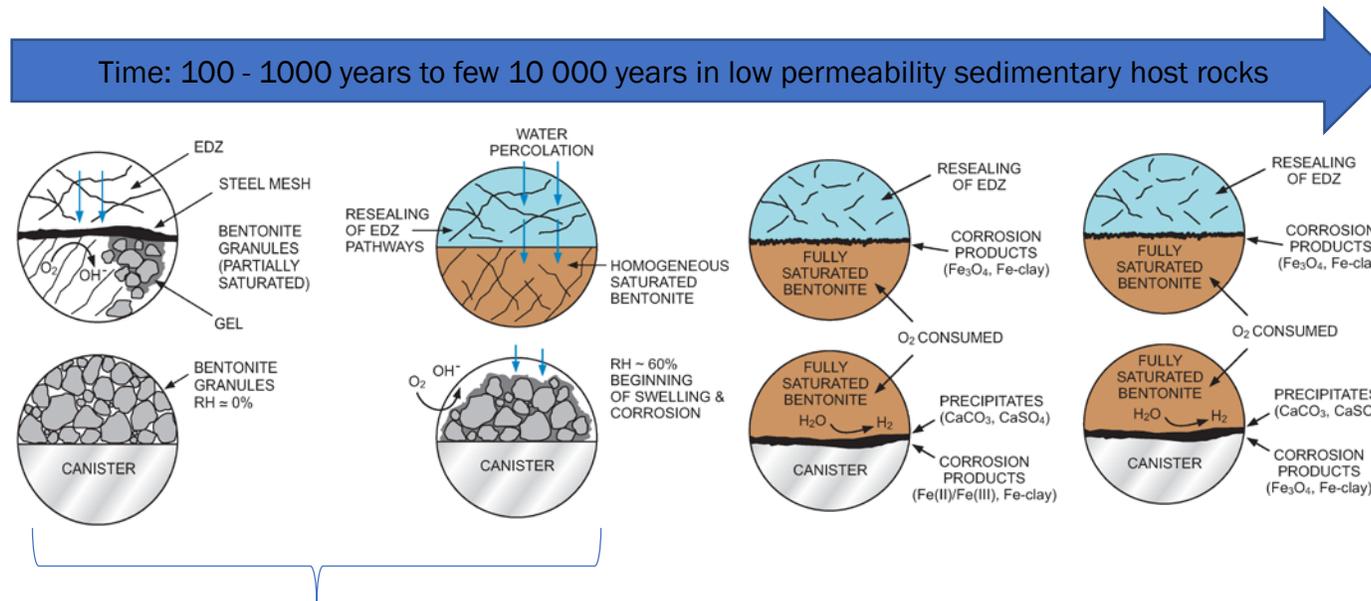
SATURATION TRANSIENTS

- When & what form of corrosion occur



SATURATION TRANSIENTS

- When & what form of corrosion occur



- Localized corrosion due to deliquescence of salts
- Non-uniform wetting
- Rate of supply of gaseous reactants higher ↔ rate of removal dissolved corrosion products ↓ → formation of protective film ↑

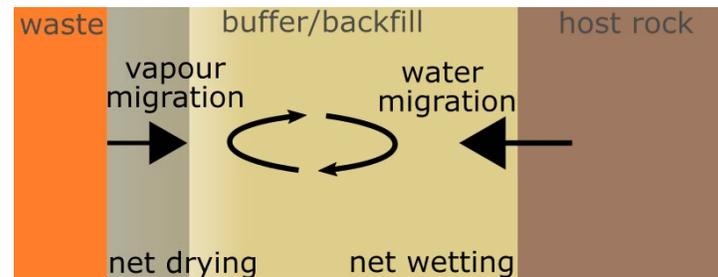


SATURATION TRANSIENTS

- Re-saturation rate controlled by intrinsic permeability & water saturation of surrounding rock

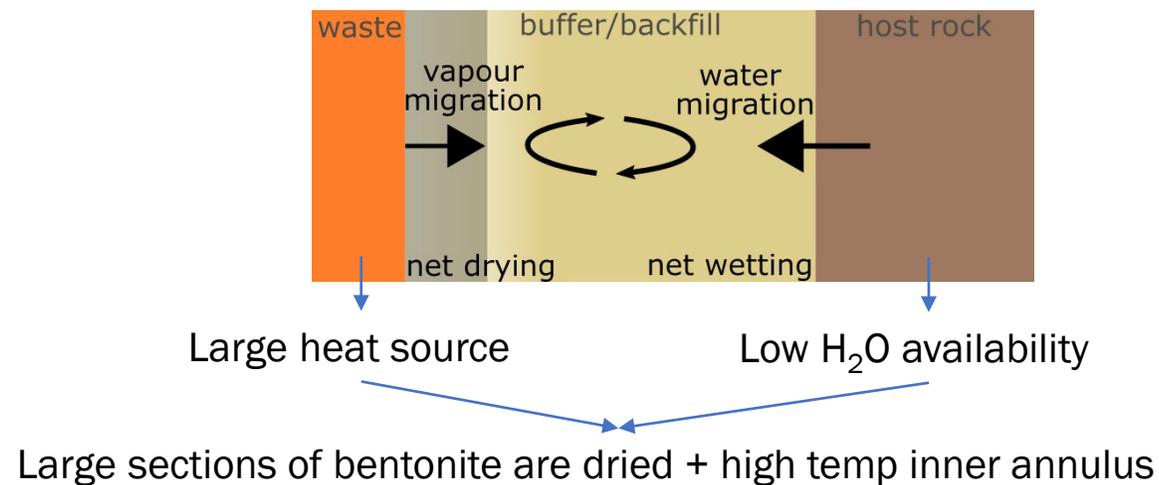
SATURATION TRANSIENTS

- Re-saturation rate controlled by intrinsic permeability & water saturation of surrounding rock
- Thermal load → acceleration of generation & diffusion H₂O vapor



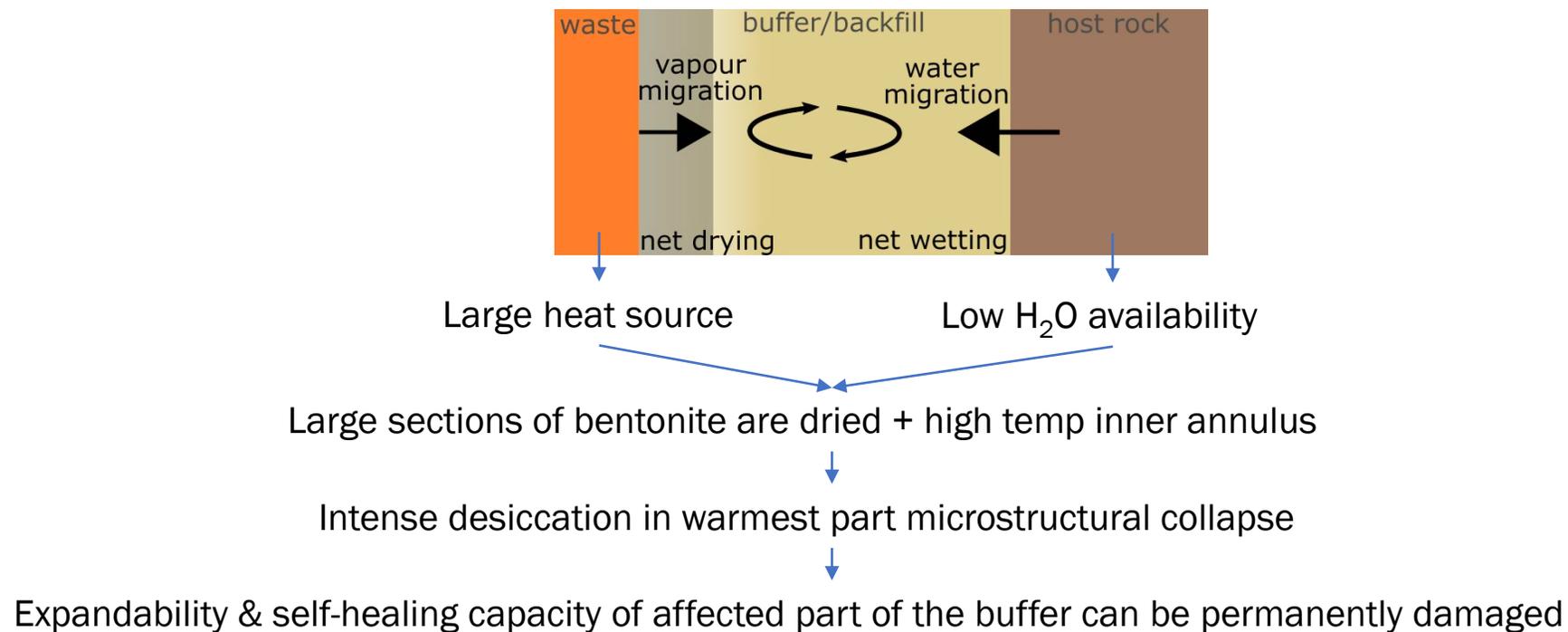
SATURATION TRANSIENTS

- Re-saturation rate controlled by intrinsic permeability & water saturation of surrounding rock
- Thermal load → acceleration of generation & diffusion H₂O vapor



SATURATION TRANSIENTS

- Re-saturation rate controlled by intrinsic permeability & water saturation of surrounding rock
- Thermal load → acceleration of generation & diffusion H₂O vapor



SATURATION TRANSIENTS

- Re-saturation rate controlled by intrinsic permeability & water saturation of surrounding rock
- Thermal load → acceleration of generation & diffusion H₂O vapor

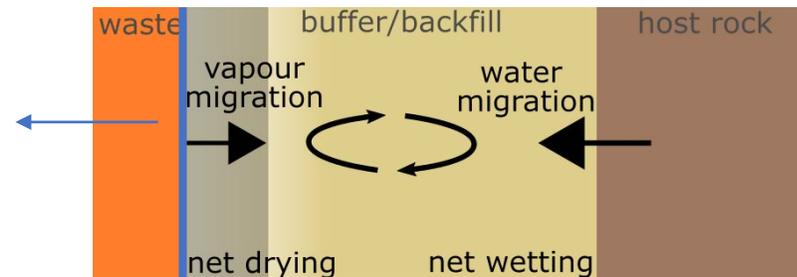
- Accumulation Cl⁻ & SO₄²⁻ salts
- Driving away dissolved silica



- Container corrosion
- Radial variation clay density



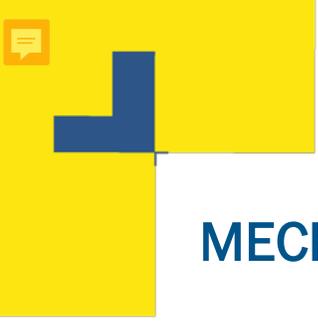
Porosity changes





CONTENT

- Introduction
- Thermal transients
- Pore water transients
- Redox transients
- Saturation transients
- **Mechanical transients**
- Transitional processes involving gas generation
- Effects of irradiation
- Effects of Microbial processes
- Example of an integrated test
- Summary

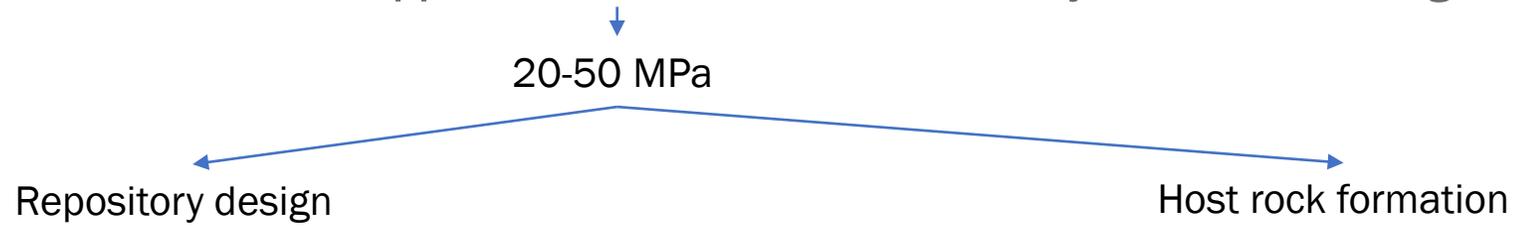


MECHANICAL TRANSIENTS

- Exposure to residual & applied stresses → environmentally assisted cracking

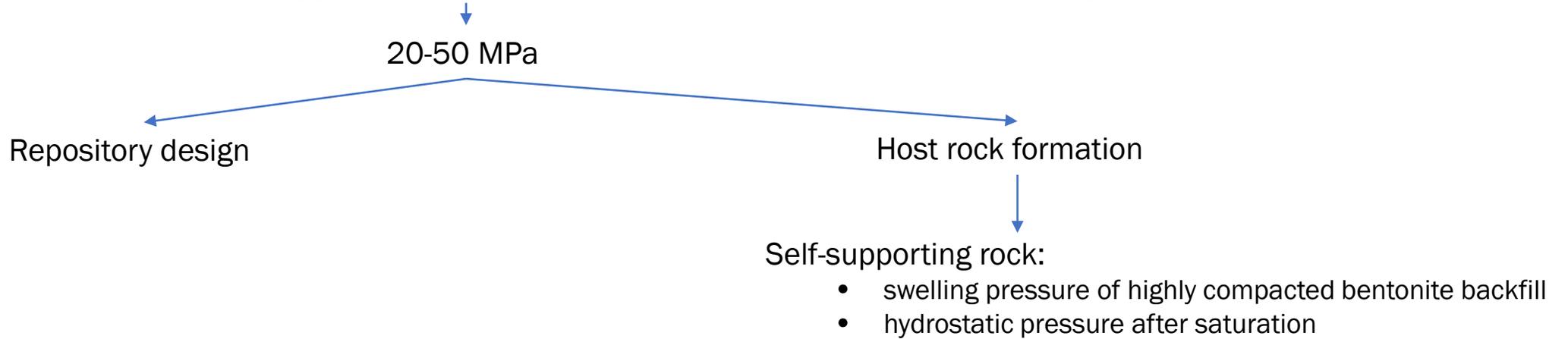
MECHANICAL TRANSIENTS

- Exposure to residual & applied stresses → environmentally assisted cracking



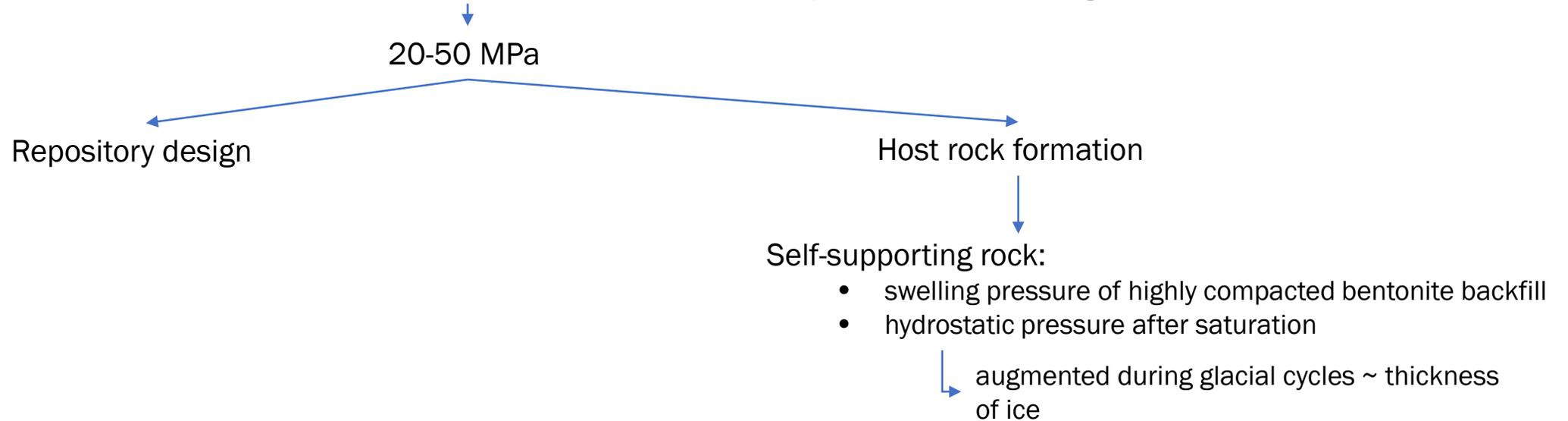
MECHANICAL TRANSIENTS

- Exposure to residual & applied stresses → environmentally assisted cracking



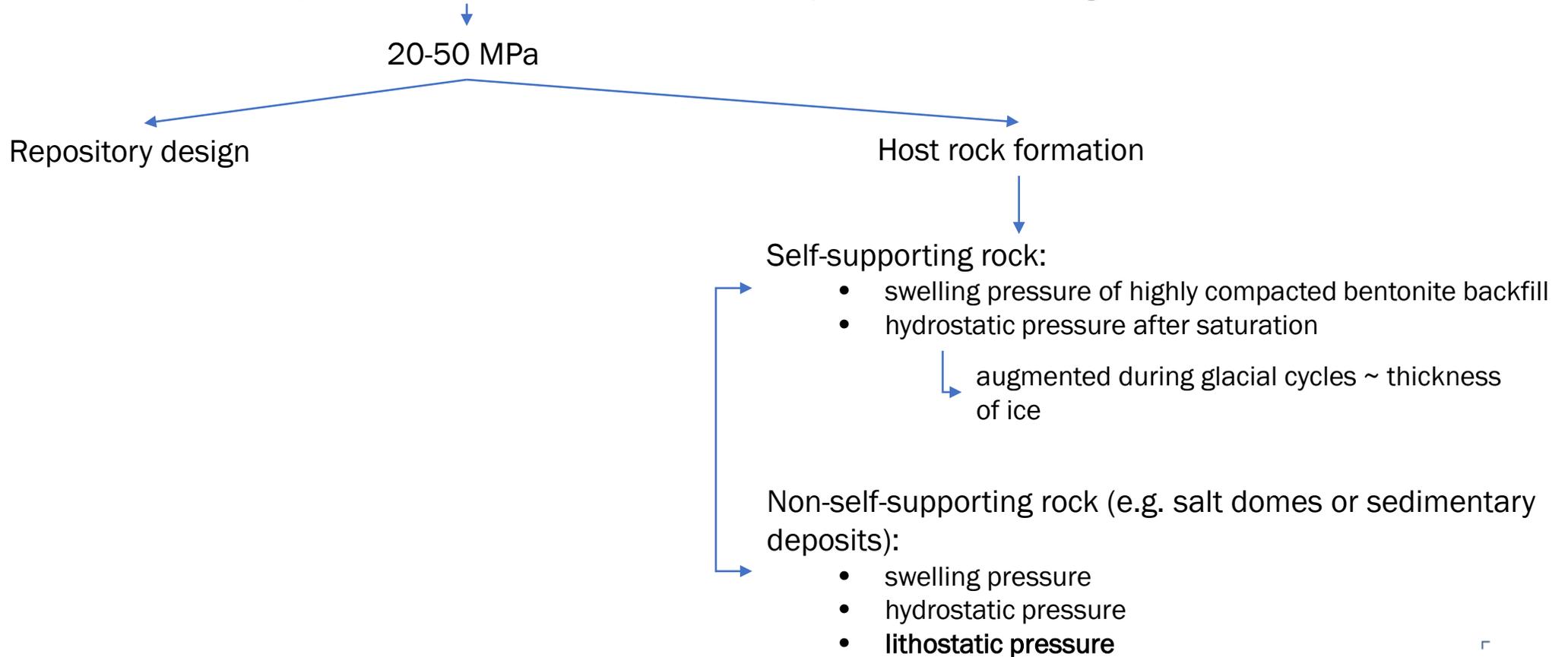
MECHANICAL TRANSIENTS

- Exposure to residual & applied stresses → environmentally assisted cracking



MECHANICAL TRANSIENTS

- Exposure to residual & applied stresses → environmentally assisted cracking



MECHANICAL TRANSIENTS

- Exposure to residual & applied stresses → environmentally assisted cracking

20-50 MPa

Repository design

- Thick-walled container designs
- In some designs: internal pressurization due to the diffusion of hydrogen produced by anaerobic corrosion through the wall of a carbon steel container

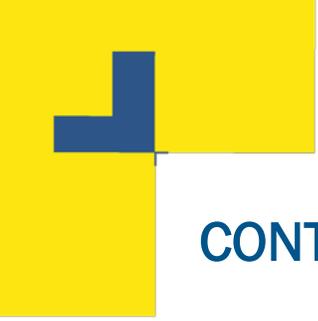
Host rock formation

Self-supporting rock:

- swelling pressure of highly compacted bentonite backfill
- hydrostatic pressure after saturation
 - ↳ augmented during glacial cycles ~ thickness of ice

Non-self-supporting rock (e.g. salt domes or sedimentary deposits):

- swelling pressure
- hydrostatic pressure
- lithostatic pressure



CONTENT

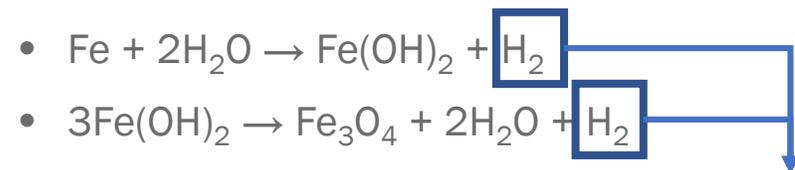
- Introduction
- Thermal transients
- Pore water transients
- Redox transients
- Saturation transients
- Mechanical transients
- **Transitional processes involving gas generation**
- Effects of irradiation
- Effects of Microbial processes
- Example of an integrated test
- Summary

TRANSITIONAL PROCESSES INVOLVING GAS GENERATION

- Anaerobic corrosion of C-steel:
 - $\text{Fe} + 2\text{H}_2\text{O} \rightarrow \text{Fe}(\text{OH})_2 + \text{H}_2$
 - $3\text{Fe}(\text{OH})_2 \rightarrow \text{Fe}_3\text{O}_4 + 2\text{H}_2\text{O} + \text{H}_2$

TRANSITIONAL PROCESSES INVOLVING GAS GENERATION

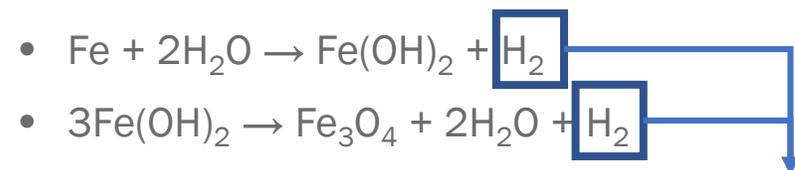
- Anaerobic corrosion of C-steel:



In gaseous & dissolved form at surface container

TRANSITIONAL PROCESSES INVOLVING GAS GENERATION

- Anaerobic corrosion of C-steel:

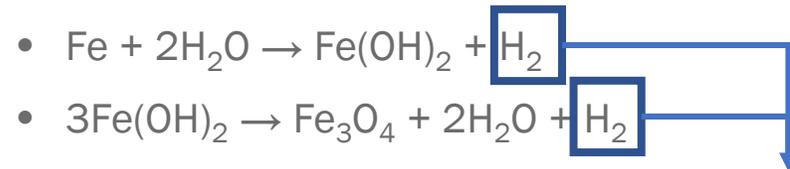


In gaseous & dissolved form at surface container

↓
Consumed by diffusion & two-phase flow

TRANSITIONAL PROCESSES INVOLVING GAS GENERATION

- Anaerobic corrosion of C-steel:



In gaseous & dissolved form at surface container



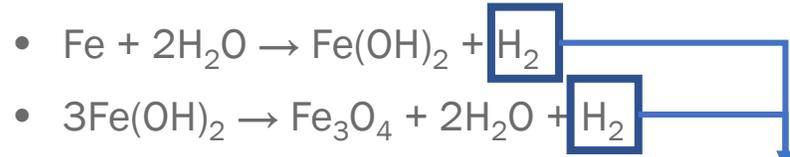
Consumed by diffusion & two-phase flow

- H degradation mechanisms of concern:

- H stress cracking (or hydrogen-induced cracking), in which H accumulates under a stress gradient leading to internal crack formation
- Blister formation, as a result of H accumulation at internal voids, laminations or inclusions

TRANSITIONAL PROCESSES INVOLVING GAS GENERATION

- Anaerobic corrosion of C-steel:



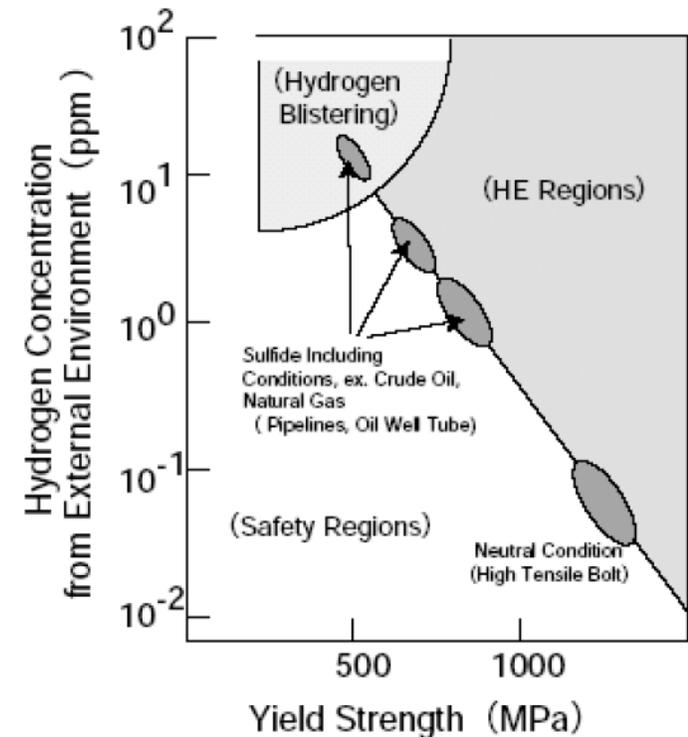
In gaseous & dissolved form at surface container

Consumed by diffusion & two-phase flow

- H degradation mechanisms of concern:

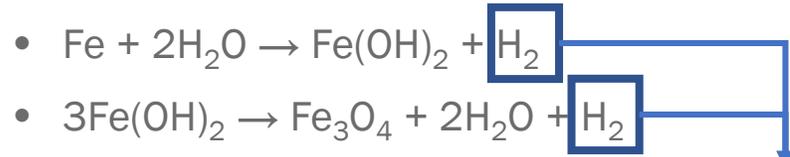
- H stress cracking (or hydrogen-induced cracking), in which H accumulates under a stress gradient leading to internal crack formation
- Blister formation, as a result of H accumulation at internal voids, laminations or inclusions

Susceptibility ↑ with material strength and [absorbed H]



TRANSITIONAL PROCESSES INVOLVING GAS GENERATION

- Anaerobic corrosion of C-steel:



In gaseous & dissolved form at surface container

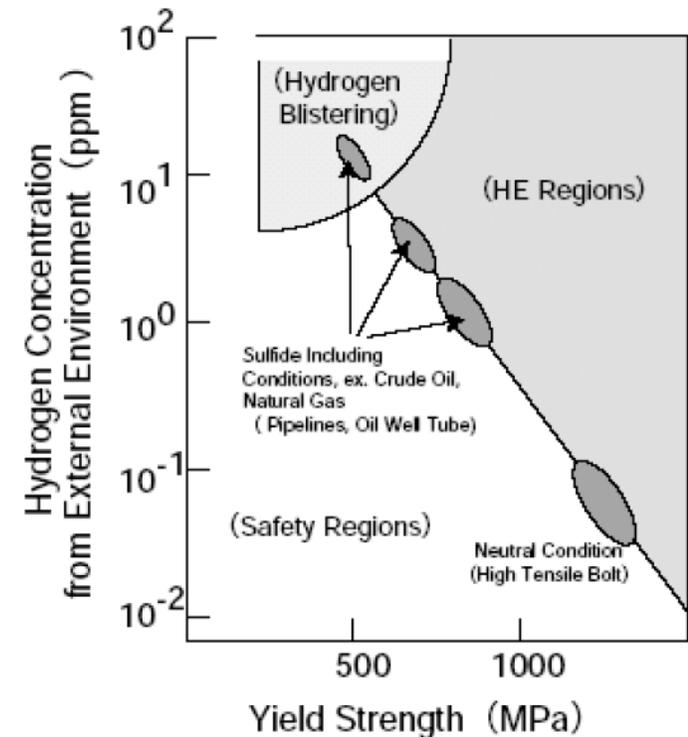
Consumed by diffusion & two-phase flow

- H degradation mechanisms of concern:

- H stress cracking (or hydrogen-induced cracking), in which H accumulates under a stress gradient leading to internal crack formation
- Blister formation, as a result of H accumulation at internal voids, laminations or inclusions

Susceptibility ↑ with material strength and [absorbed H]

Use of low-strength steel container & the nature of the repository environment



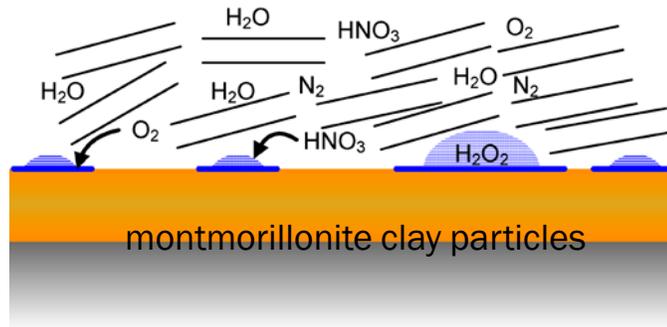


CONTENT

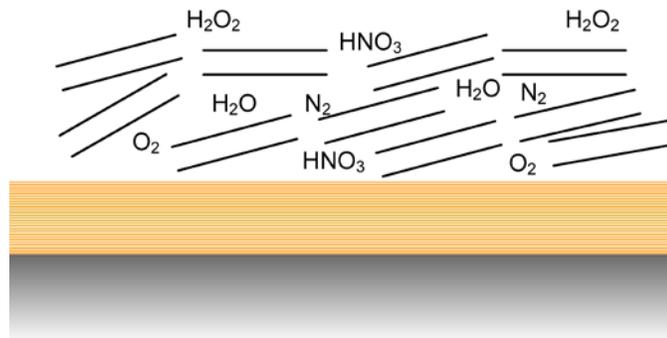
- Introduction
- Thermal transients
- Pore water transients
- Redox transients
- Saturation transients
- Mechanical transients
- Transitional processes involving gas generation
- **Effects of irradiation**
- Effects of Microbial processes
- Example of an integrated test
- Summary

RADIATION TRANSIENTS IN THE NEAR-FIELD

Absorption of HNO_3 formed by the radiolysis of humid air by liquid droplets on a non-uniformly wetted surface

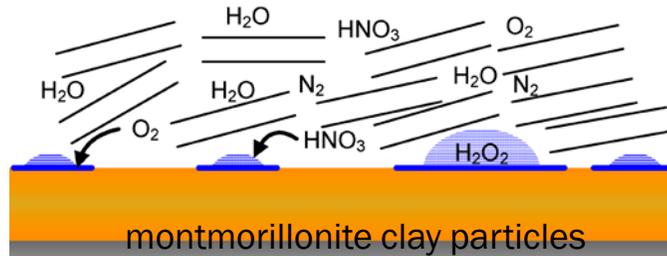


Radiolysis of humid air during a period when the container surface is dry

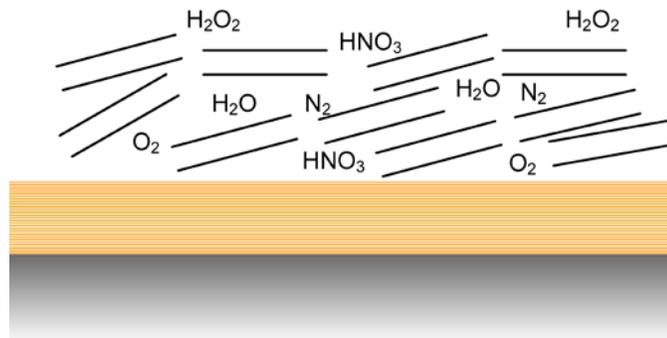


RADIATION TRANSIENTS IN THE NEAR-FIELD

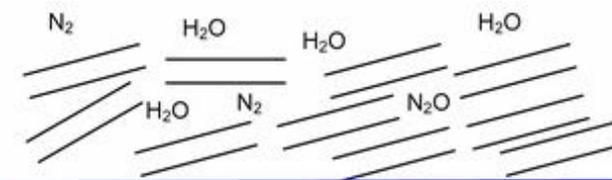
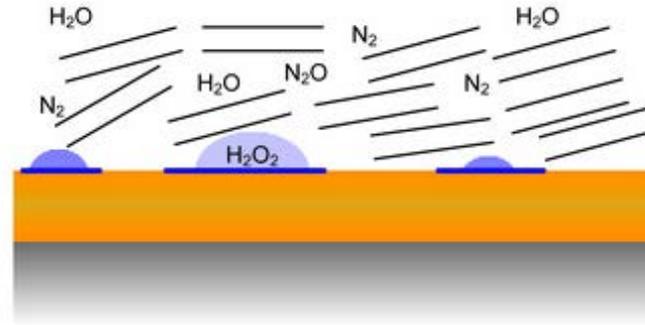
Absorption of HNO_3 formed by the radiolysis of humid air by liquid droplets on a non-uniformly wetted surface



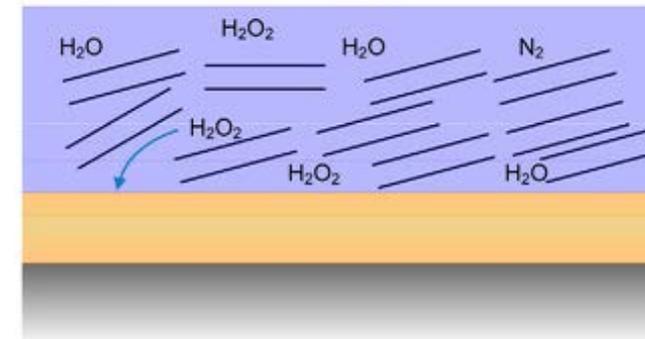
Radiolysis of humid air during a period when the container surface is dry



Saturated conditions



H_2O_2



Radiolysis of $\text{N}_2\text{-H}_2\text{O}$ following consumption of the initially trapped O_2 & radiolysis of liquid droplets following re-wetting of the container surface

Radiolysis of a thin surface water layer following complete wetting of the surface, with continued radiolysis of a humid $\text{N}_2\text{-H}_2\text{O}$ atmosphere

Radiolysis of a bulk aqueous phase following complete saturation of the buffer box



EFFECT OF IRRADIATION ON THE CORROSION OF COPPER CONTAINERS

- Dose rate ↔ total dose → impact on
 - design of experiments
 - interpretation of results
 - how to make long-term predictions

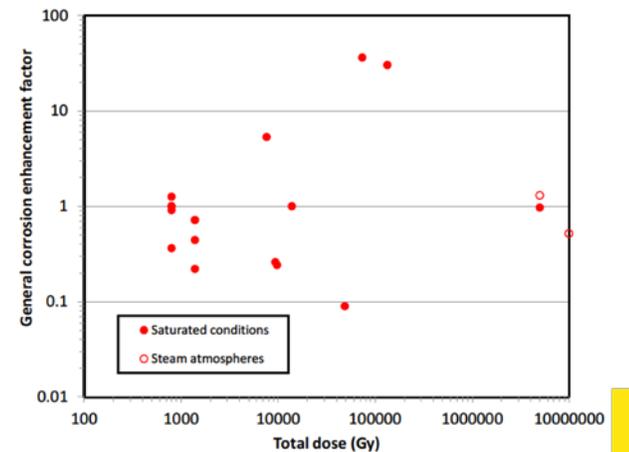
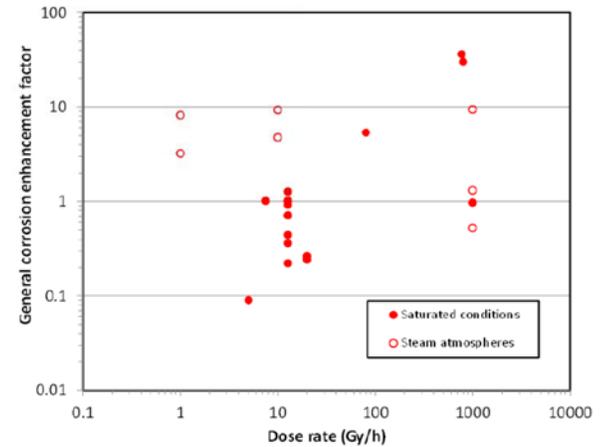


EFFECT OF IRRADIATION ON THE CORROSION OF COPPER CONTAINERS

- Dose rate ↔ total dose → impact on
 - design of experiments
 - interpretation of results
 - how to make long-term predictions
- Effects of γ -irradiation on the corrosion behavior of Cu container
 - Production of additional radiolytic oxidants to support general corrosion

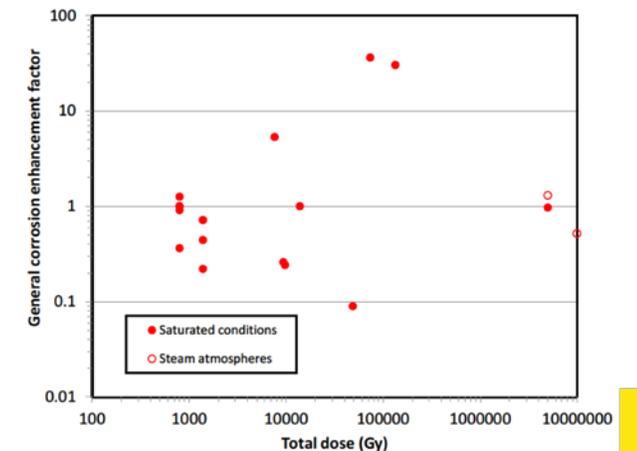
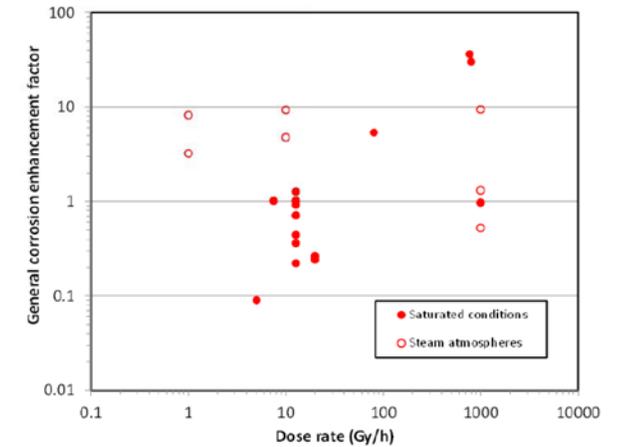
EFFECT OF IRRADIATION ON THE CORROSION OF COPPER CONTAINERS

- Dose rate \leftrightarrow total dose \rightarrow impact on
 - design of experiments
 - interpretation of results
 - how to make long-term predictions
- Effects of γ -irradiation on the corrosion behavior of Cu container
 - Production of additional radiolytic oxidants to support general corrosion
 - Saturated conditions
 - corrosion rate \uparrow only for absorbed dose rates > 20 Gy/h
 - \uparrow in degree of enhancement with \uparrow dose, no \uparrow for absorbed doses < 10 kGy



EFFECT OF IRRADIATION ON THE CORROSION OF COPPER CONTAINERS

- Dose rate \leftrightarrow total dose \rightarrow impact on
 - design of experiments
 - interpretation of results
 - how to make long-term predictions
- Effects of γ -irradiation on the corrosion behavior of Cu container
 - Production of additional radiolytic oxidants to support general corrosion
 - Saturated conditions
 - corrosion rate \uparrow only for absorbed dose rates > 20 Gy/h
 - \uparrow in degree of enhancement with \uparrow dose, no \uparrow for absorbed doses < 10 kGy
 - Unsaturated conditions \rightarrow surface area copper/volume aqueous phase is high
 - affect relative influence of interfacial & homogenous processes
 - high dose rate (470-500 Gy/h) \rightarrow No direct role for radiolytically produced HNO_3 in increased corrosion
 - low dose rate (0.35 Gy/h) \rightarrow little impact over experimental timescales and within the measurement accuracy



RADIOLYSIS TRANSIENTS IN THE NEAR-FIELD

- Effects of γ -irradiation on the corrosion behavior of Cu container
 - Increase E_{corr} & the consequences for localized corrosion & SCC
 - relevant dose rates \rightarrow no ennoblement of E_{corr}
 - high dose rates \rightarrow transient shift insufficient to increase probability of pit initiation

RADIOLYSIS TRANSIENTS IN THE NEAR-FIELD

- Effects of γ -irradiation on the corrosion behavior of Cu container
 - Increase E_{corr} & the consequences for localized corrosion & SCC
 - relevant dose rates \rightarrow no ennoblement of E_{corr}
 - high dose rates \rightarrow transient shift insufficient to increase probability of pit initiation
 - Generation of specific radiolytic species that may support localized corrosion or environmentally assisted cracking
 - NH_4^+ & NO_2^- ions can result in SCC

RADIOLYSIS TRANSIENTS IN THE NEAR-FIELD

- Effects of γ -irradiation on the corrosion behavior of Cu container
 - Increase E_{corr} & the consequences for localized corrosion & SCC
 - relevant dose rates \rightarrow no ennoblement of E_{corr}
 - high dose rates \rightarrow transient shift insufficient to increase probability of pit initiation
 - Generation of specific radiolytic species that may support localized corrosion or environmentally assisted cracking
 - NH_4^+ & NO_2^- ions can result in SCC
 - \hookrightarrow Low pH resulting from absorption of nitric acid vapor would preclude film formation
 - \hookrightarrow Pre-requisite for cracking

RADIOLYSIS TRANSIENTS IN THE NEAR-FIELD

- Effects of γ -irradiation on the corrosion behavior of Cu container
 - Increase E_{corr} & the consequences for localized corrosion & SCC
 - relevant dose rates \rightarrow no ennoblement of E_{corr}
 - high dose rates \rightarrow transient shift insufficient to increase probability of pit initiation
 - Generation of specific radiolytic species that may support localized corrosion or environmentally assisted cracking
 - NH_4^+ & NO_2^- ions can result in SCC
 - \rightarrow Low pH resulting from absorption of nitric acid vapor would preclude film formation
 - \rightarrow Pre-requisite for cracking
 - \rightarrow Forms in absence of O_2
 - \rightarrow SCC not possible as no film formation is possible without oxidant

RADIOLYSIS TRANSIENTS IN THE NEAR-FIELD

- Effects of γ -irradiation on the corrosion behavior of Cu container
 - Increase E_{corr} & the consequences for localized corrosion & SCC
 - relevant dose rates \rightarrow no ennoblement of E_{corr}
 - high dose rates \rightarrow transient shift insufficient to increase probability of pit initiation
 - Generation of specific radiolytic species that may support localized corrosion or environmentally assisted cracking
 - NH_4^+ & NO_2^- ions can result in SCC
 - \rightarrow Low pH resulting from absorption of nitric acid vapor would preclude film formation
 - \rightarrow Pre-requisite for cracking
 - \rightarrow Forms in absence of O_2
 - \rightarrow SCC not possible as no film formation is possible without oxidant
 - No H-related degradation mechanisms expected

RADIOLYSIS TRANSIENTS IN THE NEAR-FIELD

- Effects of γ -irradiation on the corrosion behavior of Cu container
 - Increase E_{corr} & the consequences for localized corrosion & SCC
 - relevant dose rates \rightarrow no ennoblement of E_{corr}
 - high dose rates \rightarrow transient shift insufficient to increase probability of pit initiation
 - Generation of specific radiolytic species that may support localized corrosion or environmentally assisted cracking
 - NH_4^+ & NO_2^- ions can result in SCC
 - \rightarrow Low pH resulting from absorption of nitric acid vapor would preclude film formation
 - \rightarrow Pre-requisite for cracking
 - \rightarrow Forms in absence of O_2
 - \rightarrow SCC not possible as no film formation is possible without oxidant
 - No H-related degradation mechanisms expected
- Radiation damage of Cu corrosion barrier negligible

EFFECT OF IRRADIATION ON C-STEEL CONTAINERS

- Water radiolysis products $\rightarrow E_{\text{corr}} \uparrow$
- Passivating film of magnetite & hematite

EFFECT OF IRRADIATION ON C-STEEL CONTAINERS

- Water radiolysis products $\rightarrow E_{\text{corr}} \uparrow$
- Passivating film of magnetite & hematite
- Factors that can have an impact on corrosion behavior under irradiation
 - Water & vapor hydration:
 - Water composition:
 - High pH & high ionic strength lower enhancement of corrosion rate

EFFECT OF IRRADIATION ON C-STEEL CONTAINERS

- Water radiolysis products $\rightarrow E_{\text{corr}} \uparrow$
- Passivating film of magnetite & hematite
- Factors that can have an impact on corrosion behavior under irradiation
 - Water & vapor hydration:
 - Water composition:
 - High pH & high ionic strength lower enhancement of corrosion rate
 - ↳ Influences Fe solubility protective ability

EFFECT OF IRRADIATION ON C-STEEL CONTAINERS

- Water radiolysis products $\rightarrow E_{\text{corr}} \uparrow$
- Passivating film of magnetite & hematite
- Factors that can have an impact on corrosion behavior under irradiation
 - Water & vapor hydration:
 - Water composition:
 - High pH & high ionic strength lower enhancement of corrosion rate
↳ Influences Fe solubility protective ability
 - Radiolytic species
 - H_2O_2 can change the nature of the formed corrosion products

EFFECT OF IRRADIATION ON C-STEEL CONTAINERS

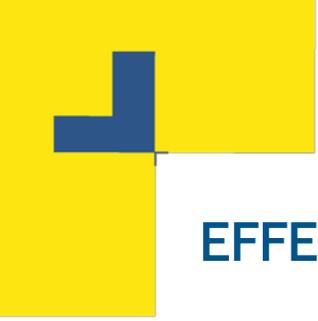
- Water radiolysis products → $E_{\text{corr}} \uparrow$
- Passivating film of magnetite & hematite
- Factors that can have an impact on corrosion behavior under irradiation
 - Water & vapor hydration:
 - Water composition:
 - High pH & high ionic strength lower enhancement of corrosion rate
↳ Influences Fe solubility protective ability
 - Radiolytic species
 - H_2O_2 can change the nature of the formed corrosion products
 - Relative humidity (under proton irradiation 3 MeV, 10 nA)
 - Max. corrosion rate observed for RH of 45 % ↔ 95 % without irradiation

EFFECT OF IRRADIATION ON C-STEEL CONTAINERS

- Water radiolysis products → $E_{\text{corr}} \uparrow$
- Passivating film of magnetite & hematite
- Factors that can have an impact on corrosion behavior under irradiation
 - Water & vapor hydration:
 - Water composition:
 - High pH & high ionic strength lower enhancement of corrosion rate
↳ Influences Fe solubility protective ability
 - Radiolytic species
 - H_2O_2 can change the nature of the formed corrosion products
 - Relative humidity (under proton irradiation 3 MeV, 10 nA)
 - Max. corrosion rate observed for RH of 45 % ↔ 95 % without irradiation
 - Irradiation source
 - Change the radiolysis products
 - High Linear Energy Transfer (LET) radiation: molecules ↑ + radicals ↓ ↔ low LET radiation: radicals ↑

EFFECT OF IRRADIATION ON C-STEEL CONTAINERS

- Water radiolysis products $\rightarrow E_{\text{corr}} \uparrow$
- Passivating film of magnetite & hematite
- Factors that can have an impact on corrosion behavior under irradiation
 - Water & vapor hydration:
 - Water composition:
 - High pH & high ionic strength lower enhancement of corrosion rate
↳ Influences Fe solubility protective ability
 - Radiolytic species
 - H_2O_2 can change the nature of the formed corrosion products
 - Relative humidity (under proton irradiation 3 MeV, 10 nA)
 - Max. corrosion rate observed for RH of 45 % \leftrightarrow 95 % without irradiation
 - Irradiation source
 - Change the radiolysis products
 - High Linear Energy Transfer (LET) radiation: molecules \uparrow + radicals \downarrow \leftrightarrow low LET radiation: radicals \uparrow
 - Buffer-container system
 - γ -irradiation + high temperature \rightarrow insignificant changes of the smectite content & physical properties of MX-80 bentonite after 1 y
 - Extensive pitting corrosion



EFFECT OF IRRADIATION ON C-STEEL CONTAINERS

- Factors with limited or no impact on corrosion behavior under irradiation
 - Steel composition & microstructure
 - Except chromium & low molybdenum steels

EFFECT OF IRRADIATION ON C-STEEL CONTAINERS

- Factors with limited or no impact on corrosion behavior under irradiation
 - Steel composition & microstructure
 - Except chromium & low molybdenum steels
 - Radiation at high temperature
 - Determines amount of corrosion products & oxide layer thickness

EFFECT OF IRRADIATION ON C-STEEL CONTAINERS

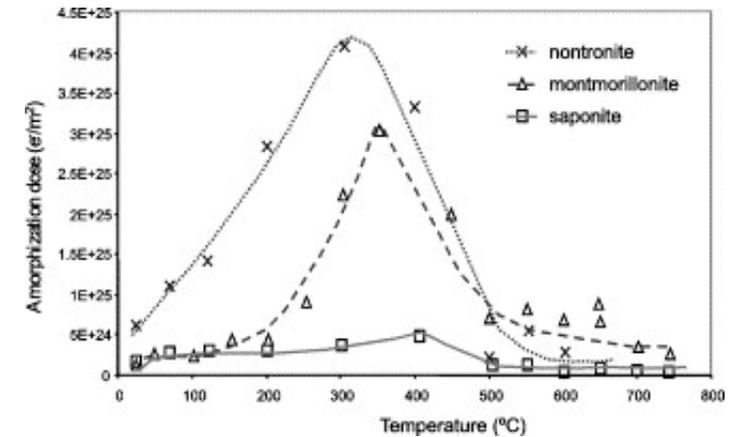
- Factors with limited or no impact on corrosion behavior under irradiation
 - Steel composition & microstructure
 - Except chromium & low molybdenum steels
 - Radiation at high temperature
 - Determines amount of corrosion products & oxide layer thickness
 - Total dose & dose rate
 - Limited in time, corrosion rates often evolve toward those in unirradiated conditions
 - Quite high doses rates (kGy/h) range are necessary to show corrosion enhancement

EFFECT OF IRRADIATION ON BUFFER MATERIALS

- Intact container ↔ container failure
 - $\gamma \leftrightarrow \alpha$

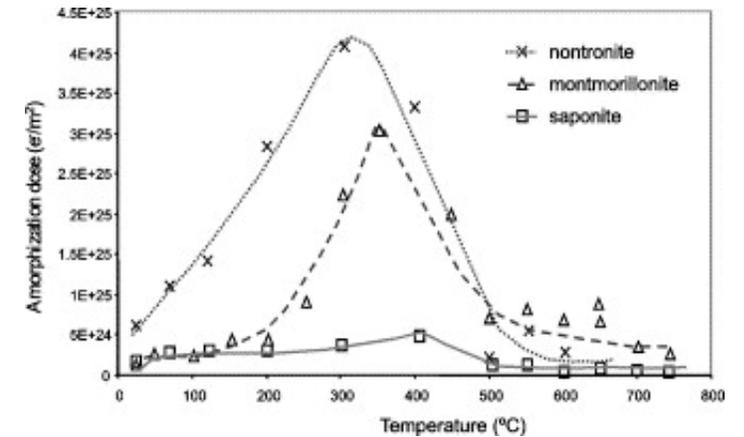
EFFECT OF IRRADIATION ON BUFFER MATERIALS

- Intact container ↔ container failure
 - $\gamma \leftrightarrow \alpha$
- Role of interlayer cations
 - Electron beam of 200 keV → amorphization dose depends on type of clay but requires extremely high doses, many orders of magnitude higher than possible in the repository
 - distinct interlayer cation substitutions
 - composition & distribution of accessory minerals



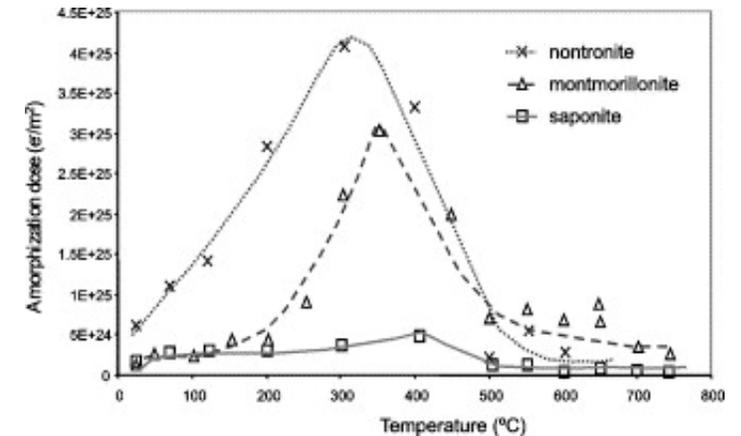
EFFECT OF IRRADIATION ON BUFFER MATERIALS

- Intact container ↔ container failure
 - $\gamma \leftrightarrow \alpha$
- Role of interlayer cations
 - Electron beam of 200 keV → amorphization dose depends on type of clay but requires extremely high doses, many orders of magnitude higher than possible in the repository
 - distinct interlayer cation substitutions
 - composition & distribution of accessory minerals
- Influence of temperature
 - Defects by radiation + their thermal annealing
 - Radiation decreases temp. at which dehydroxylation occurs



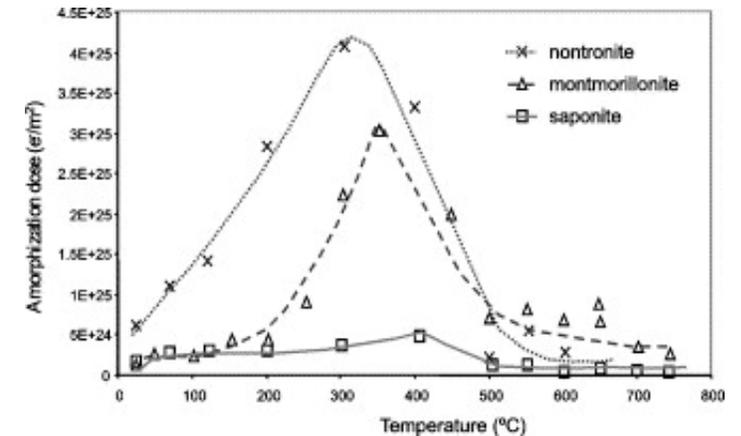
EFFECT OF IRRADIATION ON BUFFER MATERIALS

- Intact container ↔ container failure
 - $\gamma \leftrightarrow \alpha$
- Role of interlayer cations
 - Electron beam of 200 keV → amorphization dose depends on type of clay but requires extremely high doses, many orders of magnitude higher than possible in the repository
 - distinct interlayer cation substitutions
 - composition & distribution of accessory minerals
- Influence of temperature
 - Defects by radiation + their thermal annealing
 - Radiation decreases temp. at which dehydroxylation occurs
- Influence of water & vapor hydration
 - Radiation stability ↓ with water content → radiolysis of interlayer or pore water



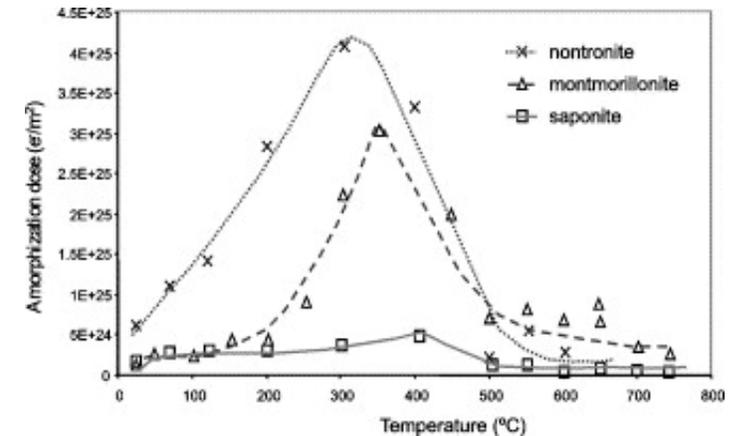
EFFECT OF IRRADIATION ON BUFFER MATERIALS

- Intact container ↔ container failure
 - $\gamma \leftrightarrow \alpha$
- Role of interlayer cations
 - Electron beam of 200 keV → amorphization dose depends on type of clay but requires extremely high doses, many orders of magnitude higher than possible in the repository
 - distinct interlayer cation substitutions
 - composition & distribution of accessory minerals
- Influence of temperature
 - Defects by radiation + their thermal annealing
 - Radiation decreases temp. at which dehydroxylation occurs
- Influence of water & vapor hydration
 - Radiation stability ↓ with water content → radiolysis of interlayer or pore water
 - Radiolytic species can react with bentonite → change redox state
 - Structural Fe^{2+} & Fe^{3+} → influence on physical properties of the clay



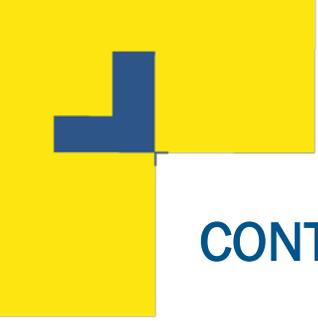
EFFECT OF IRRADIATION ON BUFFER MATERIALS

- Intact container ↔ container failure
 - $\gamma \leftrightarrow \alpha$
- Role of interlayer cations
 - Electron beam of 200 keV → amorphization dose depends on type of clay but requires extremely high doses, many orders of magnitude higher than possible in the repository
 - distinct interlayer cation substitutions
 - composition & distribution of accessory minerals
- Influence of temperature
 - Defects by radiation + their thermal annealing
 - Radiation decreases temp. at which dehydroxylation occurs
- Influence of water & vapor hydration
 - Radiation stability ↓ with water content → radiolysis of interlayer or pore water
 - Radiolytic species can react with bentonite → change redox state
 - Structural Fe^{2+} & Fe^{3+} → influence on physical properties of the clay
 - No deleterious effect on clay stability of a created gas phase



EFFECT OF IRRADIATION ON BUFFER MATERIALS

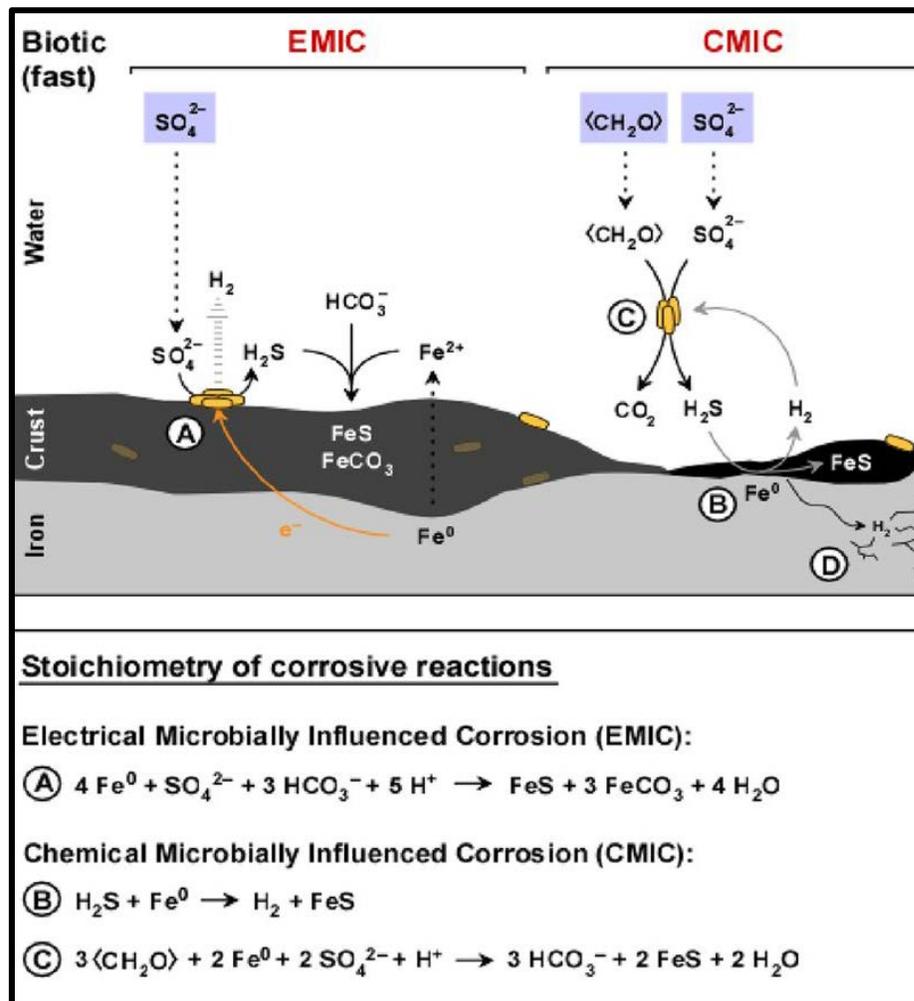
- Influence of radiation source efficiency to induce amorphization
 - Heavy ions → atomic displacements & collision cascades → origin of extended defects & amorphization
 - Ionizing radiation → thermally unstable electronic point defects
- Influence of dose rate & total dose
 - Very high doses are needed to induce changes, vastly in excess of what is possible in a repository



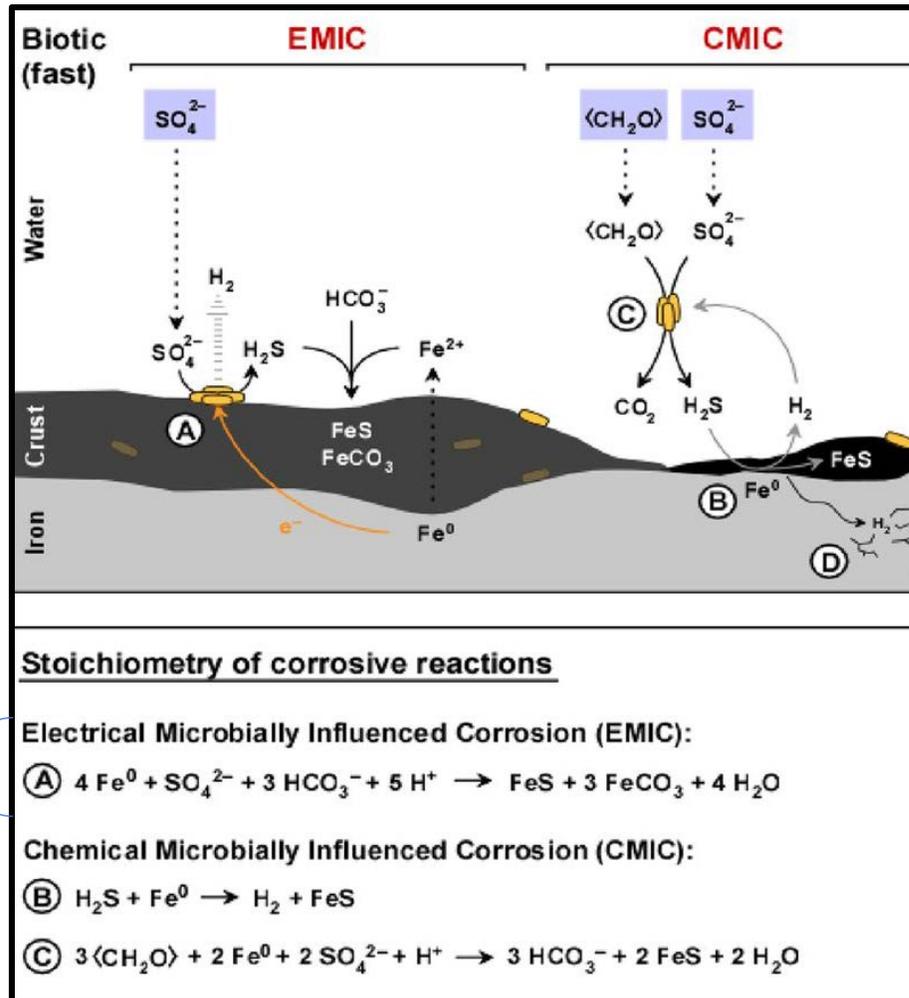
CONTENT

- Introduction
- Thermal transients
- Pore water transients
- Redox transients
- Saturation transients
- Mechanical transients
- Transitional processes involving gas generation
- Effects of irradiation
- **Effects of Microbial processes**
- Example of an integrated test
- Summary

MICROBIAL CORROSION IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL



MICROBIAL CORROSION IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL

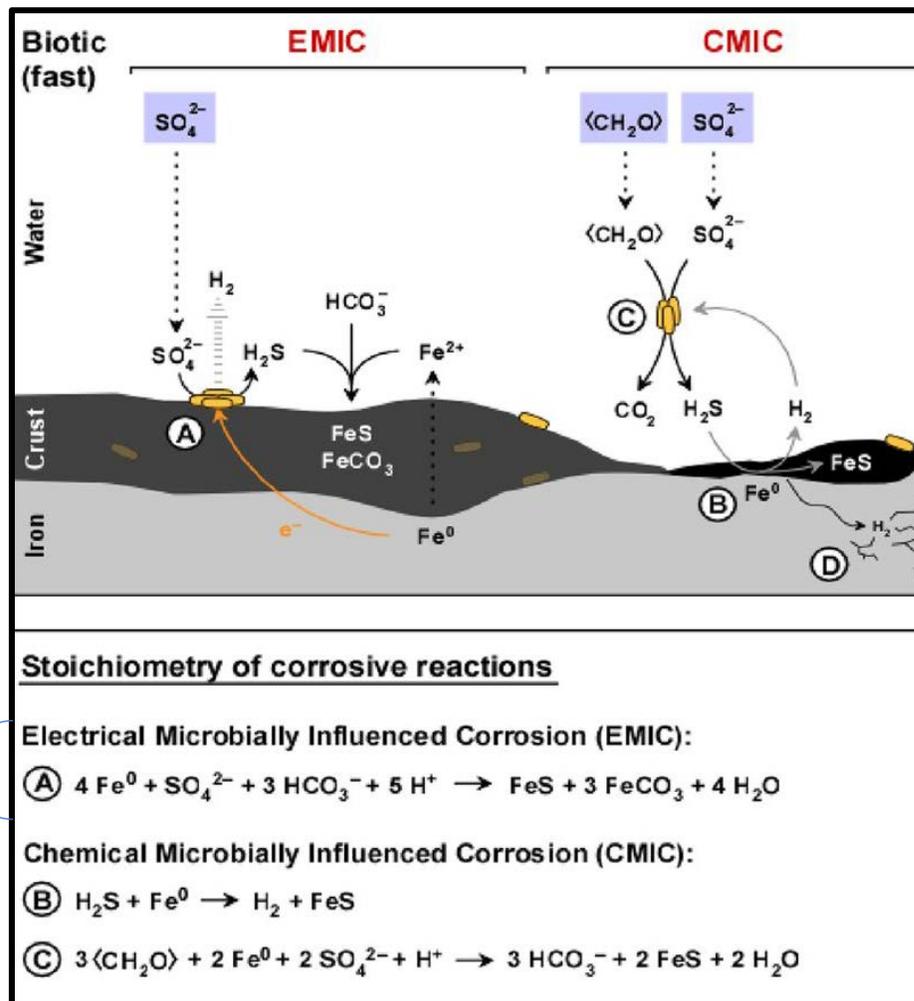


Biofilm needed



Only relevant in the absence of bentonite backfill

MICROBIAL CORROSION IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL



Anoxic corrosion

Anode: $\text{M}^0 \leftrightarrow \text{M}^{2+} + 2e^-$ (M= Fe or Cu)

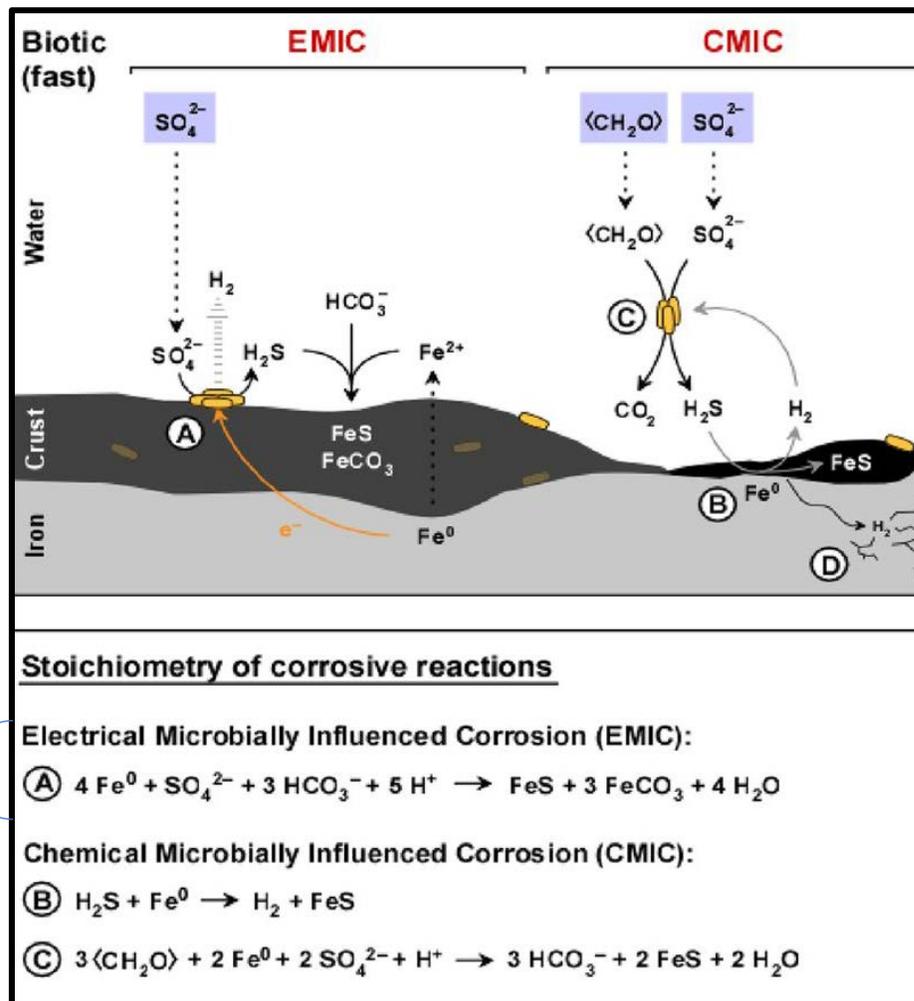
Cathode: $2\text{H}_2\text{O} + 2e^- \leftrightarrow \text{H}_2 + 2\text{OH}^-$

Biofilm needed

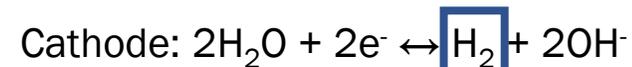
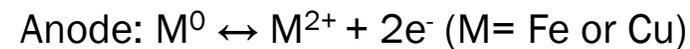


Only relevant in the absence of bentonite backfill

MICROBIAL CORROSION IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL



Anoxic corrosion



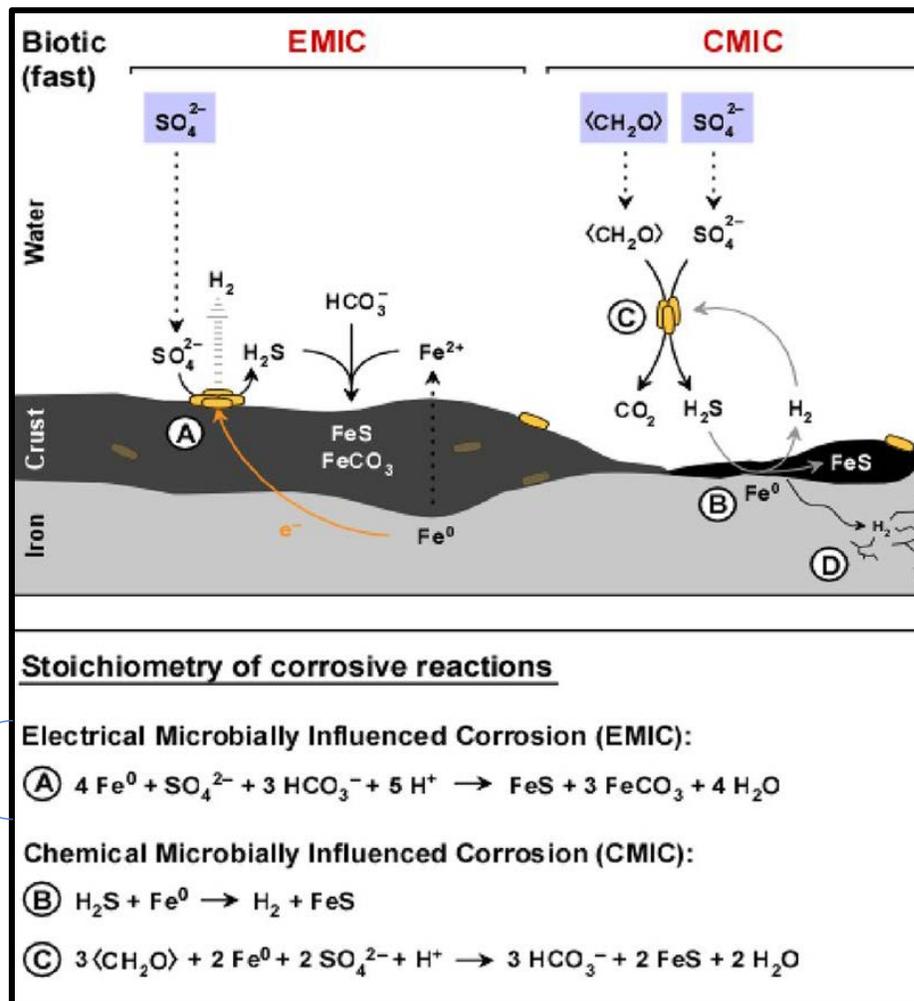
consumed by microorganisms

cathodic depolarization

Biofilm needed

Only relevant in the absence of bentonite backfill

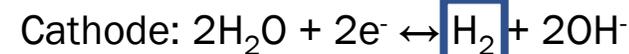
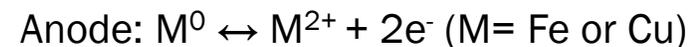
MICROBIAL CORROSION IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL



Biofilm needed

Only relevant in the absence of bentonite backfill

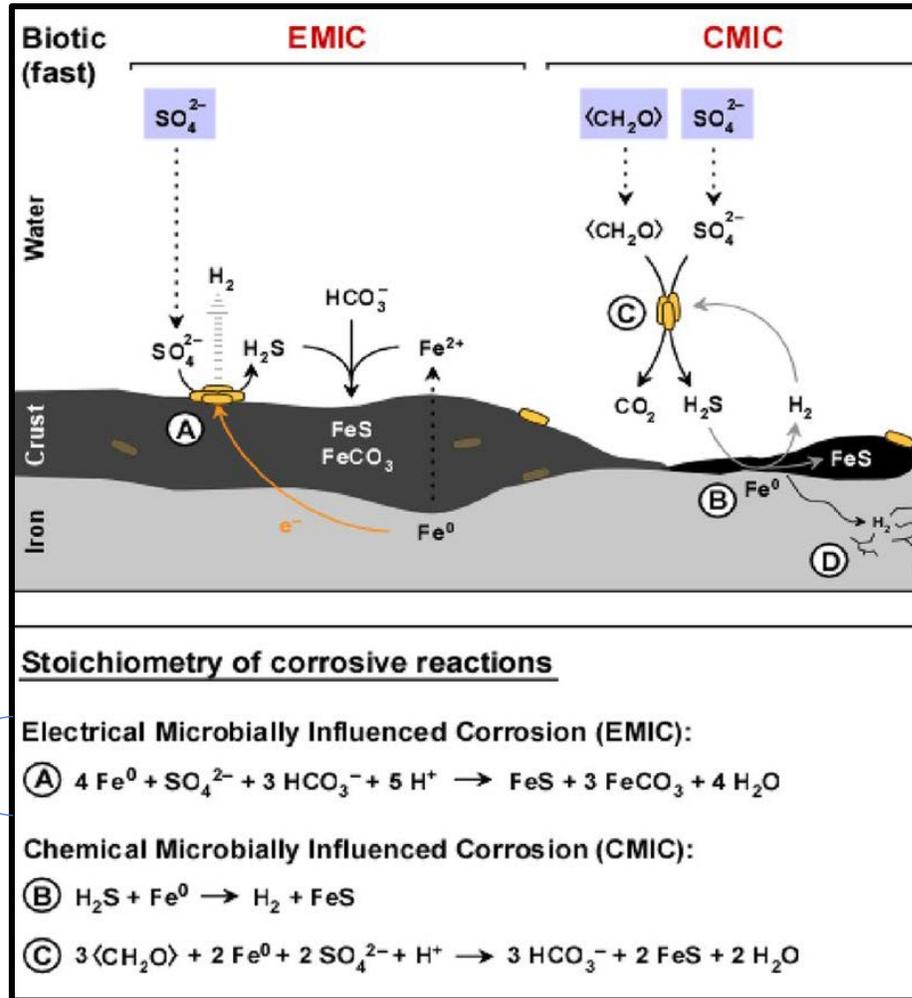
Anoxic corrosion



consumed by microorganisms

cathodic polarization

MICROBIAL CORROSION IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL



Biofilm needed

Only relevant in the absence of bentonite backfill

Anoxic corrosion

Anode: $\text{M}^0 \leftrightarrow \text{M}^{2+} + 2\text{e}^-$ (M= Fe or Cu)

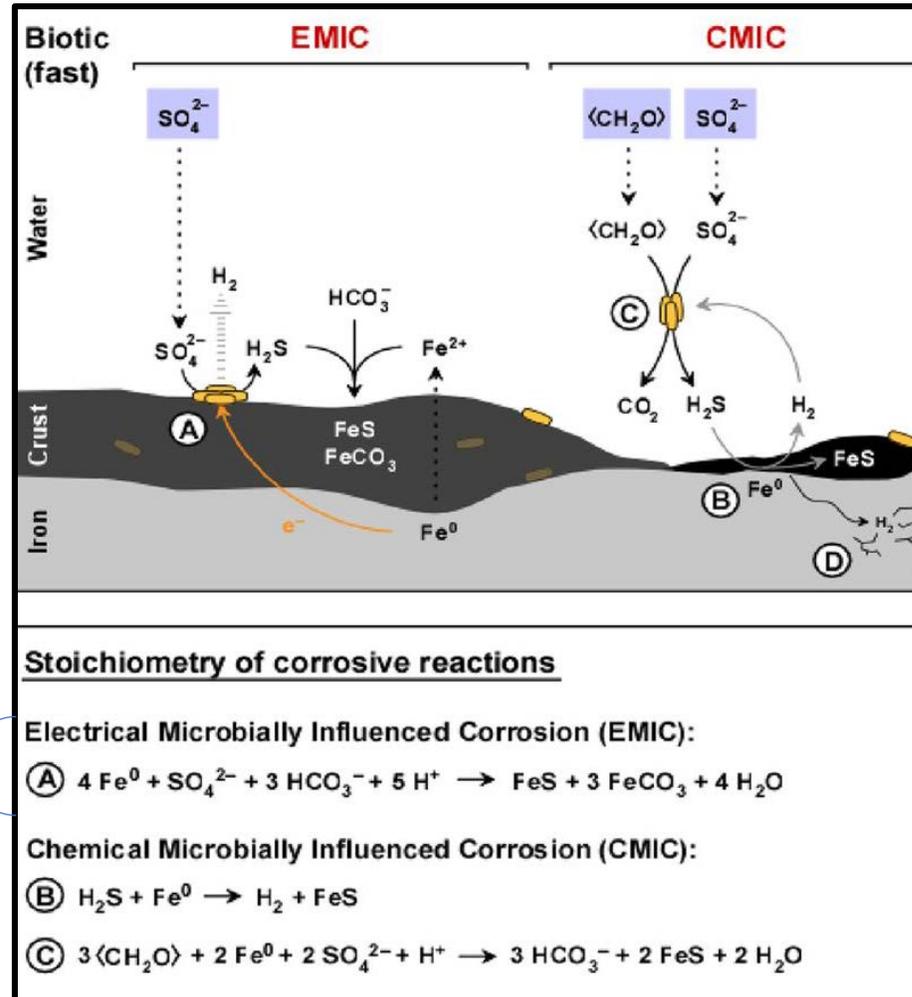
Cathode: $2\text{H}_2\text{O} + 2\text{e}^- \leftrightarrow \text{H}_2 + 2\text{OH}^-$

consumed by microorganisms

cathodic polarization

Corrosive by-products of microbial metabolism

MICROBIAL CORROSION IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL



Biofilm needed

Only relevant in the absence of bentonite backfill

Anoxic corrosion

Anode: $\text{M}^0 \leftrightarrow \text{M}^{2+} + 2\text{e}^-$ (M= Fe or Cu)

Cathode: $2\text{H}_2\text{O} + 2\text{e}^- \leftrightarrow \text{H}_2 + 2\text{OH}^-$

consumed by microorganisms

cathodic polarization

Corrosive by-products of microbial metabolism

Sulfide oxidation

Manganese oxidation

Iron oxidation

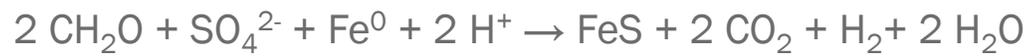
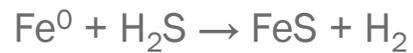
Sulfate reduction

Iron reduction

Production acidic compounds

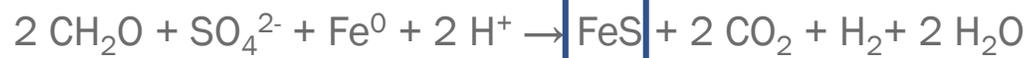
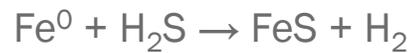
DISSIMILATORY SULFATE REDUCTION

CMIC



DISSIMILATORY SULFATE REDUCTION

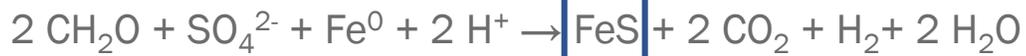
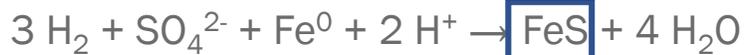
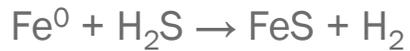
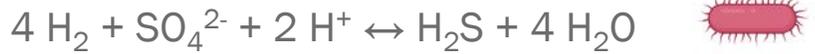
CMIC



↓
Protective layer

DISSIMILATORY SULFATE REDUCTION

CMIC



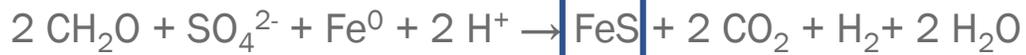
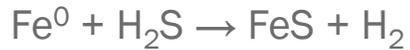
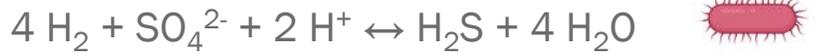
Protective layer

Decelerate in time, except when FeS film is disrupted

Can take place as long as a diffusion path for H₂S to the metal container exists

DISSIMILATORY SULFATE REDUCTION

CMIC



Protective layer

Decelerate in time, except when FeS film is disrupted

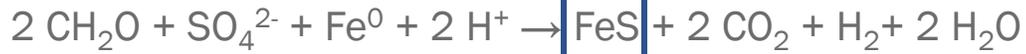
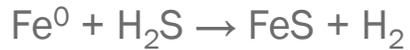
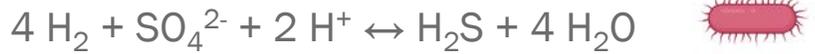
Can take place as long as a diffusion path for H₂S to the metal container exists

EMIC



DISSIMILATORY SULFATE REDUCTION

CMIC



Protective layer

Decelerate in time, except when FeS film is disrupted

Can take place as long as a diffusion path for H₂S to the metal container exists

EMIC



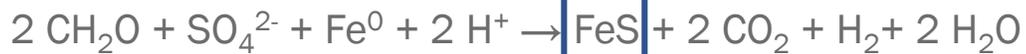
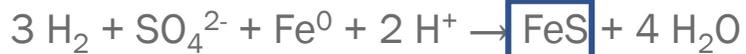
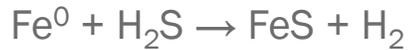
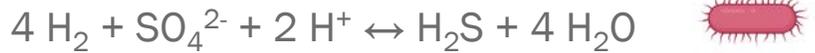
No protective layer: conductivity of FeS crust allows the extraction of e⁻ from metallic iron & their transport through the FeS

faster

Unlikely that biofilms will develop on container surfaces

DISSIMILATORY SULFATE REDUCTION

CMIC

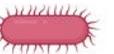


Protective layer

Decelerate in time, except when FeS film is disrupted

Can take place as long as a diffusion path for H₂S to the metal container exists

EMIC



No protective layer: conductivity of FeS crust allows the extraction of e⁻ from metallic iron & their transport through the FeS

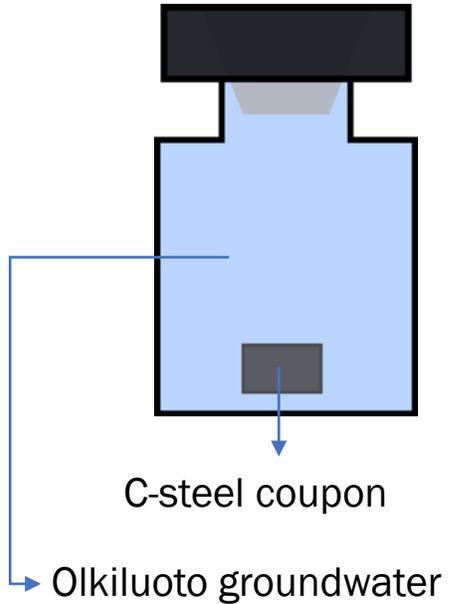
faster

Unlikely that biofilms will develop on container surfaces



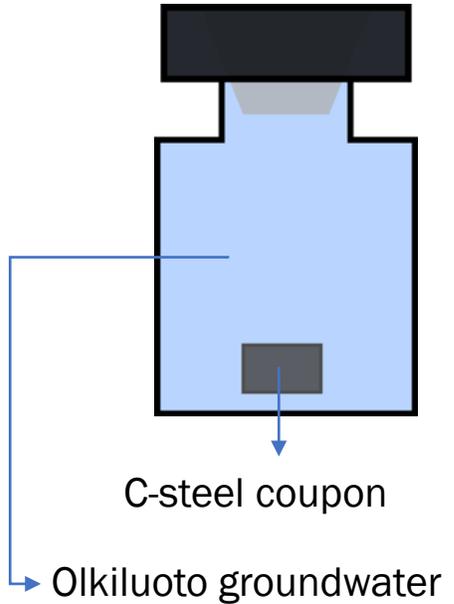
Which of the 2

MICROBIAL INDUCED CORROSION: EXPERIMENTAL WORK

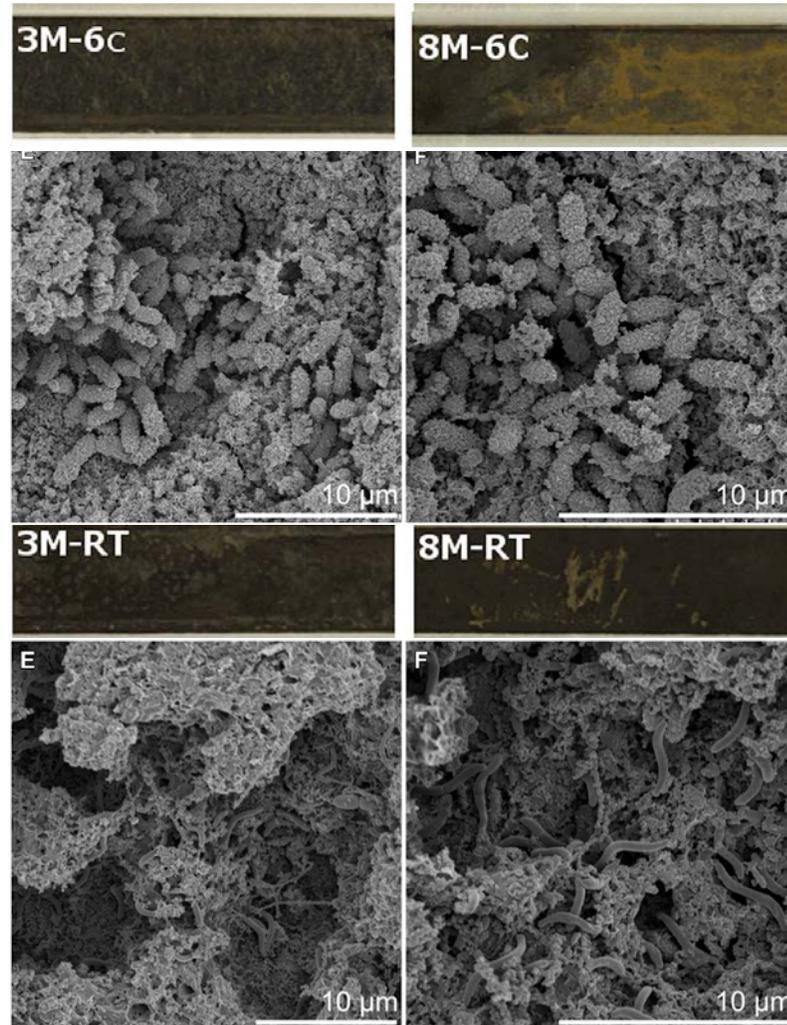


3 & 8 months at RT or 6°C in
anoxic conditions

MICROBIAL INDUCED CORROSION: EXPERIMENTAL WORK

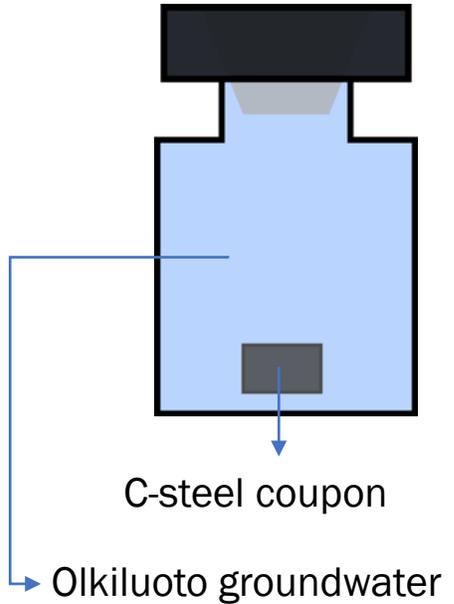


3 & 8 months at RT or 6°C in anoxic conditions

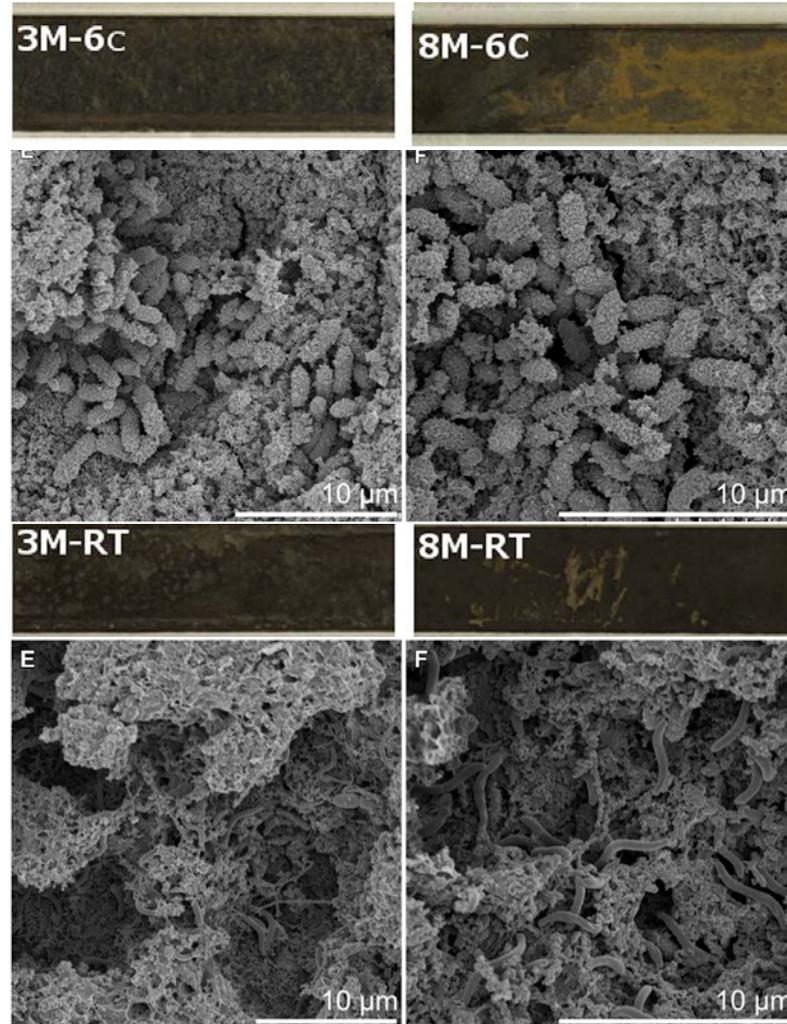


- Biofilm formation on the surface of the coupons
- Pitting corrosion

MICROBIAL INDUCED CORROSION: EXPERIMENTAL WORK



3 & 8 months at RT or 6°C in anoxic conditions

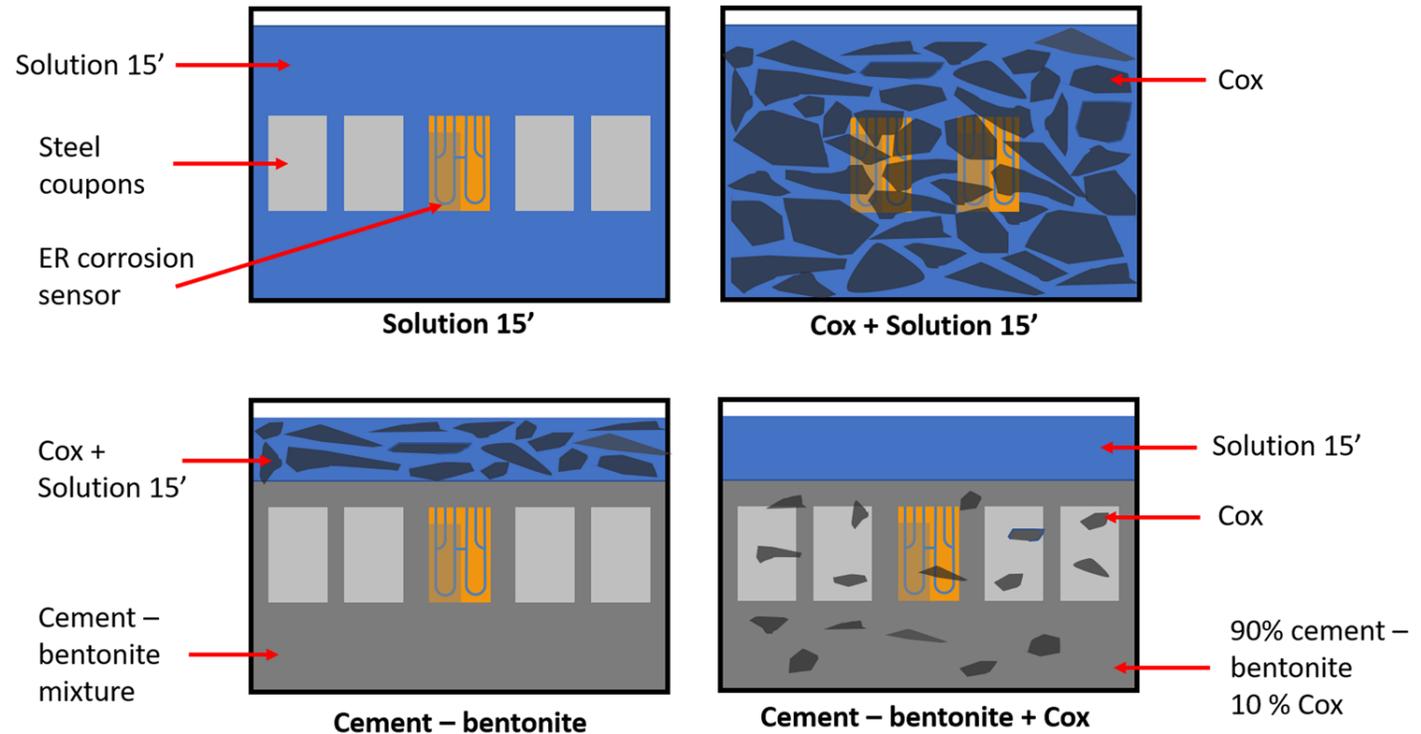


- Biofilm formation on the surface of the coupons
- Pitting corrosion
- Betaproteobacteria
- Iron oxidizers
- Iron reducers
- SRB

MICROBIAL INDUCED CORROSION: EXPERIMENTAL WORK

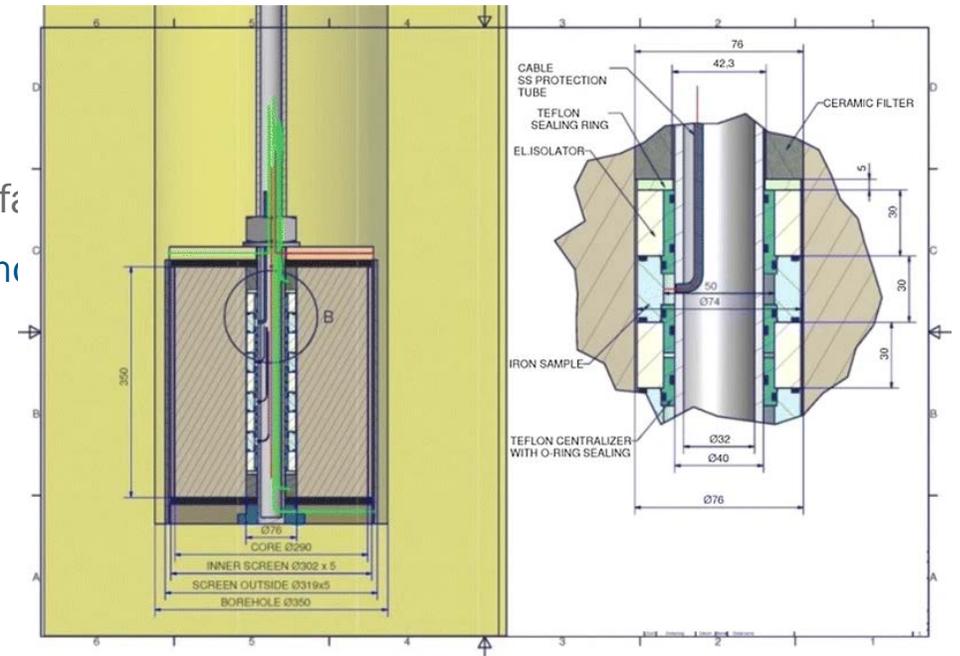
- 47 days incubation

- Strong corrosion in exp. with solution representative of the Callovo-Oxfordian (Cox) rock formation (=solution 15') where microorganisms were added
- Cement-bentonite → decrease in corrosion
- Embedding clay rock in cement/bentonite mix further decreased corrosion
- Microbial community dominated by *Firmicutes*, including SRB
- But SRB activity is inhibited by alkaline conditions



MICROBIAL INDUCED CORROSION: EXPERIMENTAL WORK

- IC experiment @ Mont Terri
 - Dismantled after 7 years
 - Several layers of corrosion products on metal surface/clay interface
 - magnetite, goethite, lepidocrocite, akaganeite, chukanovite, and siderite
 - Fe sulfide at various oxidation states & elemental S
 - Original surface replaced by FeS → MIC



MICROBIAL INDUCED CORROSION: EXPERIMENTAL WORK

- IC experiment @ Mont Terri
 - Dismantled after 7 years
 - Several layers of corrosion products on metal surface/clay interface
 - magnetite, goethite, lepidocrocite, akageneite, chukanovite, and siderite
 - Fe sulfide at various oxidation states & elemental S
 - Original surface replaced by FeS → MIC
- IC-A experiment @ Mont Terri (still ongoing)
 - C-steel coupons in MX-80 with different dry density
 - No microbial impact on corrosion
 - No growth of SRB
 - due to persistence of O₂ in bentonite
 - bentonite is fully saturated when O₂ is depleted

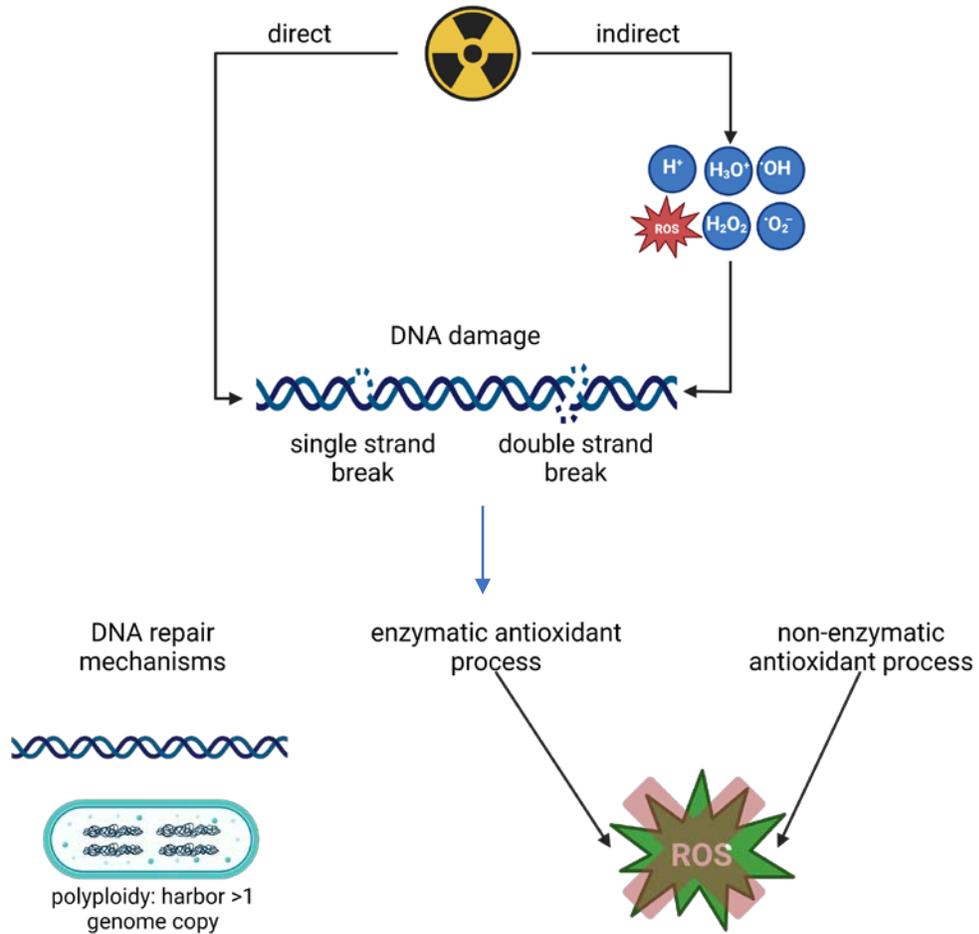


MICROBIAL INDUCED CORROSION: EXPERIMENTAL WORK

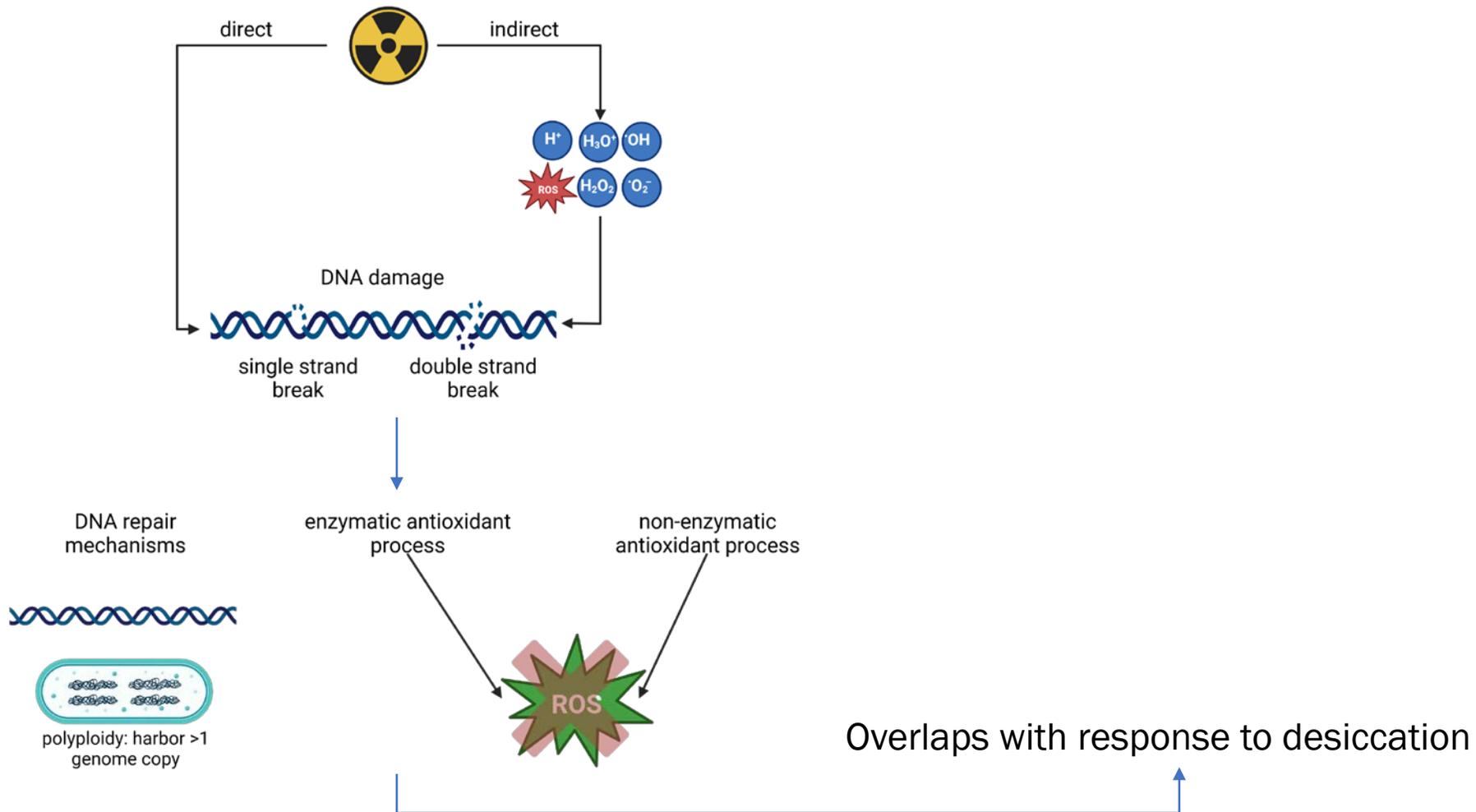
- IC experiment @ Mont Terri
 - Dismantled after 7 years
 - Several layers of corrosion products on metal surface/clay interface
 - magnetite, goethite, lepidocrocite, akageneite, chukanovite, and siderite
 - Fe sulfide at various oxidation states & elemental S
 - Original surface replaced by FeS → MIC
- IC-A experiment @ Mont Terri (still ongoing)
 - C-steel coupons in MX-80 with different dry density
 - No microbial impact on corrosion
 - No growth of SRB
 - due to persistence of O₂ in bentonite
 - bentonite is fully saturated when O₂ is depleted
 - Indigenous bentonite community grew & persisted



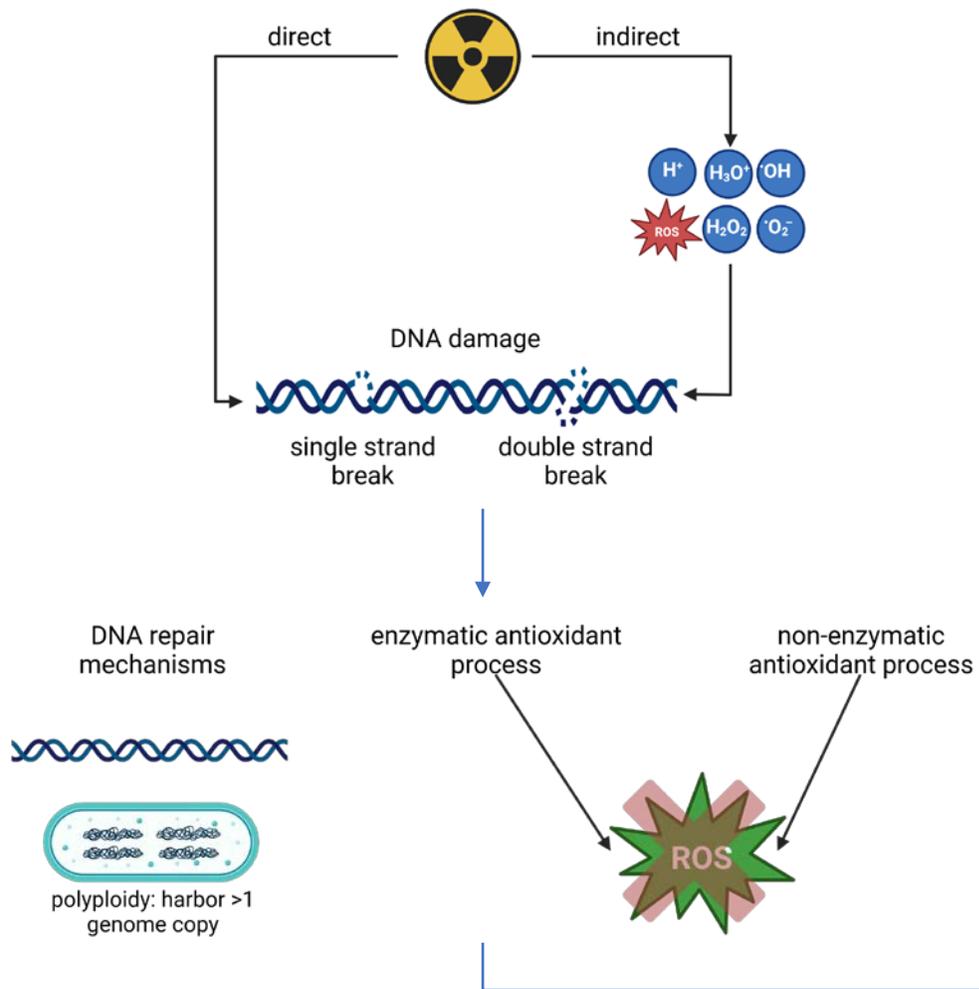
IMPACT OF IRRADIATION ON MICROBIAL VIABILITY IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL



IMPACT OF IRRADIATION ON MICROBIAL VIABILITY IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL



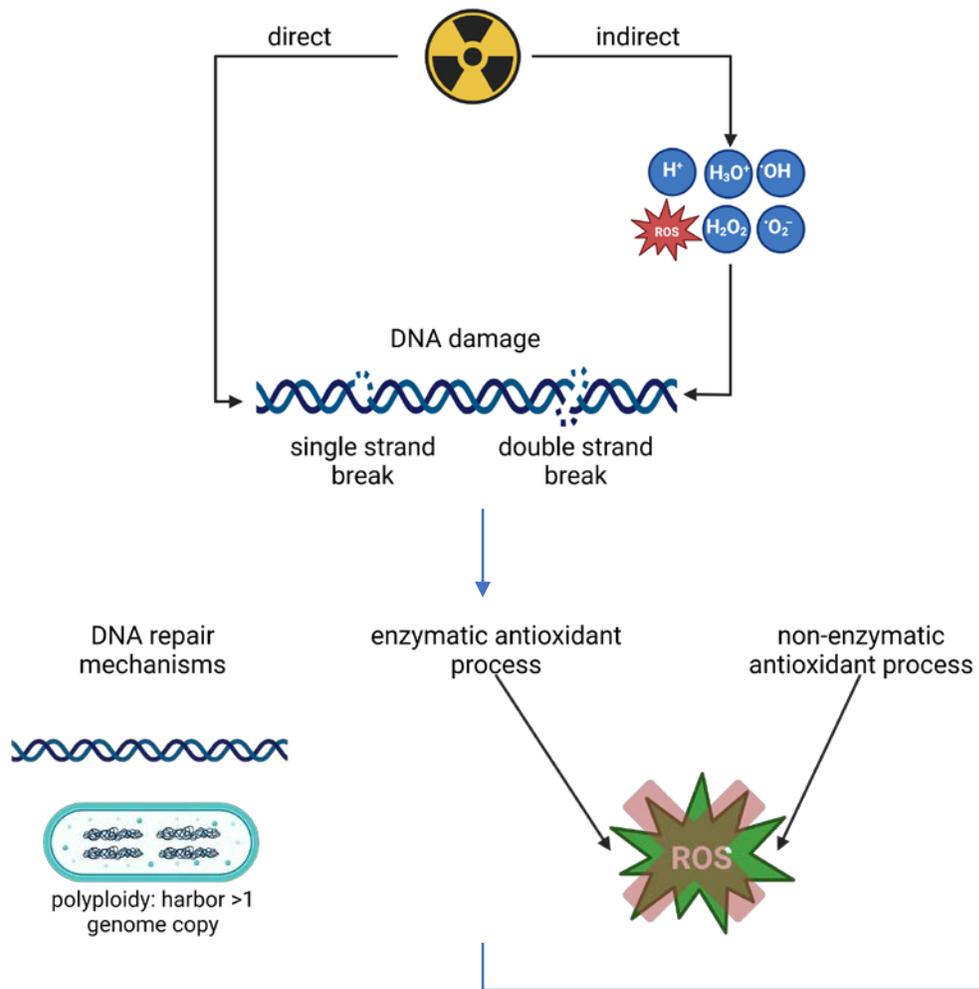
IMPACT OF IRRADIATION ON MICROBIAL VIABILITY IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL



Radiation sensitivity depends on:

- Acute or chronic irradiation
- Cell concentration
- Vegetative state
- Physiological features
- Genetic features

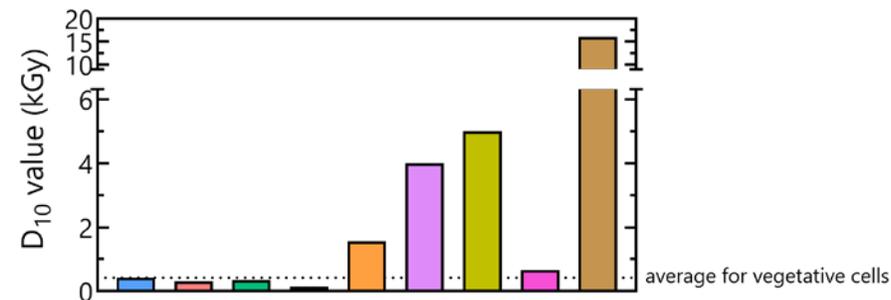
IMPACT OF IRRADIATION ON MICROBIAL VIABILITY IN THE CONTEXT OF NUCLEAR WASTE DISPOSAL



Radiation sensitivity depends on:

- Acute or chronic irradiation
- Cell concentration
- Vegetative state
- Physiological features
- Genetic features

Big differences between \neq bacteria



Overlaps with response to desiccation

IMPACT OF IRRADIATION ON MICROBIAL VIABILITY

- Contaminated sites (e.g. Chernobyl, Hanford) harbor microbial community
 - Chronic low dose exposure ↔ **acute high dose rate**
 - Soil biota exposed to 1h γ -irradiation every week during 6 weeks
 - 0.1 kGy/h/week
 - 1 kGy/h/week
 - 3 kGy/h/week
- Bacterial diversity ↓ ↔ fungi & algae diversity ↑
- Changes in community composition → potential radiation-tolerant groups were identified

IMPACT OF IRRADIATION ON MICROBIAL VIABILITY

- Contaminated sites (e.g. Chernobyl, Hanford) harbor microbial community
- Chronic low dose exposure ↔ **acute high dose rate**
 - Soil biota exposed to 1h γ -irradiation every week during 6 weeks
 - 0.1 kGy/h/week
 - 1 kGy/h/week
 - 3 kGy/h/week

Bacterial diversity ↓ ↔ fungi & algae diversity ↑

Changes in community composition → potential radiation-tolerant groups were identified
 - Sediment exposed to γ -irradiation for 8 weeks was not restrictive for microbial processes
 - 0.5 Gy/h → 0.6 kGy
 - 30 Gy/h → 38.6 kGy
 - BaM Bentonite + granitic porewater VITA exposed to γ -irradiation for 9 weeks at 13 Gy/h (19.6 kGy) did not completely eliminate bacteria

IMPACT OF IRRADIATION ON MICROBIAL VIABILITY

- Contaminated sites (e.g. Chernobyl, Hanford) harbor microbial community
- Chronic low dose exposure ↔ **acute high dose rate**
 - Soil biota exposed to 1h γ -irradiation every week during 6 weeks
 - 0.1 kGy/h/week
 - 1 kGy/h/week
 - 3 kGy/h/week

Bacterial diversity ↓ ↔ fungi & algae diversity ↑

Changes in community composition → potential radiation-tolerant groups were identified
 - Sediment exposed to γ -irradiation for 8 weeks was not restrictive for microbial processes
 - 0.5 Gy/h → 0.6 kGy
 - 30 Gy/h → 38.6 kGy
 - BaM Bentonite + granitic porewater VITA exposed to γ -irradiation for 9 weeks at 13 Gy/h (19.6 kGy) did not completely eliminate bacteria
- 25 kGy for routine sterilization procedures of foodstuff & medical application
- ± 50 kGy to sterilize bentonite
- > 70 kGy might be needed to eliminate radiation resistant bacteria from soil

IMPACT OF IRRADIATION ON MICROBIAL VIABILITY

- Contaminated sites (e.g. Chernobyl, Hanford) harbor microbial community

- Chronic low dose exposure ↔ **acute high dose rate**

- Soil biota exposed to 1h γ -irradiation every week during 6 weeks

- 0.1 kGy/h/week

- 1 kGy/h/week

- 3 kGy/h/week

Bacterial diversity ↓ ↔ fungi & algae diversity ↑

Changes in community composition → potential radiation-tolerant groups were identified

- Sediment exposed to γ -irradiation for 8 weeks was not restrictive for microbial processes

- 0.5 Gy/h → 0.6 kGy

- 30 Gy/h → 38.6 kGy

- BaM Bentonite + granitic porewater VITA exposed to γ -irradiation for 9 weeks at 13 Gy/h (19.6 kGy) did not completely eliminate bacteria

- 25 kGy for routine sterilization procedures of foodstuff & medical application

- ± 50 kGy to sterilize bentonite

- > 70 kGy might be needed to eliminate radiation resistant bacteria from soil

SKB-3 concept (0.055 Gy/h) → 145 years before it is reached



INHIBITION OF MICROBIAL ACTIVITY AND GROWTH BY BENTONITE

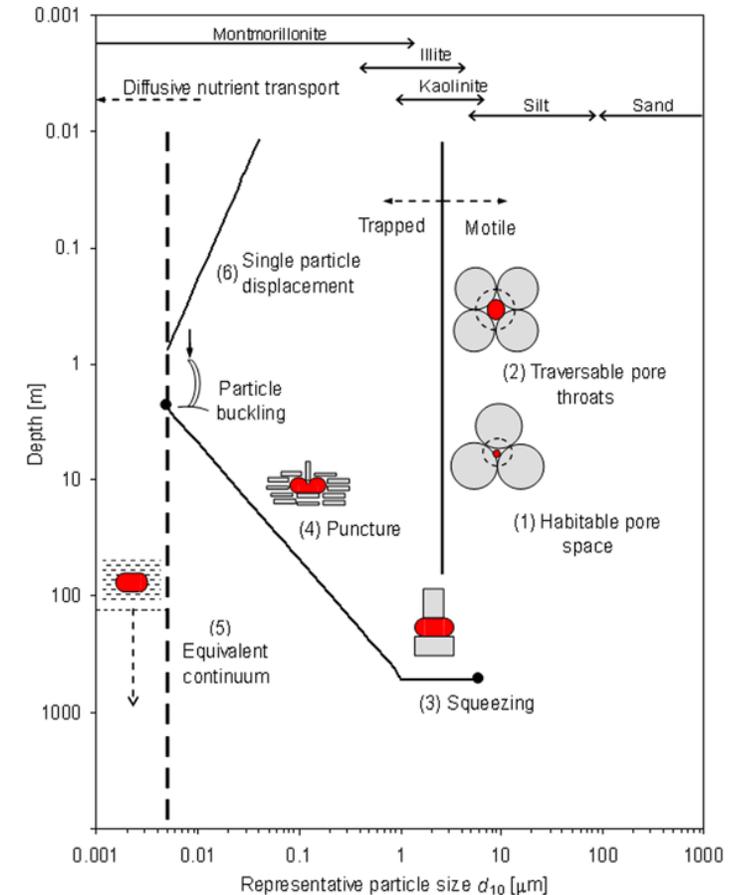
- Uncompacted bentonite harbors diverse microbial community, including SRB

INHIBITION OF MICROBIAL ACTIVITY AND GROWTH BY BENTONITE

- Uncompacted bentonite harbors diverse microbial community, including SRB
 - Compacted bentonite
 - High swelling pressure
 - Low water activity (<0.96)
- } Limit microbial activity

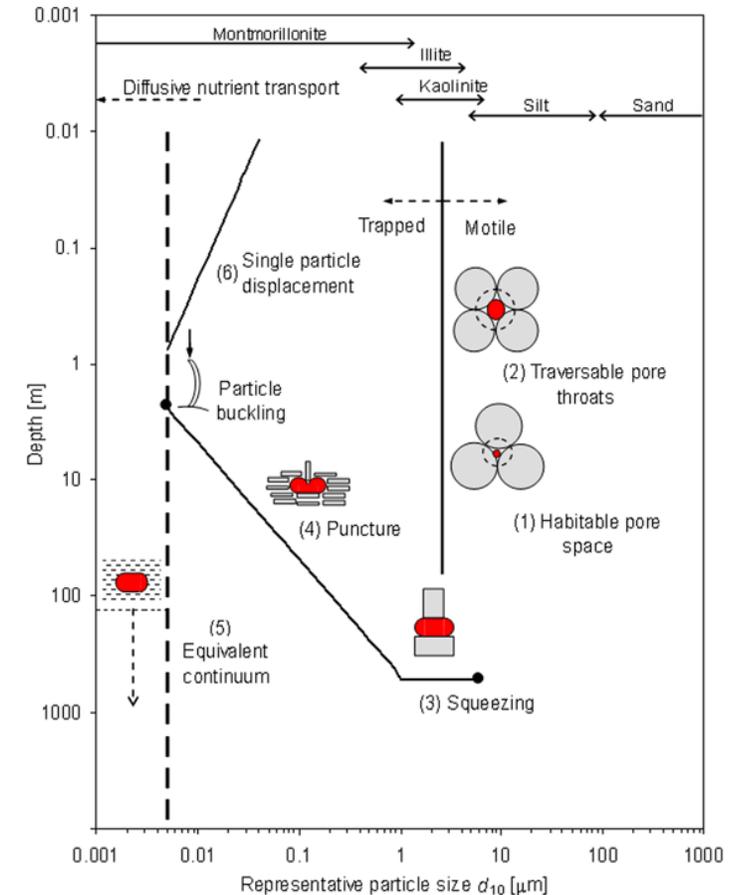
INHIBITION OF MICROBIAL ACTIVITY AND GROWTH BY BENTONITE

- Uncompacted bentonite harbors diverse microbial community, including SRB
- Compacted bentonite
 - High swelling pressure
 - Low water activity (<0.96)
 } Limit microbial activity
- High swelling pressure → space limitation
 - Direct effects
 - Indirect effects → Diffusion limited nutrient transport



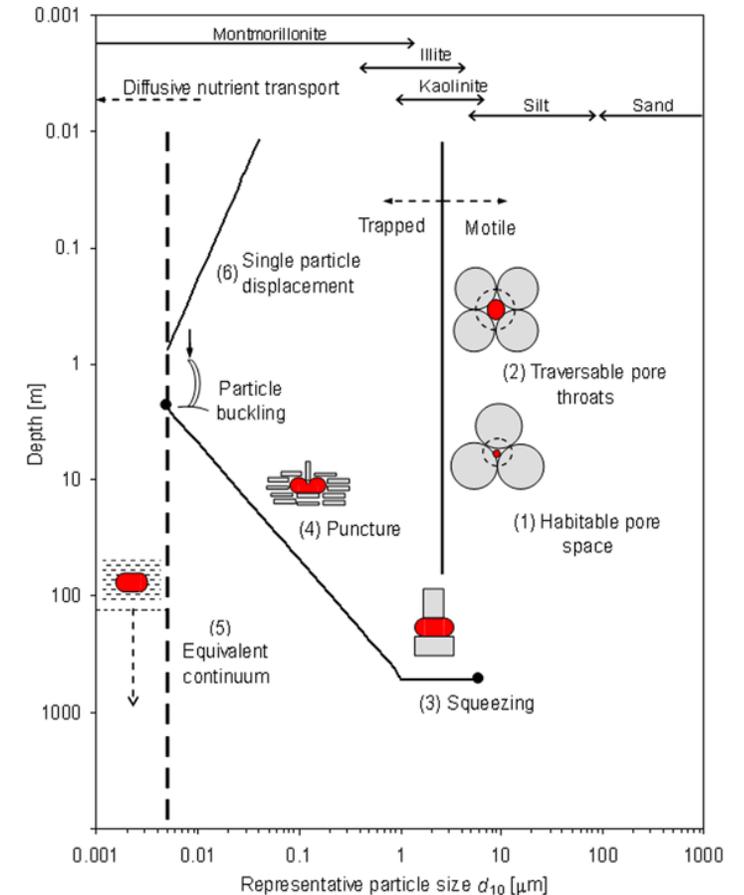
INHIBITION OF MICROBIAL ACTIVITY AND GROWTH BY BENTONITE

- Uncompacted bentonite harbors diverse microbial community, including SRB
- Compacted bentonite
 - High swelling pressure
 - Low water activity (<0.96)
 Limit microbial activity
- High swelling pressure → space limitation
 - Direct effects
 - Indirect effects → Diffusion limited nutrient transport
- Depend on dry density
 - Dry density ↑ → water activity ↓ & swelling pressure ↑
 - Uniform dry density $\geq 1600 \text{ kg/m}^3$ → microbial activity is limited



INHIBITION OF MICROBIAL ACTIVITY AND GROWTH BY BENTONITE

- Uncompacted bentonite harbors diverse microbial community, including SRB
- Compacted bentonite
 - High swelling pressure
 - Low water activity (<0.96)
 Limit microbial activity
- High swelling pressure → space limitation
 - Direct effects
 - Indirect effects → Diffusion limited nutrient transport
- Depend on dry density
 - Dry density ↑ → water activity ↓ & swelling pressure ↑
 - Uniform dry density ≥ 1600 kg/m³ → microbial activity is limited
 - Fundamental basis of this limit?
 - Why is there a difference between different bentonites?



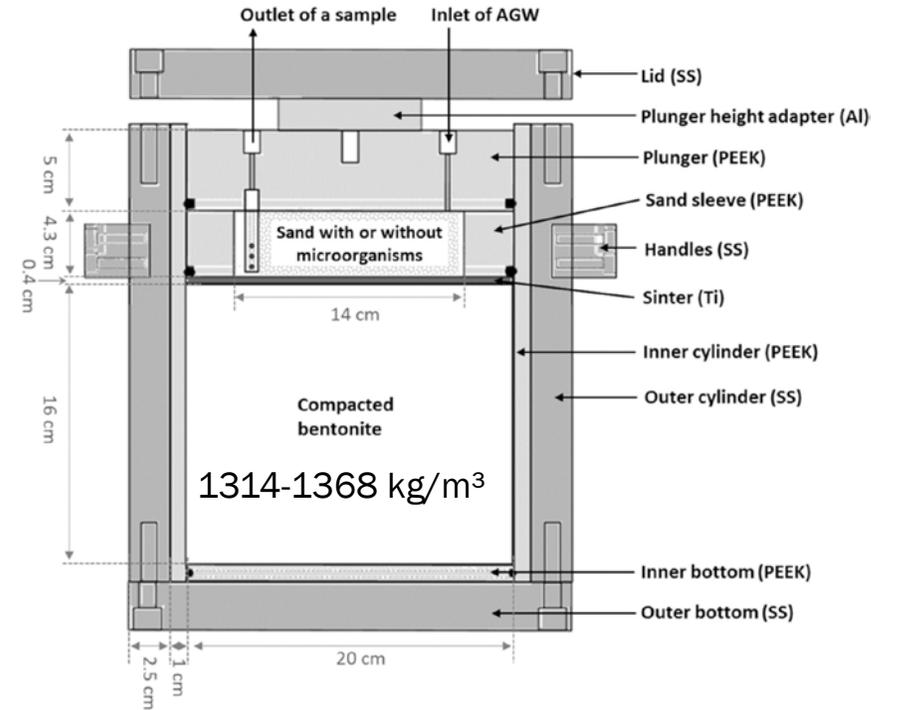
INHIBITION OF MICROBIAL ACTIVITY AND GROWTH BY BENTONITE

- Nutrient limited environment
 - Low available organic carbon mainly composed of plant-derived waxes and highly recalcitrant aromatic carbon
 - Recent analysis
 - Alkanes
 - Toluenes
 - Aromatic compounds
- } Biodegradable, but amount?

INHIBITION OF MICROBIAL ACTIVITY AND GROWTH BY BENTONITE

- Nutrient limited environment
 - Low available organic carbon mainly composed of plant-derived waxes and highly recalcitrant aromatic carbon
 - Recent analysis
 - Alkanes
 - Toluenes
 - Aromatic compounds
- Organic material in compacted bentonite is able to sustain SRB
 - Wyoming, Indian & Bulgarian

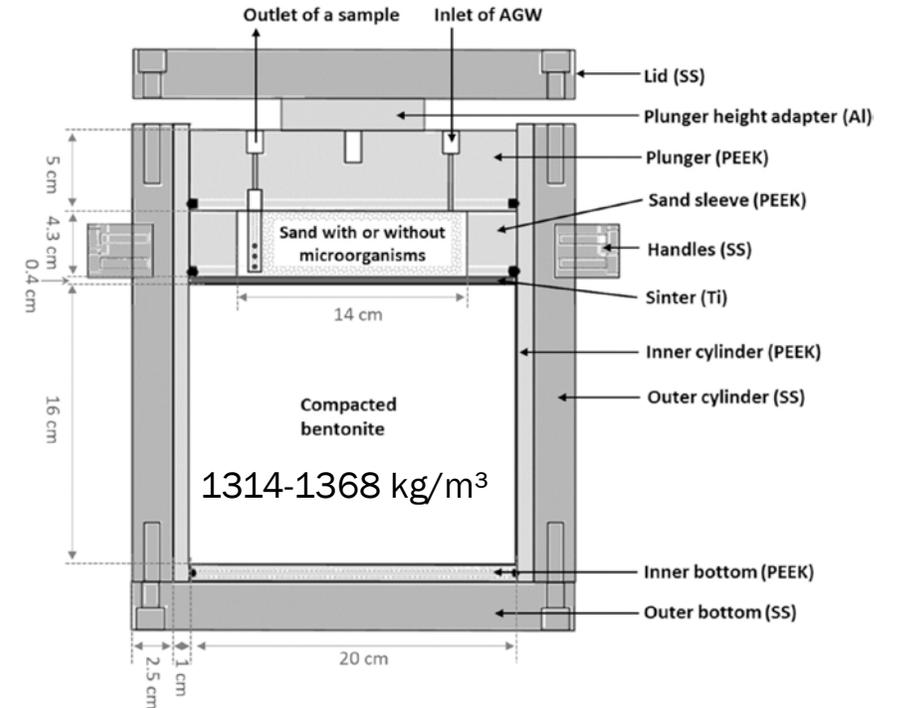
Biodegradable, but amount?



INHIBITION OF MICROBIAL ACTIVITY AND GROWTH BY BENTONITE

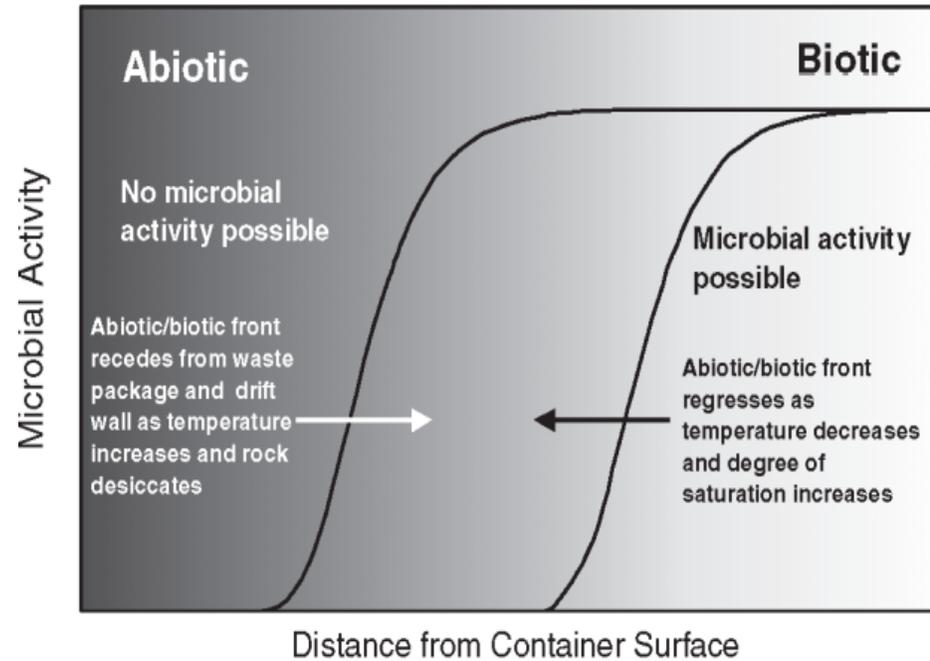
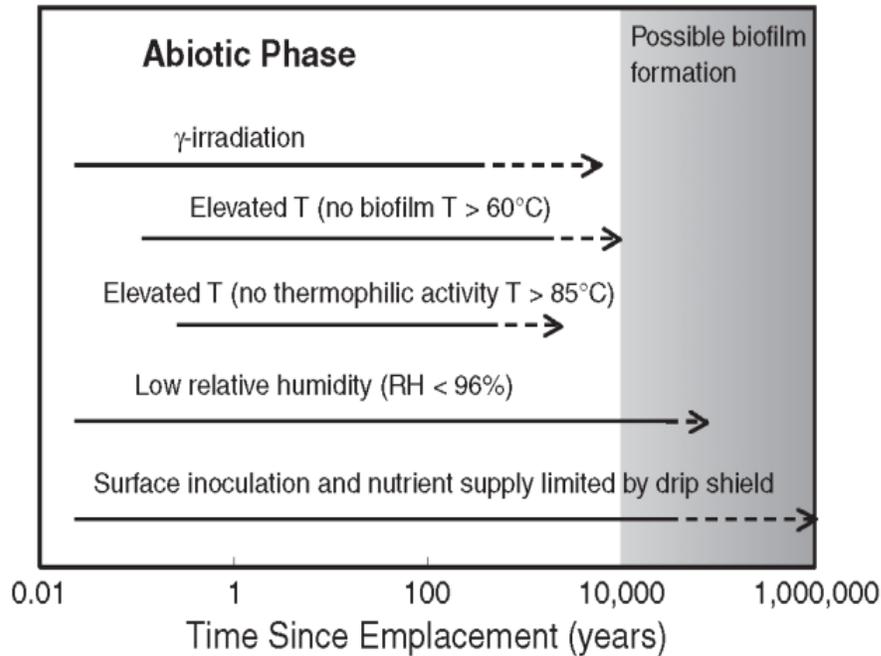
- Nutrient limited environment
 - Low available organic carbon mainly composed of plant-derived waxes and highly recalcitrant aromatic carbon
 - Recent analysis
 - Alkanes
 - Toluenes
 - Aromatic compounds
- Organic material in compacted bentonite is able to sustain SRB
 - Wyoming, Indian & Bulgarian
- Autotrophic growth?
 - H₂ as electron donor & CO₂ as carbon source

Biodegradable, but amount?

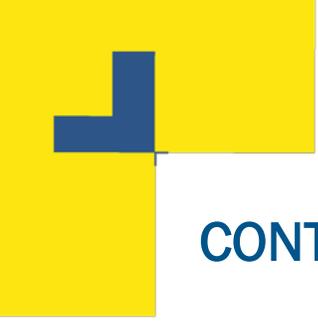


MICROBIAL TRANSIENTS

- Nuclear waste repositories are considered inhospitable for microorganisms



- Presence of microorganisms demonstrated in several *in situ* tests under certain conditions

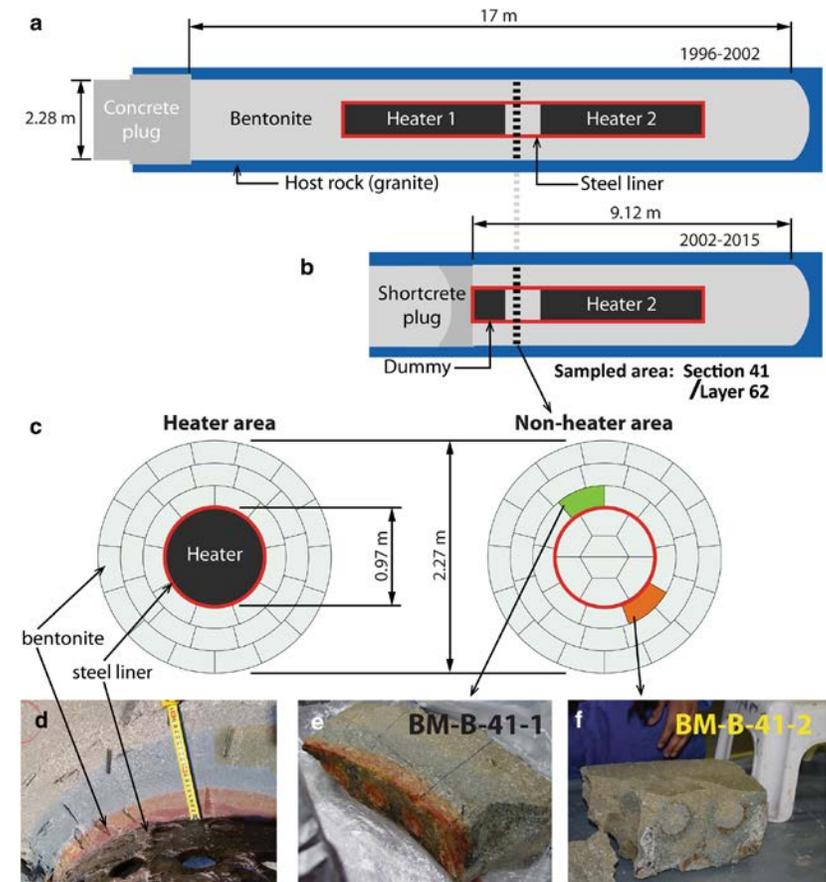


CONTENT

- Introduction
- Thermal transients
- Pore water transients
- Redox transients
- Saturation transients
- Mechanical transients
- Transitional processes involving gas generation
- Effects of irradiation
- Effects of Microbial processes
- **Example of an integrated test**
- Summary

EXAMPLE OF INTEGRATED TEST: FEBEX

- Full-scale Engineered Barriers Experiment
 - *In situ* test @ Grimsel Test site in Switzerland
 - Mock-up test @ CIEMAT in Spain
 - Laboratory tests to complement large-scale tests
- Thermal-hydrologic effects
 - Thermal expansion of pore water
 - Geochemical conditions & corrosion products
 - Geomechanical properties & stress-state



Overall layout (a) before (1996–2002) & (b) after (2002–2015) partial dismantling. (c) Cross-sections of the heater & non-heater areas, indicating the location of the sampled blocks. (d) Corrosion-impacted bentonite block still in place at the contact with the steel liner. (e–f) Studied blocks BM-B-41-2 and BM-B-42-2

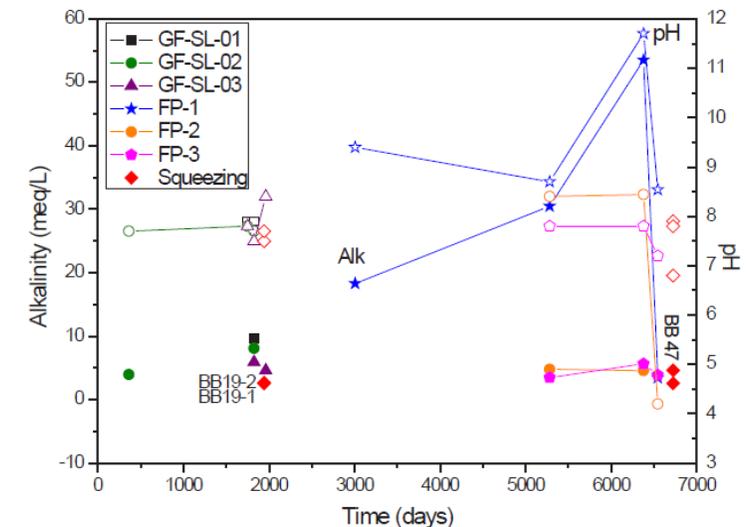
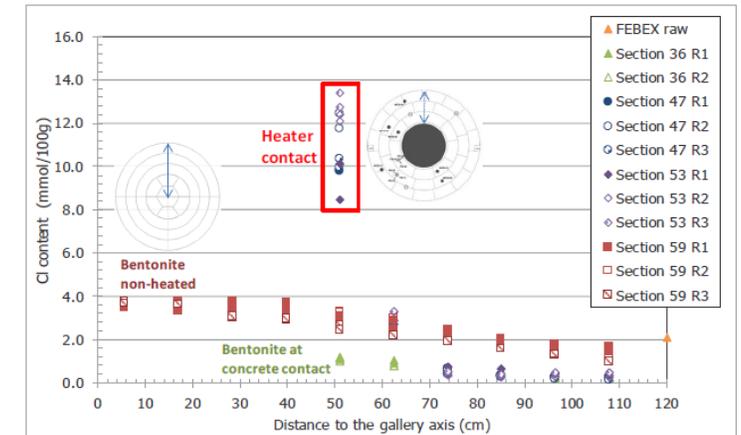
EXAMPLE OF INTEGRATED TEST: FEBEX

- Pore water transients
 - Chemical composition of the pore water evolved with time as a function of hydration of the bentonite, which was affected by
 - temperature
 - the geochemical processes in the bentonite–water system
 - Comparison of chloride content data after dismantling of Heater #1 (5 years of experiment, open symbols) and Heater #2 (18 years of experiment, filled symbols)

EXAMPLE OF INTEGRATED TEST: FEBEX

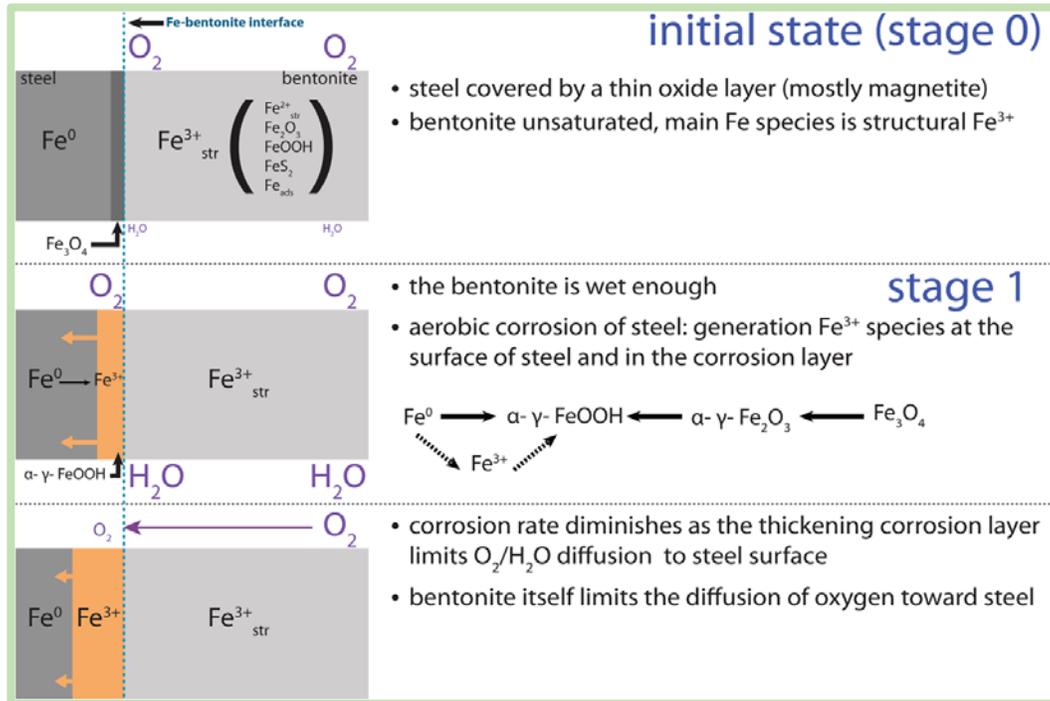
- Pore water transients

- Chemical composition of the pore water evolved with time as a function of hydration of the bentonite, which was affected by
 - temperature
 - the geochemical processes in the bentonite–water system
- Comparison of chloride content data after dismantling of Heater #1 (5 years of experiment, open symbols) and Heater #2 (18 years of experiment, filled symbols)
- Cl accumulation at the heater → Precipitation of GR-Cl (green rusts), other chloride salts and Cl-bearing Fe^{3+} oxyhydroxide (akaganeite) observed after dismantling the FEBEX *in-situ* test
- pH variations due to the thermo-hydraulic gradients in the bentonite barrier
- Formate, acetate, oxalate only in samples near heater



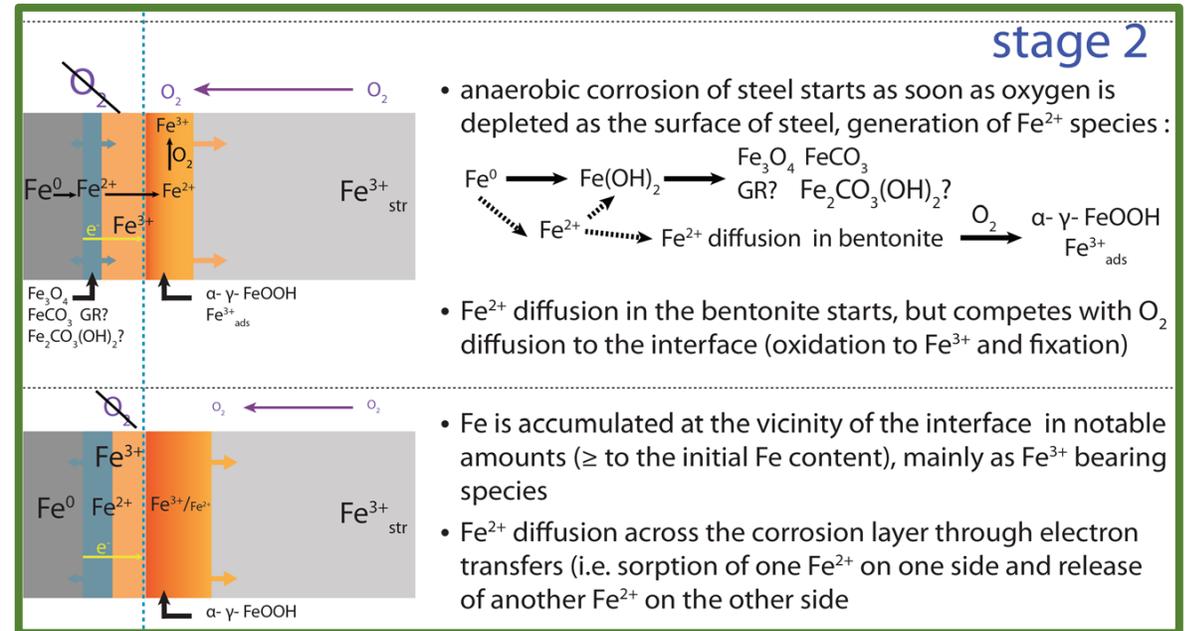
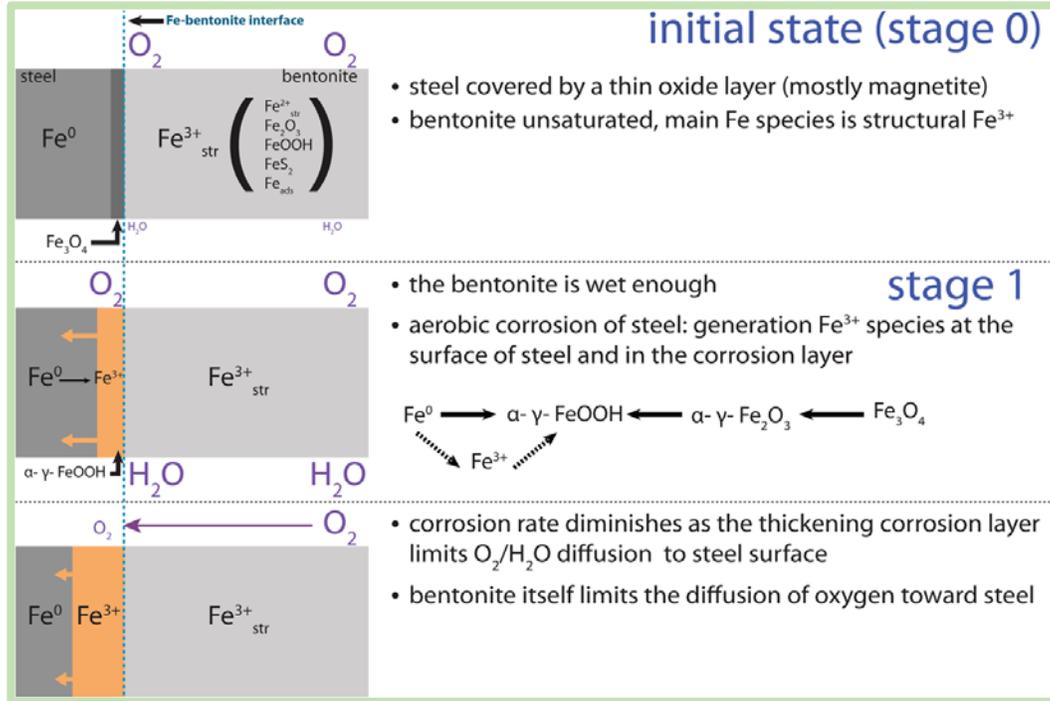
EXAMPLE OF INTEGRATED TEST: FEBEX

- Redox transients: Proposed Fe diffusion mechanism at the steel-bentonite interface



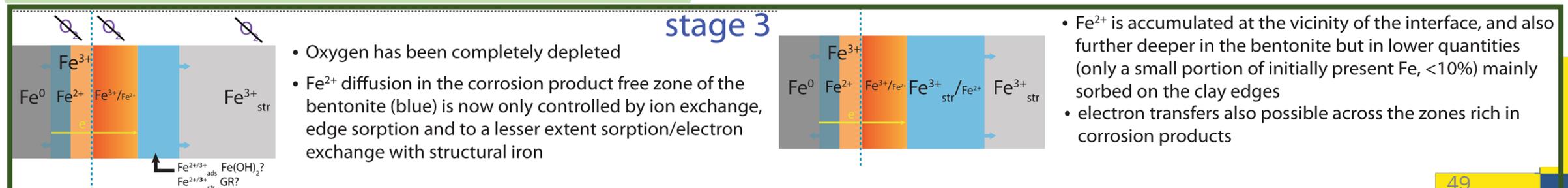
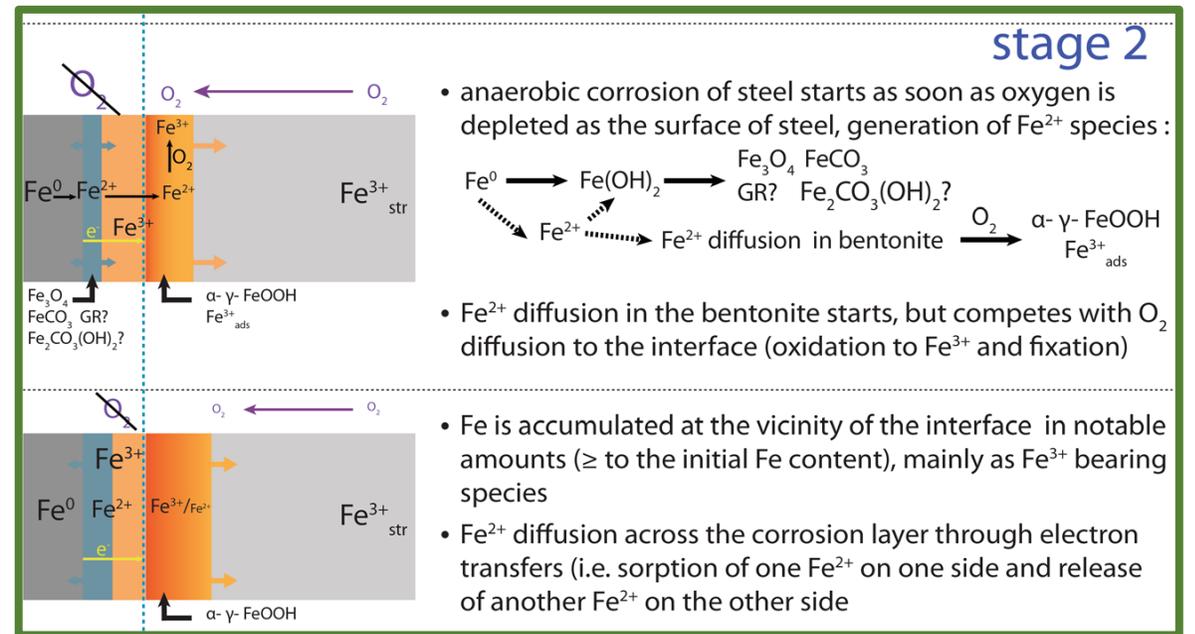
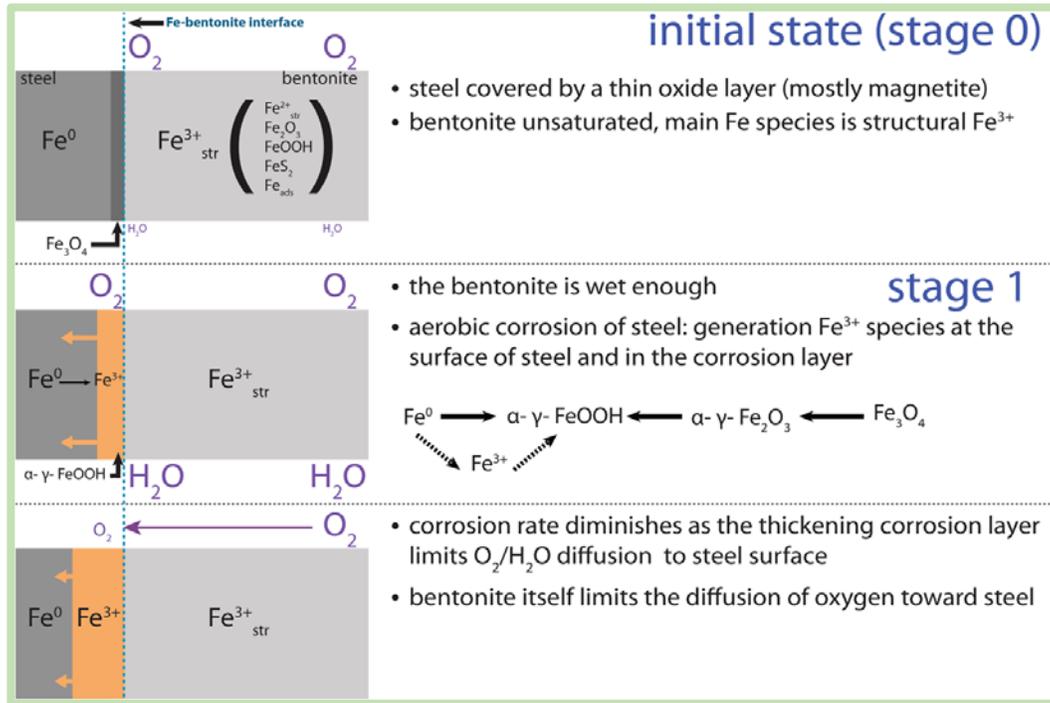
EXAMPLE OF INTEGRATED TEST: FEBEX

- Redox transients: Proposed Fe diffusion mechanism at the steel-bentonite interface



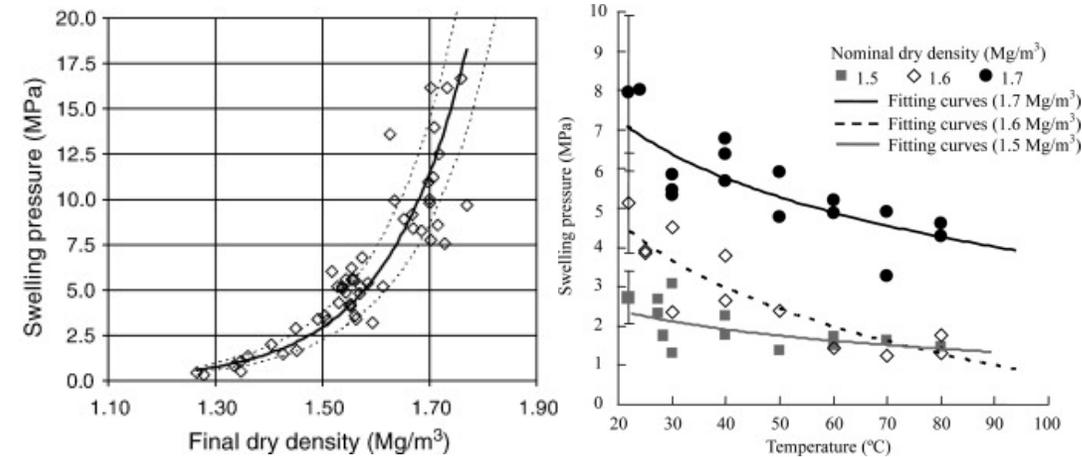
EXAMPLE OF INTEGRATED TEST: FEBEX

- Redox transients: Proposed Fe diffusion mechanism at the steel-bentonite interface



EXAMPLE OF INTEGRATED TEST: FEBEX

- Mechanical load increases with saturation
 - Depends on:
 - Dry density
 - Temperature
 - Pore water composition



Figures from Villar, M. V. and A. Lloret (2008). "Influence of Dry Density and Water Content on the Swelling of a Compacted Bentonite." Applied Clay Science 39(1);

Villar, M. V., R. Gómez-Espina and A. Lloret (2010). "Experimental Investigation into Temperature Effect on Hydro-Mechanical Behaviours of Bentonite." Journal of Rock Mechanics and Geotechnical Engineering 2(1).

EXAMPLE OF INTEGRATED TEST: FEBEX

- Mechanical load increases with saturation

- Depends on:

- Dry density
 - Temperature
 - Pore water composition

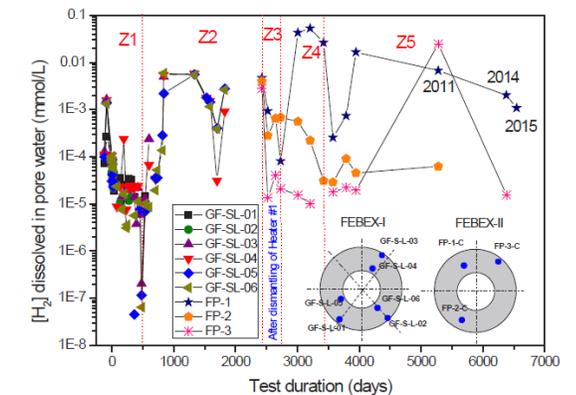
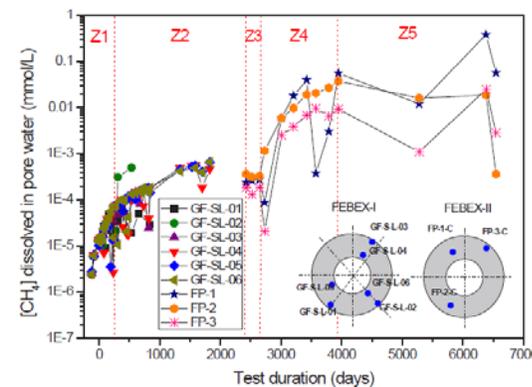
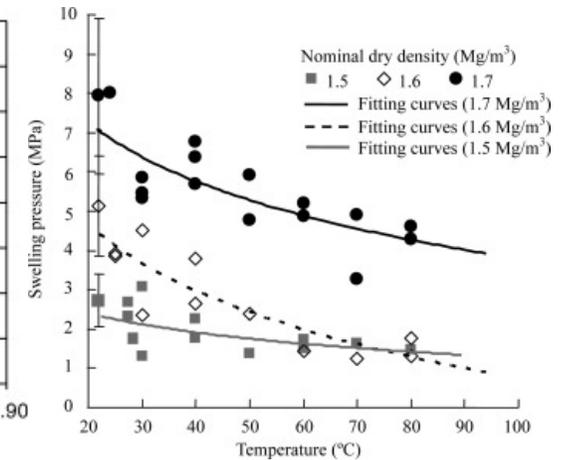
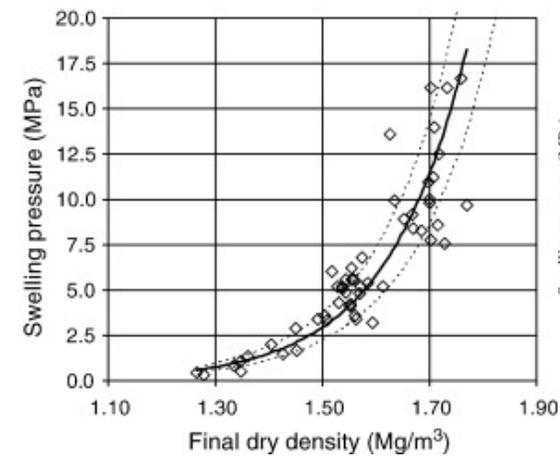
- Gas generation

- Corrosion of metallic compounds

- Consumes O_2 , H_2O and CO_2
 - Produces H_2

- Degradation organic compounds

- Consumes O_2
 - Produces H_2 , CO_2 , CO & CH_4

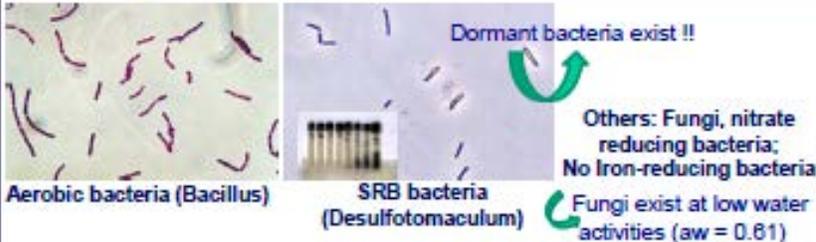


EXAMPLE OF INTEGRATED TEST: FEBEX

- Microbial community

- very few or no cultivable cells from the sections around & adjacent to the heater
 - Temp.: 84 - 99 °C
 - dry densities: 1.6 - 1.7 g/cm³
- significantly higher number of cultivable cells on different media: SRB, NRB and IRB
 - Temp 20-30 °C
 - dry density 1.4-1.5 g/cm³
 - the water content >20%
- Viable ↔ activity

Microorganisms cultivated in "as received" Febex bentonite



Aerobic bacteria (Bacillus) SRB bacteria (Desulfotomaculum)

Dormant bacteria exist !!

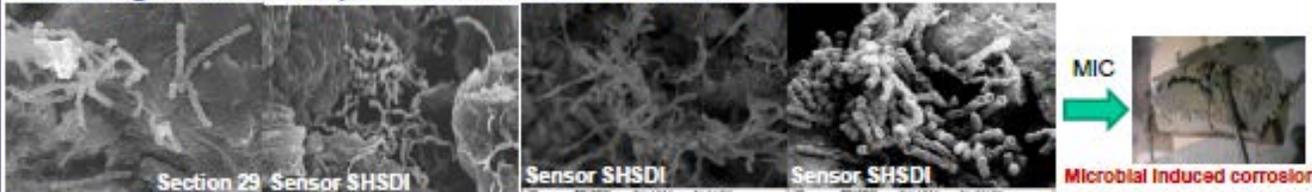
Others: Fungi, nitrate reducing bacteria; No Iron-reducing bacteria

Fungi exist at low water activities ($a_w = 0.61$)

Microorganisms after Thermohydraulic treatments

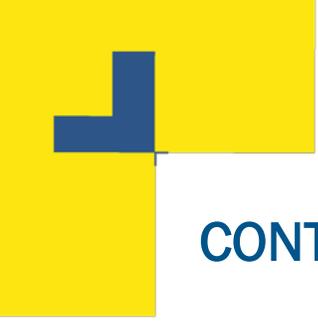


Microorganisms in samples from the FEBEX in situ test



Section 29 Sensor SHSDI Sensor SHSDI Sensor SHSDI

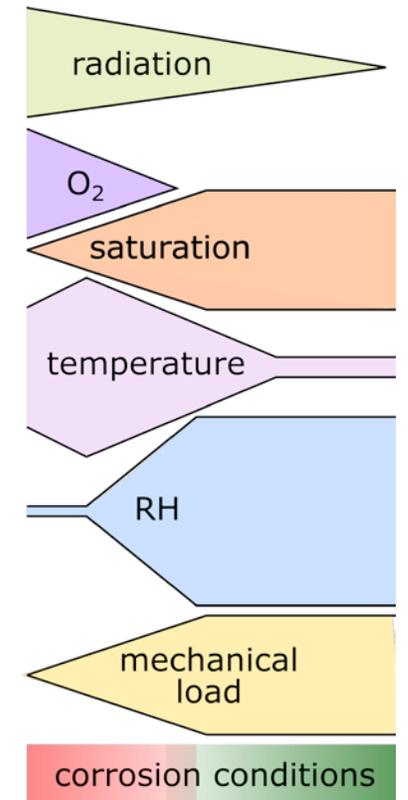
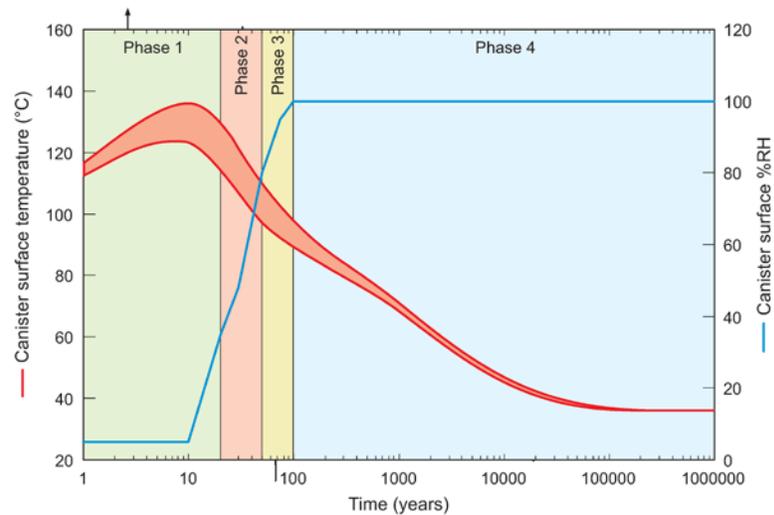
MIC → Microbial Induced corrosion



CONTENT

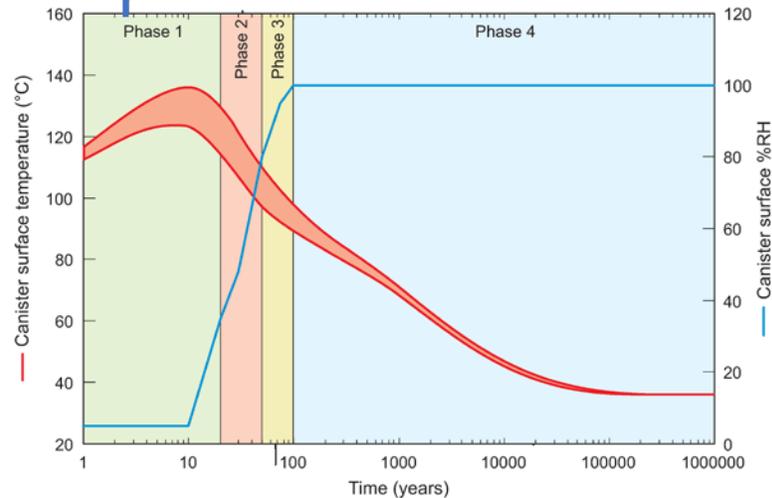
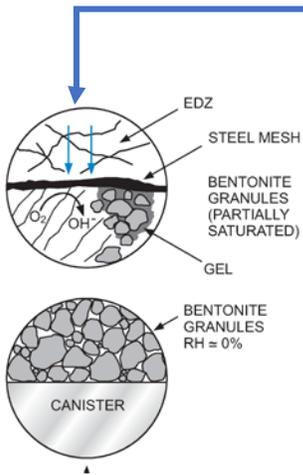
- Introduction
- Thermal transients
- Pore water transients
- Redox transients
- Saturation transients
- Mechanical transients
- Transitional processes involving gas generation
- Effects of irradiation
- Effects of Microbial processes
- Example of an integrated test
- **Summary**

OVERVIEW: GENERIC SCHEME OF 4 IDENTIFIED PHASES & EXPECTED CORROSION PRODUCTS

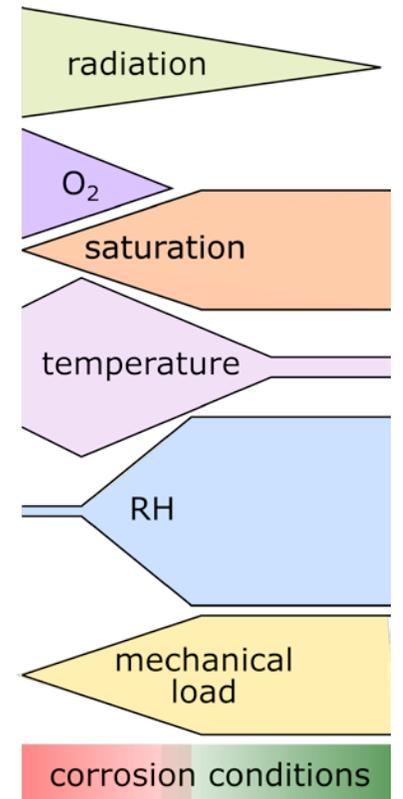


OVERVIEW: GENERIC SCHEME OF 4 IDENTIFIED PHASES & EXPECTED CORROSION PRODUCTS

1: aerobic dry

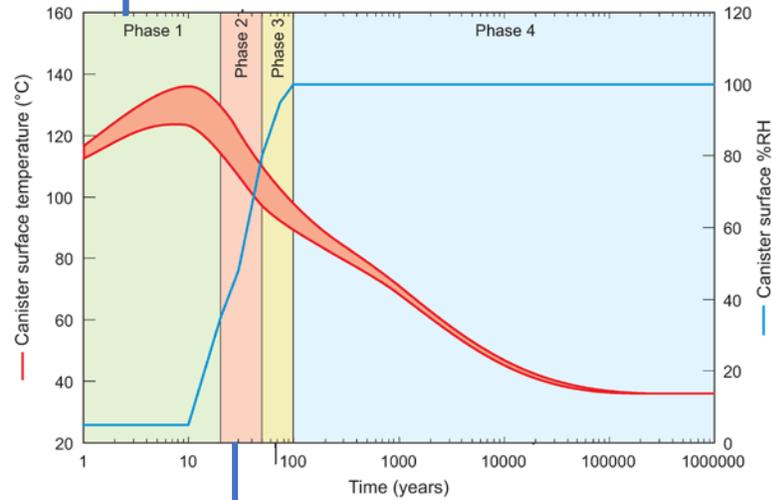
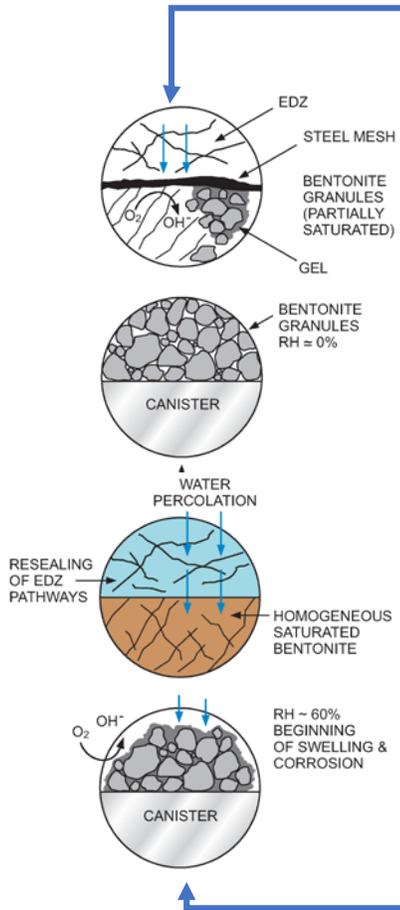


- Uniform dry oxidation → FeO_2
- Redistribution of salts → salt precipitation assisted by desiccation → swelling pressure around periphery of the tunnel



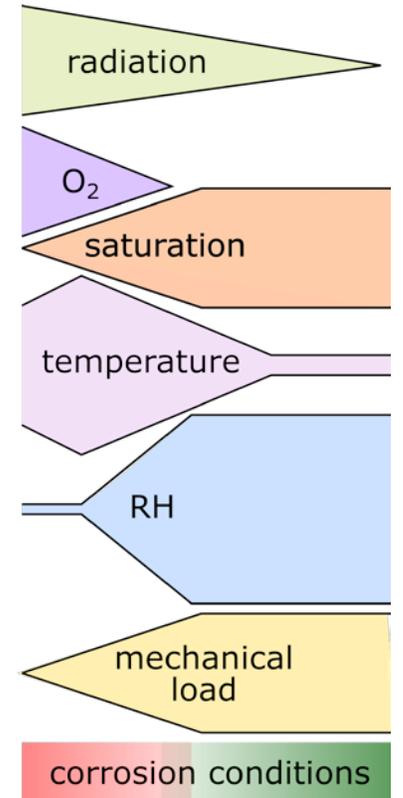
OVERVIEW: GENERIC SCHEME OF 4 IDENTIFIED PHASES & EXPECTED CORROSION PRODUCTS

1: aerobic dry

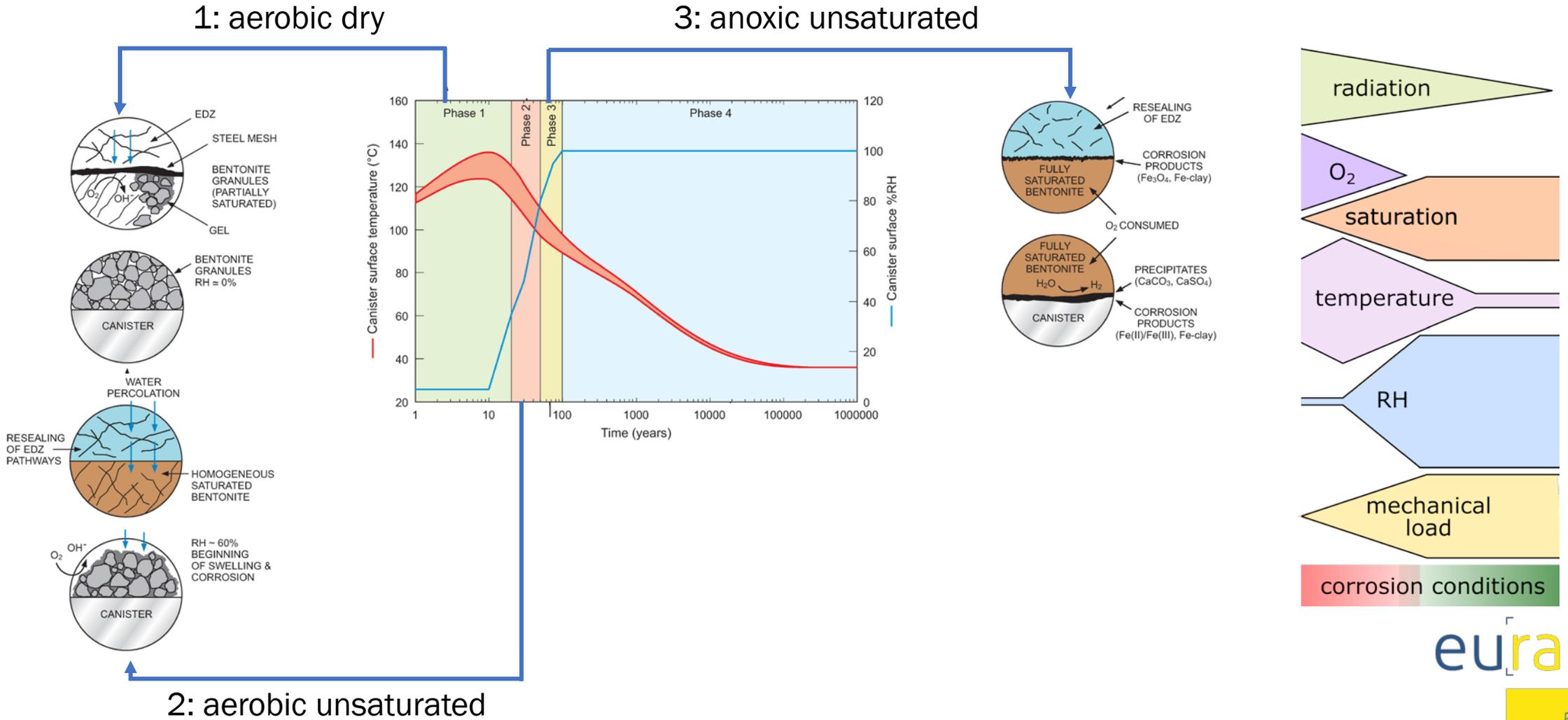


- RH reaches critical value for formation of thin films of moisture on metal surface → start aqueous corrosion

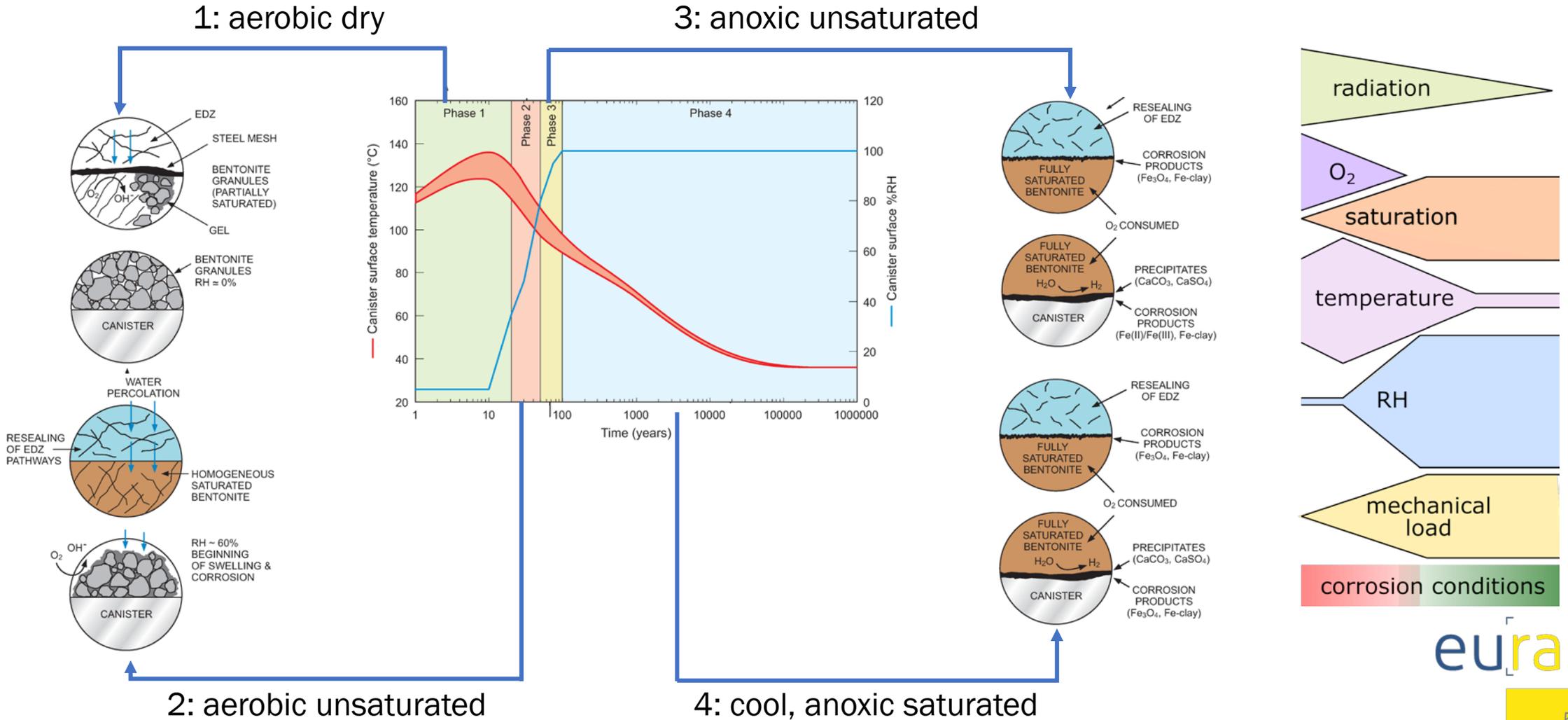
2: aerobic unsaturated



OVERVIEW: GENERIC SCHEME OF 4 IDENTIFIED PHASES & EXPECTED CORROSION PRODUCTS



OVERVIEW: GENERIC SCHEME OF 4 IDENTIFIED PHASES & EXPECTED CORROSION PRODUCTS



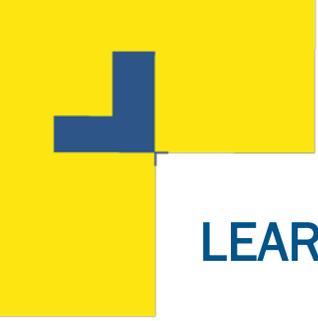
FURTHER READING

- <https://www.ejp-eurad.eu/publications/eurad-d151-concord-initial-sota>
- Allard, T., E. Balan, G. Calas, C. Fourdrin, E. Morichon and S. Sorieul (2012). Radiation-induced defects in clay minerals: A review. *Nuclear Instruments and Methods in Physics Research Section B: Beam Interactions with Materials and Atoms* 277: 112-120
- Dixon, D. (2019). Review of the THMC Properties of MX-80 Bentonite, NWMO-TR-2019-07
- Enning, D. and J. Garrelfs (2014). Corrosion of iron by sulfate-reducing bacteria: new views of an old problem. *Appl Environ Microbiol* 80: 1226-1236
- King, F. (2017). 13 - Nuclear waste canister materials: Corrosion behavior and long-term performance in geological repository systems. *Geological Repository Systems for Safe Disposal of Spent Nuclear Fuels and Radioactive Waste (Second Edition)*. M. J. Apted and J. Ahn, Woodhead Publishing: 365-408
- King, F. and M. Behazin (2021). A Review of the Effect of Irradiation on the Corrosion of Copper-Coated Used Fuel Containers. *Corrosion and Materials Degradation* 2: 678-707
- Fraser King, 2017 - 13 - Nuclear waste canister materials: Corrosion behavior and long-term performance in geological repository systems - doi.org/10.1016/B978-0-08-100642-9.00013-X
- Landolt, D., A. W. Davenport, J. H. Payer and D. W. Shoesmith (2011). A Review of Materials and Corrosion Issues Regarding Canisters for Disposal of Spent Fuel and High-Level Waste in Opalinus Clay. *ChemInform* 42

NOVEL MATERIAL SOLUTIONS FOR NUCLEAR WASTE DISPOSAL CONTAINER CONCEPTS

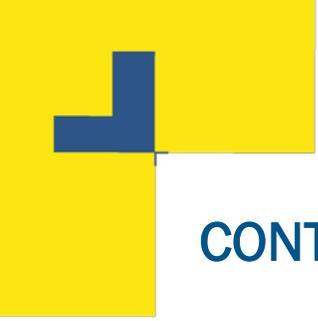


This project has received funding from the European Union's Horizon 2020 research and innovation programme 2014-2018 under grant agreement N°847593



LEARNING OUTCOMES

- Understand the advantages & disadvantages of the use of ceramic/metallic materials in nuclear waste disposal
- Identify the current knowledge gaps of the use of ceramic/metallic materials in nuclear waste disposal
- Give an historical overview of the use of ceramic materials in nuclear waste disposal



CONTENTS

- Introduction
- Alumina solutions: historical overview
 - SKB, Swedish concept
 - Lawrence Livermore National Laboratory, USA
 - BNL/Nucon, USA
 - Andra, France
- Silicon carbide concept
- Ceramic coatings
 - Titanium oxide
 - Chromium nitride
- Metallic containers
- Metallic coatings
- Outlook

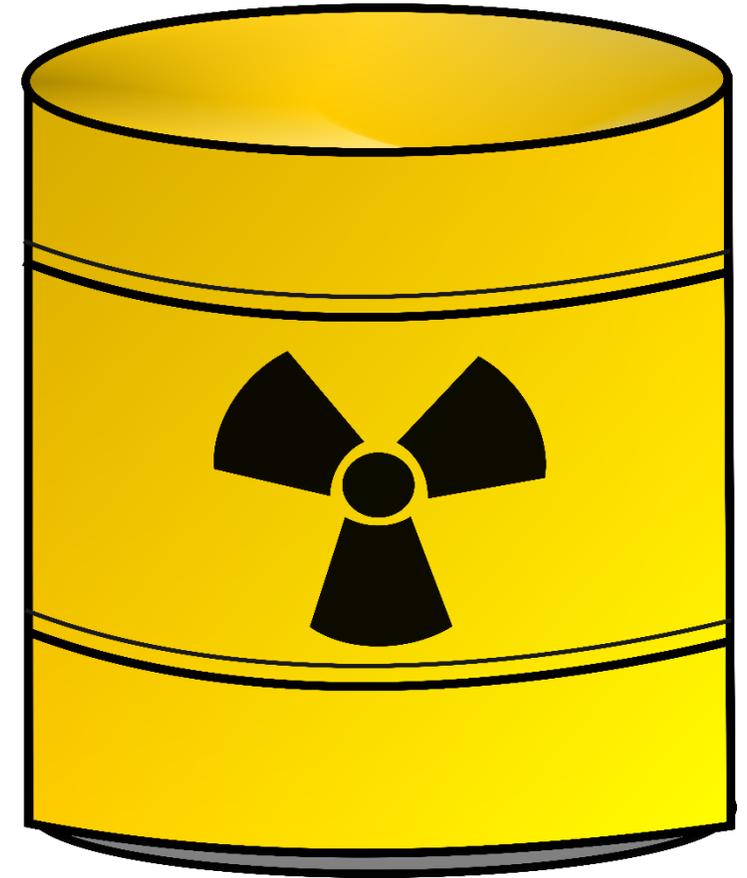


CONTENTS

- **Introduction**
- **Alumina solutions: historical overview**
 - SKB, Swedish concept
 - Lawrence Livermore National Laboratory, USA
 - BNL/Nucon, USA
 - Andra, France
- **Silicon carbide concept**
- **Ceramic coatings**
 - Titanium oxide
 - Chromium nitride
- **Metallic containers**
- **Metallic coatings**
- **Outlook**

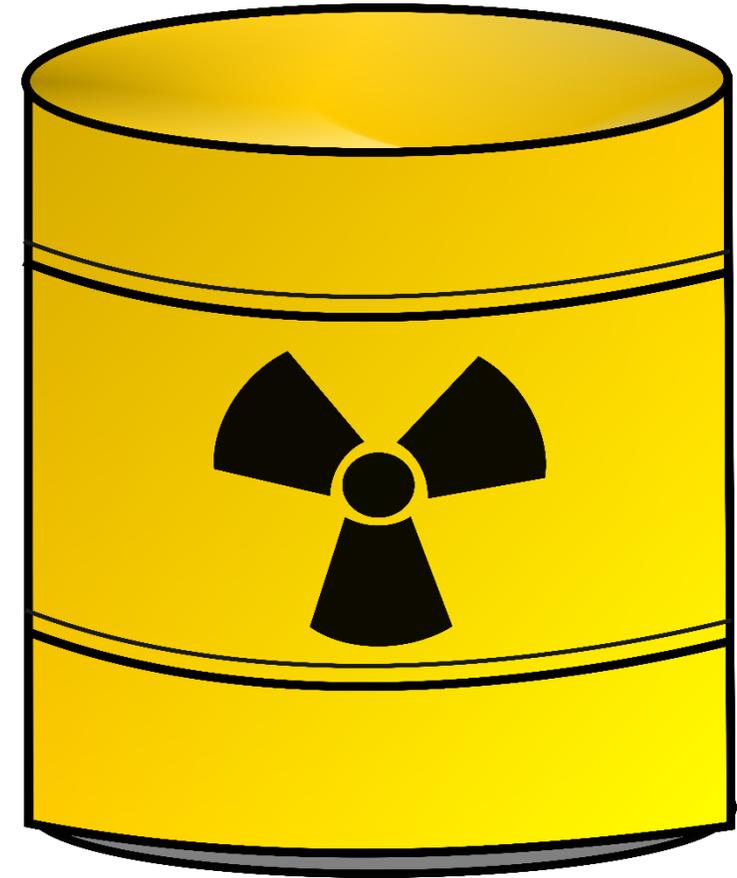
WASTE CONTAINER IS ESSENTIAL IN THE DISPOSAL OF HLW/SF

- Designed to contain, physically protect, and/or radiologically shield the waste form during the various activities involved during the period from conditioning until emplacement and closure of a disposal facility



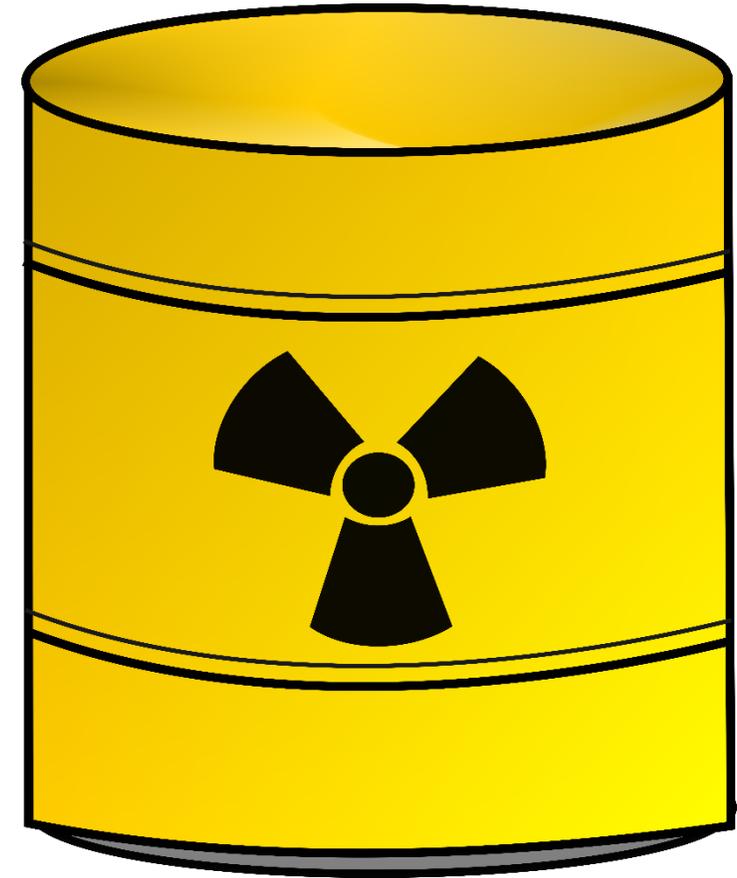
WASTE CONTAINER IS ESSENTIAL IN THE DISPOSAL OF HLW/SF

- Designed to contain, physically protect, and/or radiologically shield the waste form during the various activities involved during the period from conditioning until emplacement and closure of a disposal facility
- In some cases the container also plays a role in the near field containment of the radionuclides for a certain period after closure



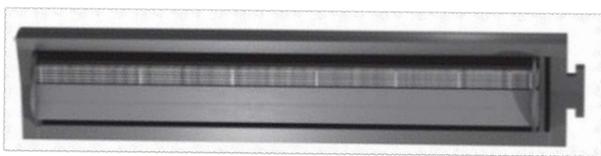
WASTE CONTAINER IS ESSENTIAL IN THE DISPOSAL OF HLW/SF

- Designed to contain, physically protect, and/or radiologically shield the waste form during the various activities involved during the period from conditioning until emplacement and closure of a disposal facility
- In some cases the container also plays a role in the near field containment of the radionuclides for a certain period after closure
- Main parameters & control methods according to IAEA (2006):
 - Material itself
 - Geometric shape & dimensions
 - Design & operation of internal features
 - Lifting arrangements
 - Container internal corrosion
 - Container strength
 - Selection of surface coating & texture
 - Design & operation of closure features
 - Resistance to environmental conditions

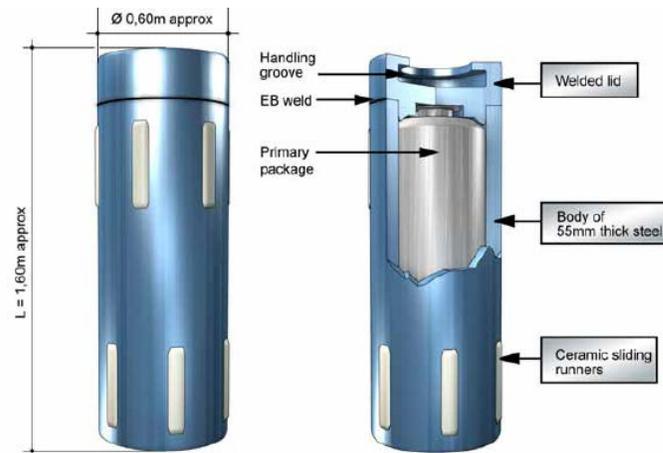


DIFFERENT TYPES OF WASTE CONTAINERS EXIST

- Configuration & life time requirements depend on
 - Type of waste
 - Surrounding geological structure
 - Material used to increase canister integrity



NAGRA



ANDRA



SKB/POSIVA



CANADA

DIFFERENT CONTAINER CONCEPTS & EXPECTED EXPOSURE CONDITIONS

WMO	Container concept	Estimated or target lifetime (year)	Nominal buffer dry density (g/cm ³)	Max. container temp. (°C)	Time to full nearfield saturation (year)	Max. surface absorbed dose (Gy/h)	Expected mechanical loads (MPa)
SKB	Cu-cast Fe	>10 ⁶	1.6	95	Few 10s – few 1000	0.2	15 50 (glacial)
Posiva	Cu-cast Fe	>10 ⁶	1.55	95	Few 10s – few 1000	0.3	14 50 (glacial)
Andra	Carbon steel	>500	Cementitious buffer on the external face of the casing	90		10	10 (on casing)
Ondraf-Niras	Carbon steel	Several thousand	Cementitious buffer	100	5-10 to few 1000	25	8
Nagra	Carbon steel	10 000	>1.45	±120	Few centuries	0.2	22-29 max
SURAO	Carbon steel	10 000	1.4	95	100	0.3	20
NMWO	Cu-coated steel	>10 ⁶	1.6	85	50-5000 ~ host rock	0.8	15 45 (glacial)
NUMO	Carbon steel	> 1000	1.6	100	<1000 ~ host rock	0.006-0.011	11 (hard rock)

DIFFERENT CONTAINER CONCEPTS & EXPECTED EXPOSURE CONDITIONS

WMO	Container concept	Estimated or target lifetime (year)	Nominal buffer dry density (g/cm ³)	Max. container temp. (°C)	Time to full nearfield saturation (year)	Max. surface absorbed dose (Gy/h)	Expected mechanical loads (MPa)
SKB	Cu-cast Fe	>10 ⁶	1.6	95	Few 10s – few 1000	0.2	15 50 (glacial)
Posiva	Cu-cast Fe	>10 ⁶	1.55	95	Few 10s – few 1000	0.3	14 50 (glacial)
Andra	Carbon steel	>500	Cementitious buffer on the external face of the casing	90		10	10 (on casing)
Ondraf-Niras	Carbon steel	Several thousand	Cementitious buffer	100	5-10 to few 1000	25	8
Nagra	Carbon steel	10 000	>1.45	±120	Few centuries	0.2	22-29 max
SURAO	Carbon steel	10 000	1.4	95	100	0.3	20
NMWO	Cu-coated steel	>10 ⁶	1.6	85	50-5000 ~ host rock	0.8	15 45 (glacial)
NUMO	Carbon steel	> 1000	1.6	100	<1000 ~ host rock	0.006-0.011	11 (hard rock)

→ Although studied very well, they also have some disadvantages → study alternative materials

CERAMIC MATERIALS & COATINGS

- First interest in the 1970s >> early 2000s
 - Insufficient motivation to invest in the research
 - Insufficient customer demand

half-scale model of $\text{Al}_2\text{O}_3/\text{SiO}_2$ VHLW container



CERAMIC MATERIALS & COATINGS

- First interest in the 1970s >> early 2000s
 - Insufficient motivation to invest in the research
 - Insufficient customer demand
- High corrosion resistance
- Lack of gas generation

half-scale model of $\text{Al}_2\text{O}_3/\text{SiO}_2$ VHLW container



CERAMIC MATERIALS & COATINGS

- First interest in the 1970s >> early 2000s
 - Insufficient motivation to invest in the research
 - Insufficient customer demand
- High corrosion resistance
- Lack of gas generation
- Variable compressive strength
- Variable hardness
- Low tensile strength
- Low toughness (except in form of composites)
- Manufacturing challenges:
 - Efficient handling of very large lumps in the green state just after shaping
 - Achieving adequate density with section thicknesses of 50 mm
 - R&D is needed to obtain effective sealing of thick ceramics
 - Funding is limited to the nuclear waste disposal community

half-scale model of $\text{Al}_2\text{O}_3/\text{SiO}_2$ VHLW container





POTENTIAL CERAMICS CANDIDATES

- Alumina (Al_2O_3)
- Alumina in combination with silicon oxide (SiO_2)
- Silicon carbide (SiC)
- Silicon nitride (Si_3N_4)
- Partially stabilized zirconia
- Titania (TiO_2)



POTENTIAL CERAMICS CANDIDATES

- Alumina (Al_2O_3)
- Alumina in combination with silicon oxide (SiO_2)
- Silicon carbide (SiC)
- Silicon nitride (Si_3N_4)
- Partially stabilized zirconia
- Titania (TiO_2)

POTENTIAL CERAMICS CANDIDATES

- Alumina (Al_2O_3)
- Alumina in combination with silicon oxide (SiO_2)
- Silicon carbide (SiC)
- Silicon nitride (Si_3N_4)
- Partially stabilized zirconia
- Titania (TiO_2)

- Chemical stability
- Reasonable mechanical properties
- Availability



EXISTING MATERIALS & PROCESSES

- **Alumina**

- Refractory polycrystalline ceramic
- Chemically inert
- Good mechanical strength
- Known properties
- Produced industrially



EXISTING MATERIALS & PROCESSES

- **Alumina**

- Refractory polycrystalline ceramic
- Chemically inert
- Good mechanical strength
- Known properties
- Produced industrially

- **Zirconia**

- > mechanically resistant
- < chemically resistant
- > expensive
- difficult to manufacture large non-porous parts

EXISTING MATERIALS & PROCESSES

- **Alumina**

- Refractory polycrystalline ceramic
- Chemically inert
- Good mechanical strength
- Known properties
- Produced industrially

- **Alumina-Zirconia composites**

- Zirconia toughened alumina → mechanical properties ↑
- Alumina containing tetragonal zirconia → hydrothermal aging of zirconia ↓
- Mechanical properties > alumina
- Manufacturing cost < zirconia

- **Zirconia**

- > mechanically resistant
- < chemically resistant
- > expensive
- difficult to manufacture large non-porous parts

EXISTING MATERIALS & PROCESSES

- **Alumina**

- Refractory polycrystalline ceramic
- Chemically inert
- Good mechanical strength
- Known properties
- Produced industrially

- **Alumina-Zirconia composites**

- Zirconia toughened alumina → mechanical properties ↑
- Alumina containing tetragonal zirconia → hydrothermal aging of zirconia ↓
- Mechanical properties > alumina
- Manufacturing cost < zirconia

- **Zirconia**

- > mechanically resistant
- < chemically resistant
- > expensive
- difficult to manufacture large non-porous parts

- **Silicon carbide**

- Light, tough, refractory material
- Chemically resistant in acid & alkaline environments
- Industrially produced at some scale but porous
- Possible corrosion in geological environments

EXISTING MATERIALS & PROCESSES

- Silicate materials

- Interest in

- Silica
 - Mullite
 - Forsterite
 - Cordierite
 - High level of glassy phase
 - Facilitates densification
 - Chemical resistance ↓
 - Alters mechanical properties

EXISTING MATERIALS & PROCESSES

- Silicate materials

- Interest in

- Silica
 - Mullite
 - Forsterite
 - Cordierite

High level of glassy phase

- Facilitates densification
 - Chemical resistance ↓
 - Alters mechanical properties

- Spinel phases

- Properties ~ alumina
 - - phase transition during thermal spraying
 - Coatings

EXISTING MATERIALS & PROCESSES

- Silicate materials

- Interest in

- Silica
 - Mullite
 - Forsterite
 - Cordierite

High level of glassy phase

- Facilitates densification
- Chemical resistance ↓
- Alters mechanical properties

- Titanium oxide

- Refractory < alumina
 - Sinters at lower temperatures
 - > expensive
 - Chemically inert (except high alkaline pH + soluble in H_2SO_4)
 - Sealing aid for alumina containers
 - Addition of TiO_2 → thermal gradients → cracks

- Spinel phases

- Properties ~ alumina
 - - phase transition during thermal spraying
 - Coatings

EXISTING MATERIALS & PROCESSES

- Silicate materials

- Interest in

- Silica
 - Mullite
 - Forsterite
 - Cordierite

High level of glassy phase

- Facilitates densification
- Chemical resistance ↓
- Alters mechanical properties

- Titanium oxide

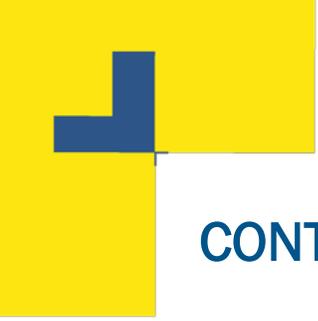
- Refractory < alumina
 - Sinters at lower temperatures
 - > expensive
 - Chemically inert (except high alkaline pH + soluble in H₂SO₄)
 - Sealing aid for alumina containers
 - Addition of TiO₂ → thermal gradients → cracks

- Spinel phases

- Properties ~ alumina
 - - phase transition during thermal spraying
 - Coatings

- Graphite

- Porous : density 80 – 92 %
 - Can be filled by vapor deposition of SiC but expensive & time consuming

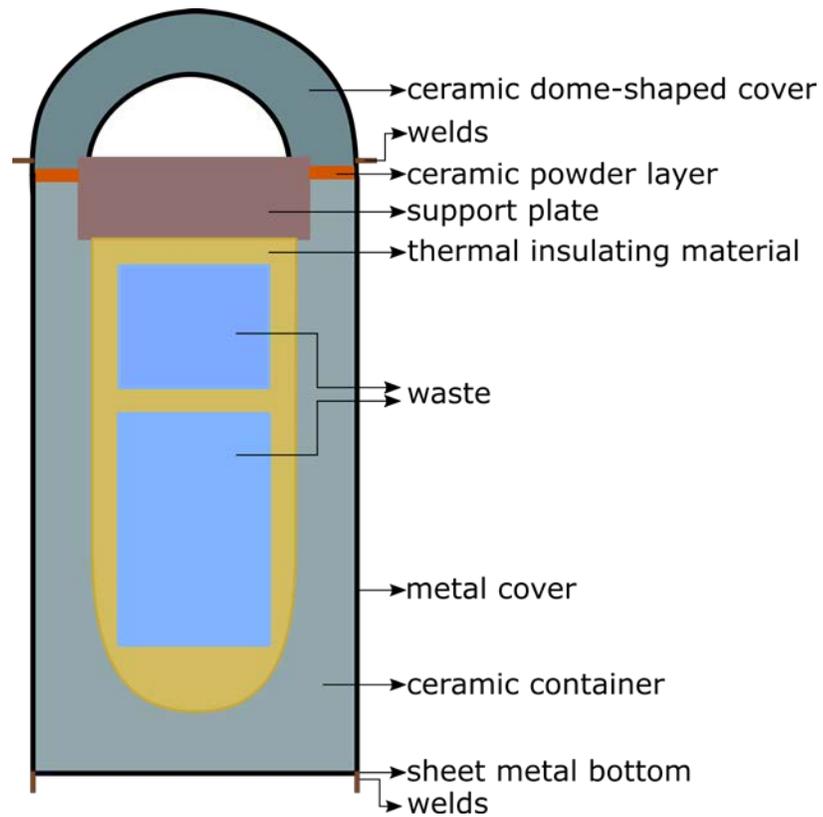


CONTENTS

- Introduction
- **Alumina solutions: historical overview**
 - SKB, Swedish concept
 - Lawrence Livermore National Laboratory, USA
 - BNL/Nucon, USA
 - Andra, France
- **Silicon carbide concept**
- **Ceramic coatings**
 - Titanium oxide
 - Chromium nitride
- **Metallic containers**
- **Metallic coatings**
- **Outlook**

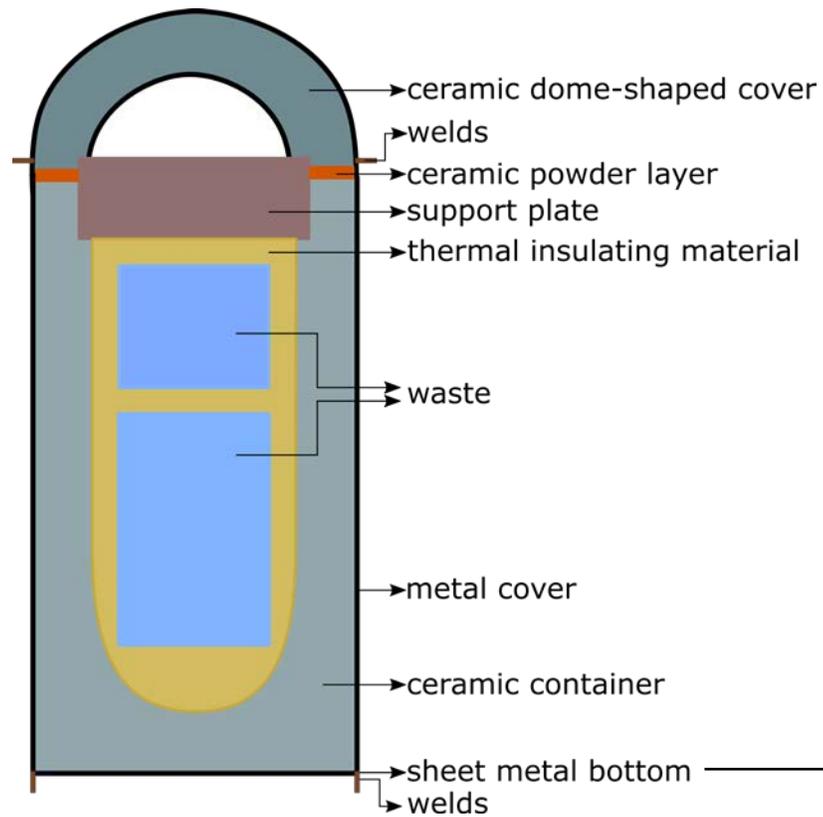
ALUMINA SOLUTIONS: SKB, SWEDISH CONCEPT (1977)

- Waste can be stored in a single cavity or in multiple separated ones



ALUMINA SOLUTIONS: SKB, SWEDISH CONCEPT (1977)

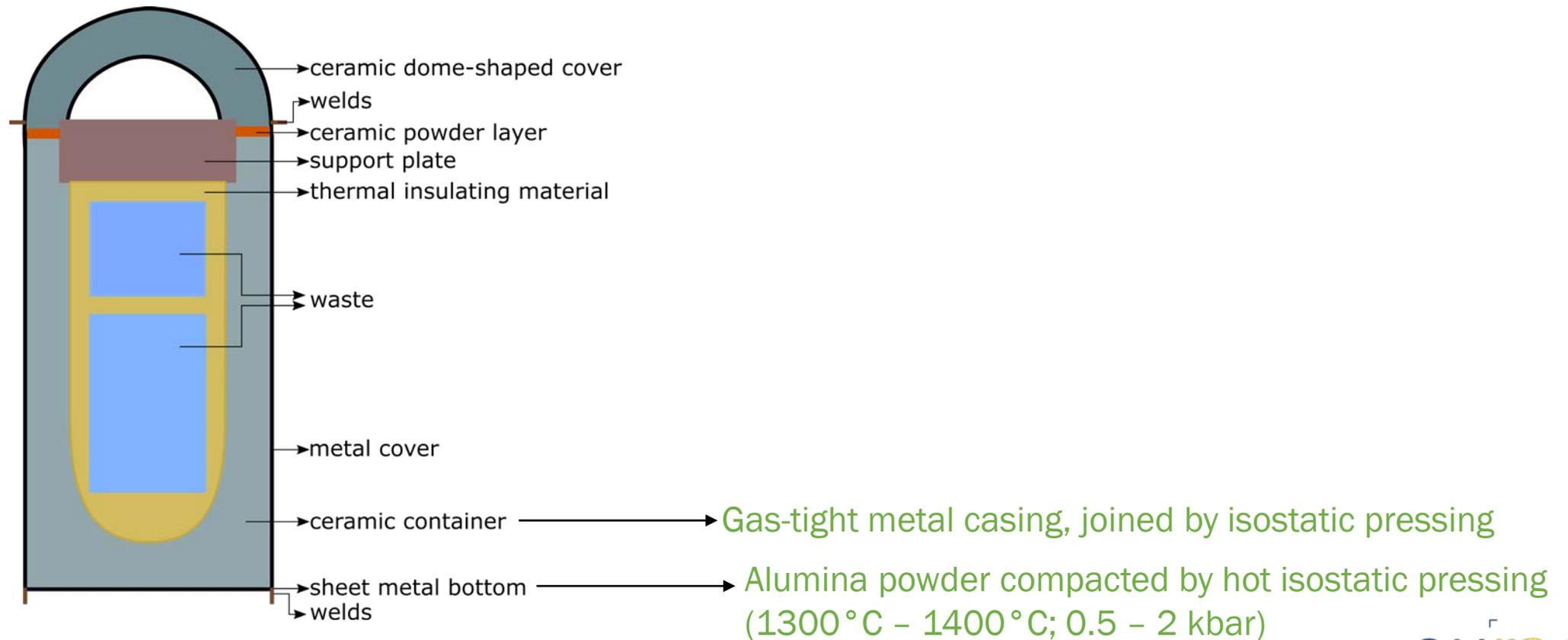
- Waste can be stored in a single cavity or in multiple separated ones



Alumina powder compacted by hot isostatic pressing
(1300°C – 1400°C; 0.5 – 2 kbar)

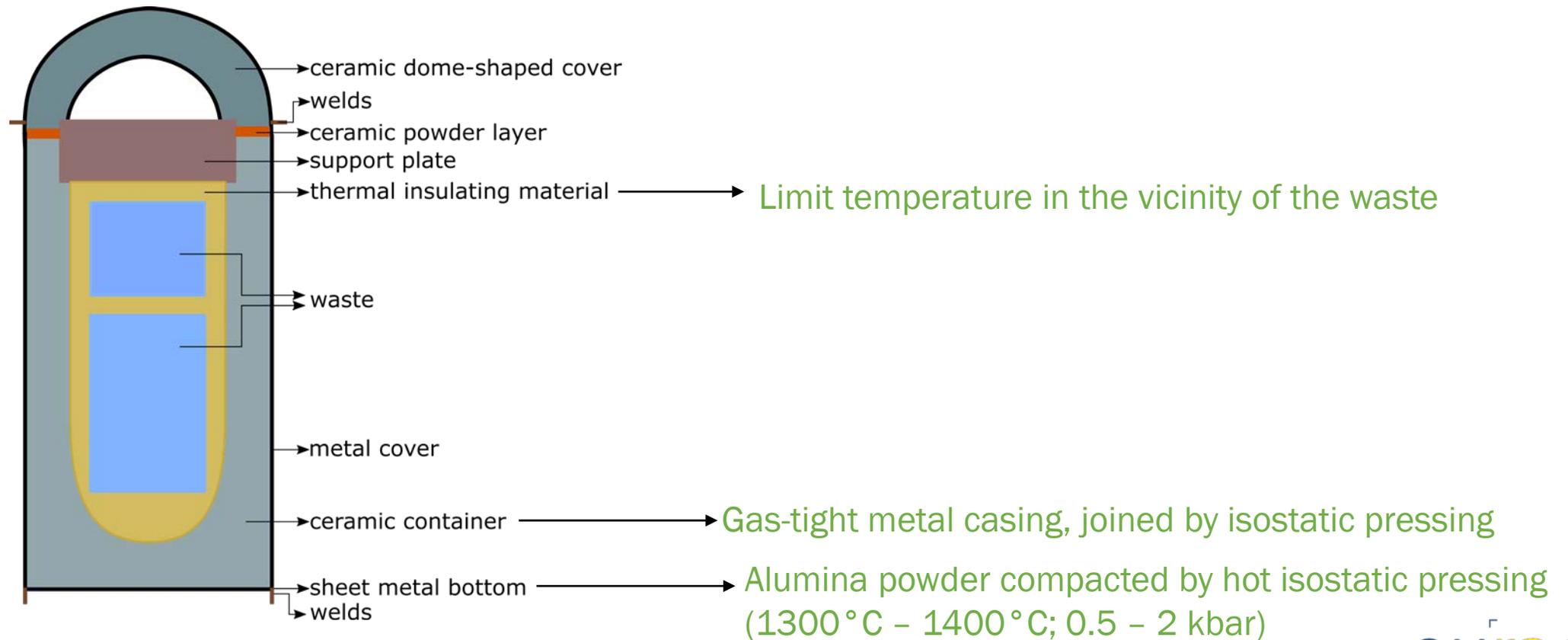
ALUMINA SOLUTIONS: SKB, SWEDISH CONCEPT (1977)

- Waste can be stored in a single cavity or in multiple separated ones



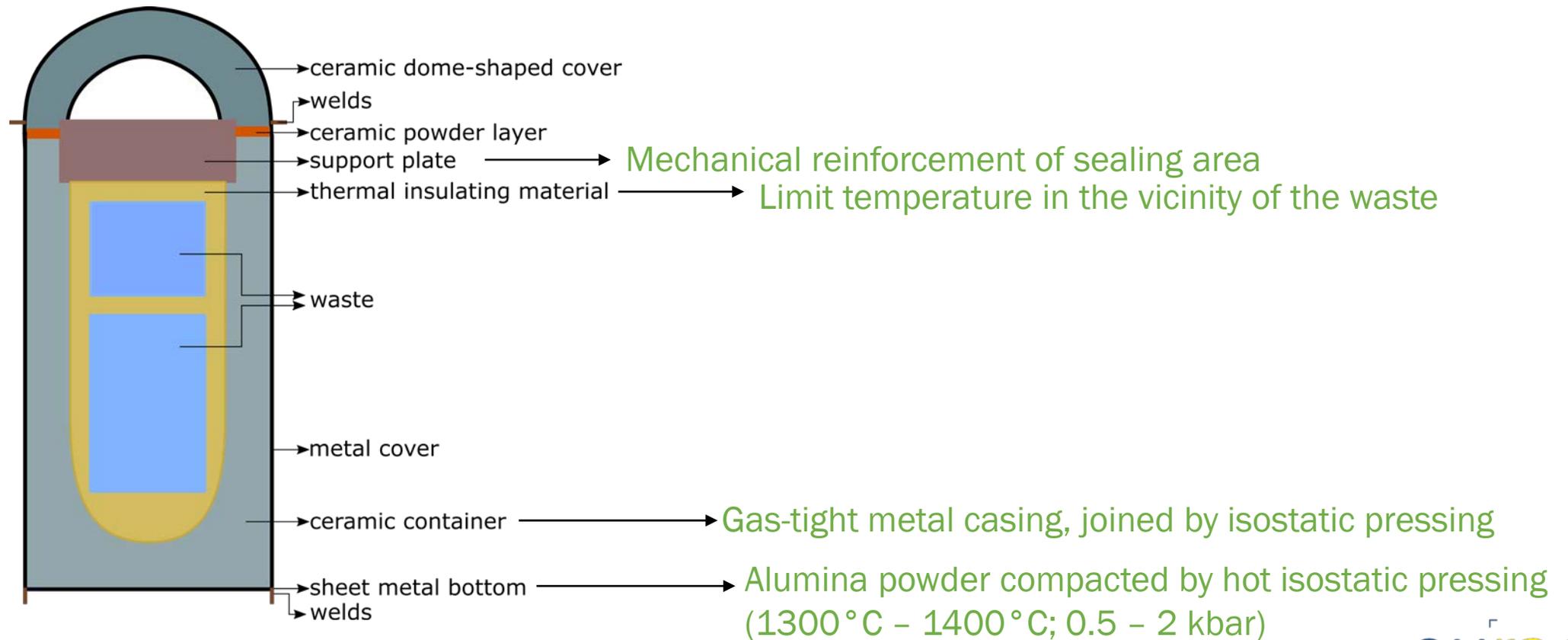
ALUMINA SOLUTIONS: SKB, SWEDISH CONCEPT (1977)

- Waste can be stored in a single cavity or in multiple separated ones



ALUMINA SOLUTIONS: SKB, SWEDISH CONCEPT (1977)

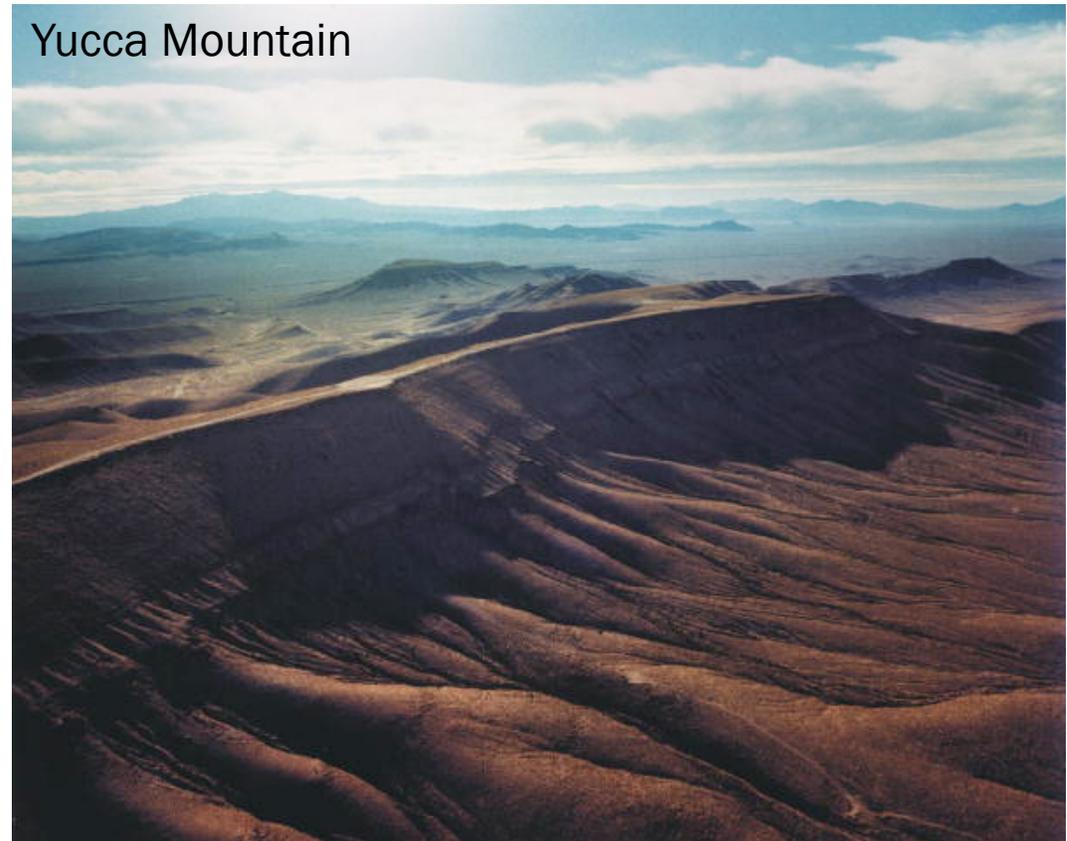
- Waste can be stored in a single cavity or in multiple separated ones



ALUMINA SOLUTIONS: LAWRENCE LIVERMORE NATIONAL LABORATORY, USA (EARLY 1990)

- **Specifications:**
 - Cylindrical containers placed nose to nose in horizontal tunnels
 - No transport function
 - Storage of spent fuel assemblies or vitrified waste
 - Identifiable & retrievable for 50 years
 - Leak proof for 300-1000 years
 - Closure system feasible remotely in a hot cell without thermal damage to the waste package
- **Two exploratory routes:**
 - Solid ceramic containers
 - Composite containers: metal structure + ceramic coating/liner

Yucca Mountain

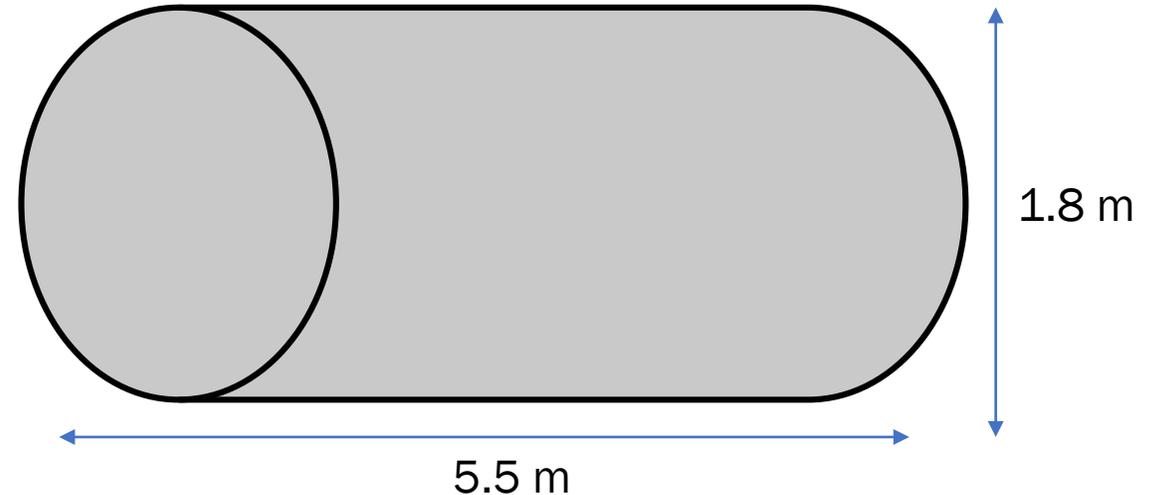


https://en.wikipedia.org/wiki/Yucca_Mountain_nuclear_waste_repository

LAWRENCE LIVERMORE NATIONAL LABORATORY, USA (EARLY 1990)

- Selection criteria

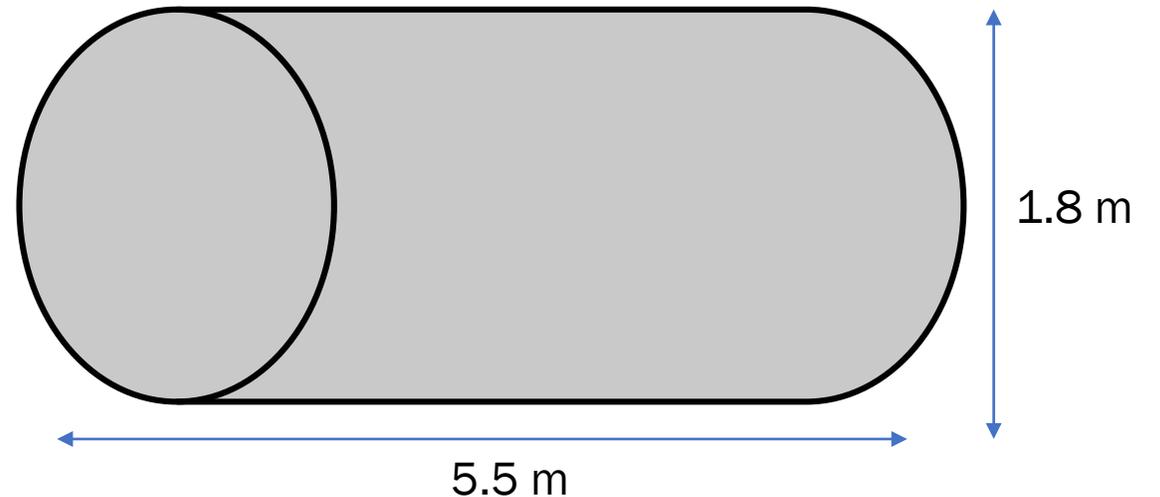
- Good tensile strength and impact resistance of the material
- High toughness material
- Dense material with no open pores or cracks
- Joint or weld areas must have the same properties as the body material
- Good chemical resistance of the material in the storage environment
- Sufficient thermal conductivity to remove heat from the waste
- Use of conventional processes requiring only minor adaptations



LAWRENCE LIVERMORE NATIONAL LABORATORY, USA (EARLY 1990)

- Selection criteria

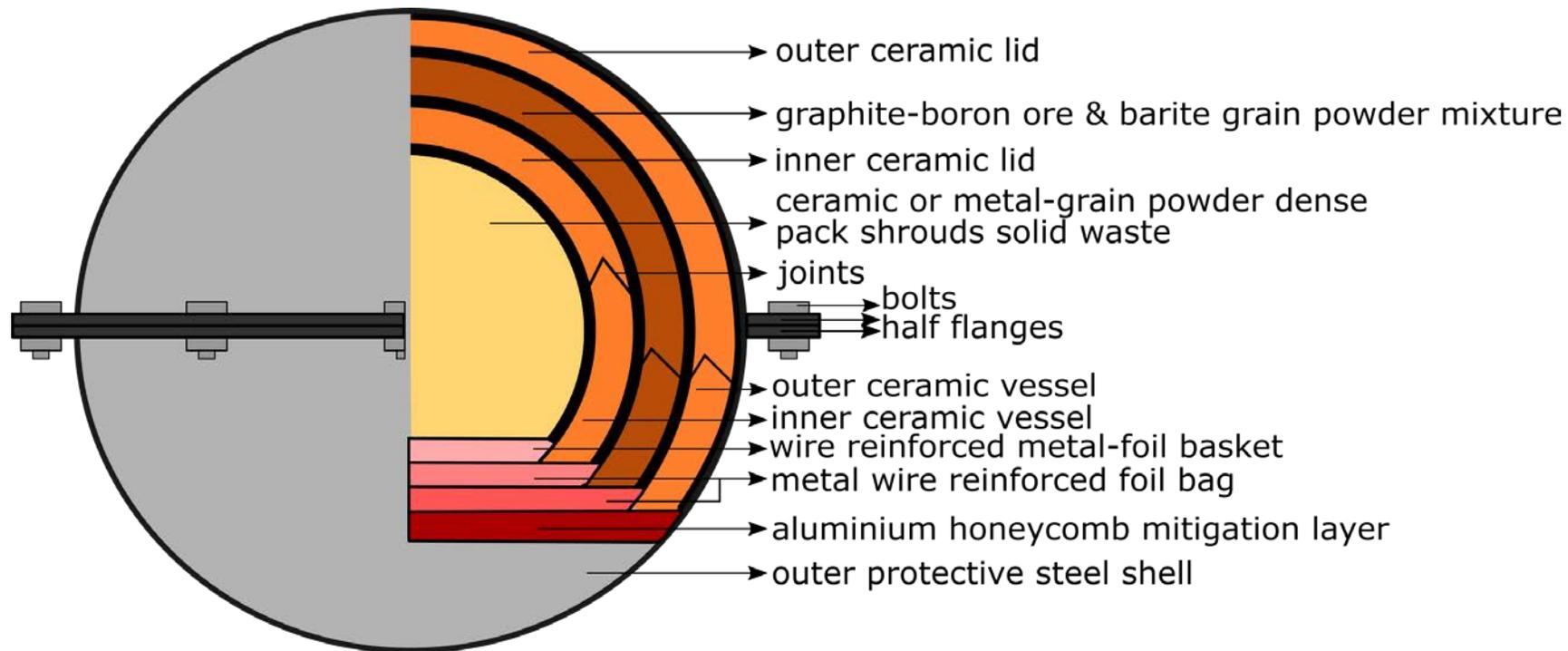
- Good tensile strength and impact resistance of the material
- High toughness material
- Dense material with no open pores or cracks
- Joint or weld areas must have the same properties as the body material
- Good chemical resistance of the material in the storage environment
- Sufficient thermal conductivity to remove heat from the waste
- Use of conventional processes requiring only minor adaptations



Highlights difficulty of manufacturing large ceramic parts

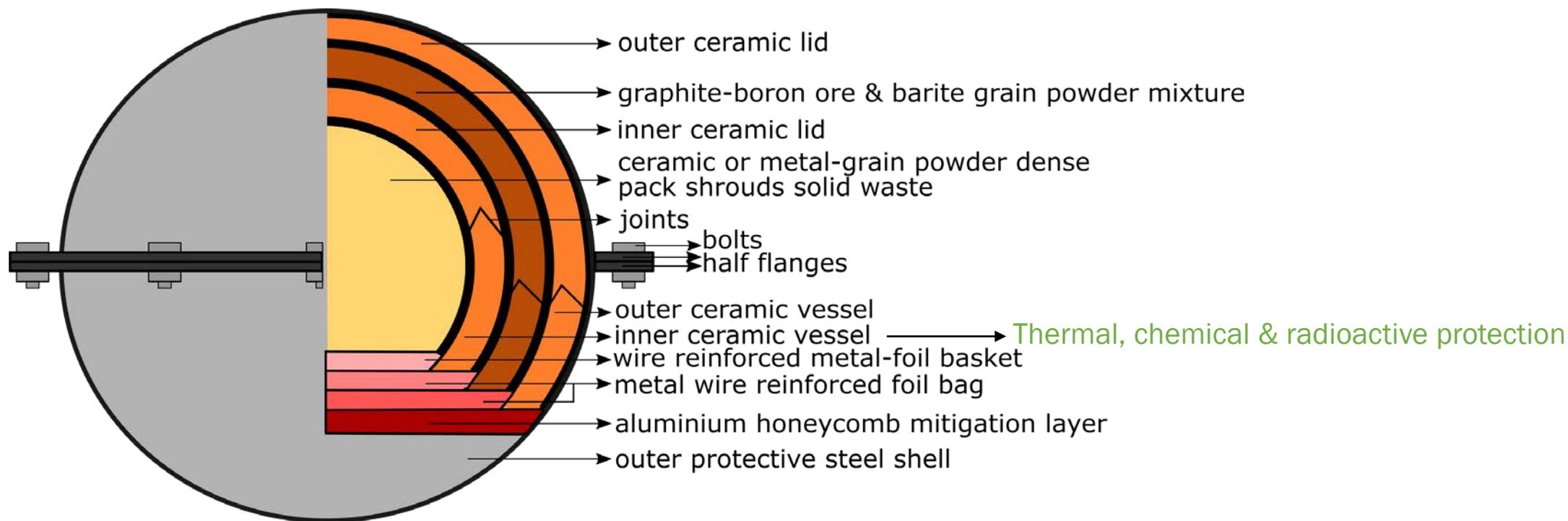
ALUMINA SOLUTIONS: BNL/NUCON, USA (LATE 1990)

- Onion-like system



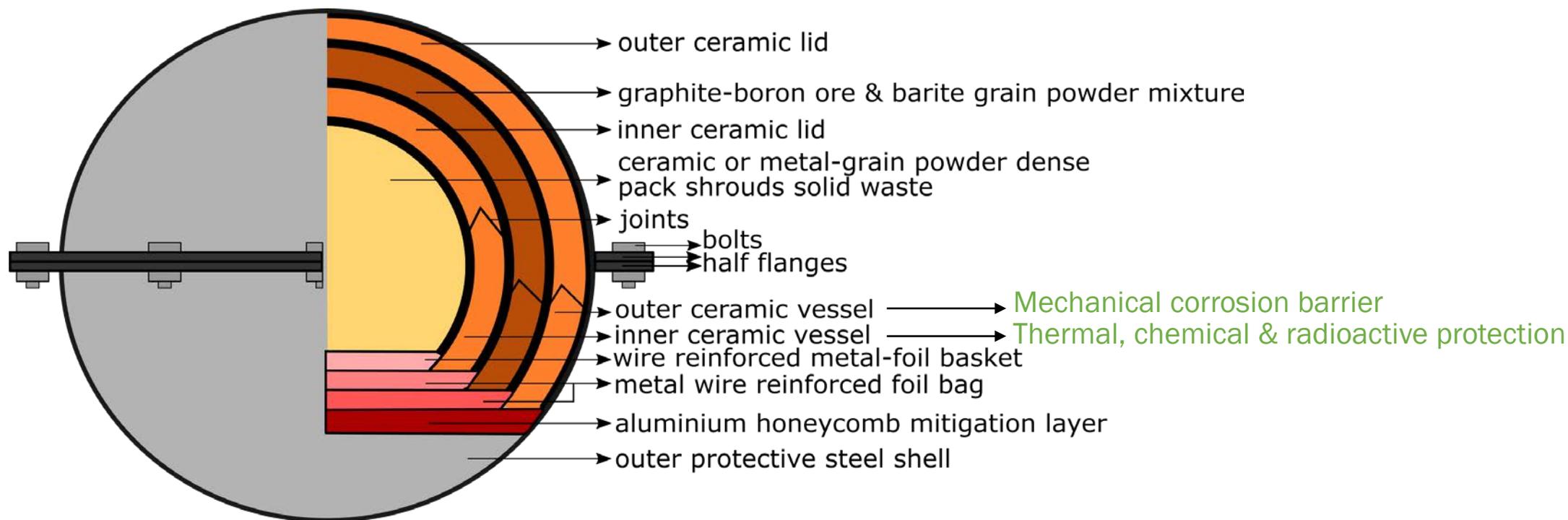
ALUMINA SOLUTIONS: BNL/NUCON, USA (LATE 1990)

- Onion-like system



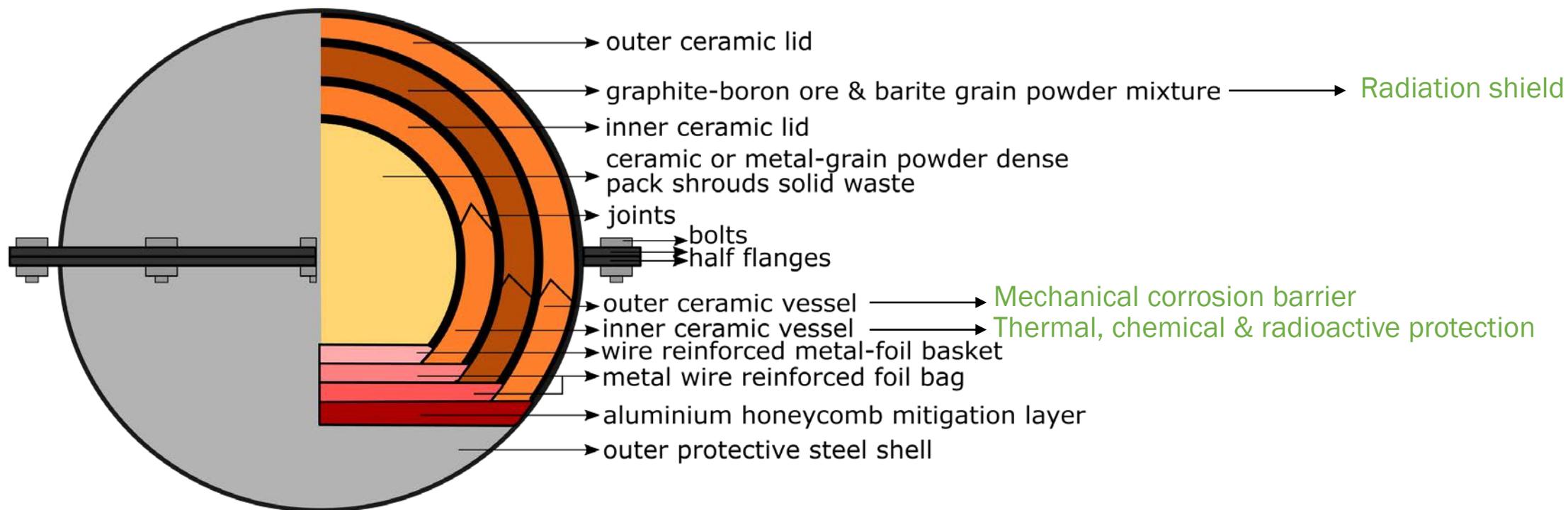
ALUMINA SOLUTIONS: BNL/NUCON, USA (LATE 1990)

- Onion-like system



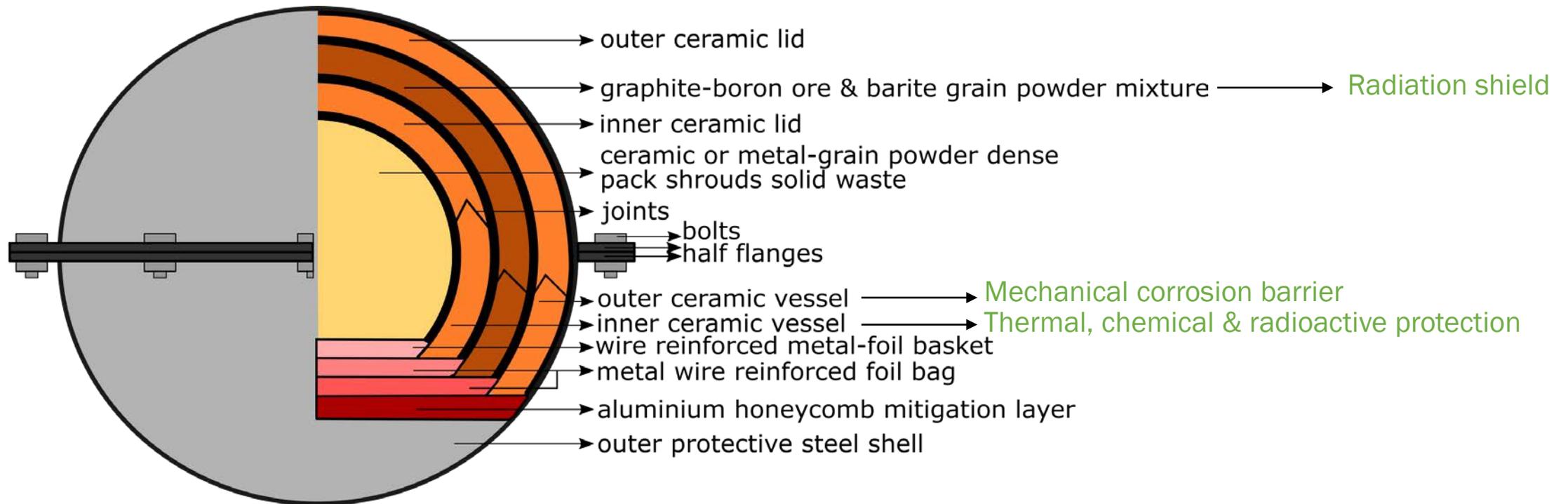
ALUMINA SOLUTIONS: BNL/NUCON, USA (LATE 1990)

- Onion-like system



ALUMINA SOLUTIONS: BNL/NUCON, USA (LATE 1990)

- Onion-like system

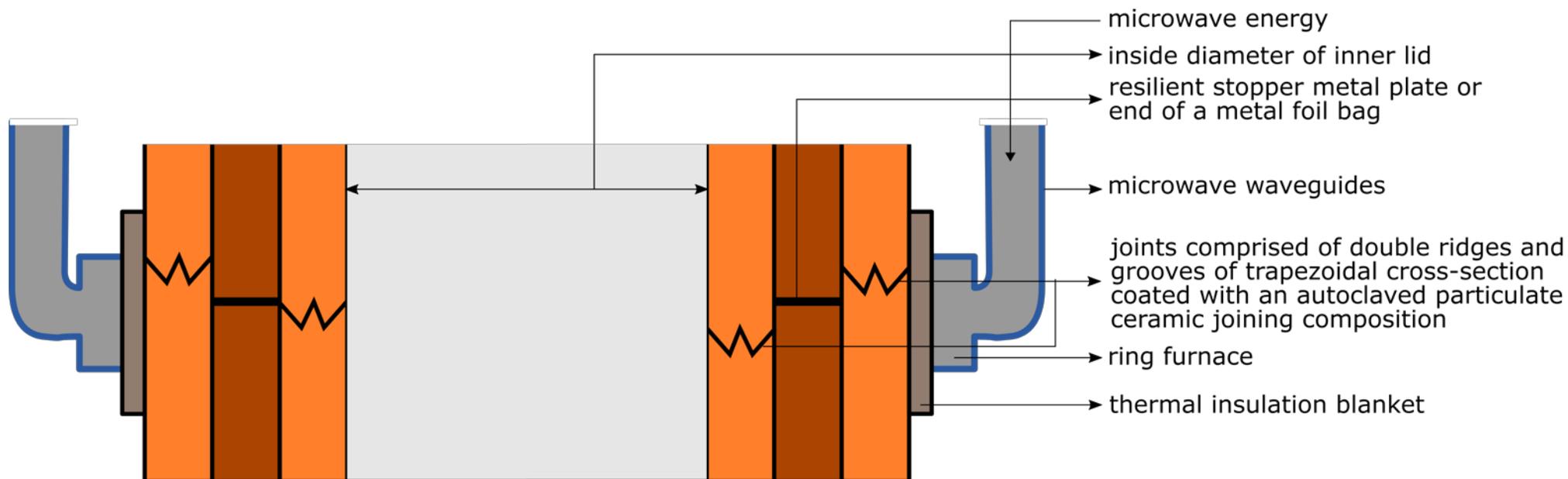


- Depending on the size of the waste



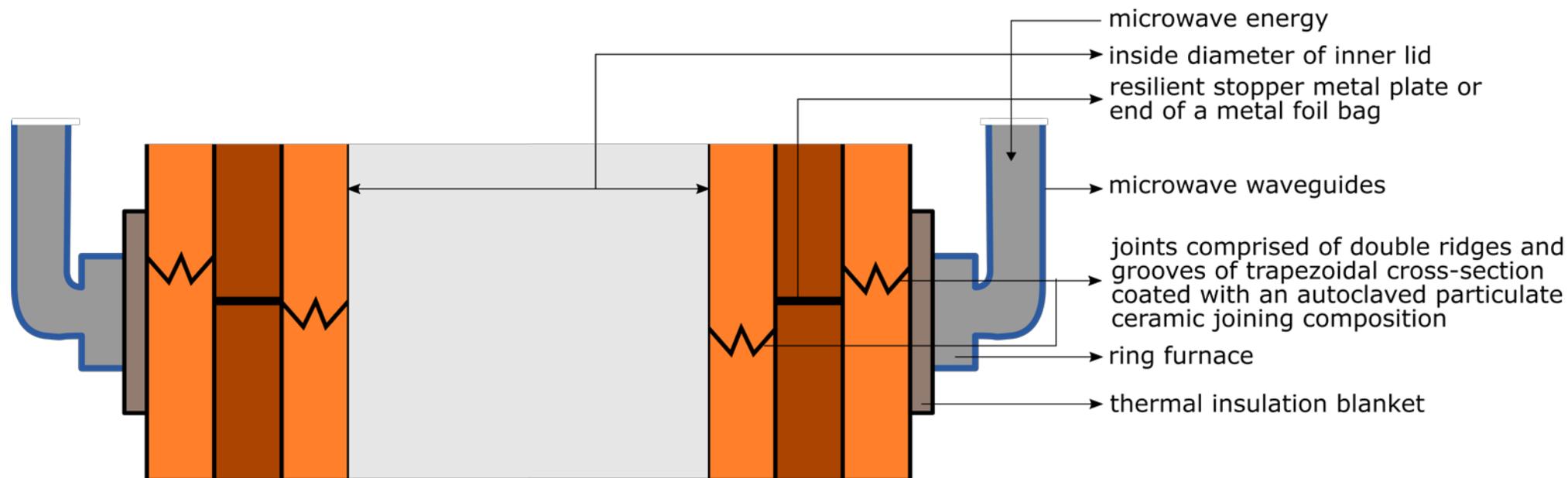
ALUMINA SOLUTIONS: BNL/NUCON, USA (LATE 1990)

- Watertight sealing of ceramic containers made of $MgAl_2O_4$ using microwave process



ALUMINA SOLUTIONS: BNL/NUCON, USA (LATE 1990)

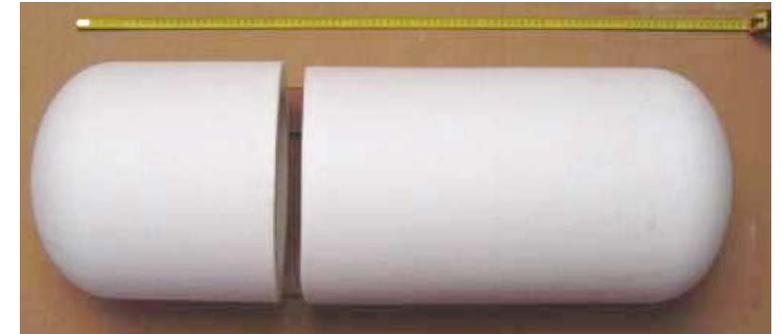
- Watertight sealing of ceramic containers made of $MgAl_2O_4$ using microwave process



- Addition of ceramic fibers
 - Mechanical reinforcement of the container
 - Favor the thermal treatment of the material
 - Increase radiological properties of the container

ALUMINA SOLUTIONS: ANDRA, FRANCE (2007-2009)

- Development & characterization of alumino-silicate ceramics >> conventional silicate ceramics
 - Suitable chemical durability → thickness reduction of ~ 3 - 4 mm over 1000 years
 - Adapted design of a container for HLW
 - Adapted casting, drying & sintering processes



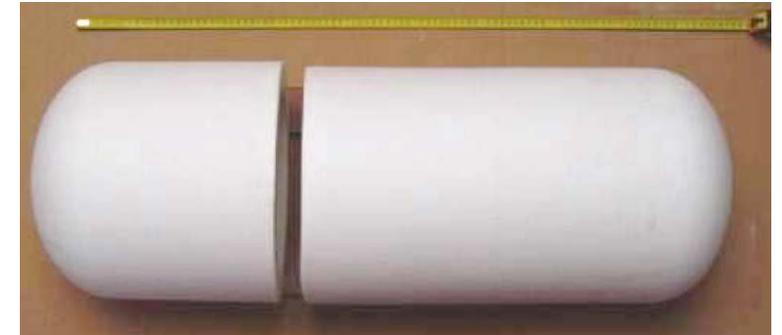
half-scale model of $\text{Al}_2\text{O}_3/\text{SiO}_2$ VHLW container



Lid: thickness at scale, ~4 cm

ALUMINA SOLUTIONS: ANDRA, FRANCE (2007-2009)

- Development & characterization of alumino-silicate ceramics >> conventional silicate ceramics
 - Suitable chemical durability → thickness reduction of ~ 3 - 4 mm over 1000 years
 - Adapted design of a container for HLW
 - Adapted casting, drying & sintering processes
- Closure of the system?
 - Focus on the sealing technology
 - Two major constraints to preserve the containment properties of the glass matrix
 - Max surface temperature of the ceramic container of 600-700 °C
 - Heating technology localized to the closure area
 - Microwaves & interaction of ceramic materials to assemble ceramic parts



half-scale model of $\text{Al}_2\text{O}_3/\text{SiO}_2$ VHLW container



Lid: thickness at scale, ~4 cm

ALUMINA SOLUTIONS: ANDRA, FRANCE (2007- ONGOING)

- It is possible to:
 - Improve the quality of the ceramic/glass sealing interface via a two-stage enameling process:
 - Firing in a conventional furnace → sealing the enameled parts by microwave heat treatment
 - Confirm that the selected and tested glasses have processing temperatures compatible with the constraints imposed by the presence of the primary package
 - Confirm the feasibility of sealing by microwave heating
 - Improve the quality of the joints for heating under minimal load
 - Verify the viability of the process

ALUMINA SOLUTIONS: ANDRA, FRANCE (2007- ONGOING)

- It is possible to:
 - Improve the quality of the ceramic/glass sealing interface via a two-stage enameling process:
 - Firing in a conventional furnace → sealing the enameled parts by microwave heat treatment
 - Confirm that the selected and tested glasses have processing temperatures compatible with the constraints imposed by the presence of the primary package
 - Confirm the feasibility of sealing by microwave heating
 - Improve the quality of the joints for heating under minimal load
 - Verify the viability of the process
- Considerations for the design & testing of a first prototype
 - Production of a prototype furnace for testing the annular shapes of test bodies and the localized heating of these parts
 - Understanding the resistance of the ceramic to the thermal gradients resulting from localized heating
 - Improve the coupling with the microwaves
 - Optimization of the compositions of sealing glasses to reinforce their mechanical and leaching resistance

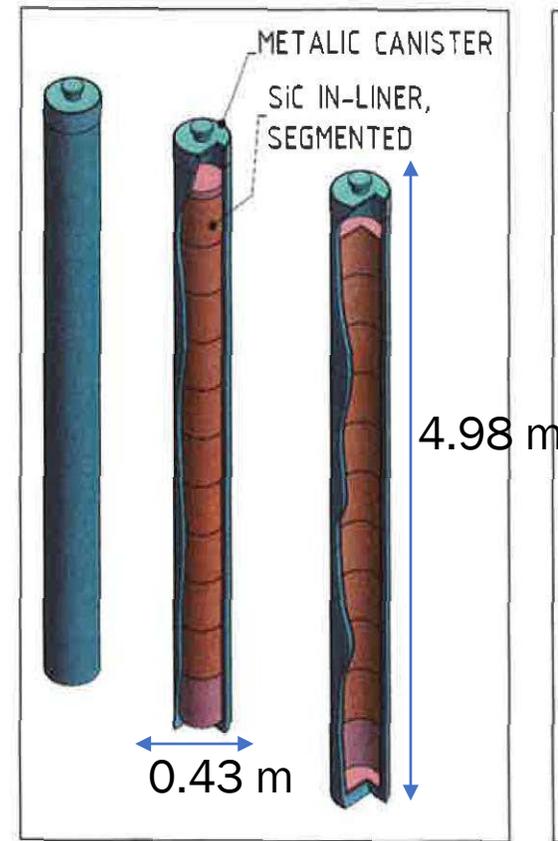


SILICON CARBIDE CONCEPT

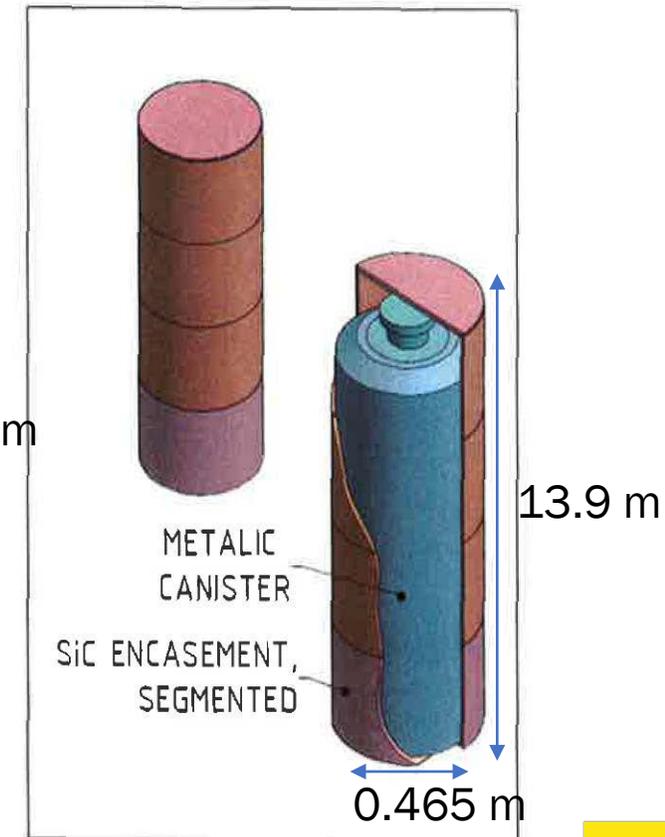
- Until recently only possible to manufacture large pieces out of:
 - Silicon impregnated silicon carbide
 - Recrystallized silicon carbide

SILICON CARBIDE CONCEPT

- Until recently only possible to manufacture large pieces out of:
 - Silicon impregnated silicon carbide
 - Recrystallized silicon carbide
- Currently also from conventional sintered silicon carbide



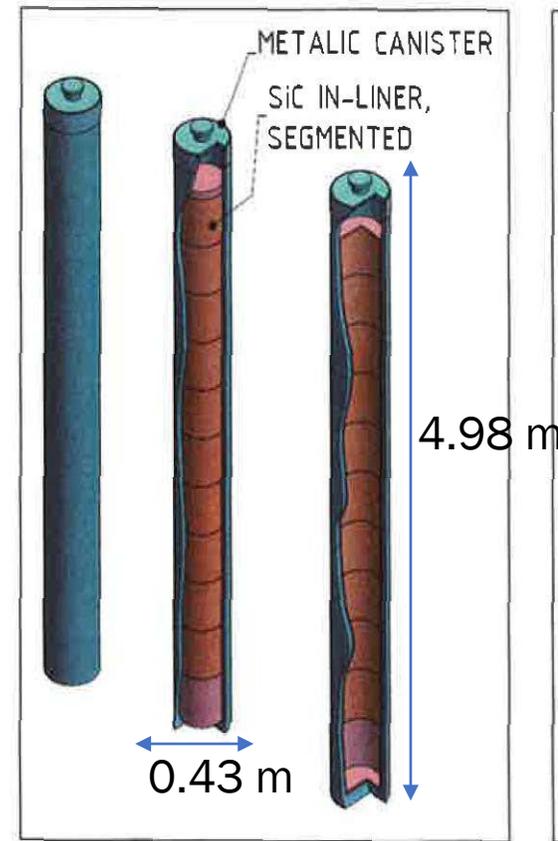
SSiC encasement for SF



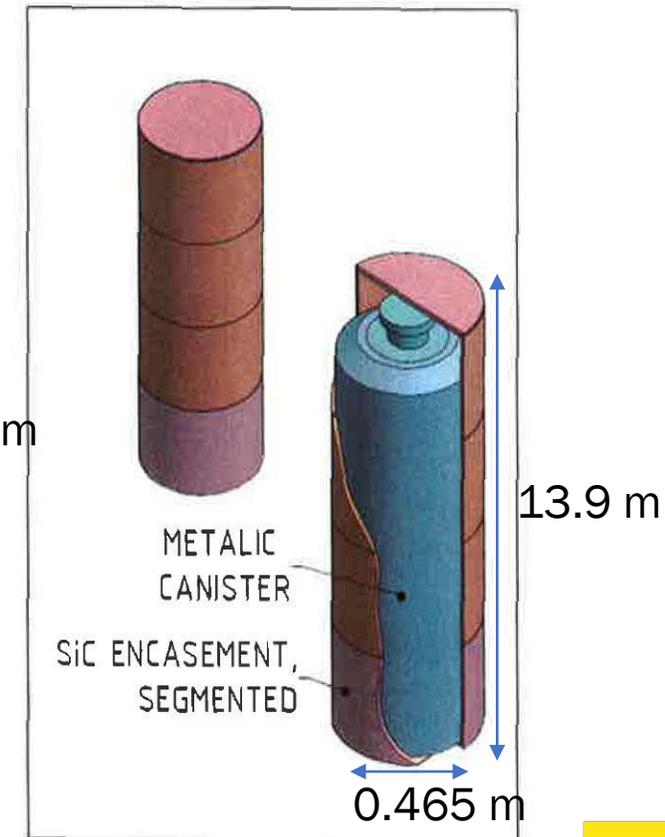
SSiC encasement for VHLW

SILICON CARBIDE CONCEPT

- Until recently only possible to manufacture large pieces out of:
 - Silicon impregnated silicon carbide
 - Recrystallized silicon carbide
- Currently also from conventional sintered silicon carbide
- High corrosion resistance (3 month test)
 - Dissolution rate $1 \mu\text{m}/\text{year}$ \rightarrow 1 % total thickness fuel cladding



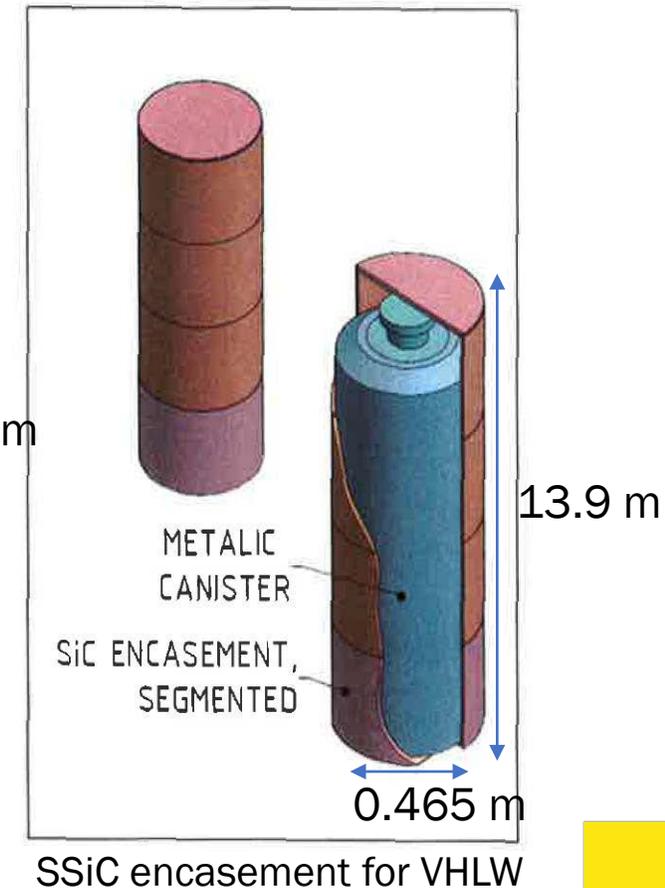
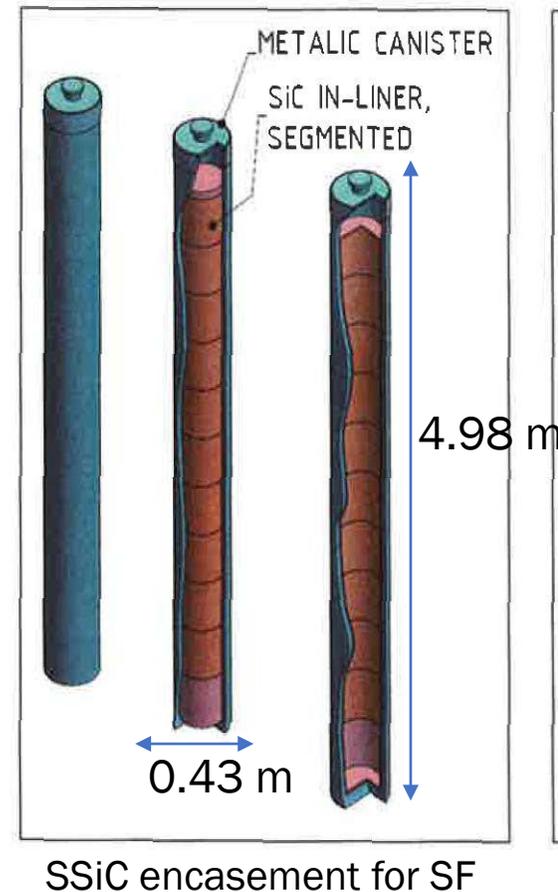
SSiC encasement for SF



SSiC encasement for VHLW

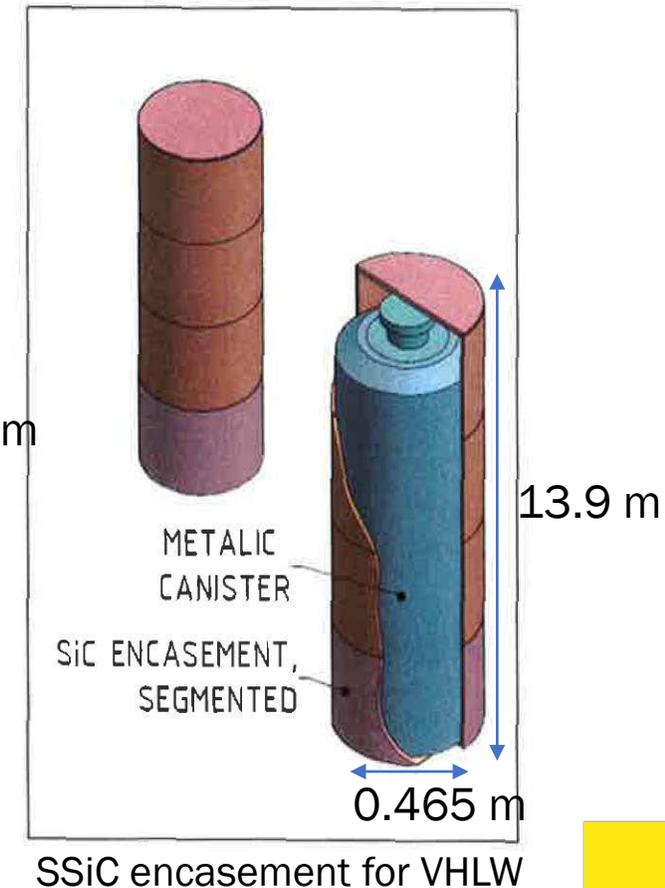
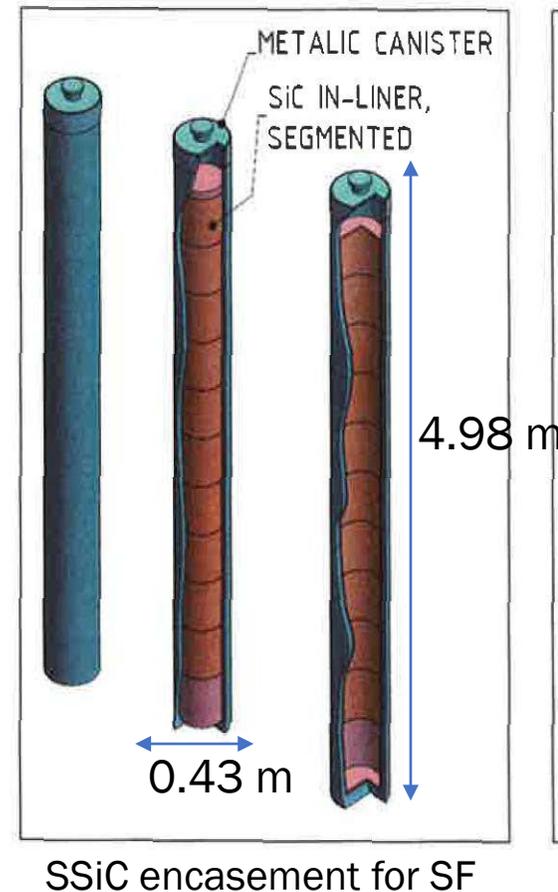
SILICON CARBIDE CONCEPT

- Until recently only possible to manufacture large pieces out of:
 - Silicon impregnated silicon carbide
 - Recrystallized silicon carbide
- Currently also from conventional sintered silicon carbide
- High corrosion resistance (3 month test)
 - Dissolution rate $1 \mu\text{m}/\text{year}$ \rightarrow 1 % total thickness fuel cladding
- Addition of Cr:
 - Dissolution rate \downarrow
 - Fracture toughness \uparrow
 - High level hardness =



SILICON CARBIDE CONCEPT

- Until recently only possible to manufacture large pieces out of:
 - Silicon impregnated silicon carbide
 - Recrystallized silicon carbide
- Currently also from conventional sintered silicon carbide
- High corrosion resistance (3 month test)
 - Dissolution rate $1 \mu\text{m}/\text{year} \rightarrow 1\%$ total thickness fuel cladding
- Addition of Cr:
 - Dissolution rate \downarrow
 - Fracture toughness \uparrow
 - High level hardness =
- R&D under geological disposal conditions is needed



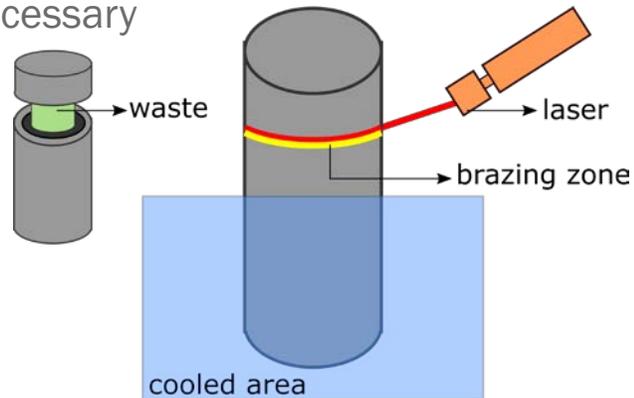


CONTENTS

- Introduction
- Alumina solutions: historical overview
 - SKB, Swedish concept
 - Lawrence Livermore National Laboratory, USA
 - BNL/Nucon, USA
 - Andra, France
- **Silicon carbide concept**
- **Ceramic coatings**
 - Titanium oxide
 - Chromium nitride
- **Metallic containers**
- **Metallic coatings**
- Outlook

SILICON CARBIDE CONCEPT

- Interconnecting SiC segments:
 - Laser joining method → no pretreatment necessary



Joining process of SiC-capsule

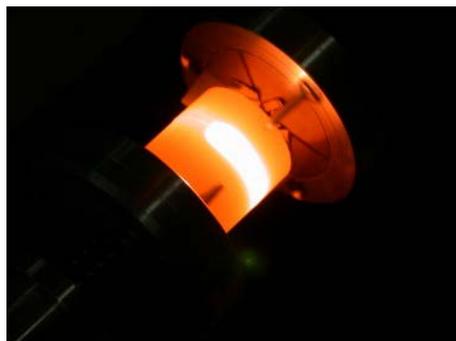
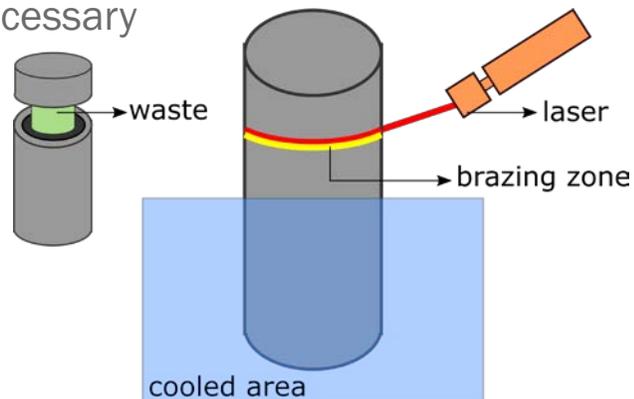


SiC compact

SILICON CARBIDE CONCEPT

- Interconnecting SiC segments:

- Laser joining method → no pretreatment necessary

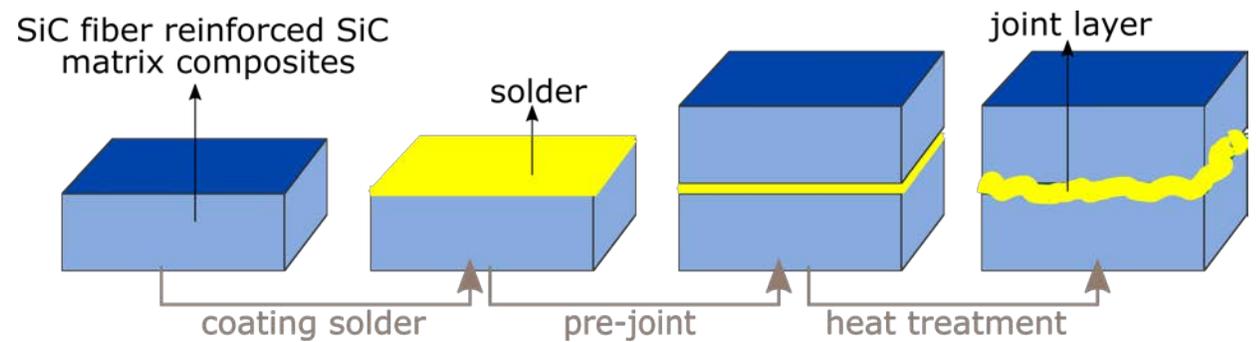


Joining process of SiC-capsule

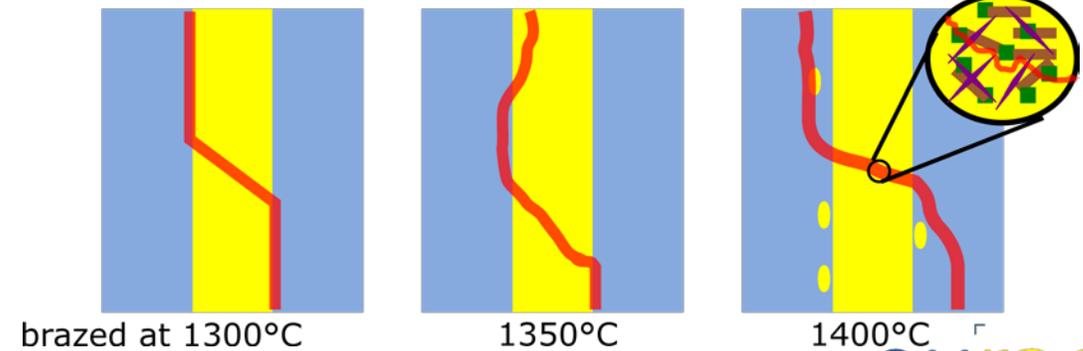


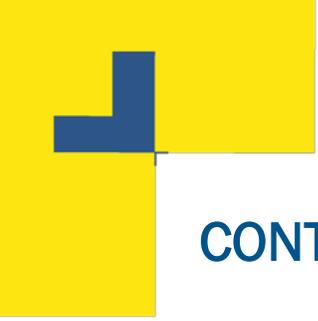
SiC compact

- Soldering based on various materials



crack propagation path





CONTENTS

- Introduction
- Alumina solutions: historical overview
 - SKB, Swedish concept
 - Lawrence Livermore National Laboratory, USA
 - BNL/Nucon, USA
 - Andra, France
- Silicon carbide concept
- **Ceramic coatings**
 - Titanium oxide
 - Chromium nitride
- **Metallic containers**
- **Metallic coatings**
- Outlook



CERAMIC COATINGS

- Prevent access of bentonite and/or clay pore waters to the substrate via cracking or leaching over a period of ≥ 10000 years



CERAMIC COATINGS

- Prevent access of bentonite and/or clay pore waters to the substrate via cracking or leaching over a period of ≥ 10000 years
- Less mature than metallic coatings

CERAMIC COATINGS

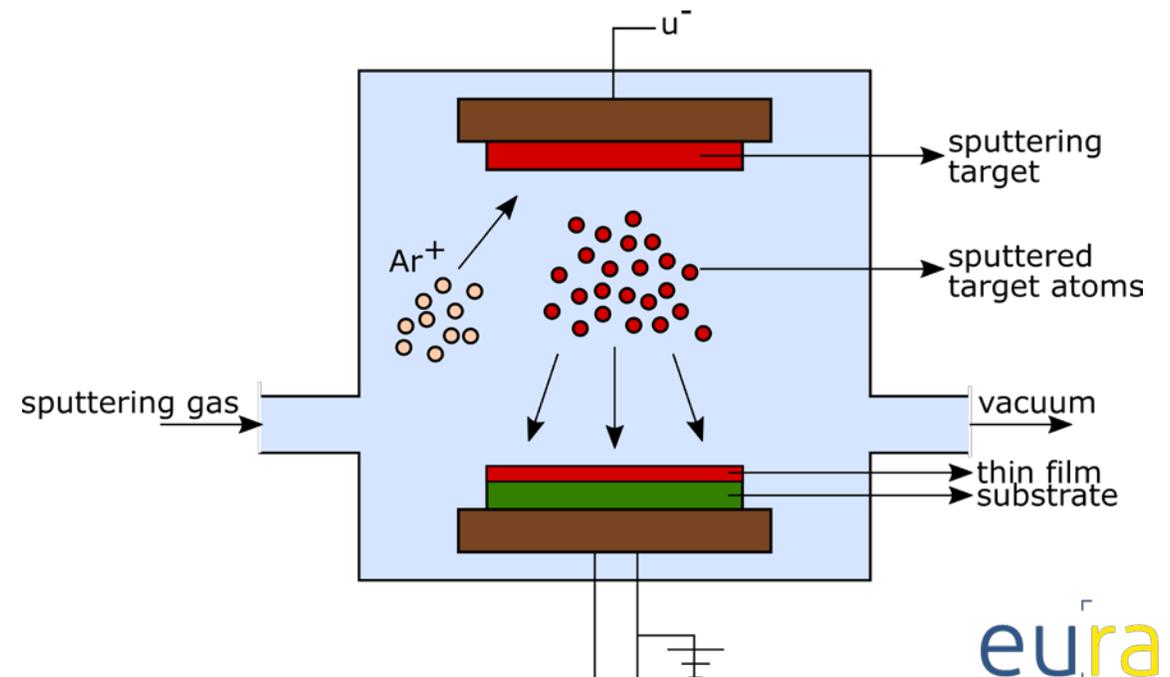
- Prevent access of bentonite and/or clay pore waters to the substrate via cracking or leaching over a period of ≥ 10000 years
- Less mature than metallic coatings
- **Inherent brittleness**
- **Mismatch of the thermal expansion coefficient with the underlying steel**
- **Requirement for relatively large thickness**
- **Very low porosity**
- **Damage tolerance**
- **Methods needs to be developed for**
 - Covering the lid-to-container weld
 - Coating repair

CERAMIC COATINGS

- Prevent access of bentonite and/or clay pore waters to the substrate via cracking or leaching over a period of ≥ 10000 years
- Less mature than metallic coatings
- **Inherent brittleness**
- **Mismatch of the thermal expansion coefficient with the underlying steel**
- **Requirement for relatively large thickness**
- **Very low porosity**
- **Damage tolerance**
- **Methods needs to be developed for**
 - Covering the lid-to-container weld
 - Coating repair
- **Promising options:**
 - yttria-stabilised zirconia
 - graded multilayer coatings of alumina & titania

CERAMIC COATINGS

- Prevent access of bentonite and/or clay pore waters to the substrate via cracking or leaching over a period of ≥ 10000 years
- Less mature than metallic coatings
- **Inherent brittleness**
- **Mismatch of the thermal expansion coefficient with the underlying steel**
- **Requirement for relatively large thickness**
- **Very low porosity**
- **Damage tolerance**
- **Methods needs to be developed for**
 - Covering the lid-to-container weld
 - Coating repair
- Promising options:
 - yttria-stabilised zirconia
 - graded multilayer coatings of alumina & titania
- Physical vapor deposition





CERAMIC COATINGS: TITANIUM OXIDE-BASED COATINGS

- Titanium nitrides & carbides

CERAMIC COATINGS: TITANIUM OXIDE-BASED COATINGS

- Titanium nitrides & carbides
- Coating thickness of 12 μm :
 - Slower corrosion correlated with coating porosity \downarrow
 - Corrosion current density decreased by 2.5-3 orders of magnitude
- TiO_2 films deposited on $\text{MgCa}_2\text{Zn}_1\text{Gd}_3$ effectively protected this alloy from corrosion in Ringer's solution at 37 °C

CERAMIC COATINGS: TITANIUM OXIDE-BASED COATINGS

- Titanium nitrides & carbides
- Coating thickness of 12 μm :
 - Slower corrosion correlated with coating porosity \downarrow
 - Corrosion current density decreased by 2.5-3 orders of magnitude
- TiO_2 films deposited on $\text{MgCa}_2\text{Zn}_1\text{Gd}_3$ effectively protected this alloy from corrosion in Ringer's solution at 37 °C
- Titanium oxide coatings deposited by PVD methods are promising for corrosion protection of the low carbon steel containers
- Additional studies are needed on long-term corrosion processes under relevant geological disposal conditions



CERAMIC COATINGS: CHROMIUM NITRIDE COATINGS



CERAMIC COATINGS: CHROMIUM NITRIDE COATINGS

- High hardness
- Excellent wear resistance
- High corrosion resistance

CERAMIC COATINGS: CHROMIUM NITRIDE COATINGS

- High hardness
- Excellent wear resistance
- High corrosion resistance
- Corrosion resistance of 2-4 μm thick Zry-4 alloy $\text{CrN} > \text{TiAlN} > \text{AlCrN}$
- CrN coating (7 μm) on cobalt based alloy in high temperature and high-pressure water with γ -rays of 100 Gy/h by ^{60}Co source irradiation during testing

CERAMIC COATINGS: CHROMIUM NITRIDE COATINGS

- High hardness
- Excellent wear resistance
- High corrosion resistance
- Corrosion resistance of 2-4 μm thick Zry-4 alloy $\text{CrN} > \text{TiAlN} > \text{AlCrN}$
- CrN coating (7 μm) on cobalt based alloy in high temperature and high-pressure water with γ -rays of 100 Gy/h by ^{60}Co source irradiation during testing
- Chromium nitride coatings are promising for corrosion protection of the carbon steel
- Additional studies are needed on long-term corrosion processes under relevant geological disposal conditions

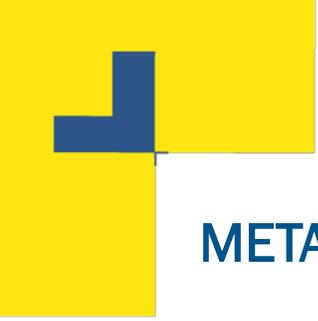


CONTENTS

- Introduction
- Alumina solutions: historical overview
 - SKB, Swedish concept
 - Lawrence Livermore National Laboratory, USA
 - BNL/Nucon, USA
 - Andra, France
- Silicon carbide concept
- Ceramic coatings
 - Titanium oxide
 - Chromium nitride
- **Metallic containers**
- **Metallic coatings**
- Outlook

METALLIC CONTAINERS: OVERVIEW OF CURRENT CONCEPTS AND PLANNED INNOVATIONS FOR STORAGE CONTAINERS

Material	+	-	e.g. Countries	Remark
Low alloyed steel	<ul style="list-style-type: none"> • Cost • Fabrication • Mechanical strength • Radiation shielding 	<ul style="list-style-type: none"> • Corrosion resistance < copper but low • SCC 	France, Japan, Switzerland	Carbon steel
Stainless steel	Corrosion resistance (passive film)	<ul style="list-style-type: none"> • Localized corrosion • Some classes SCC 	UK, Spain, Japan, USA	Focus on austenitic alloys
Titanium	Corrosion resistance	<ul style="list-style-type: none"> • Crevice corrosion in O₂ phase • HIC 	Canada, Belgium, Japan	Alloys with Pd or Ru could avoid crevice corrosion
Nickel alloys	<ul style="list-style-type: none"> • Corrosion resistance • Mechanical properties in high-temp applications • Fabrication 	<ul style="list-style-type: none"> • Localized corrosion in certain environments • Uncertainties associated with MIC 	Germany, Belgium, USA, Argentina	Ni-Cr-Mo or Ni-Fe-Cr-Mo
Copper	<ul style="list-style-type: none"> • Corrosion resistance • Mechanical properties 	cost	UK, Japan, Sweden, Finland, Canada, Switzerland	Fi, Sw: O ₂ free, phosphorous doped copper; J, Ca, Swi: relatively pure cold spray & electrodeposited copper
Lead	<ul style="list-style-type: none"> • Cost • Radiation shielding 	<ul style="list-style-type: none"> • Corrosion behavior? • Mechanical strength? • Environmental aspects? 	Argentina, Brazil, Russia	Not considered



METALLIC COATINGS

- Titanium, chromium & copper
- Open questions:
 - Required thickness to exclude through porosity
 - Effect of through defects and irradiation on corrosion resistance

METALLIC COATINGS

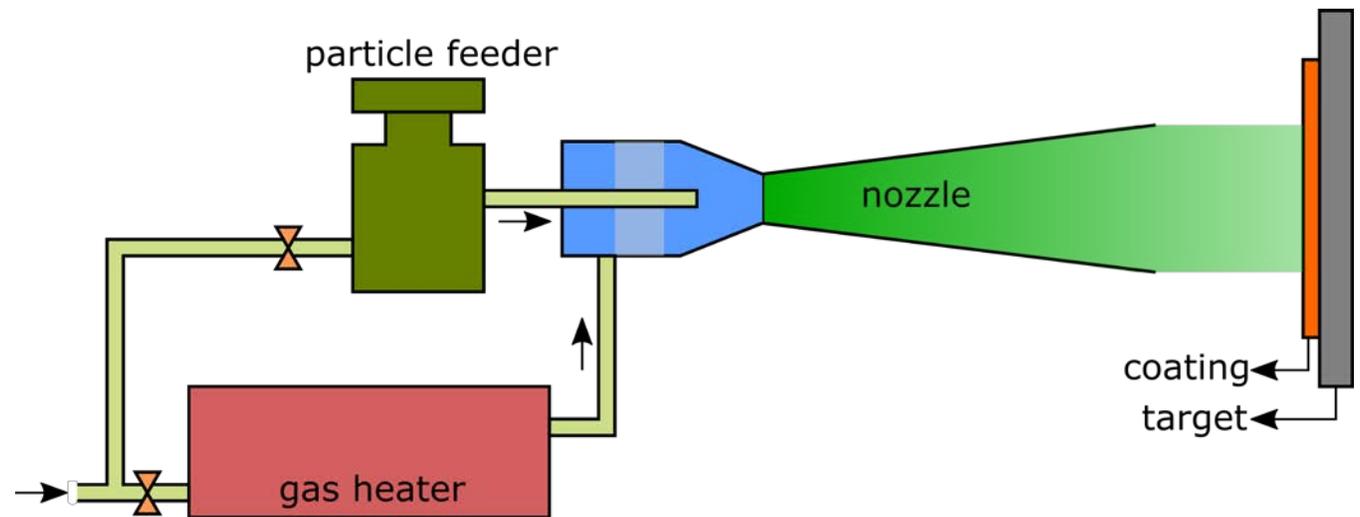
- Titanium, chromium & copper
- Open questions:
 - Required thickness to exclude through porosity
 - Effect of through defects and irradiation on corrosion resistance
- **Dual-wall container with copper coating:**
 - Copper layer is directly on the steel vessel → no gap between layers → no fabrication issues
 - ↔ standard design → gap between outer copper layer and cast iron insert can introduce creep & SCC of the copper shell
 - Welding joint could be covered after welding steel cover



Canadian design of dual wall-container

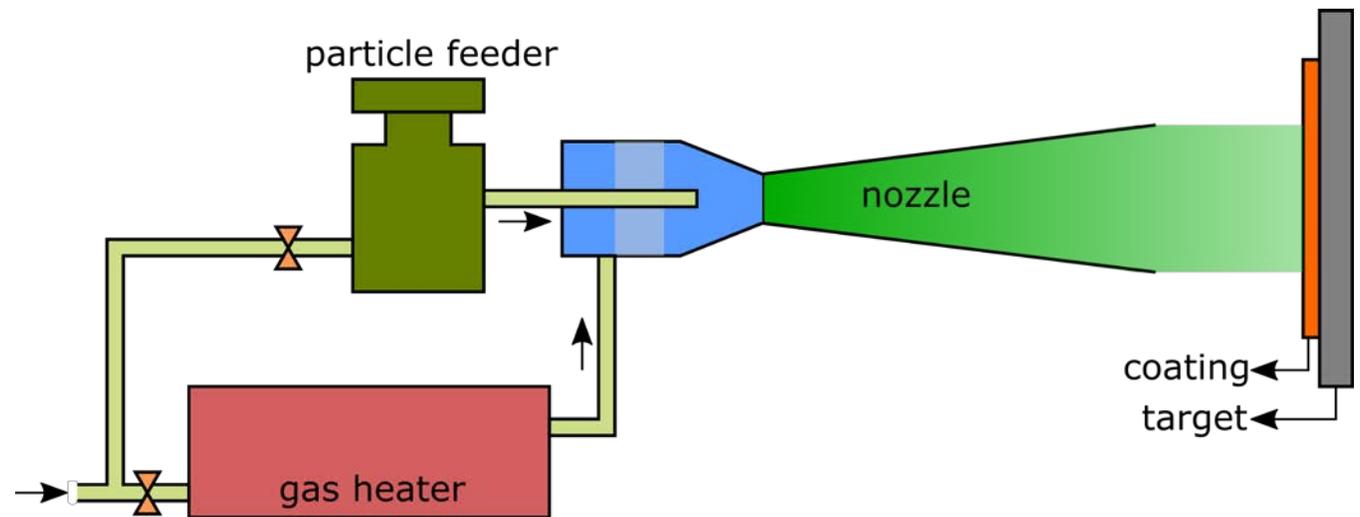
COPPER DEPOSITION PROCESSES

- Electrodeposition
 - To coat 95% of the container
- Cold gas dynamic spray
 - To coat the region of the closure weld
 - Production of metal deposits
 - Metal-ceramic coatings:
 - Corrosion resistance ↑
 - Mechanical properties ↑
 - Wear resistance ↑



COPPER DEPOSITION PROCESSES

- Electrodeposition
 - To coat 95% of the container
- Cold gas dynamic spray
 - To coat the region of the closure weld
 - Production of metal deposits
 - Metal-ceramic coatings:
 - Corrosion resistance ↑
 - Mechanical properties ↑
 - Wear resistance ↑
- Quality of the coating depends on:
 - Nozzle displacement
 - Carrier gas type & velocity





CONTENTS

- Introduction
- Alumina solutions: historical overview
 - SKB, Swedish concept
 - Lawrence Livermore National Laboratory, USA
 - BNL/Nucon, USA
 - Andra, France
- Silicon carbide concept
- Ceramic coatings
 - Titanium oxide
 - Chromium nitride
- Metallic containers
- Metallic coatings
- **Outlook**



OUTLOOK

- Each concept has advantages & disadvantages



OUTLOOK

- Each concept has advantages & disadvantages
- Diversity of the envisaged solutions leads to a large variability of experiments needed



OUTLOOK

- Each concept has advantages & disadvantages
- Diversity of the envisaged solutions leads to a large variability of experiments needed
 - Ceramics
 - Production of large-scale pieces
 - Optimization of the sintering process
 - Optimization of the sealing process



OUTLOOK

- Each concept has advantages & disadvantages
- Diversity of the envisaged solutions leads to a large variability of experiments needed
 - Ceramics
 - Production of large-scale pieces
 - Optimization of the sintering process
 - Optimization of the sealing process
 - Alternative copper grades (DLP, XLP or HCP copper)
 - How do they behave in relevant geological disposal conditions?



OUTLOOK

- Each concept has advantages & disadvantages
- Diversity of the envisaged solutions leads to a large variability of experiments needed
 - Ceramics
 - Production of large-scale pieces
 - Optimization of the sintering process
 - Optimization of the sealing process
 - Alternative copper grades (DLP, XLP or HCP copper)
 - How do they behave in relevant geological disposal conditions?
 - Coatings



OUTLOOK

- Each concept has advantages & disadvantages
- Diversity of the envisaged solutions leads to a large variability of experiments needed
 - Ceramics
 - Production of large-scale pieces
 - Optimization of the sintering process
 - Optimization of the sealing process
 - Alternative copper grades (DLP, XLP or HCP copper)
 - How do they behave in relevant geological disposal conditions?
 - Coatings
 - Damage resistance
 - Long-term corrosion data & archaeological analogues do not exist
 - Development new metal/ceramic coatings

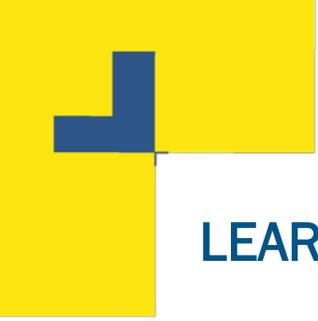
FURTHER READING

- <https://www.ejp-eurad.eu/publications/eurad-d151-concord-initial-sota>
- Holdsworth, S.R., (2013). Ceramic Material Solutions for Nuclear Waste Disposal containers. NAGRA report NAB12-45.
- Holdsworth, S.R., (2014). Feasibility evaluation study of candidate container solutions for the disposal of spent nuclear fuel and high-level waste-A status review. NAGRA report NAB14-90.
- Holdsworth, S.R. (2018). Alternative coating Materials as Corrosion Barriers for SF and HLW Disposal containers. NAGRA report NAB18-19.
- INTERNATIONAL ATOMIC ENERGY AGENCY (2006). Development of Specifications for Radioactive Waste Packages. IAEA-TECDOC-1515. IAEA, Vienna

PREDICTION TOOLS FOR ASSESSMENT OF LONG-TIME BARRIER INTEGRITY

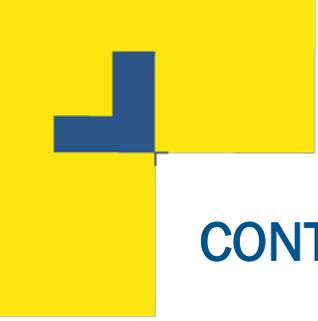


This project has received funding from the European Union's Horizon 2020 research and innovation programme 2014-2018 under grant agreement N°847593



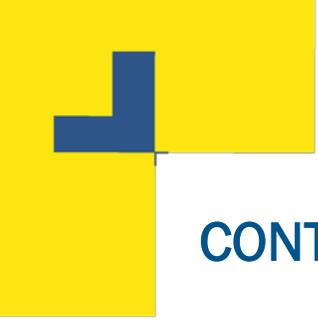
LEARNING OUTCOMES

- Identify principles of different modelling approaches for several corrosion processes
- Understand advantages & disadvantages of different modelling tools
- Compare processes relevant for copper & steel containers
- Understand how corrosion processes can be integrated in performance assessments (PA)
- Get acquainted with basic modelling tools



CONTENT

- Introduction
- Copper container corrosion
 - Reactive transport models in bentonite
 - Modeling sulfide fluxes
 - Modelling irradiation-induced corrosion
- Steel-bentonite models
- Integration of corrosion phenomena in performance assessments
- Performance assessments for copper-based canister corrosion
- Performance assessments for iron-based alloy canister corrosion



CONTENT

- **Introduction**
- **Copper container corrosion**
 - Reactive transport models in bentonite
 - Modeling sulfide fluxes
 - Modelling irradiation-induced corrosion
- **Steel-bentonite models**
- **Integration of corrosion phenomena in performance assessments**
- **Performance assessments for copper-based canister corrosion**
- **Performance assessments for iron-based alloy canister corrosion**

GENERIC CORROSION MODELLING APPROACHES: GENERAL CORROSION

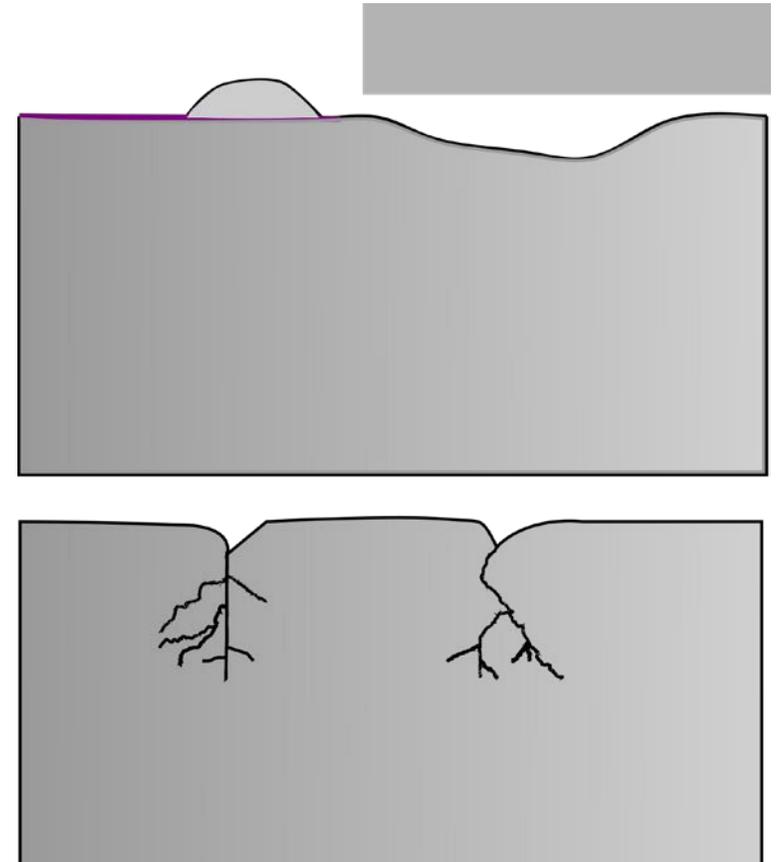
Method	Principle	Assumptions	Remarks
Empirical extrapolation	Extrapolate corrosion rate short-term lab exp. to long-term corrosion rates	<ul style="list-style-type: none"> Stable environmental conditions No step changes in corrosion mechanisms 	<ul style="list-style-type: none"> Built-in conservatism Useful to consider validation with archaeological analogues
Mass balance	With O ₂ → amount of O ₂ after closure determines extent of corrosion Without O ₂ → anaerobic corrosion		Anaerobic corrosion → corrosion rate is not determined by the total available mass of the cathodic reactant
Mass transport	Corrosion rate determined by rate of supply of the corrodent	<ul style="list-style-type: none"> Correct calculation of the mass transport Reactant is irreversibly consumed in the corrosion reaction 	Also the mass transport of corrosion products could be limiting
Reactive transport modeling (e.g. PhreeqcRM, Geochemist Workbench)	Use of available software systems to perform equilibrium & kinetic reaction calculations for reactive transport simulators		<ul style="list-style-type: none"> May require a lot of input data Can be mathematically complex Once developed, very useful

GENERIC CORROSION MODELLING APPROACHES: LOCALIZED CORROSION

Method	Principle	Remarks	Disadvantages
Pitting factors	max. loss of thickness on a surface/average loss of thickness on the same surface	<ul style="list-style-type: none"> For surfaces that exhibit true corrosion pits or uneven/patchy general corrosion Can be measured over the short-term 	Long-term data estimated using archaeological analogues → direct applicability?
Empirical roughening factor	Provide a topographical model of a corroded surface not necessarily based on mechanistic understanding	Assume the production of a given surface profile that deviates from the mean line of the surface within a predefined constraint	Not suitable for true corrosion pitting of passive materials
Empirical localized corrosion growth rate	Measure pit depths ~ time → develop growth rate curve → develop model e.g. $P = kt^n$		
Electrochemical prediction	Comparison of the free corrosion potential with the critical potential for localized corrosion	Reasonable accuracy over comparatively long-time scales if transient conditions are well-known	<ul style="list-style-type: none"> No prediction of localized corrosion rates or penetration depth over time Large database necessary

MODELLING CHEMISTRY WITHIN SITES OF LOCALIZED CORROSION

- Models to predict the chemistry within cracks and crevices
- To understand fundamental processes within sites of localized corrosion
- No reliable predictions of growth rates
- **Defining & justifying the size of the coupled cathode**



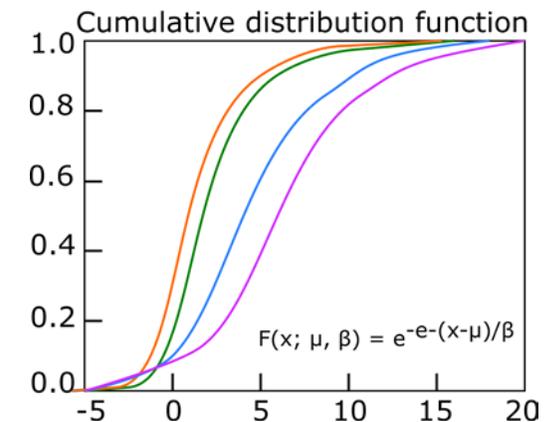
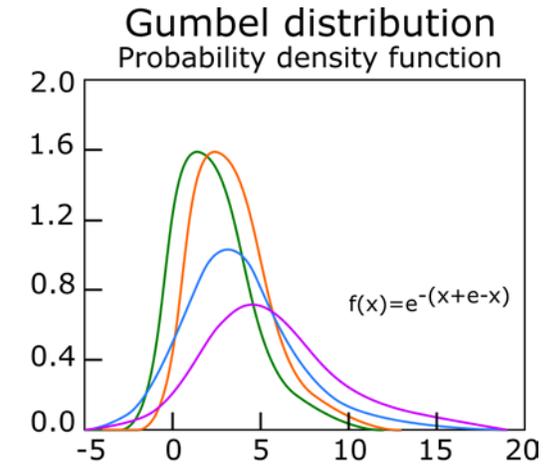


STATISTICAL APPROACHES

- To analyze experimental results from pitting corrosion studies
- To analyze inspection results to estimate corrosion rates

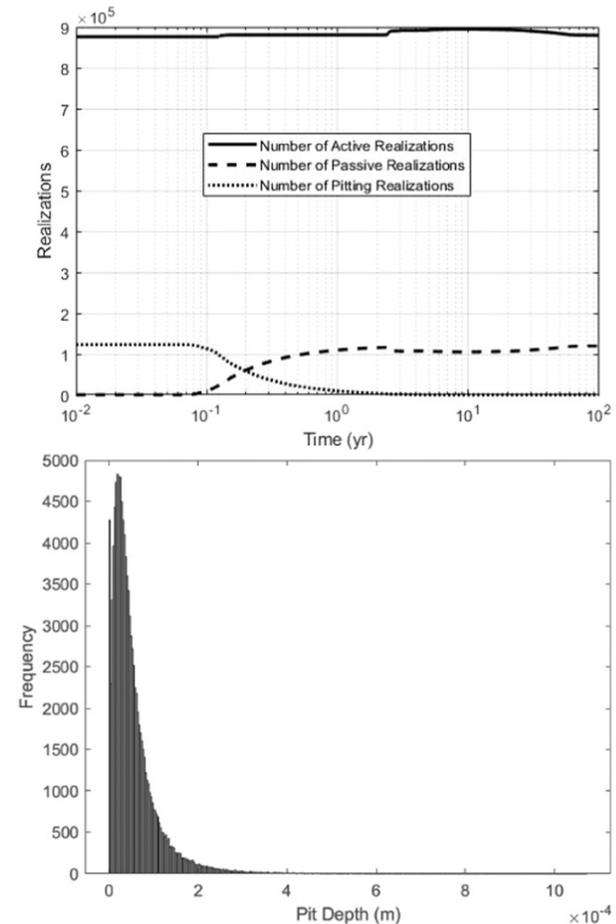
STATISTICAL APPROACHES

- To analyze experimental results from pitting corrosion studies
- To analyze inspection results to estimate corrosion rates
- Extreme value statistics
 - Extrapolation from small test coupons or inspection sites to real structures
 - Pitting corrosion → max pit depth over time
 - **Very conservative**



STATISTICAL APPROACHES

- To analyze experimental results from pitting corrosion studies
- To analyze inspection results to estimate corrosion rates
- Extreme value statistics
 - Extrapolation from small test coupons or inspection sites to real structures
 - Pitting corrosion → max pit depth over time
 - **Very conservative**
- Probabilistic assessment of pitting corrosion of copper containers based on:
 - Consideration of breakdown & repassivation potentials for pitting of copper
 - Predicted evolution of the environment
 - Combined with machine learning techniques



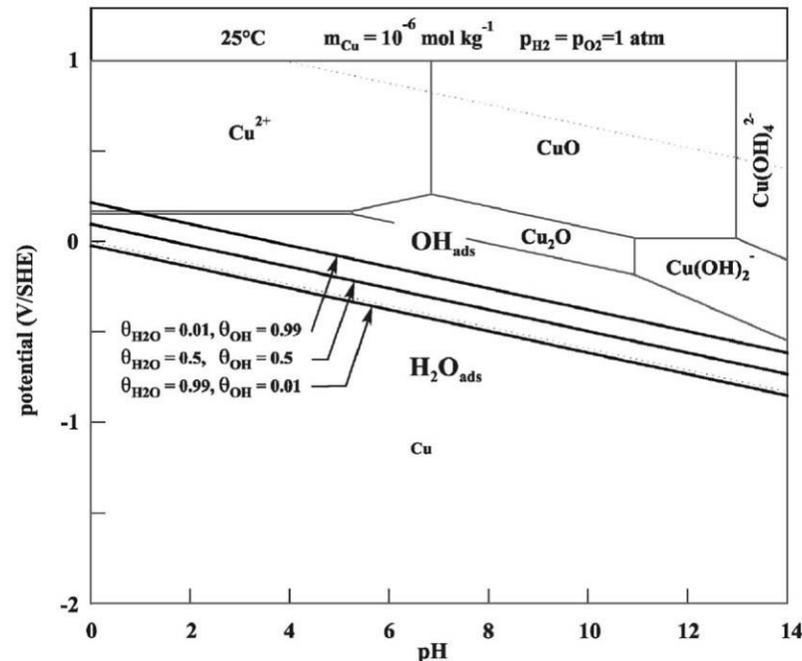


THERMODYNAMIC MODELLING OF ENVIRONMENTAL CHEMISTRY

- To predict the conditions under which a given metal may react with a given environment leading to the formation of dissolved ions or solid reaction products
- To predict properties of a system in equilibrium or how equilibrium is reached
- No corrosion rate

THERMODYNAMIC MODELLING OF ENVIRONMENTAL CHEMISTRY

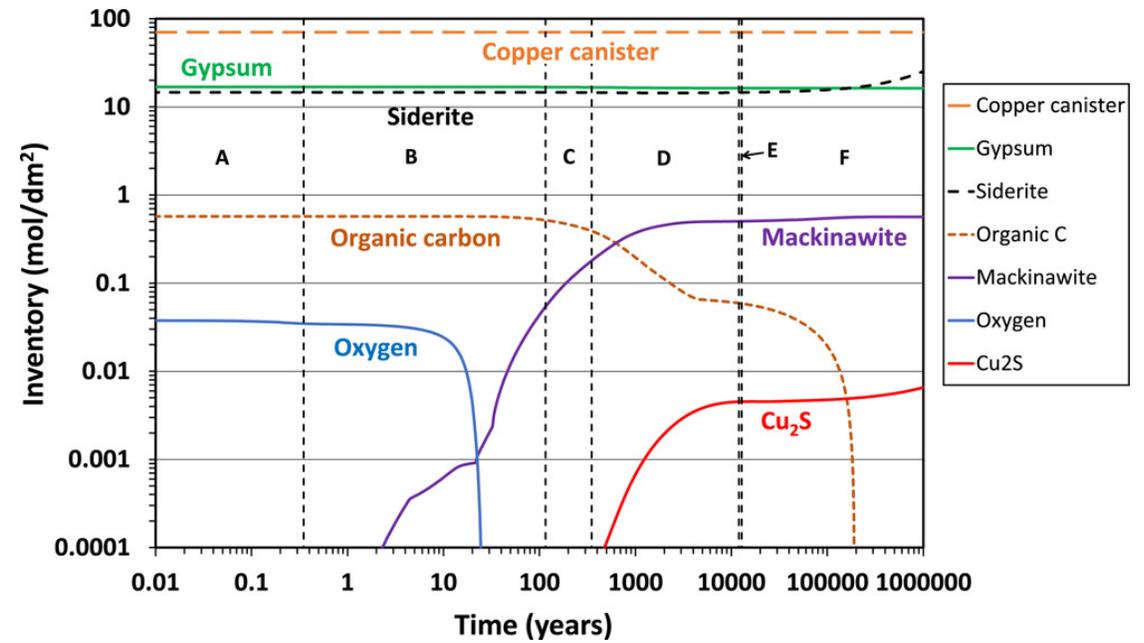
- To predict the conditions under which a given metal may react with a given environment leading to the formation of dissolved ions or solid reaction products
- To predict properties of a system in equilibrium or how equilibrium is reached
- No corrosion rate
- Pourbaix diagrams
 - Potential – pH stability diagrams



Pourbaix diagram for the Cu-H₂O system at 25 °C including the regions of stability of Cu(OH)_{ads} for various surface coverages θ

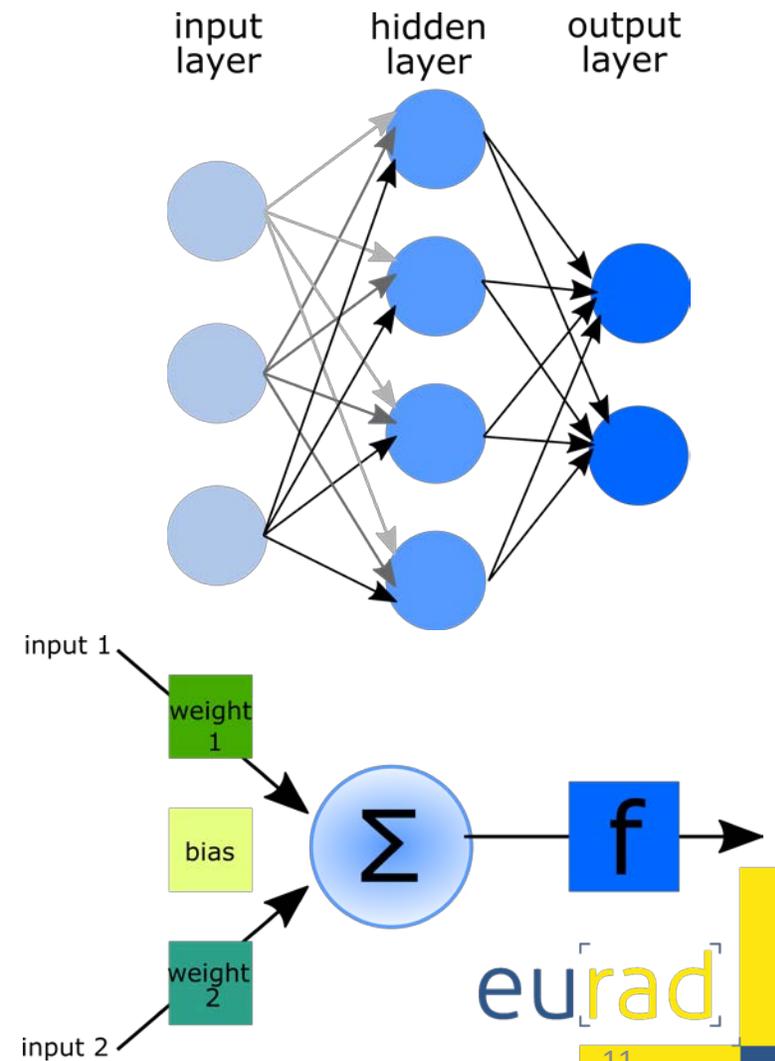
REACTIVE TRANSPORT MODELS

- Estimate max. amount of corrosion
- Species of interest & transport-related factors:
 - Sources
 - Sinks
- Assumptions:
 - Zero-concentration boundary condition
 - Gradual accumulation over time



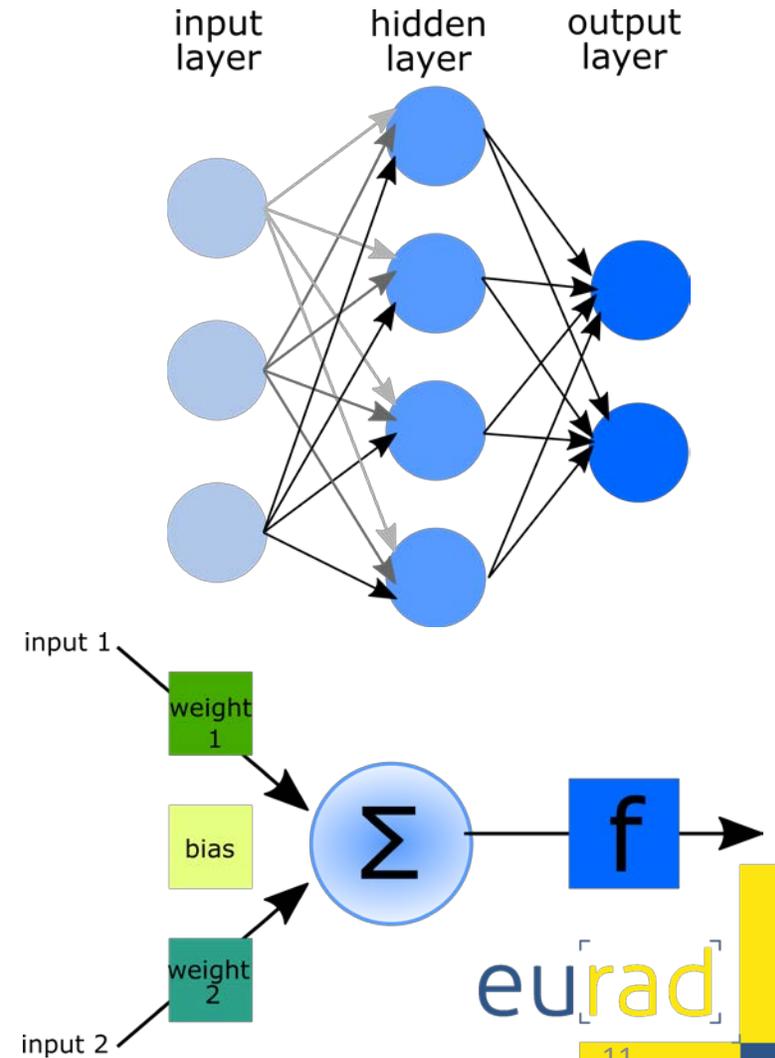
ARTIFICIAL INTELLIGENCE: NEURAL NETWORKS

- Principle:
 - Set up series of artificial neurons in a layered structure ~ brain



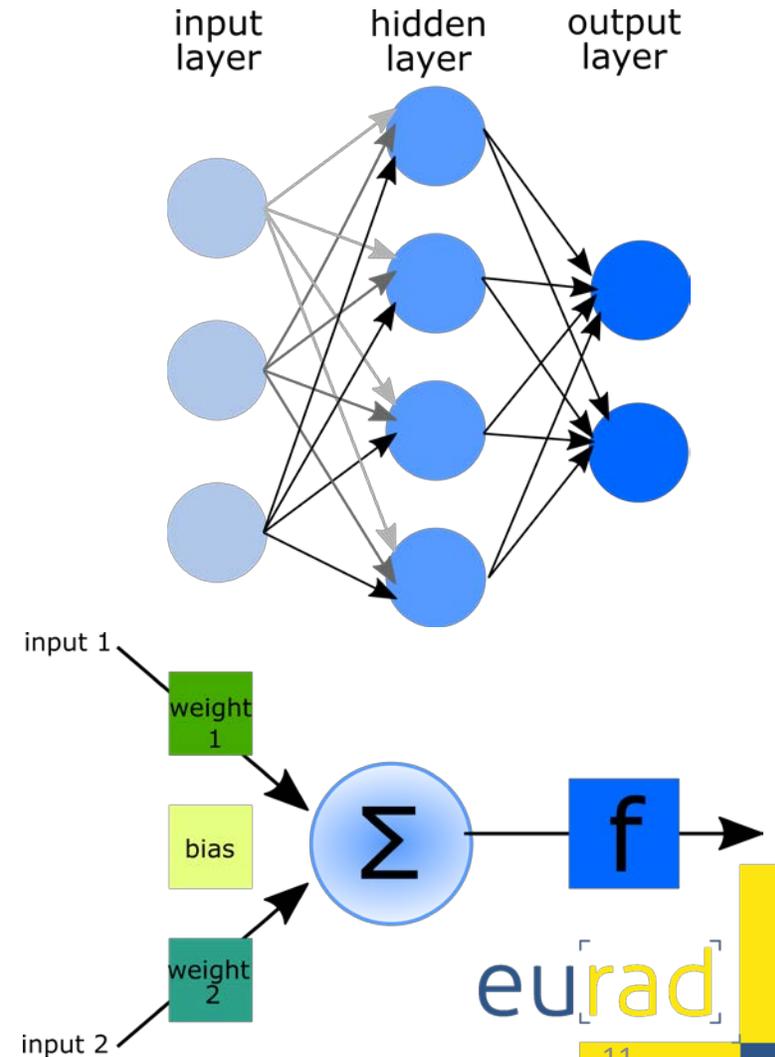
ARTIFICIAL INTELLIGENCE: NEURAL NETWORKS

- Principle:
 - Set up series of artificial neurons in a layered structure ~ brain
- Train:
 - Apply weights to the connections



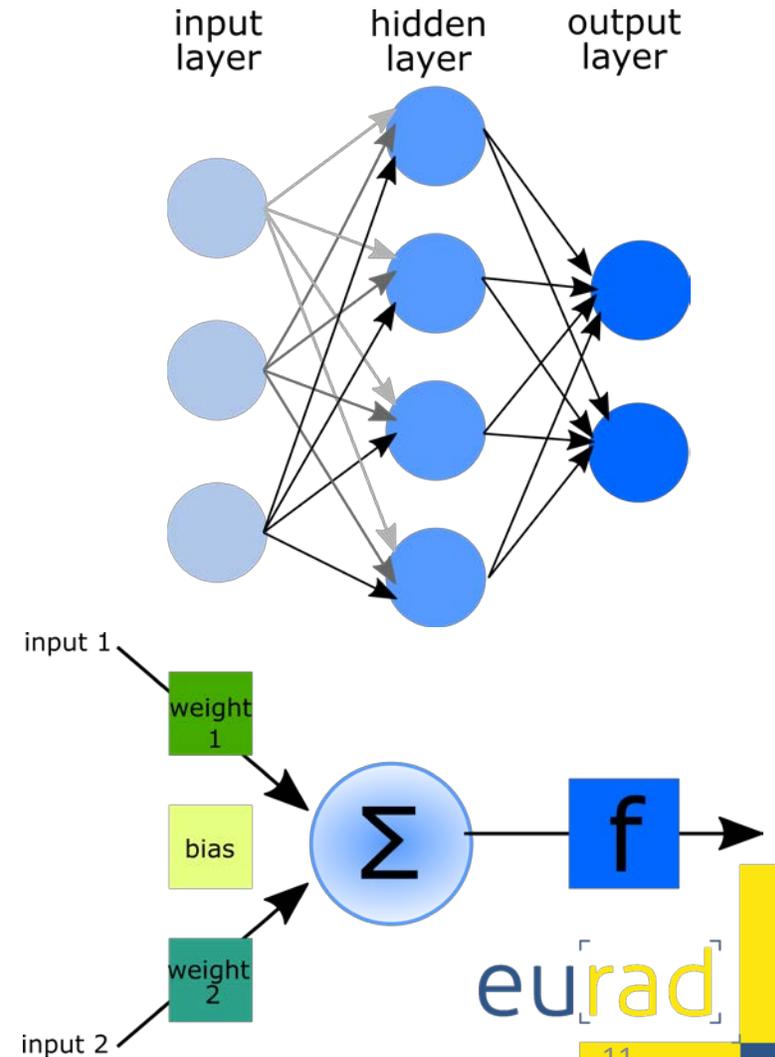
ARTIFICIAL INTELLIGENCE: NEURAL NETWORKS

- Principle:
 - Set up series of artificial neurons in a layered structure ~ brain
- Train:
 - Apply weights to the connections
- If conventional rule-based programming techniques don't work
- If several variables control the behavior of the system in a non-linear manner
- Software is commercially available



ARTIFICIAL INTELLIGENCE: NEURAL NETWORKS

- Principle:
 - Set up series of artificial neurons in a layered structure ~ brain
- Train:
 - Apply weights to the connections
- If conventional rule-based programming techniques don't work
- If several variables control the behavior of the system in a non-linear manner
- Software is commercially available
- No physical understanding of the processes & mechanisms
- Large data set needed

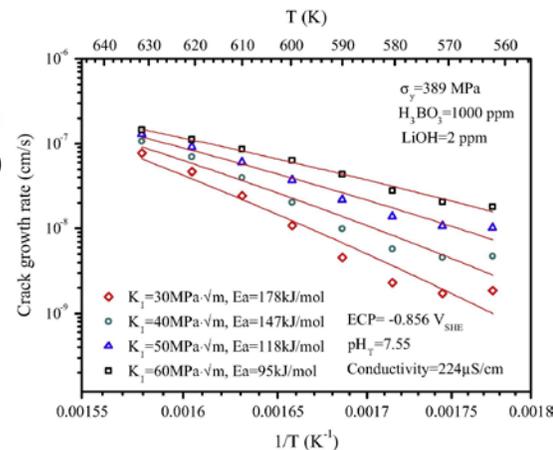


ARTIFICIAL INTELLIGENCE: NEURAL NETWORKS

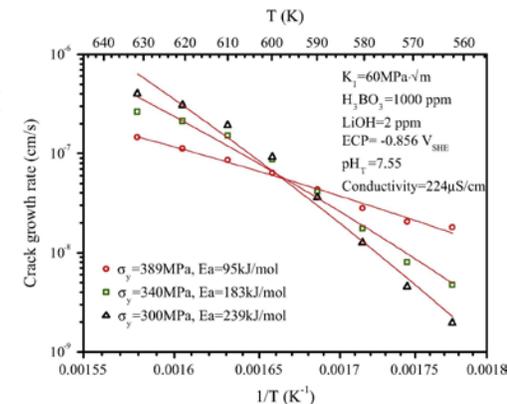
- When can it be used?
 - To map out the regions of stability and environmental conditions
 - To analyze data from monitoring sensors
 - To predict time of failure as a function of multiple variables

Effect of temperature on crack growth rate in Alloy 600 in PWR primary coolant

as a function of stress intensity factor



for different values of yield strength

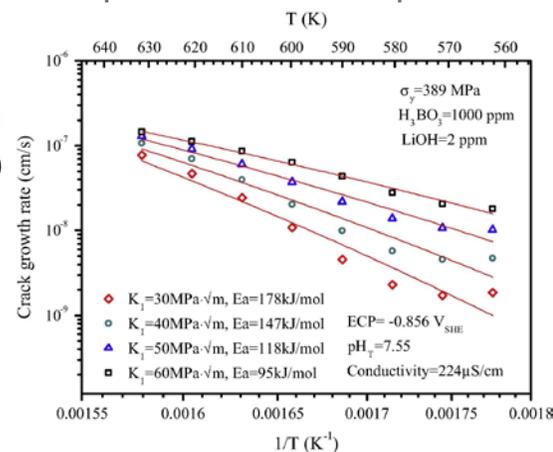


ARTIFICIAL INTELLIGENCE: NEURAL NETWORKS

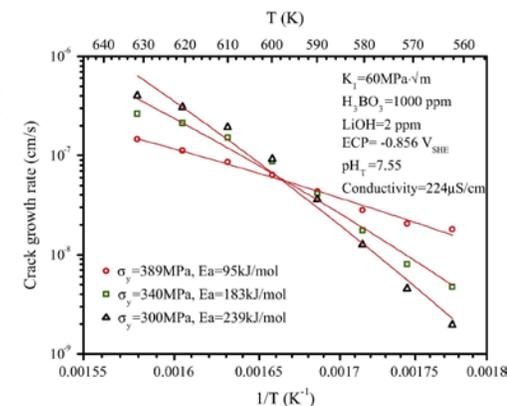
- When can it be used?
 - To map out the regions of stability and environmental conditions
 - To analyze data from monitoring sensors
 - To predict time of failure as a function of multiple variables
- Program of experimental research needed to generate data under disposal conditions:
 - Measurement of breakdown or pitting potentials using electrochemical techniques
 - Measurement of electrochemical noise
 - Execution of a matrix of experiments to map out conditions that lead to corrosion as a function of key variables

Effect of temperature on crack growth rate in Alloy 600 in PWR primary coolant

as a function of stress intensity factor



for different values of yield strength



MODELLING CORROSION PROCESSES CHALLENGES

- Numerous methods exist for making long-term predictions
 - 'Simple' extrapolation of empirical corrosion rates ↔ sophisticated numerical models

MODELLING CORROSION PROCESSES CHALLENGES

- Numerous methods exist for making long-term predictions
 - 'Simple' extrapolation of empirical corrosion rates ↔ sophisticated numerical models
- **! Justification of extremely long-term predictions**
 - How much confidence do we have in the estimated container lifetime?
 - How robust is the prediction?

MODELLING CORROSION PROCESSES CHALLENGES

- Numerous methods exist for making long-term predictions
 - 'Simple' extrapolation of empirical corrosion rates ↔ sophisticated numerical models
- **! Justification of extremely long-term predictions**
 - How much confidence do we have in the estimated container lifetime?
 - How robust is the prediction?
- **Confidence building by:**
 - Simplification of performance through repository design
 - Development of alternative models
 - For some container materials, the study of archaeological and natural analogs
 - Large scale, *in situ* tests under realistic repository conditions

Landscape of the excavated area of the Oda Castle remains



Roman iron nail (almost 2000 years old), courtesy of Bill Miller



MODELLING CORROSION PROCESSES CHALLENGES

- Numerous methods exist for making long-term predictions
 - 'Simple' extrapolation of empirical corrosion rates ↔ sophisticated numerical models
- **! Justification of extremely long-term predictions**
 - How much confidence do we have in the estimated container lifetime?
 - How robust is the prediction?
- **Confidence building by:**
 - Simplification of performance through repository design
 - Development of alternative models
 - For some container materials, the study of archaeological and natural analogs
 - Large scale, *in situ* tests under realistic repository conditions

➔ Generate sound mechanistic understanding of the underlying corrosion processes

Landscape of the excavated area of the Oda Castle remains



Roman iron nail (almost 2000 years old), courtesy of Bill Miller



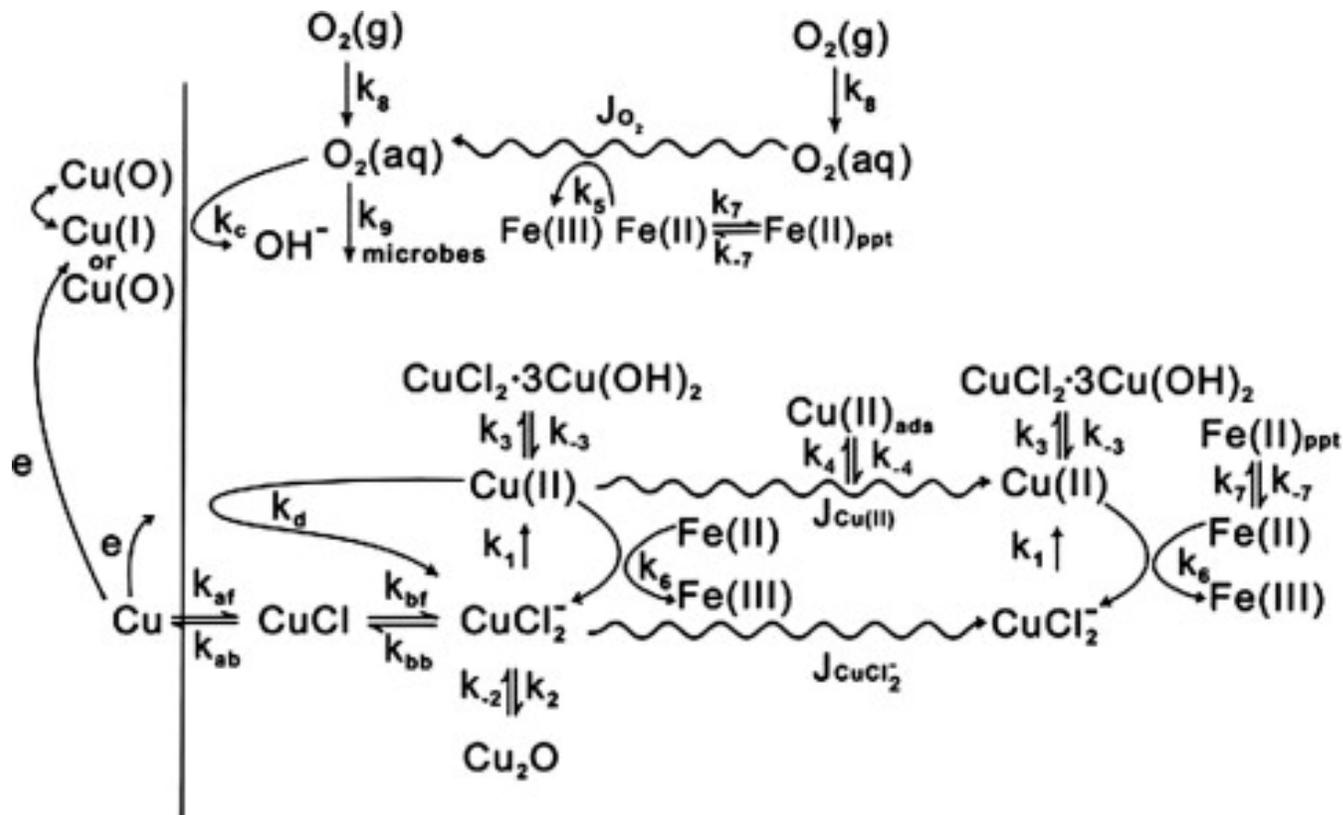


CONTENT

- Introduction
- **Copper container corrosion**
 - Reactive transport models in bentonite
 - Modeling sulfide fluxes
 - Modelling irradiation-induced corrosion
- Steel-bentonite models
- Integration of corrosion phenomena in performance assessments
- Performance assessments for copper-based canister corrosion
- Performance assessments for iron-based alloy canister corrosion

COPPER CONTAINER CORROSION

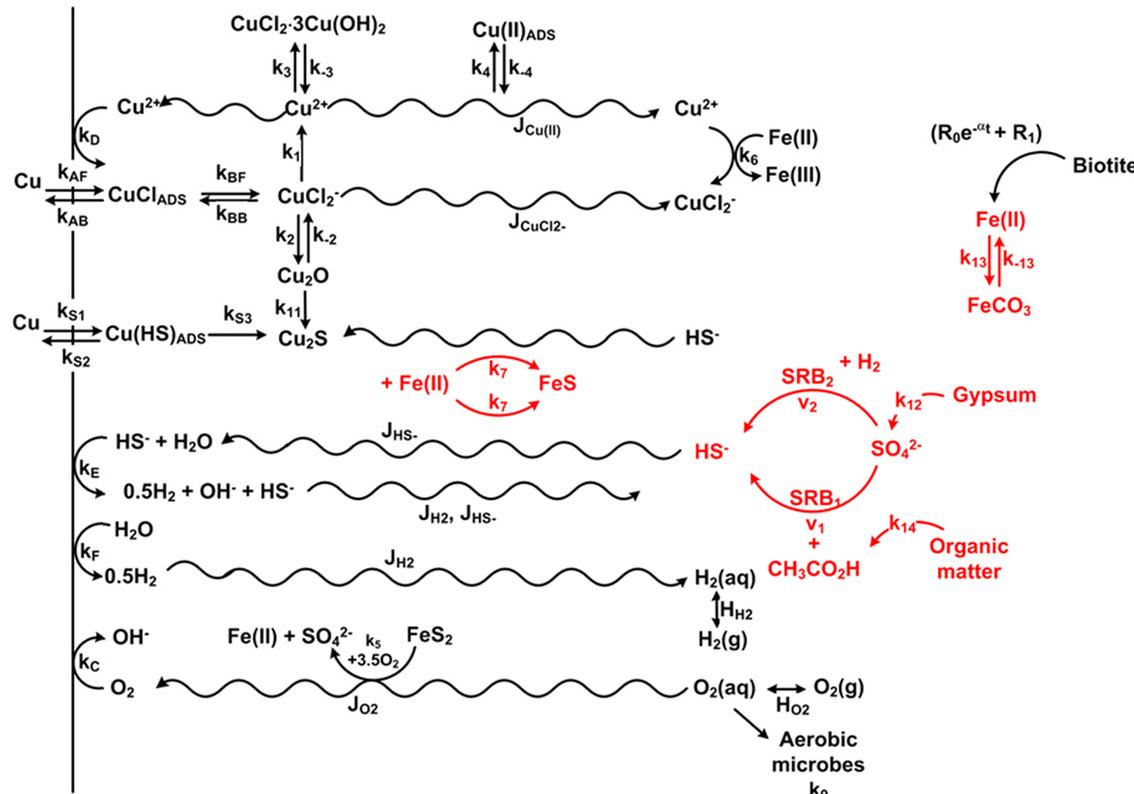
- Copper corrosion model (CCM)
 - Uniform copper corrosion focusing on Cl^- and O_2 transport-controlled corrosion



j : diffusive fluxes
 k : rate constants

COPPER CONTAINER CORROSION

- Copper corrosion model (CCM)
 - Uniform copper corrosion focusing on Cl^- and O_2 transport-controlled corrosion
 - Has been progressively updated, e.g. copper sulfide model (CSM)



microbial sulfate reduction in red

j : diffusive fluxes
 k : rate constants



COPPER CONTAINER CORROSION: REACTIVE TRANSPORT MODELS IN BENTONITE

- Limited mass transport rate in compacted bentonite → corrosion influenced by diffusion coefficient of dissolved species

COPPER CONTAINER CORROSION: REACTIVE TRANSPORT MODELS IN BENTONITE

- Limited mass transport rate in compacted bentonite → corrosion influenced by diffusion coefficient of dissolved species
- Mechanistic & empiric approaches for diffusion of ions through compacted bentonite
 1. Table of values of available porosity, effective diffusivity & distribution coefficients for 38 elements & oxidation states

COPPER CONTAINER CORROSION: REACTIVE TRANSPORT MODELS IN BENTONITE

- Limited mass transport rate in compacted bentonite → corrosion influenced by diffusion coefficient of dissolved species
- Mechanistic & empiric approaches for diffusion of ions through compacted bentonite
 1. Table of values of available porosity, effective diffusivity & distribution coefficients for 38 elements & oxidation states
 2. Empirical approach: available porosity ~ ionic strength external solution (0.01 - 1 mM) → Archie's law

COPPER CONTAINER CORROSION: REACTIVE TRANSPORT MODELS IN BENTONITE

- Limited mass transport rate in compacted bentonite → corrosion influenced by diffusion coefficient of dissolved species
- Mechanistic & empiric approaches for diffusion of ions through compacted bentonite
 1. Table of values of available porosity, effective diffusivity & distribution coefficients for 38 elements & oxidation states
 2. Empirical approach: available porosity ~ ionic strength external solution (0.01 - 1 mM) → Archie's law
 3. Donnan equilibrium model: single interlayer porosity with net positive charge to compensate the structural negative charge of the smectite sheets → anion exclusion at clay-water interface

COPPER CONTAINER CORROSION: REACTIVE TRANSPORT MODELS IN BENTONITE

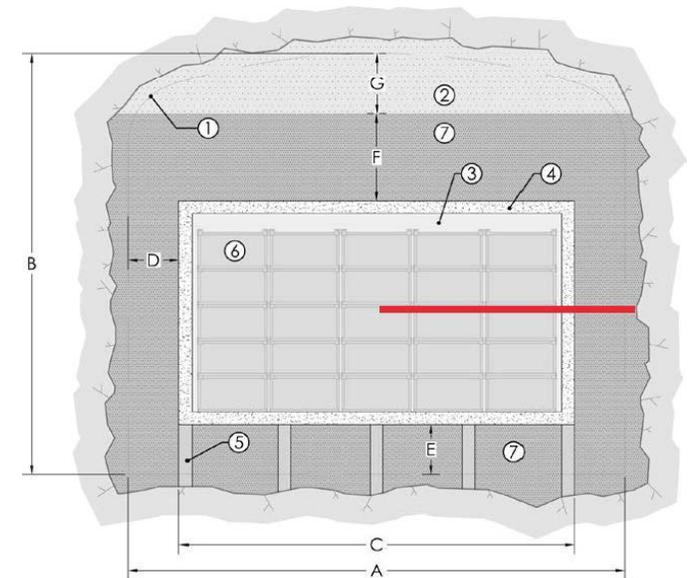
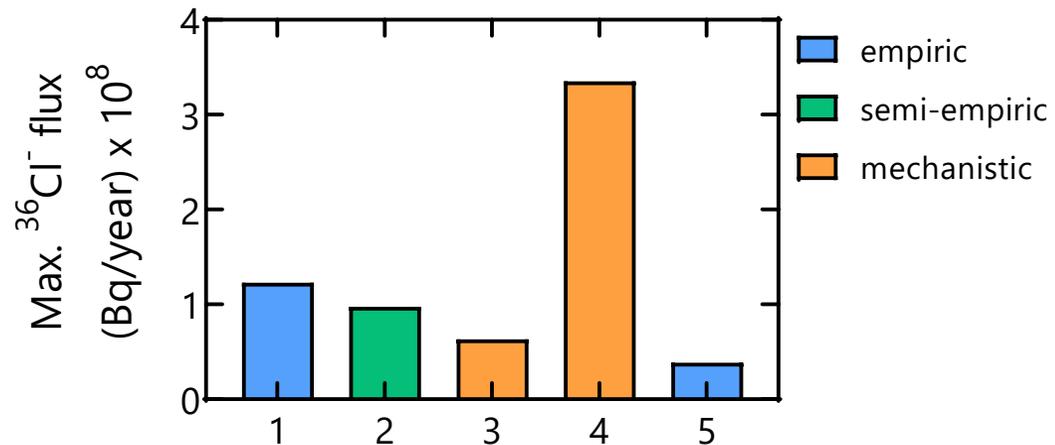
- Limited mass transport rate in compacted bentonite → corrosion influenced by diffusion coefficient of dissolved species
- Mechanistic & empiric approaches for diffusion of ions through compacted bentonite
 1. Table of values of available porosity, effective diffusivity & distribution coefficients for 38 elements & oxidation states
 2. Empirical approach: available porosity ~ ionic strength external solution (0.01 - 1 mM) → Archie's law
 3. Donnan equilibrium model: single interlayer porosity with net positive charge to compensate the structural negative charge of the smectite sheets → anion exclusion at clay-water interface
 4. Multi-porosity model → three porosity types:
 - Free
 - Electrical double layer: size is coupled with ionic strength of pore water (computationally demanding)
 - Interlayer: inaccessible to anions

COPPER CONTAINER CORROSION: REACTIVE TRANSPORT MODELS IN BENTONITE

- Limited mass transport rate in compacted bentonite → corrosion influenced by diffusion coefficient of dissolved species
- Mechanistic & empiric approaches for diffusion of ions through compacted bentonite
 1. Table of values of available porosity, effective diffusivity & distribution coefficients for 38 elements & oxidation states
 2. Empirical approach: available porosity ~ ionic strength external solution (0.01 - 1 mM) → Archie's law
 3. Donnan equilibrium model: single interlayer porosity with net positive charge to compensate the structural negative charge of the smectite sheets → anion exclusion at clay-water interface
 4. Multi-porosity model → three porosity types:
 - Free
 - Electrical double layer: size is coupled with ionic strength of pore water (computationally demanding)
 - Interlayer: inaccessible to anions
 5. Simplified multi-porosity model
 - Effective diffusion coefficient as a function of bentonite dry density & ionic strength
 - Interlayer porosity is devoid of anions

VALIDATION OF THE MODELS WITH $^{36}\text{Cl}^-$ IN THE BHA VAULT OF THE SFL REPOSITORY (SE)

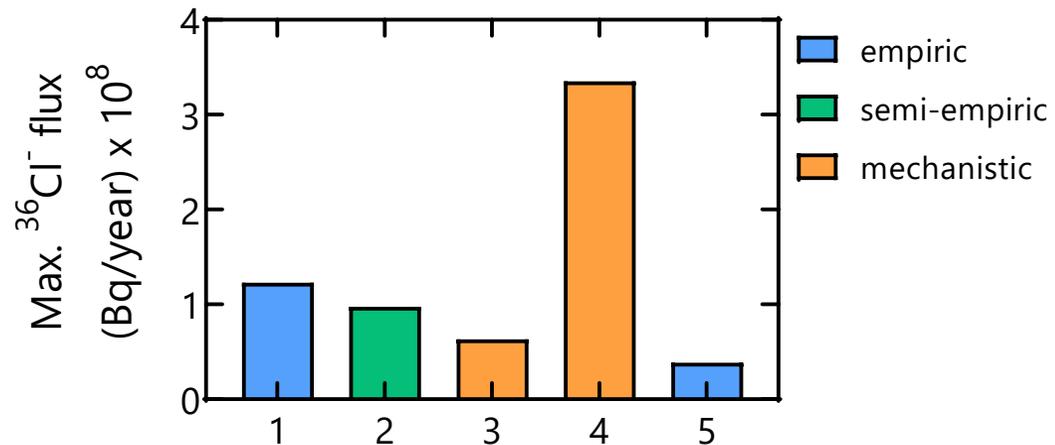
- Implemented in Comsol Multiphysics version 5.3



Position of the 2D studied domain (in red) referred to the **2D cross-sectional** view of the BHA vault. 1) Theoretical tunnel contour. 2) Bentonite pellets. 3) Grout. 4) Concrete structure for the operating period (0.5 meter). 5) Granite pillars. 6) Waste containers. 7) Bentonite blocks. Approximate dimensions: $A = 20.6 \text{ m}$, $B = 18.5 \text{ m}$, $C = 16 \text{ m}$, $D = 2.3 \text{ m}$, $E = 2.4 \text{ m}$, $F = 4 \text{ m}$, $G = 3.7 \text{ m}$.

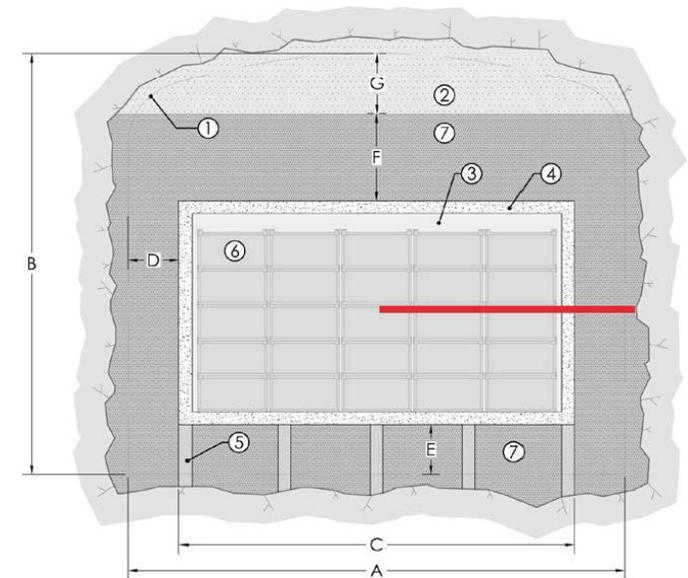
VALIDATION OF THE MODELS WITH $^{36}\text{Cl}^-$ IN THE BHA VAULT OF THE SFL REPOSITORY (SE)

- Implemented in Comsol Multiphysics version 5.3



Lack of detailed description of several necessary parameters

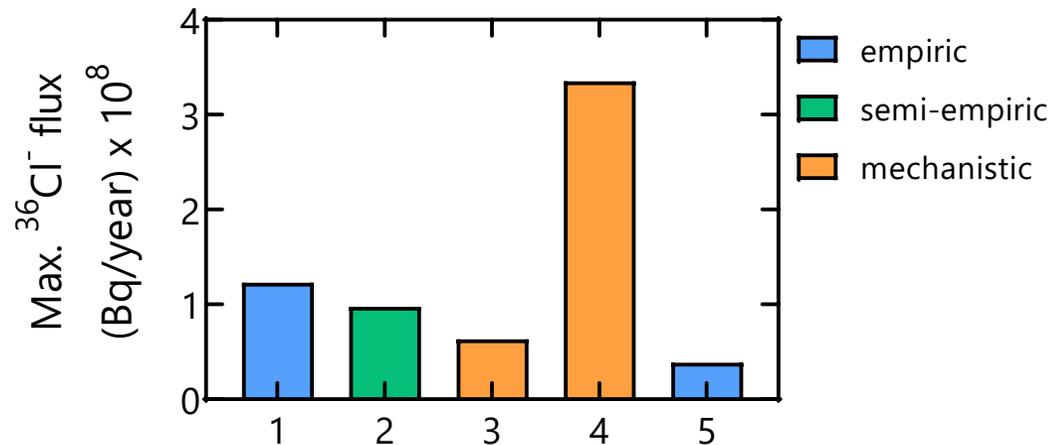
overestimation



Position of the 2D studied domain (in red) referred to the **2D cross-sectional** view of the BHA vault. 1) Theoretical tunnel contour. 2) Bentonite pellets. 3) Grout. 4) Concrete structure for the operating period (0.5 meter). 5) Granite pillars. 6) Waste containers. 7) Bentonite blocks. Approximate dimensions: $A = 20.6\text{ m}$, $B = 18.5\text{ m}$, $C = 16\text{ m}$, $D = 2.3\text{ m}$, $E = 2.4\text{ m}$, $F = 4\text{ m}$, $G = 3.7\text{ m}$.

VALIDATION OF THE MODELS WITH $^{36}\text{Cl}^-$ IN THE BHA VAULT OF THE SFL REPOSITORY (SE)

- Implemented in Comsol Multiphysics version 5.3

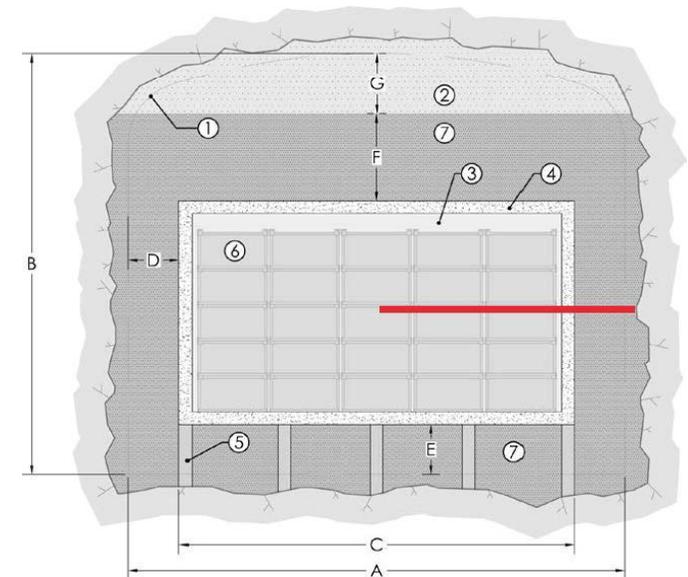


Lack of detailed description of several necessary parameters

overestimation

Most reliable because parameters obtained specifically for chloride diffusion through bentonite.

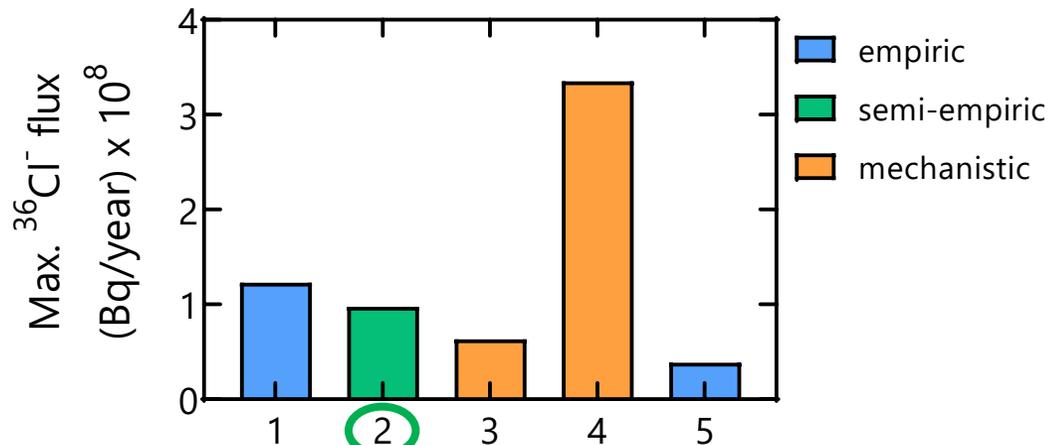
But not sensitive to the ionic strength of background solution



Position of the 2D studied domain (in red) referred to the **2D cross-sectional** view of the BHA vault. 1) Theoretical tunnel contour. 2) Bentonite pellets. 3) Grout. 4) Concrete structure for the operating period (0.5 meter). 5) Granite pillars. 6) Waste containers. 7) Bentonite blocks. Approximate dimensions: A = 20.6 m, B = 18.5 m, C = 16 m, D = 2.3 m, E = 2.4 m, F = 4 m, G = 3.7 m.

VALIDATION OF THE MODELS WITH $^{36}\text{Cl}^-$ IN THE BHA VAULT OF THE SFL REPOSITORY (SE)

- Implemented in Comsol Multiphysics version 5.3



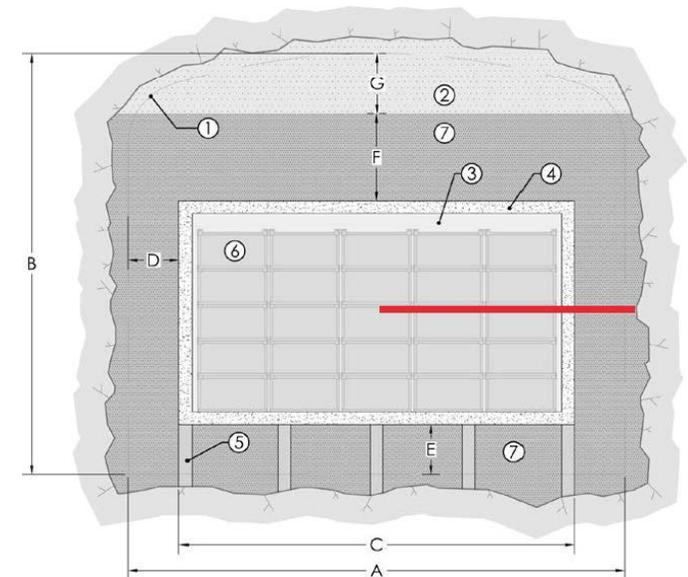
Lack of detailed description of several necessary parameters

overestimation

Most reliable because parameters obtained specifically for chloride diffusion through bentonite.

But not sensitive to the ionic strength of background solution

If ionic strength differs significantly from the base Case value of value used here



Position of the 2D studied domain (in red) referred to the **2D cross-sectional** view of the BHA vault. 1) Theoretical tunnel contour. 2) Bentonite pellets. 3) Grout. 4) Concrete structure for the operating period (0.5 meter). 5) Granite pillars. 6) Waste containers. 7) Bentonite blocks. Approximate dimensions: A = 20.6 m, B = 18.5 m, C = 16 m, D = 2.3 m, E = 2.4 m, F = 4 m, G = 3.7 m.

COPPER CONTAINER CORROSION: REACTIVE TRANSPORT MODELS IN BENTONITE

- Copper corrosion in container of KBS-3V repository
 - Dual continuum approaches:
 - Reactive transport modelling iCP framework: interface coupling Comsol Multiphysics & PhreeqC
 - Adapted PFLOTRAN: Nernst-Planck equation accounting for immobile charge & Donnan equilibrium → allowed a coupled transport simulation of all components while preserving different diffusivities depending on their charge & concentration of the electrolyte

COPPER CONTAINER CORROSION: REACTIVE TRANSPORT MODELS IN BENTONITE

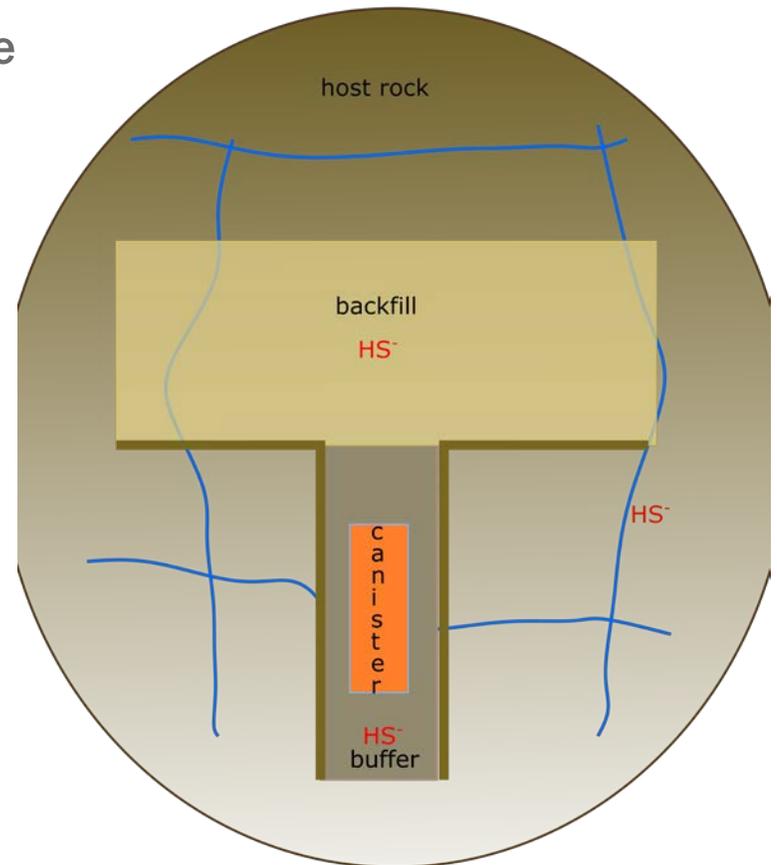
- Copper corrosion in container of KBS-3V repository
 - Dual continuum approaches:
 - Reactive transport modelling iCP framework: interface coupling Comsol Multiphysics & PhreeqC
 - Adapted PFLOTRAN: Nernst-Planck equation accounting for immobile charge & Donnan equilibrium → allowed a coupled transport simulation of all components while preserving different diffusivities depending on their charge & concentration of the electrolyte
 - Comparison with traditional approaches:
 - Slightly reduced mackinawite precipitation
 - Increased sulfide fluxes reaching the container
 - Did not account for barriers outside bentonite buffer

COPPER CONTAINER CORROSION: REACTIVE TRANSPORT MODELS IN BENTONITE

- Copper corrosion in container of KBS-3V repository
 - Dual continuum approaches:
 - Reactive transport modelling iCP framework: interface coupling Comsol Multiphysics & PhreeqC
 - Adapted PFLOTRAN: Nernst-Planck equation accounting for immobile charge & Donnan equilibrium → allowed a coupled transport simulation of all components while preserving different diffusivities depending on their charge & concentration of the electrolyte
 - Comparison with traditional approaches:
 - Slightly reduced mackinawite precipitation
 - Increased sulfide fluxes reaching the container
 - **Did not account for barriers outside bentonite buffer**
 - Further research is needed into the effect of the Donnan equilibrium

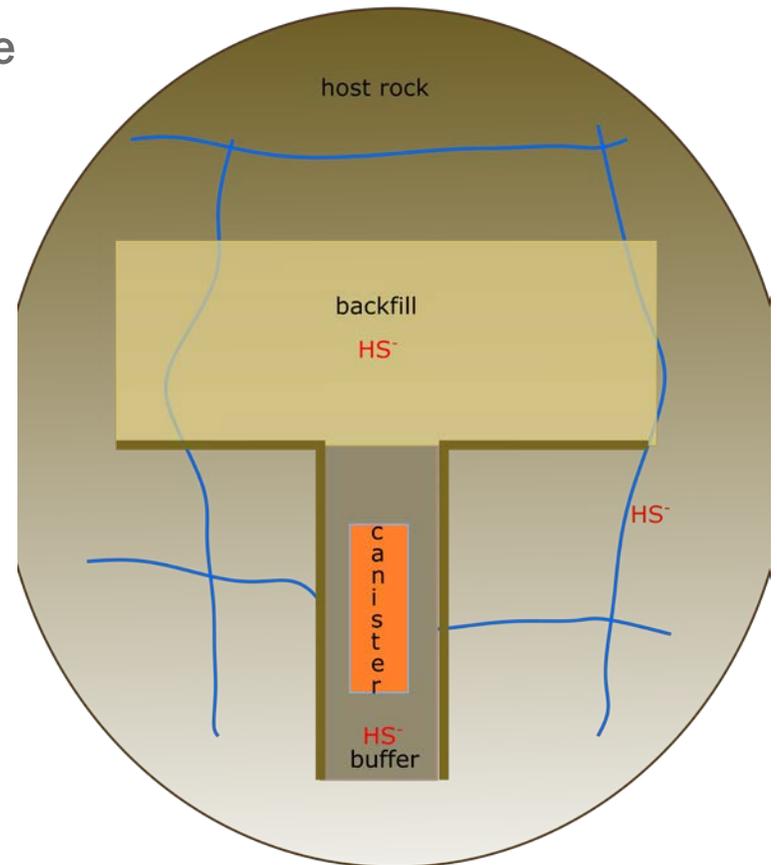
MODELLING OF SULFIDE FLUXES

- Sulfide: main corroding agent for copper containers in anoxic phase



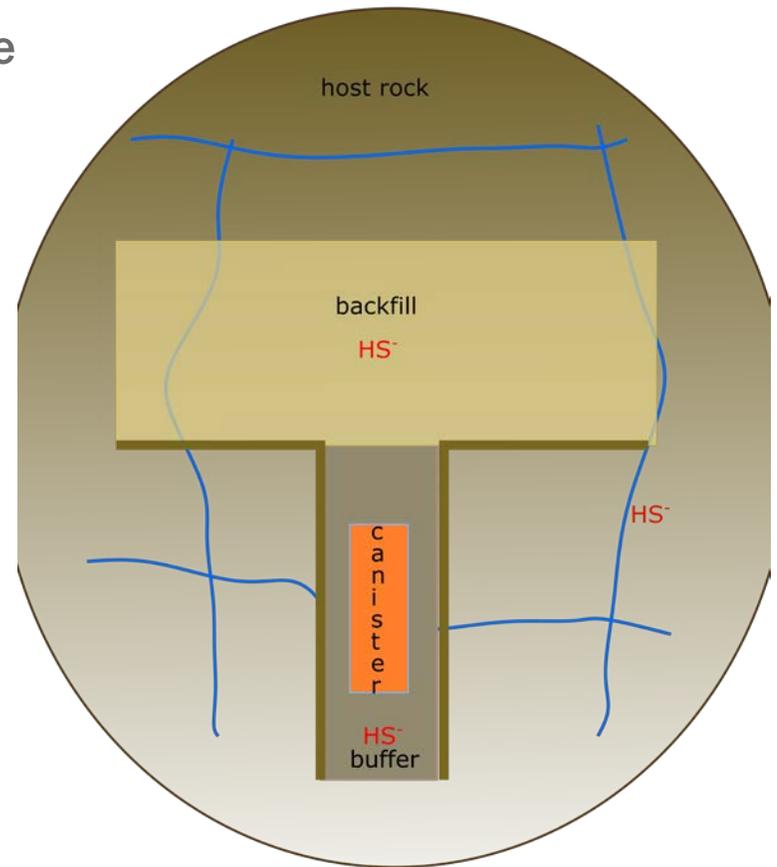
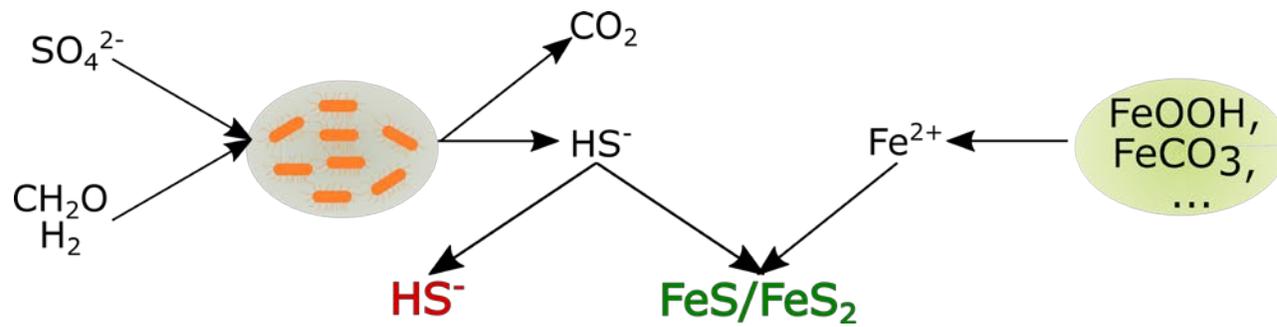
MODELLING OF SULFIDE FLUXES

- Sulfide: main corroding agent for copper containers in anoxic phase
- Sulfate-bearing waters and SRB ↔ dissolution of ferrous minerals



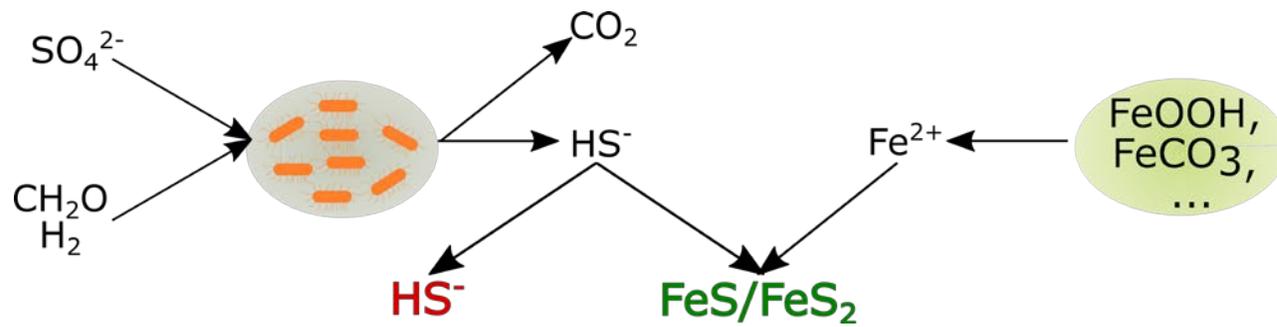
MODELLING OF SULFIDE FLUXES

- Sulfide: main corroding agent for copper containers in anoxic phase
- **Sulfate-bearing waters and SRB** ↔ **dissolution of ferrous minerals**

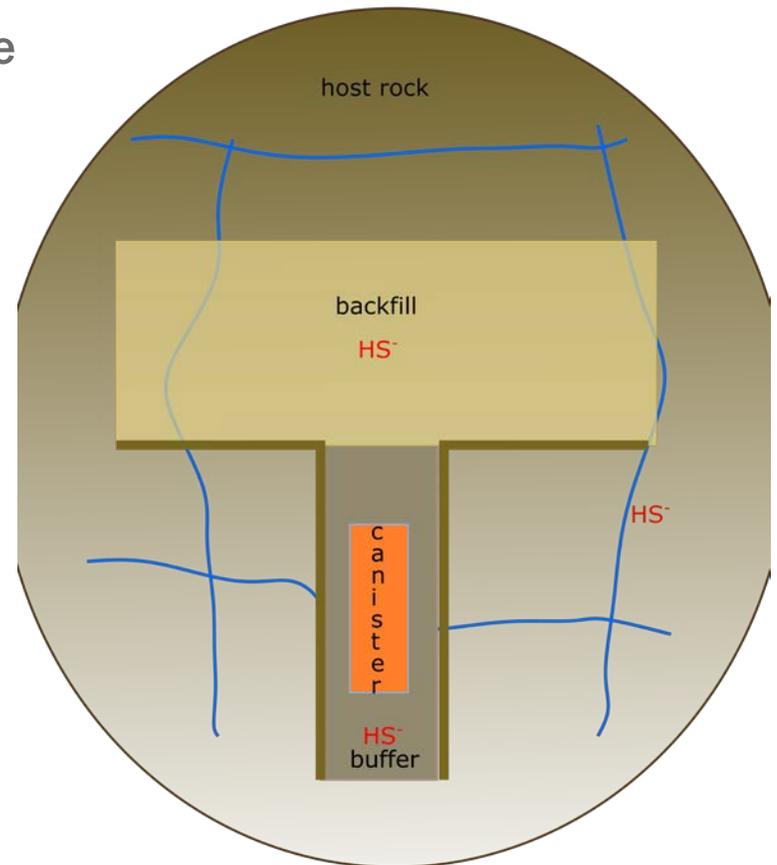


MODELLING OF SULFIDE FLUXES

- Sulfide: main corroding agent for copper containers in anoxic phase
- **Sulfate-bearing waters and SRB** ↔ **dissolution of ferrous minerals**

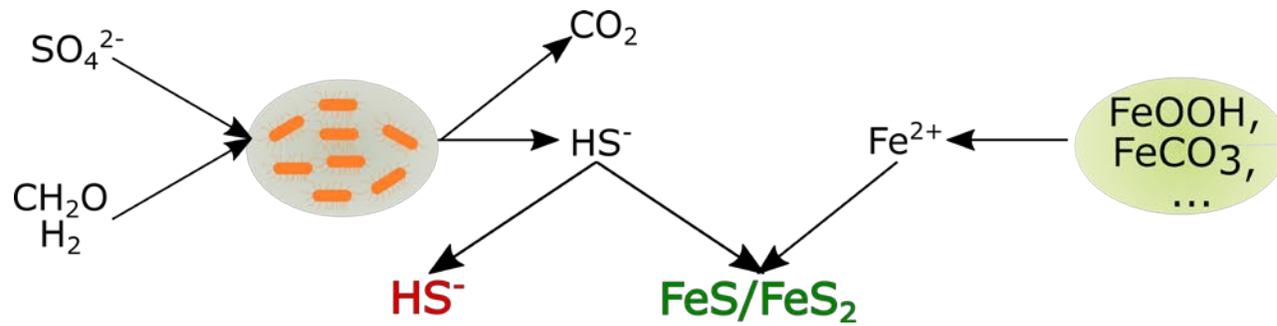


- Levels foreseen too low for significant corrosion to occur

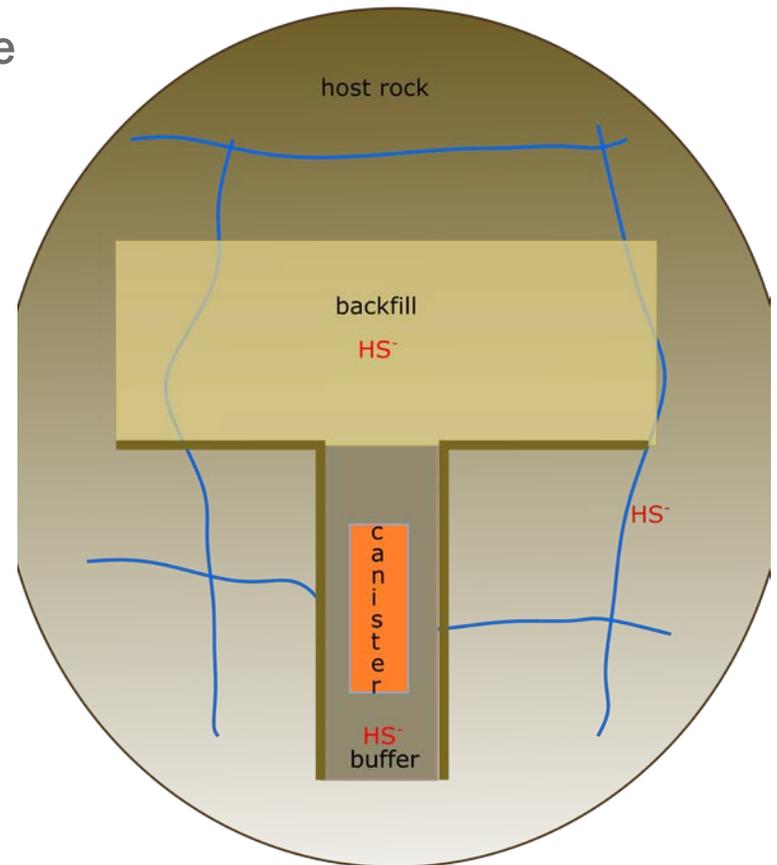


MODELLING OF SULFIDE FLUXES

- Sulfide: main corroding agent for copper containers in anoxic phase
- **Sulfate-bearing waters and SRB** ↔ **dissolution of ferrous minerals**

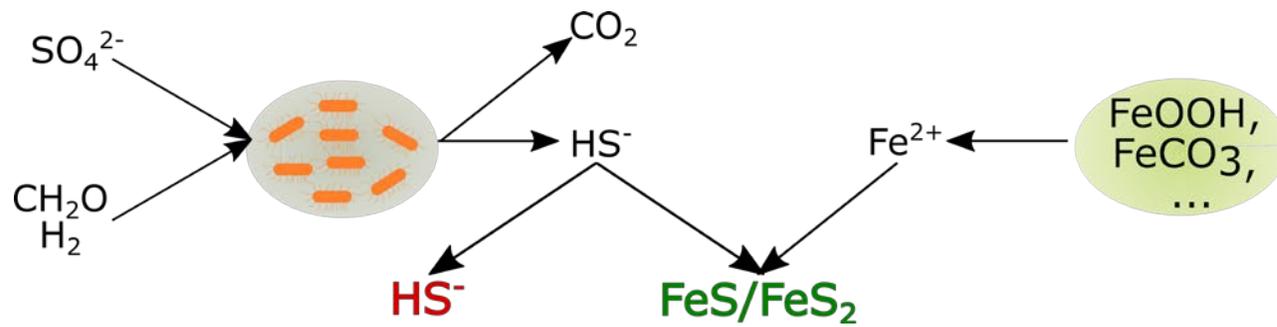


- Levels foreseen too low for significant corrosion to occur
- But, no hypothetical early transient stage was considered



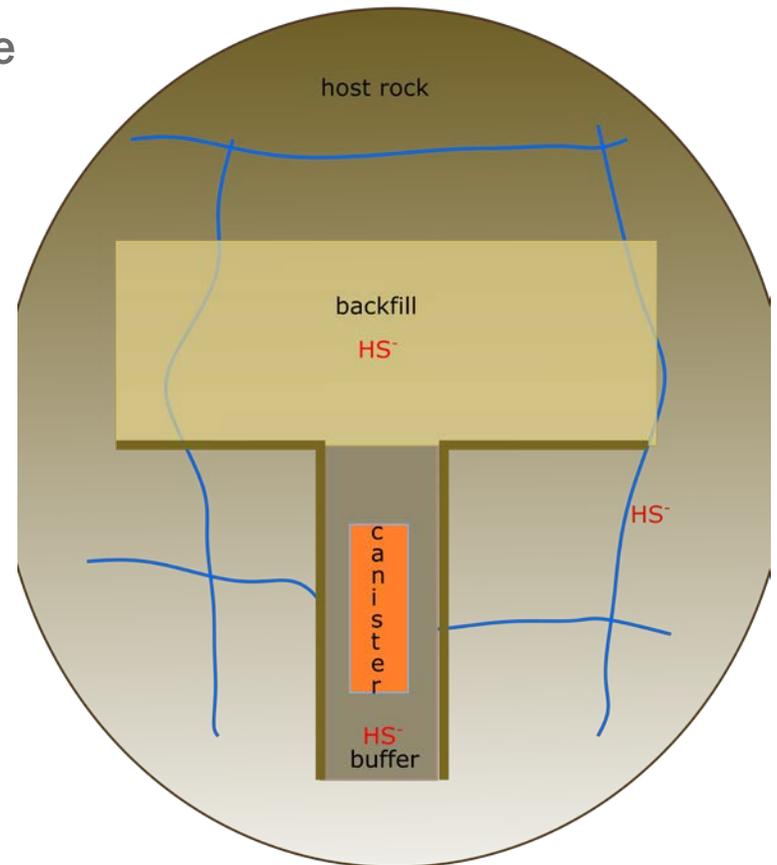
MODELLING OF SULFIDE FLUXES

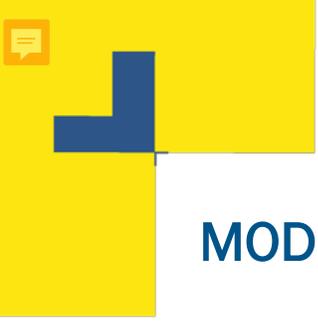
- Sulfide: main corroding agent for copper containers in anoxic phase
- **Sulfate-bearing waters and SRB** ↔ **dissolution of ferrous minerals**



- Levels foreseen too low for significant corrosion to occur
- But, no hypothetical early transient stage was considered

Possible when relevant sulfide sources together with limited iron availability





MODELLING OF SULFIDE FLUXES IN THE EARLY TRANSIENT STAGE (2 PHASE FLOW)

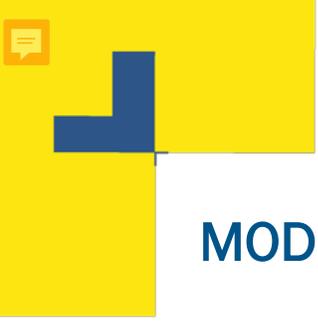
- Geochemistry & thermal & hydrological conditions should be considered
- Effect of two-phase flow:
 - High temperatures at container surface & heat dissipation in near field → significant vapor & liquid fluxes
 - Motion of trapped gas bubbles

MODELLING OF SULFIDE FLUXES IN THE EARLY TRANSIENT STAGE (2 PHASE FLOW)

- Geochemistry & thermal & hydrological conditions should be considered
 - Effect of two-phase flow:
 - High temperatures at container surface & heat dissipation in near field → significant vapor & liquid fluxes
 - Motion of trapped gas bubbles
- irregular fluxes in the short-term ↔ modelling transport under stable saturated conditions in anoxic period

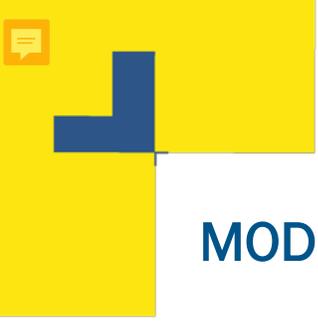
MODELLING OF SULFIDE FLUXES IN THE EARLY TRANSIENT STAGE (2 PHASE FLOW)

- Geochemistry & thermal & hydrological conditions should be considered
 - Effect of two-phase flow:
 - High temperatures at container surface & heat dissipation in near field → significant vapor & liquid fluxes
 - Motion of trapped gas bubbles
- irregular fluxes in the short-term ↔ modelling transport under stable saturated conditions in anoxic period
- **Gaseous H₂S**
 - Can be transported in during unsaturated period
 - Highly corrosive also in dry atmospheres



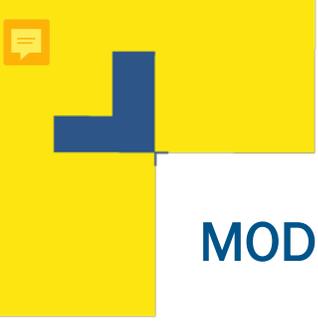
MODELLING OF MICROBIAL SULFIDE PRODUCTION

- Evolution in time:
 - 2006 assumed that in the initial phase:
 - high temperature + lack of water → limited microbial presence & activity in near-field
 - mackinawite precipitation in buffer and backfill → low sulfide concentrations reaching the container



MODELLING OF MICROBIAL SULFIDE PRODUCTION

- Evolution in time:
 - 2006 assumed that in the initial phase:
 - high temperature + lack of water → limited microbial presence & activity in near-field
 - mackinawite precipitation in buffer and backfill → low sulfide concentrations reaching the container
 - 2008 CCM model included protective effect on corrosion from oxygen consumption by aerobic microbes



MODELLING OF MICROBIAL SULFIDE PRODUCTION

- Evolution in time:
 - 2006 assumed that in the initial phase:
 - high temperature + lack of water → limited microbial presence & activity in near-field
 - mackinawite precipitation in buffer and backfill → low sulfide concentrations reaching the container
 - 2008 CCM model included protective effect on corrosion from oxygen consumption by aerobic microbes
 - 2010 updated CCM model (CCM-MIC) which included:
 - Microbial sulfide production
 - Mass balance for each organic agent

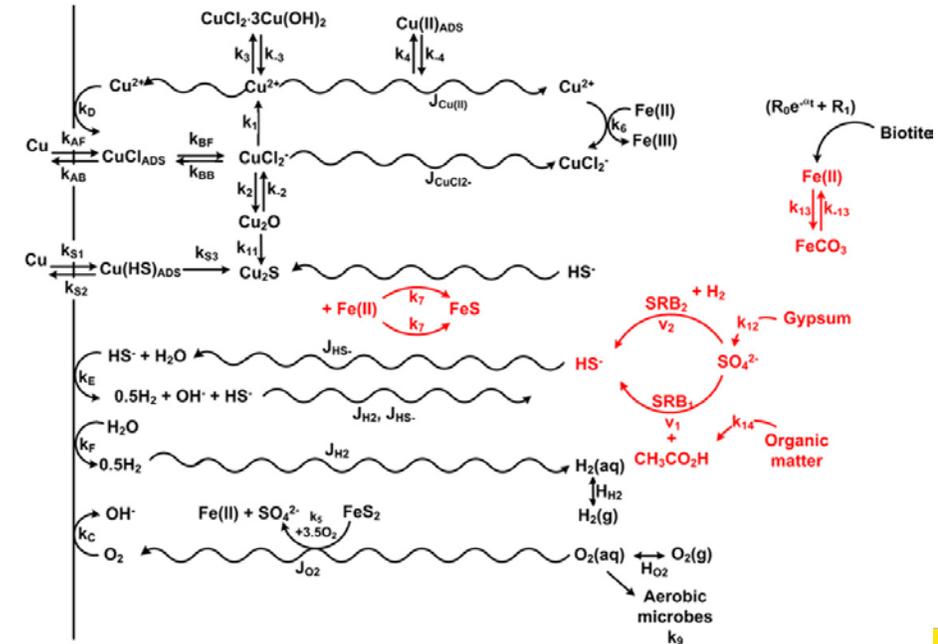
MODELLING OF MICROBIAL SULFIDE PRODUCTION

- Evolution in time:
 - 2006 assumed that in the initial phase:
 - high temperature + lack of water → limited microbial presence & activity in near-field
 - mackinawite precipitation in buffer and backfill → low sulfide concentrations reaching the container
 - 2008 CCM model included protective effect on corrosion from oxygen consumption by aerobic microbes
 - 2010 updated CCM model (CCM-MIC) which included:
 - Microbial sulfide production
 - Mass balance for each organic agent
 - 2017 experimental quantification of the kinetic rate constant for microbial sulfate reduction

MODELLING OF MICROBIAL SULFIDE PRODUCTION

- Evolution in time:

- 2006 assumed that in the initial phase:
 - high temperature + lack of water → limited microbial presence & activity in near-field
 - mackinawite precipitation in buffer and backfill → low sulfide concentrations reaching the container
- 2008 CCM model included protective effect on corrosion from oxygen consumption by aerobic microbes
- 2010 updated CCM model (CCM-MIC) which included:
 - Microbial sulfide production
 - Mass balance for each organic agent
- 2017 experimental quantification of the kinetic rate constant for microbial sulfate reduction
- 2021 update of CSM model including organotrophic and chemotrophic sulfate reduction
 - Outcome is dependent on amount of organic material, gypsum and reactive Fe^{2+}
- 2021 3D reactive transport sulfide model → kinetic Monod model for SRB
 - Max rate constant 5×10^{-5} and 10^{-4} mol sulphide/L water



MODELLING THE INTERACTION OF SULFIDE WITH FE-BEARING MINERAL PHASE

- Extreme low solubility of pyrite → rate constant for anaerobic dissolution of pyrite excluded from CSM

MODELLING THE INTERACTION OF SULFIDE WITH FE-BEARING MINERAL PHASE

- Extreme low solubility of pyrite → rate constant for anaerobic dissolution of pyrite excluded from CSM
- Wider description of sulfide – ferrous minerals interaction
 - Biotite ($K(\text{Mg}_{0.6-1.8}\text{Fe}^{2+}_{2.4-1.2})(\text{Si}_3\text{Al})\text{O}_{10}(\text{OH},\text{F})_2$):
 - Initially present in backfill & rock layers
 - Temp-dependent dissolution releasing Fe^{2+}
 - Pyrite (FeS_2):
 - Expected to be fully oxidized during aerobic phase
 - Iron carbonate (FeCO_3):
 - Initially present in buffer & backfill materials
 - Precipitates reversibly in the presence of excess Fe^{2+}
 - Mackinawite (FeS):
 - Precipitates if dissolved Fe^{2+} and HS^- concentrations exceed the value of the solubility product

MODELLING THE INTERACTION OF SULFIDE WITH FE-BEARING MINERAL PHASE

- Extreme low solubility of pyrite → rate constant for anaerobic dissolution of pyrite excluded from CSM

- Wider description of sulfide – ferrous minerals interaction

- Biotite ($K(Mg_{0.6-1.8}Fe^{2+}_{2.4-1.2})(Si_3Al)O_{10}(OH,F)_2$):

- Initially present in backfill & rock layers
- Temp-dependent dissolution releasing Fe^{2+}

- Pyrite (FeS_2):

- Expected to be fully oxidized during aerobic phase

- Iron carbonate ($FeCO_3$):

- Initially present in buffer & backfill materials
- Precipitates reversibly in the presence of excess Fe^{2+}

- Mackinawite (FeS):

- Precipitates if dissolved Fe^{2+} and HS^- concentrations exceed the value of the solubility product

+ conditions in KBS-3 repository: corrosion
< 10 μm after 1 million years

MODELLING THE INTERACTION OF SULFIDE WITH FE-BEARING MINERAL PHASE

- Extreme low solubility of pyrite → rate constant for anaerobic dissolution of pyrite excluded from CSM

- Wider description of sulfide – ferrous minerals interaction

- Biotite ($K(Mg_{0.6-1.8}Fe^{2+}_{2.4-1.2})(Si_3Al)O_{10}(OH,F)_2$):

- Initially present in backfill & rock layers
- Temp-dependent dissolution releasing Fe^{2+}

- Pyrite (FeS_2):

- Expected to be fully oxidized during aerobic phase

- Iron carbonate ($FeCO_3$):

- Initially present in buffer & backfill materials
- Precipitates reversibly in the presence of excess Fe^{2+}

- Mackinawite (FeS):

- Precipitates if dissolved Fe^{2+} and HS^- concentrations exceed the value of the solubility product

+ conditions in KBS-3 repository: corrosion
< 10 μm after 1 million years

Similar outcome with hydrogeochemical
model using PhreeqC

MODELLING THE INTERACTION OF SULFIDE WITH FE-BEARING MINERAL PHASE

- Extreme low solubility of pyrite → rate constant for anaerobic dissolution of pyrite excluded from CSM

- Wider description of sulfide – ferrous minerals interaction

- Biotite ($K(Mg_{0.6-1.8}Fe^{2+}_{2.4-1.2})(Si_3Al)O_{10}(OH,F)_2$):

- Initially present in backfill & rock layers
- Temp-dependent dissolution releasing Fe^{2+}

- Pyrite (FeS_2):

- Expected to be fully oxidized during aerobic phase

- Iron carbonate ($FeCO_3$):

- Initially present in buffer & backfill materials
- Precipitates reversibly in the presence of excess Fe^{2+}

- Mackinawite (FeS):

- Precipitates if dissolved Fe^{2+} and HS^- concentrations exceed the value of the solubility product

+ conditions in KBS-3 repository: corrosion
< 10 μm after 1 million years

Similar outcome with hydrogeochemical
model using PhreeqC

- 3D reactive transport model for safety case of the spent fuel repository in Olkiluoto (Finland):

- Main sources are ferric (oxyhydr)oxides

- $Fe^{3+} + HS^- \rightarrow S + polysulfides + Fe^{2+} \rightarrow FeS$

MODELLING IRRADIATION-INDUCED CORROSION

- Radiolysis → molecular & radical oxidants/reductants with concentration dependent on:
 - Type of radiation
 - Dose
 - Dose rate
 - Composition of aqueous solution
 - Material of fabrication
 - Wall thickness of container

<https://www.mcpa-software.com>

MODELLING IRRADIATION-INDUCED CORROSION

- Radiolysis → molecular & radical oxidants/reductants with concentration dependent on:
 - Type of radiation
 - Dose
 - Dose rate
 - Composition of aqueous solution
 - Material of fabrication
 - Wall thickness of container
 - **MAKSIMA-CHEMIST:**
 - full set of chemical reactions describing radiation chemistry of water + reaction of Cu oxidized by O₂
 - O₂ produced by
 - Radiolysis of water
 - Catalytic decomposition of radiolytically produced H₂O₂ on the oxide surface
- } Account for the observed corrosion in the experiment
- **FACSIMILE** → modelling complex reaction kinetics (<https://www.mcpa-software.com>)

MODELLING IRRADIATION-INDUCED CORROSION

- Radiolysis → molecular & radical oxidants/reductants with concentration dependent on:
 - Type of radiation
 - Dose
 - Dose rate
 - Composition of aqueous solution
 - Material of fabrication
 - Wall thickness of container
 - **MAKSIMA-CHEMIST:**
 - full set of chemical reactions describing radiation chemistry of water + reaction of Cu oxidized by O₂
 - O₂ produced by
 - Radiolysis of water
 - Catalytic decomposition of radiolytically produced H₂O₂ on the oxide surface
- } Account for the observed corrosion in the experiment
- FACSIMILE → modelling complex reaction kinetics (<https://www.mcpa-software.com>)
 - SIMFONY → temporal evolution of O₂, H₂, and H₂O₂ by γ-radiation

MODELLING IRRADIATION-INDUCED CORROSION

- Radiolysis → molecular & radical oxidants/reductants with concentration dependent on:
 - Type of radiation
 - Dose
 - Dose rate
 - Composition of aqueous solution
 - Material of fabrication
 - Wall thickness of container
 - **MAKSIMA-CHEMIST:**
 - full set of chemical reactions describing radiation chemistry of water + reaction of Cu oxidized by O₂
 - O₂ produced by
 - Radiolysis of water
 - Catalytic decomposition of radiolytically produced H₂O₂ on the oxide surface
- } Account for the observed corrosion in the experiment
- FACSIMILE → modelling complex reaction kinetics (<https://www.mcpa-software.com>)
 - SIMFONY → temporal evolution of O₂, H₂, and H₂O₂ by γ-radiation
 - Comsol Multiphysics → complete set of kinetic reactions dealing with recombination of H₂O radiolysis species

CONTENT

- Introduction
- Copper container corrosion
 - Reactive transport models in bentonite
 - Modeling sulfide fluxes
 - Modelling irradiation-induced corrosion
- **Steel-bentonite models**
- Integration of corrosion phenomena in performance assessments
- Performance assessments for copper-based canister corrosion
- Performance assessments for iron-based alloy canister corrosion

STEEL – BENTONITE MODELS

- Focused on the geochemical aspects of bentonite alteration
- Mechanistic reactive transport models in porous media
- Long term simulations > 10000 years:
 - Principle corrosion product of steel in contact with bentonite: magnetite
 - Significant alteration of the clay minerals to a mixture of non-swelling silicates

STEEL – BENTONITE MODELS

- Focused on the geochemical aspects of bentonite alteration
- Mechanistic reactive transport models in porous media
- Long term simulations > 10000 years:
 - Principle corrosion product of steel in contact with bentonite: magnetite
 - Significant alteration of the clay minerals to a mixture of non-swelling silicates
- Earlier models → mineral dissolution-precipitation ~ equilibrium reactions
- Later models → mineral dissolution-precipitation processes ~ kinetic reactions

STEEL – BENTONITE MODELS

- Focused on the geochemical aspects of bentonite alteration
- Mechanistic reactive transport models in porous media
- Long term simulations > 10000 years:
 - Principle corrosion product of steel in contact with bentonite: magnetite
 - Significant alteration of the clay minerals to a mixture of non-swelling silicates
- Earlier models → mineral dissolution-precipitation ~ equilibrium reactions
- Later models → mineral dissolution-precipitation processes ~ kinetic reactions
- More advanced models include
 - aqueous speciation
 - cation exchange
 - clay edge protolysis

STEEL – BENTONITE MODELS

- Focused on the geochemical aspects of bentonite alteration
- Mechanistic reactive transport models in porous media
- Long term simulations > 10000 years:
 - Principle corrosion product of steel in contact with bentonite: magnetite
 - Significant alteration of the clay minerals to a mixture of non-swelling silicates
- Earlier models → mineral dissolution-precipitation ~ equilibrium reactions
- Later models → mineral dissolution-precipitation processes ~ kinetic reactions
- More advanced models include
 - aqueous speciation
 - cation exchange
 - clay edge protolysis
- Most recent models include
 - Dissolved/precipitated solids expected in the system
 - Modifications of mineral properties
 - Transport properties



STEEL – BENTONITE MODELS

- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate



STEEL – BENTONITE MODELS

- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate
 - Magnetite as most abundant corrosion product



STEEL – BENTONITE MODELS

- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate
 - Magnetite as most abundant corrosion product
 - Choice of Fe solubility-limiting solids at the corroding steel surface

STEEL – BENTONITE MODELS

- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate
 - Magnetite as most abundant corrosion product
 - Choice of Fe solubility-limiting solids at the corroding steel surface
 - Transformation of clay minerals in Fe-chlorite and the timing depend on whether it is included as a secondary mineral or it results from a ripening process

STEEL – BENTONITE MODELS

- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate
 - Magnetite as most abundant corrosion product
 - Choice of Fe solubility-limiting solids at the corroding steel surface
 - Transformation of clay minerals in Fe-chlorite and the timing depend on whether it is included as a secondary mineral or it results from a ripening process
 - Numerical studies often differ on the precise nature of the main secondary minerals

STEEL – BENTONITE MODELS

- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate
 - Magnetite as most abundant corrosion product
 - Choice of Fe solubility-limiting solids at the corroding steel surface
 - Transformation of clay minerals in Fe-chlorite and the timing depend on whether it is included as a secondary mineral or it results from a ripening process
 - Numerical studies often differ on the precise nature of the main secondary minerals
 - Strong evidence that the physical properties of compacted bentonite in contact with steel degrade over very short timescales

STEEL – BENTONITE MODELS

- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate
 - Magnetite as most abundant corrosion product
 - Choice of Fe solubility-limiting solids at the corroding steel surface
 - Transformation of clay minerals in Fe-chlorite and the timing depend on whether it is included as a secondary mineral or it results from a ripening process
 - Numerical studies often differ on the precise nature of the main secondary minerals
 - Strong evidence that the physical properties of compacted bentonite in contact with steel degrade over very short timescales
 - Primary minerals in clay are often destabilized in favor of Fe-phyllsilicates or zeolites if they are allowed to precipitate

STEEL – BENTONITE MODELS

- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate
 - Magnetite as most abundant corrosion product
 - Choice of Fe solubility-limiting solids at the corroding steel surface
 - Transformation of clay minerals in Fe-chlorite and the timing depend on whether it is included as a secondary mineral or it results from a ripening process
 - Numerical studies often differ on the precise nature of the main secondary minerals
 - Strong evidence that the physical properties of compacted bentonite in contact with steel degrade over very short timescales
 - Primary minerals in clay are often destabilized in favor of Fe-phyllsilicates or zeolites if they are allowed to precipitate
 - Fe penetrates into the bentonite matrix along hairline microfractures that radiate outwards from the corroding metal

STEEL – BENTONITE MODELS

- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate
 - Magnetite as most abundant corrosion product
 - Choice of Fe solubility-limiting solids at the corroding steel surface
 - Transformation of clay minerals in Fe-chlorite and the timing depend on whether it is included as a secondary mineral or it results from a ripening process
 - Numerical studies often differ on the precise nature of the main secondary minerals
 - Strong evidence that the physical properties of compacted bentonite in contact with steel degrade over very short timescales
 - Primary minerals in clay are often destabilized in favor of Fe-phyllsilicates or zeolites if they are allowed to precipitate
 - Fe penetrates into the bentonite matrix along hairline microfractures that radiate outwards from the corroding metal
 - The extent of the perturbation is always predicted to be limited to a few centimeters

STEEL – BENTONITE MODELS

- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate
 - Magnetite as most abundant corrosion product
 - Choice of Fe solubility-limiting solids at the corroding steel surface
 - Transformation of clay minerals in Fe-chlorite and the timing depend on whether it is included as a secondary mineral or it results from a ripening process
 - Numerical studies often differ on the precise nature of the main secondary minerals
 - Strong evidence that the physical properties of compacted bentonite in contact with steel degrade over very short timescales
 - Primary minerals in clay are often destabilized in favor of Fe-phyllsilicates or zeolites if they are allowed to precipitate
 - Fe penetrates into the bentonite matrix along hairline microfractures that radiate outwards from the corroding metal
 - The extent of the perturbation is always predicted to be limited to a few centimeters
 - Porosity clogging is considered in some simulations under different assumptions

STEEL – BENTONITE MODELS

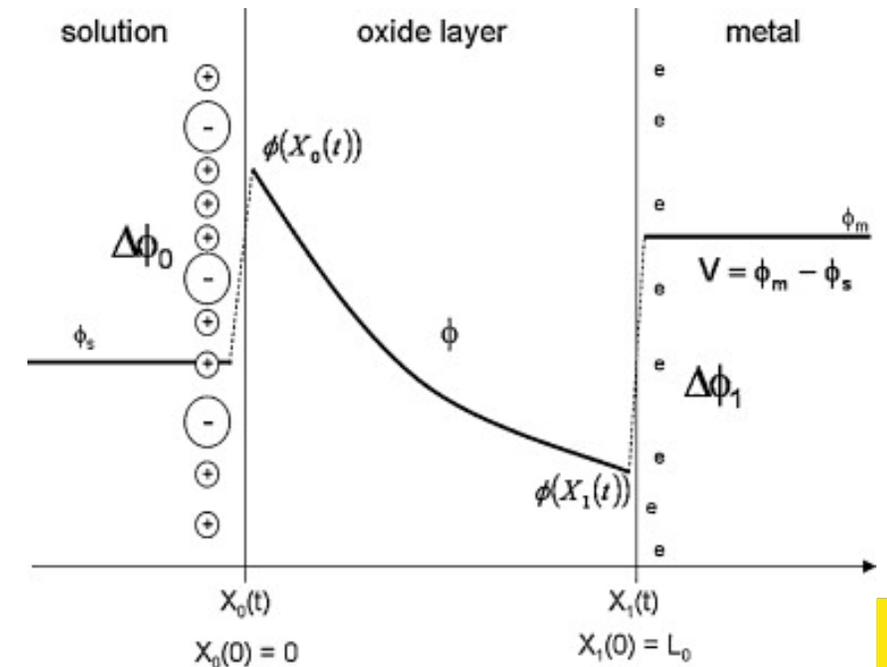
- Key issues for modelling iron-bentonite interactions:
 - Corrosion rate
 - Magnetite as most abundant corrosion product
 - Choice of Fe solubility-limiting solids at the corroding steel surface
 - Transformation of clay minerals in Fe-chlorite and the timing depend on whether it is included as a secondary mineral or it results from a ripening process
 - Numerical studies often differ on the precise nature of the main secondary minerals
 - Strong evidence that the physical properties of compacted bentonite in contact with steel degrade over very short timescales
 - Primary minerals in clay are often destabilized in favor of Fe-phyllsilicates or zeolites if they are allowed to precipitate
 - Fe penetrates into the bentonite matrix along hairline microfractures that radiate outwards from the corroding metal
 - The extent of the perturbation is always predicted to be limited to a few centimeters
 - Porosity clogging is considered in some simulations under different assumptions
 - Complete inhibition of the corrosion process has never been observed

STEEL – BENTONITE MODELS

- Hydrogen has been ignored in current simulations
 - Catalyst for chemical reduction of aqueous sulfate but thermal sulfate reduction by H₂ is inconsequential at the temperatures and pressures in the repository
 - Damage EBS structures
 - Transport of gaseous radionuclides to the biosphere

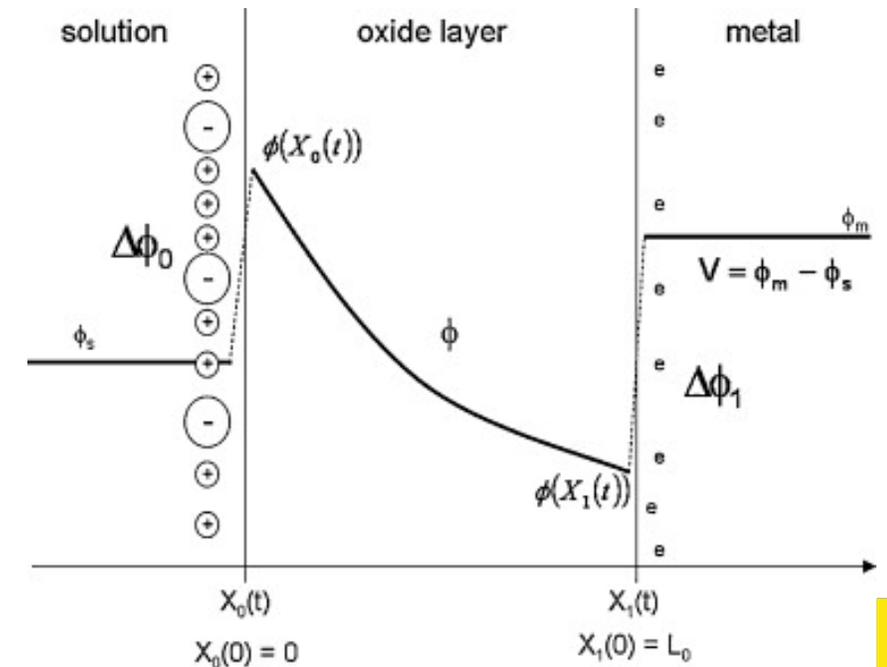
STEEL – BENTONITE MODELS

- Hydrogen has been ignored in current simulations
 - Catalyst for chemical reduction of aqueous sulfate but thermal sulfate reduction by H_2 is inconsequential at the temperatures and pressures in the repository
 - Damage EBS structures
 - Transport of gaseous radionuclides to the biosphere
- Diffusion Poisson Coupled Model (DPCM)
 - Numerical code implemented in CALIPSO
 - 2 interfaces bound the oxide layer
 - Inner interface: metal/oxide \rightarrow electronic conductor
 - Outer interface: solution \rightarrow ionic conductor
 - Can move with time



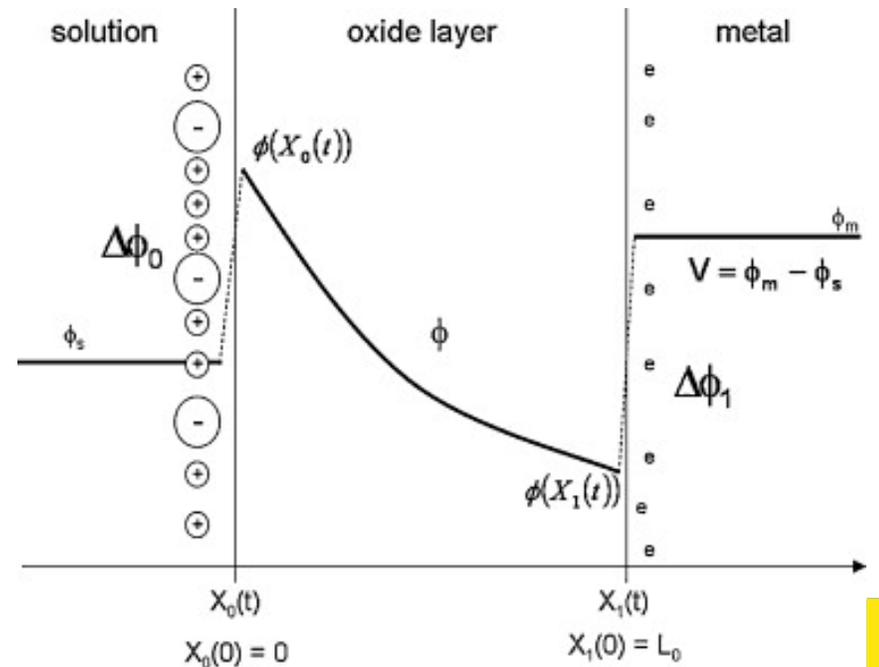
STEEL – BENTONITE MODELS

- Hydrogen has been ignored in current simulations
 - Catalyst for chemical reduction of aqueous sulfate but thermal sulfate reduction by H_2 is inconsequential at the temperatures and pressures in the repository
 - Damage EBS structures
 - Transport of gaseous radionuclides to the biosphere
- Diffusion Poisson Coupled Model (DPCM)
 - Numerical code implemented in CALIPSO
 - 2 interfaces bound the oxide layer
 - Inner interface: metal/oxide → electronic conductor
 - Outer interface: solution → ionic conductor
 - Can move with time
 - 3 coupled modules in the model:
 - Electrostatic → potential profile in solution-oxide layer-metal system
 - Kinetic concentration → profiles (one per each charge carrier)
 - Moving boundaries → locations of the interfaces



STEEL – BENTONITE MODELS

- Hydrogen has been ignored in current simulations
 - Catalyst for chemical reduction of aqueous sulfate but thermal sulfate reduction by H_2 is inconsequential at the temperatures and pressures in the repository
 - Damage EBS structures
 - Transport of gaseous radionuclides to the biosphere
- Diffusion Poisson Coupled Model (DPCM)
 - Numerical code implemented in CALIPSO
 - 2 interfaces bound the oxide layer
 - Inner interface: metal/oxide → electronic conductor
 - Outer interface: solution → ionic conductor
 - Can move with time
 - 3 coupled modules in the model:
 - Electrostatic → potential profile in solution-oxide layer-metal system
 - Kinetic concentration → profiles (one per each charge carrier)
 - Moving boundaries → locations of the interfaces
 - Estimate lifetime of the carbon steel overpack & pressure increase from H_2

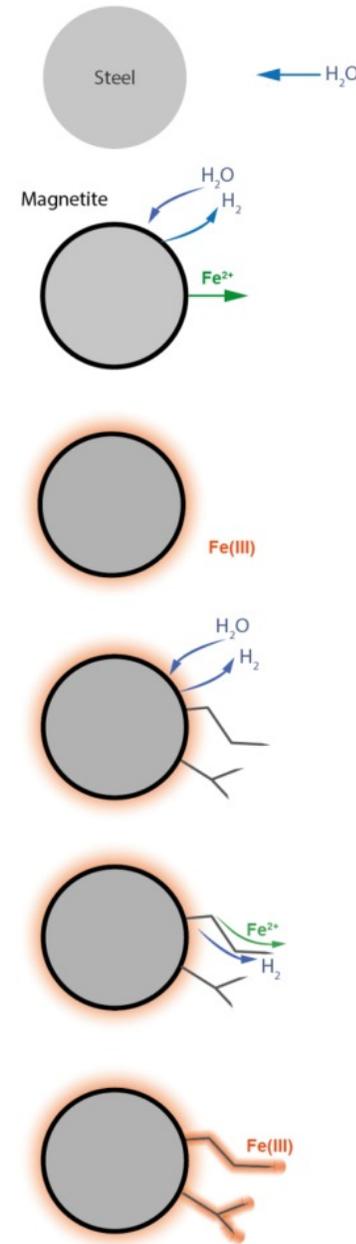
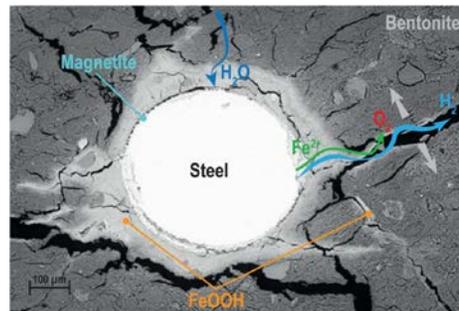


STEEL – BENTONITE MODELS

- DPCM in CALIPSO
 - Coupled with geochemistry-transport code, Kirmat
 - Realistic representation of corrosion of iron & alteration clay

STEEL – BENTONITE MODELS

- DPCM in CALIPSO
 - Coupled with geochemistry-transport code, Kirmat
 - Realistic representation of corrosion of iron & alteration clay
- Two-phase modelling
 - Consumption of H_2O by corrosion \gg diffusion of H_2O through bentonite \rightarrow shrinkage micro-fractures in bentonite acting as preferential pathways for corrosion products



During saturation water diffuses through the bentonite towards the steel surface.

The anaerobic corrosion of iron leads to the production of magnetite and Fe^{2+} ions. The cathodic reaction is the reduction of H_2O producing H_2 . Fe^{2+} diffuses into the bentonite resulting in an iron enriched zone.

Fe^{2+} is oxidized by residual O_2 leading to precipitation of red $Fe(III)$ corrosion products. The magnetite remains unaffected because the O_2 is not mobile.

The high rate of water consumption and H_2 production leads to local desiccation and shrinkage microfractures because the hydraulic conductivity of saturated bentonite is low.

Fe^{2+} and H_2 continuously produced by corrosion preferentially diffuse along the shrinkage microfractures into the bentonite.

Fe^{2+} reacts with residual O_2 at the walls of the microfractures and precipitates as $Fe(III)$. As the corrosion product layer grows the corrosion rate decreases and the bentonite resaturates. The microfractures cannot re-seal because their walls are coated with $Fe(III)$.

COMPARISON OF MAIN ASSUMPTIONS & RESULTS OF EXISTING MODELLING EXERCISES AT DISPOSAL SCALE AT FE-MX80 BENTONITE INTERFACE

T (°C)	Simulation time (years)	Corrosion rate	Assumptions	Main secondary minerals	Max. perturbation extent	Relevant results
50	10.000	Constant (4,3 µm/y)	<ul style="list-style-type: none"> • 1D diffusive model • Porosity feedback effect 	Cronstedtite Berthierine	5 cm	Porosity clogging after 5.000 years
100	500.000	Constant (1 µm/y)	<ul style="list-style-type: none"> • 1D model (Test case D0) • Porosity update • Clay reactions are considered • Use of cation exchange and surface complexation 	Cronstedtite Berthierine	Few cm	Interaction of Fe with bentonite spatially limited for very long times → Fe clay re-precipitation & diffusional limitation
-	1.000.000	Constant (~2 µm/y)	<ul style="list-style-type: none"> • Time-dependent variation of reactive surface areas for the Fe-bearing minerals • The sequence of the alteration of the clay by Fe-rich fluids may proceed via an Ostwald step sequence 	Cronstedtite Berthierine	-	<ul style="list-style-type: none"> • Secondary minerals evolution ≠ predicted by the fixed surface area model • Sequence of precipitation: magnetite-cronstedtite-berthierine-chlorite
100	100.000	Decreases from 5 to 0.2 µm/y	<ul style="list-style-type: none"> • Porosity update • Clay reactions are considered 	Fe-chlorite Fe-saponite	15 cm	Porosity clogging after 100.000 years
100	10.000	Decreases from 5 to 0.2 µm/y	<ul style="list-style-type: none"> • Porosity update • Clay reactions are considered • - & + influence of the reactive surface areas of the primary minerals 	Greenalite Fe-saponite Fe-chlorite Berthierine	10 cm	Large surface area primary clay minerals provides a significant porosity ↓ in the zone in contact with the steel overpack → limited the diffusion aqueous corrosion products toward the bentonite barrier → porosity ↓ & mineralogical transformation in the bentonite zone close to the bentonite/steel overpack interface.

COMPARISON OF MAIN ASSUMPTIONS & RESULTS OF EXISTING MODELLING EXERCISES AT DISPOSAL SCALE AT FE-FEBEX & FE-BENTONITE INTERFACE

T (°C)	Simulation time (years)	Corrosion rate	Assumptions	Main secondary minerals	Max. perturbation extent	Relevant results
25	300.000	Constant (0.2 µm/y)	<ul style="list-style-type: none"> 1D and 2D model No reactivity for clay minerals Use of cation exchange & surface complexation 	Siderite Goethite	7 cm	<ul style="list-style-type: none"> Magnetite precipitation (no clogging) → bentonite porosity ↓ Proton surface complexation is highly effective in buffering pH in bentonite
25	300.000	Constant (0.1 µm/y) & φ (max. 0.7 µm/y)	<ul style="list-style-type: none"> 1D model Use of cation exchange & 3 types of sorption sites in the bentonite Kinetically-controlled container corrosion & magnetite precipitation 		-	<ul style="list-style-type: none"> Kinetically-controlled container corrosion → significant ↓ in the corrosion rate [dissolved Fe] computed with kinetic magnetite precipitation is < [obtained at equilibrium]
≠	1.000.000	Constant (2 µm/y) & φ	<ul style="list-style-type: none"> 1D model Use of cation exchange & 3 types of sorption sites in the bentonite Kinetically-controlled container corrosion & magnetite precipitation Smectite dissolution is considered 	Analcime Cronstedtite	7 cm	<ul style="list-style-type: none"> Magnetite precipitation → bentonite porosity ↓ near the container (7 cm thickness of the zone of reduced porosity at 1 Ma) Thickness: < 5 cm for a corrosion rate of 5 µm/year - 12 cm for a rate of 0.5 mm/year. Corrosion rate ~ chemical conditions → thickness ↑ when Smectite dissolution & analcime precipitation → thickness ↓ 3 cm
≠	1.000.000	Constant (2 µm/y)	<ul style="list-style-type: none"> 1D model Use of cation exchange and 3 types of sorption sites in the bentonite. Smectite dissolution is considered 	Gypsum Sepiolite	1 cm	<ul style="list-style-type: none"> Pore clogging at the container-bentonite interface Narrow alteration zones Limited smectite dissolution after 1 Ma
70	100.000	Constant (1 µm/y) & φ (M2)	<ul style="list-style-type: none"> Model 1: fixed steel corrosion rate Model 2: diffusion-limited corrosion rate Model 3: corrosion cell approach 	M1: Berthierine Fe-saponite Greenalite M2 and M3: Berthierine	2 cm	<ul style="list-style-type: none"> Extent & nature of the alteration predicted by the models sensitive to model conceptualization M1 and M2: - M3: Magnetite Siderite



CONTENT

- Introduction
- Copper container corrosion
 - Reactive transport models in bentonite
 - Modeling sulfide fluxes
 - Modelling irradiation-induced corrosion
- Steel-bentonite models
- **Integration of corrosion phenomena in performance assessments**
- Performance assessments for copper-based canister corrosion
- Performance assessments for iron-based alloy canister corrosion



INTEGRATION OF CORROSION PHENOMENA IN PERFORMANCE ASSESSMENTS

- Definition according to NRC in US:
 - *A performance assessment (PA) is a 'quantitative evaluation of potential releases of radioactivity from a disposal facility into the environment, and assessment of the resultant radiological doses*

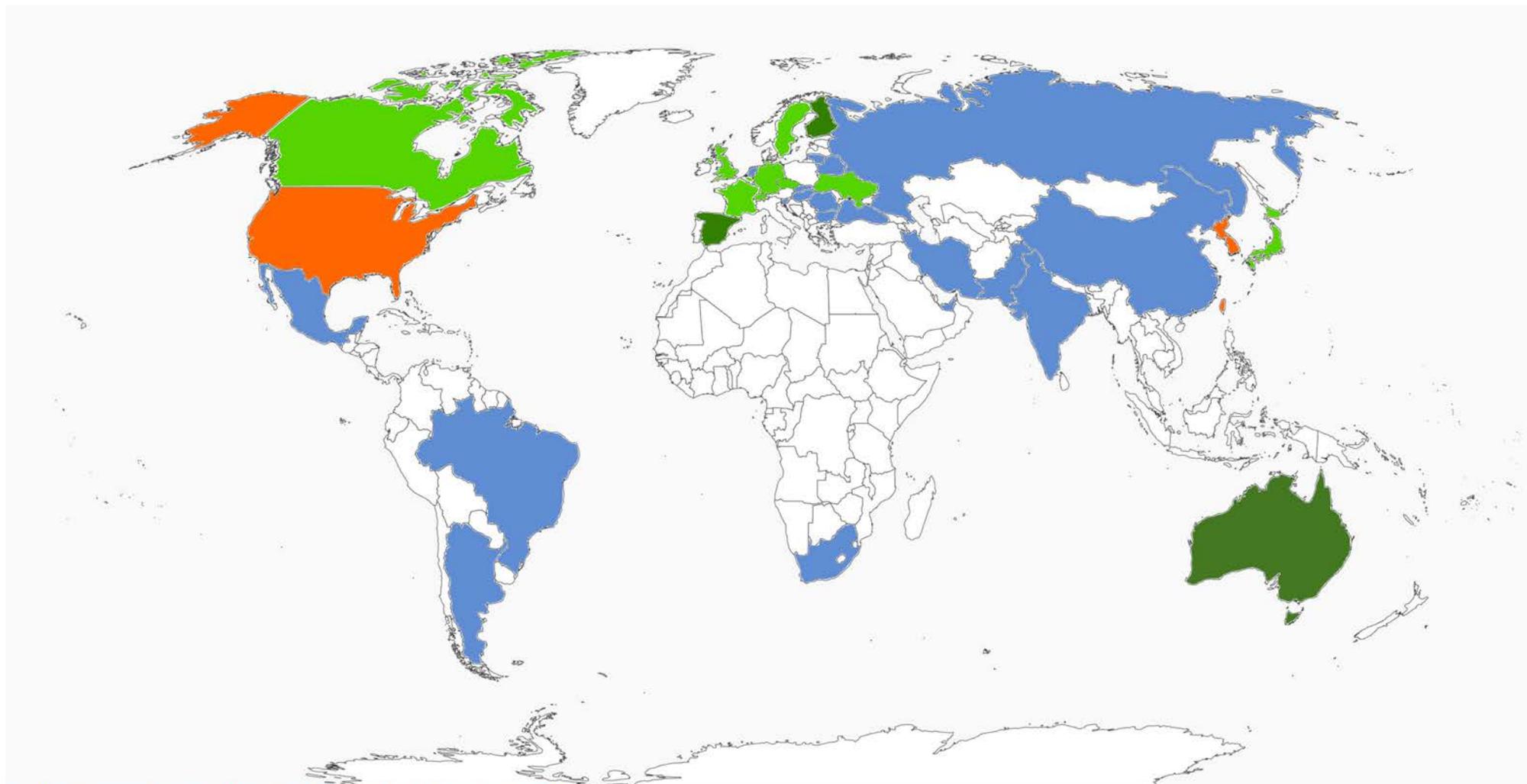
INTEGRATION OF CORROSION PHENOMENA IN PERFORMANCE ASSESSMENTS

- Definition according to NRC in US:
 - *A performance assessment (PA) is a 'quantitative evaluation of potential releases of radioactivity from a disposal facility into the environment, and assessment of the resultant radiological doses*
- Corrosion key factor in determining the durability of the disposal container → PA important for radionuclide release in the:
 - Groundwater
 - Gaseous phase

INTEGRATION OF CORROSION PHENOMENA IN PERFORMANCE ASSESSMENTS

- Definition according to NRC in US:
 - *A performance assessment (PA) is a 'quantitative evaluation of potential releases of radioactivity from a disposal facility into the environment, and assessment of the resultant radiological doses*
- Corrosion key factor in determining the durability of the disposal container → PA important for radionuclide release in the:
 - Groundwater
 - Gaseous phase
- No standardized prescriptive approach to include corrosion in PA → specific to each concept & environmental conditions
- General guidance of safety assessment provided by IAEA

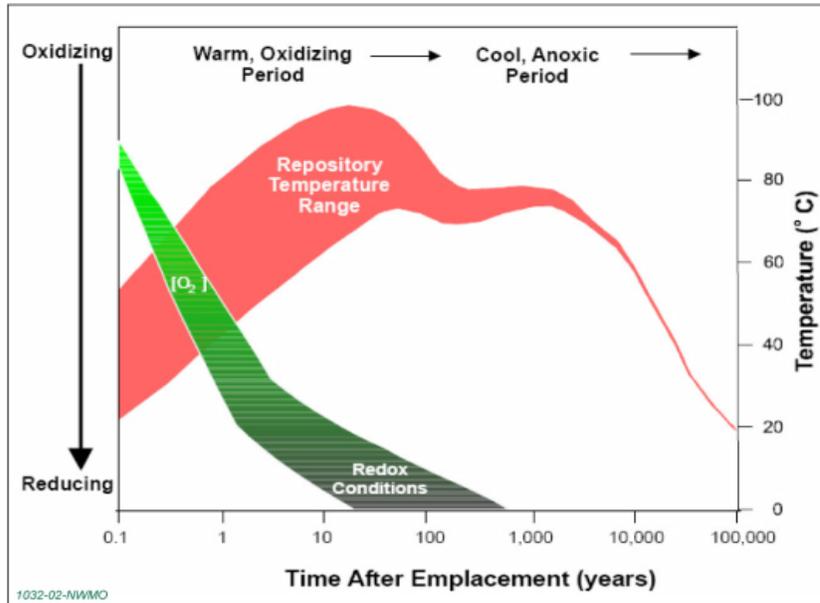
COUNTRIES OPERATING NUCLEAR POWER PLANTS (36) & PROGRESS IN PA



- nuclear countries who performed/will perform PA
- nuclear countries who performed/will perform PA with WMO involved in ConCorD
- nuclear countries who performed/will perform PA with research institutes involved in ConCorD
- nuclear countries who plan deep geological disposal but didn't do PA

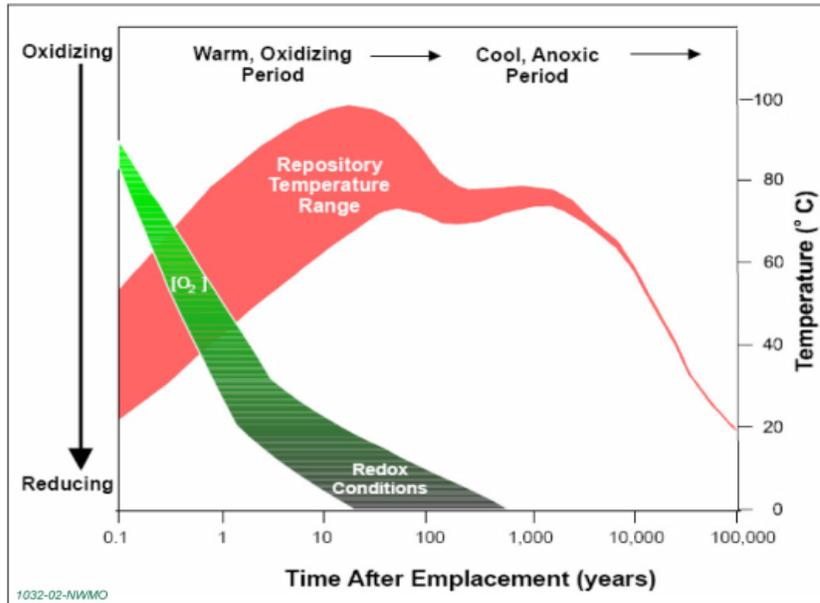
INTEGRATION OF CORROSION PHENOMENA IN PERFORMANCE ASSESSMENTS

- Variation between different disposal concepts but in general:



INTEGRATION OF CORROSION PHENOMENA IN PERFORMANCE ASSESSMENTS

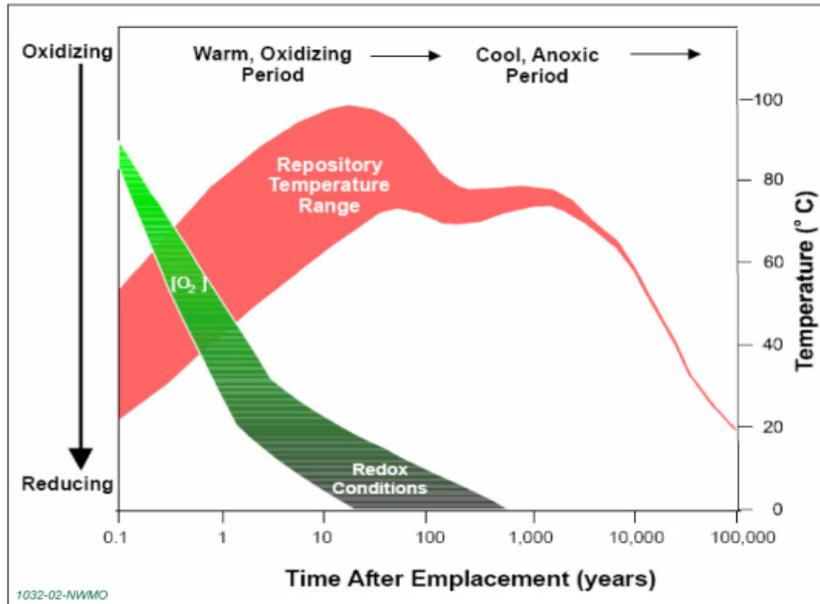
- Variation between different disposal concepts but in general:



- Aim of PA is to reflect these phenomena in a pragmatic way → simplifying assumptions

INTEGRATION OF CORROSION PHENOMENA IN PERFORMANCE ASSESSMENTS

- Variation between different disposal concepts but in general:



- Aim of PA is to reflect these phenomena in a pragmatic way → simplifying assumptions
- Copper-based waste container ↔ iron-based container

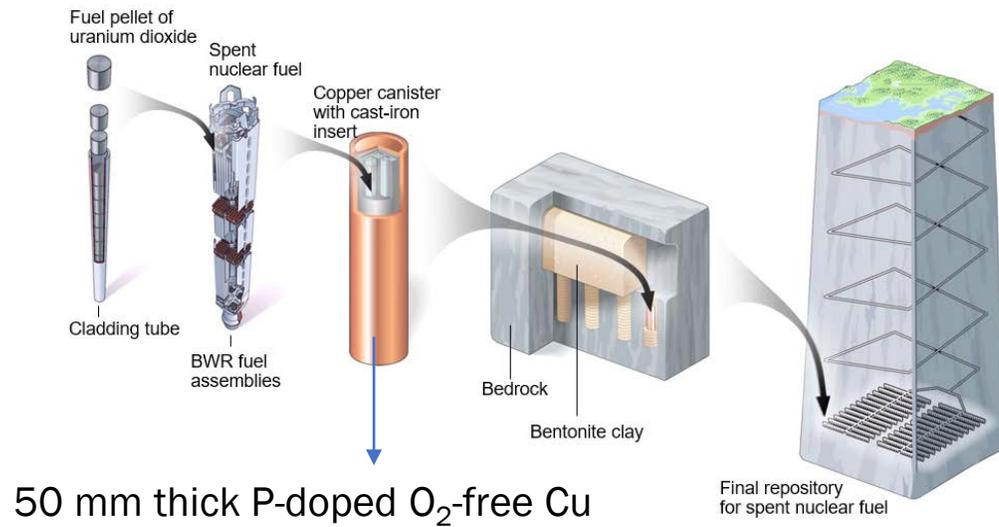
CONTENT

- Introduction
- Copper container corrosion
- Steel-bentonite models
- Integration of corrosion phenomena in performance assessments
- **Performance assessments for copper-based canister corrosion**
 - Corrosion in unsaturated conditions
 - General corrosion
 - Localised corrosion
 - Radiation assisted corrosion
 - Microbially influenced corrosion
 - Environmental-assisted cracking
 - Mechanical degradation & combined corrosion-mechanical effects
 - In-situ testing of copper spent fuel canisters
 - Prediction of canister lifetimes and implications for PA
- Performance assessments for iron-based alloy canister corrosion

PA FOR COPPER-BASED CONTAINER CORROSION

- O₂-free copper → Sweden, Finland, Switzerland, Canada

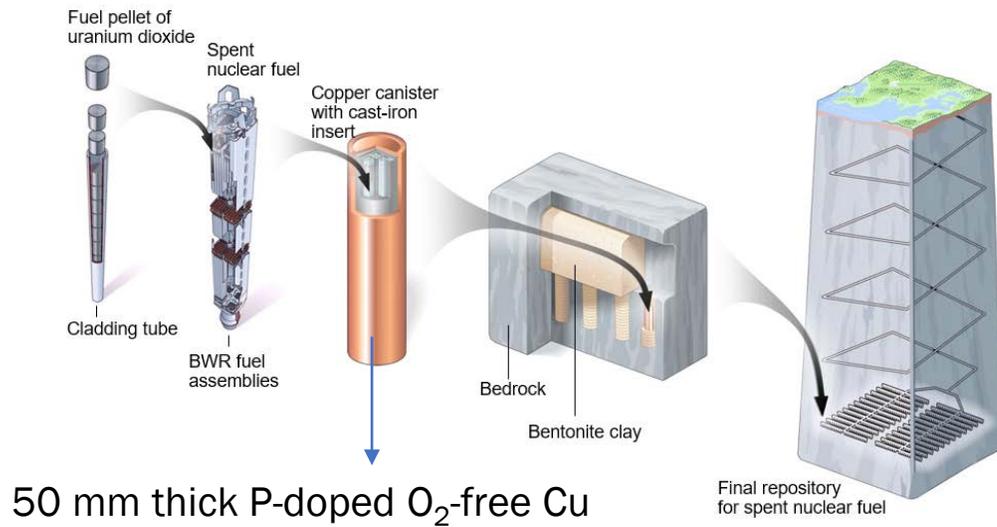
Furthest developed concept:
KBS-3 concept considered in
Sweden & Finland



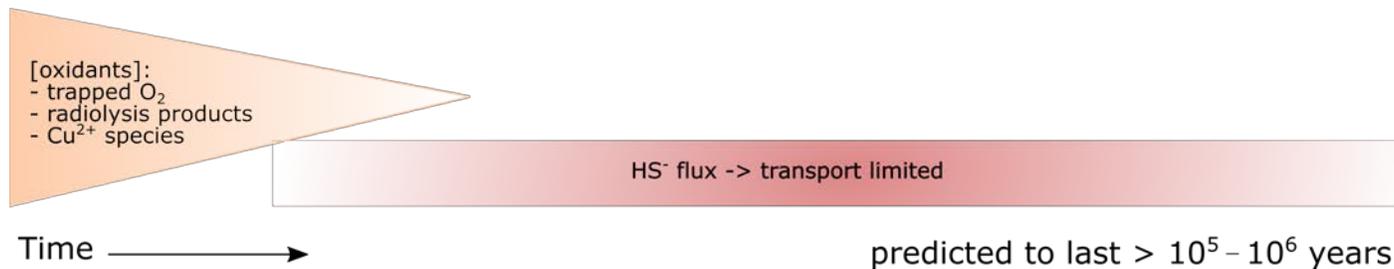
PA FOR COPPER-BASED CONTAINER CORROSION

- O₂-free copper → Sweden, Finland, Switzerland, Canada

Furthest developed concept:
KBS-3 concept considered in
Sweden & Finland



- Cu is not expected to passivate prediction lifetime based on general corrosion with moderate uniformity



PA FOR COPPER-BASED CONTAINER CORROSION

- PA typically indicate that expected depths of corrosion $<$ container wall thickness
- Corrosion allowance for coated designs is much less \rightarrow requires greater certainty regarding the prevailing corrosion mechanisms

PA FOR COPPER-BASED CONTAINER CORROSION

- PA typically indicate that expected depths of corrosion $<$ container wall thickness
- Corrosion allowance for coated designs is much less \rightarrow requires greater certainty regarding the prevailing corrosion mechanisms
- Types of corrosion that need to be considered in PA:
 - Corrosion under unsaturated conditions
 - General corrosion
 - Localized corrosion
 - Microbial influenced corrosion
 - Environmentally assisted cracking

CORROSION IN UNSATURATED CONDITIONS

- Unsaturated phase: including any corrosion before emplacement in the buffer and within the buffer before groundwater re-saturation occurs
- Evaluated in KBS-3 environment
- Temp 50 °C → relative humidity < critical value of 50-70% ↔ dry air → corrosion rate ↑ with temp: 10s of nm/year if 50-150°C
- ~ measurements Äspo Hard Rock Lab : < 0.1 μm at 75°C



Final repository
for spent nuclear fuel

CORROSION IN UNSATURATED CONDITIONS

- Unsaturated phase: including any corrosion before emplacement in the buffer and within the buffer before groundwater re-saturation occurs
- Evaluated in KBS-3 environment
- Temp 50 °C → relative humidity < critical value of 50-70% ↔ dry air → corrosion rate ↑ with temp: 10s of nm/year if 50-150 °C
- ~ measurements Äspo Hard Rock Lab : < 0.1 μm at 75 °C
- Pessimistically bounded by assuming that:
 - atmospheric corrosion < 1 μm
 - production of copper oxide surface film



Final repository
for spent nuclear fuel

CORROSION IN UNSATURATED CONDITIONS

- Unsaturated phase: including any corrosion before emplacement in the buffer and within the buffer before groundwater re-saturation occurs
- Evaluated in KBS-3 environment
- Temp 50 °C → relative humidity < critical value of 50-70% ↔ dry air → corrosion rate ↑ with temp: 10s of nm/year if 50-150°C
- ~ measurements Äspo Hard Rock Lab : < 0.1 μm at 75°C
- Pessimistically bounded by assuming that:
 - atmospheric corrosion < 1 μm
 - production of copper oxide surface film

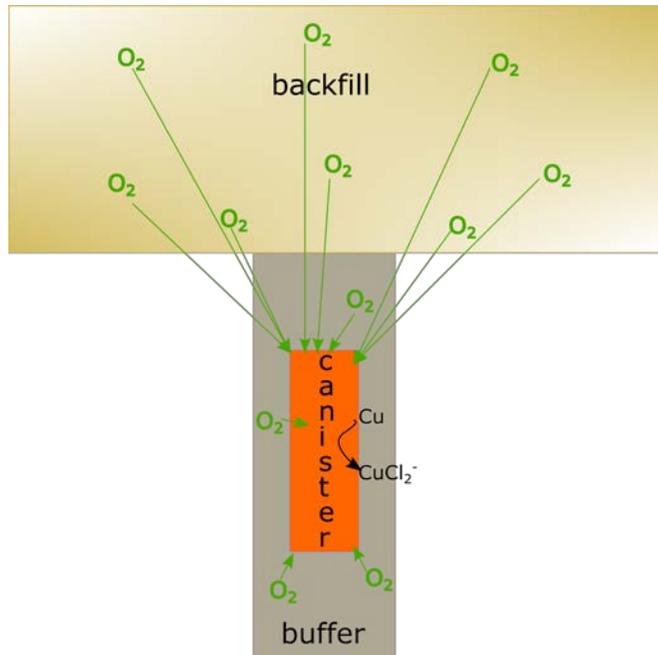
➔ Extent of corrosion expected to be negligible



Final repository
for spent nuclear fuel

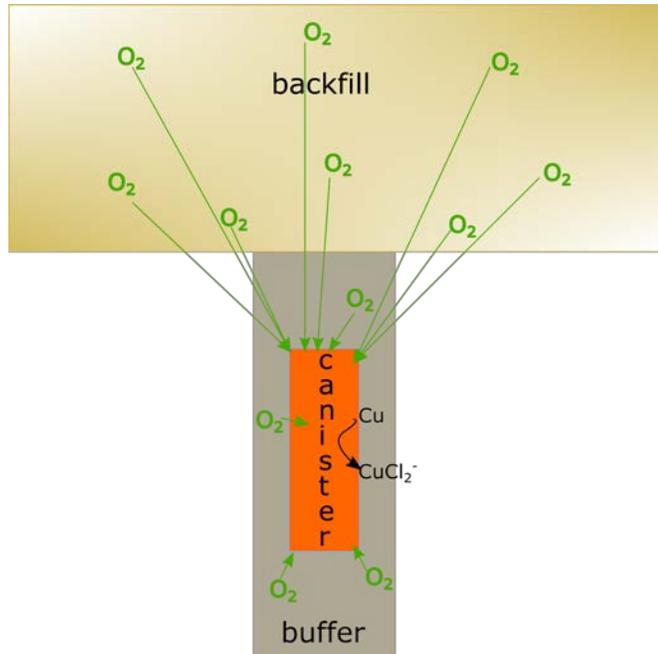
GENERAL CORROSION

- All oxygen in voids reaches container → highly conservative

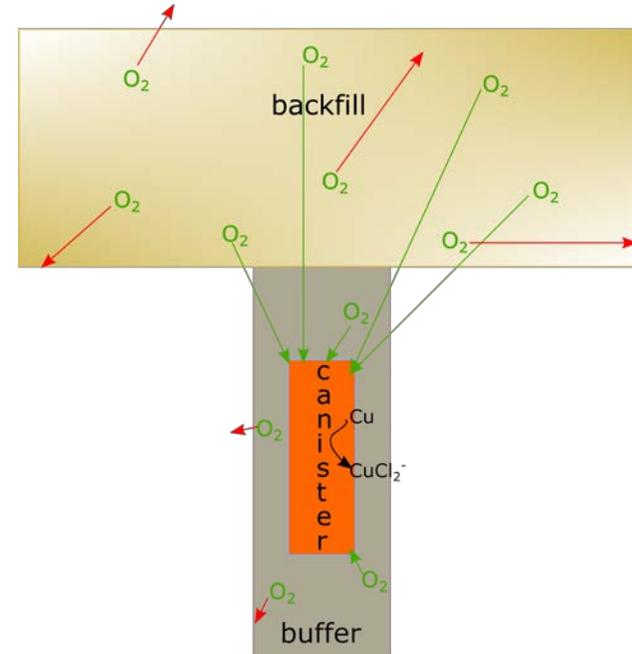


GENERAL CORROSION

- All oxygen in voids reaches container → highly conservative

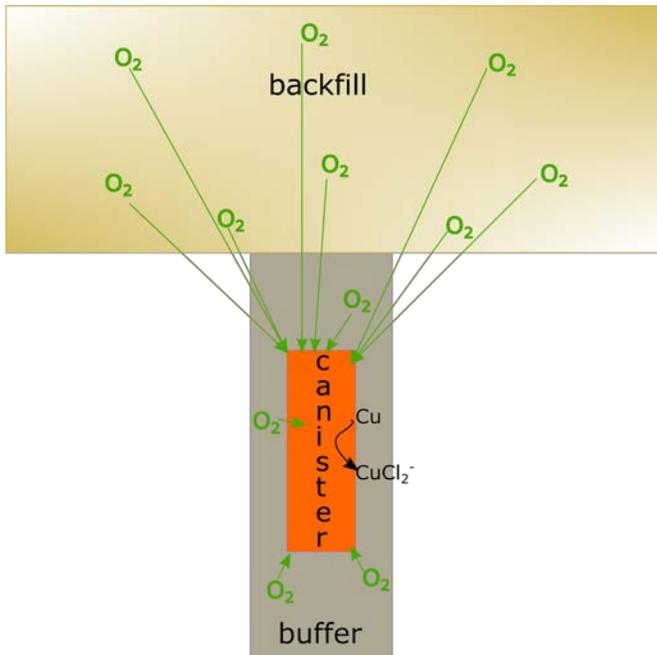


- KBS-3 design: 50 % reaches surface → corrosion loss of 17 μm (max. 36 μm)

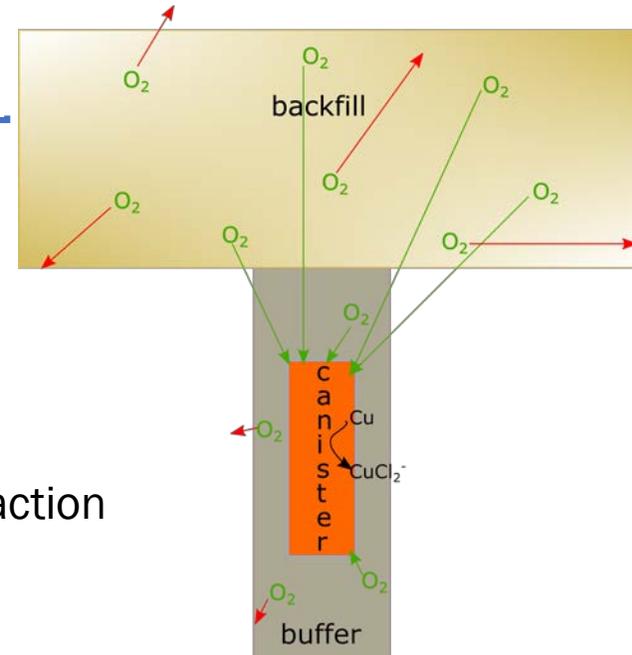


GENERAL CORROSION

- All oxygen in voids reaches container → highly conservative



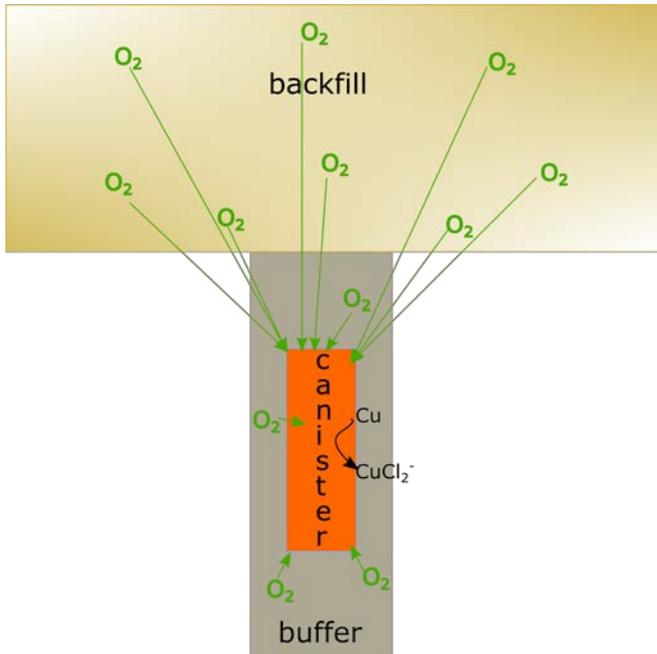
KBS-3 design: 50 % reaches surface → corrosion loss of 17 μm (max. 36 μm)



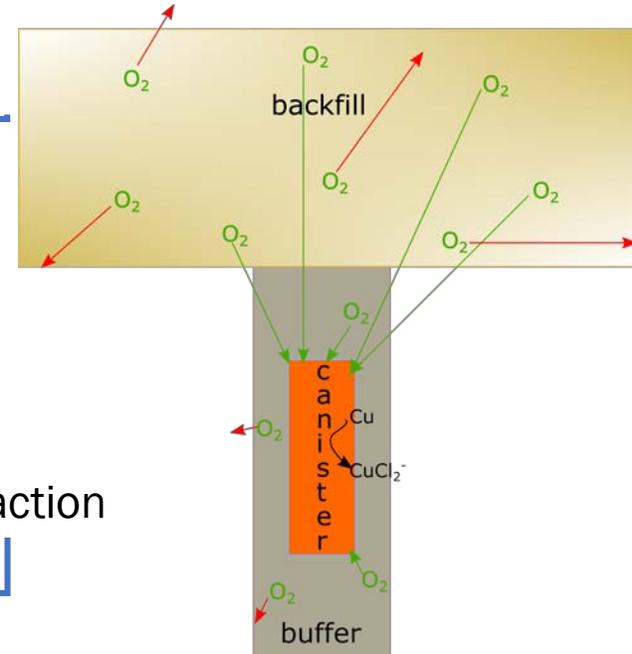
> O₂ but smaller fraction reach container

GENERAL CORROSION

- All oxygen in voids reaches container → highly conservative



KBS-3 design: 50 % reaches surface → corrosion loss of 17 μm (max. 36 μm)

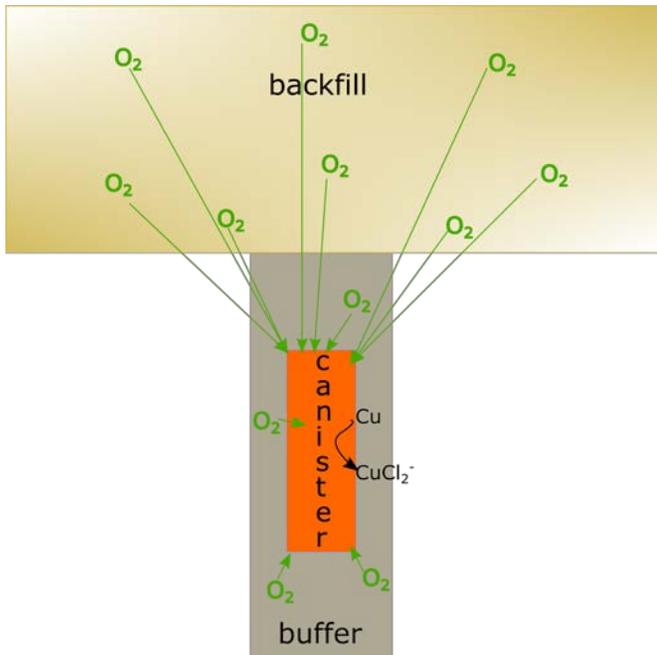


> O₂ but smaller fraction reach container

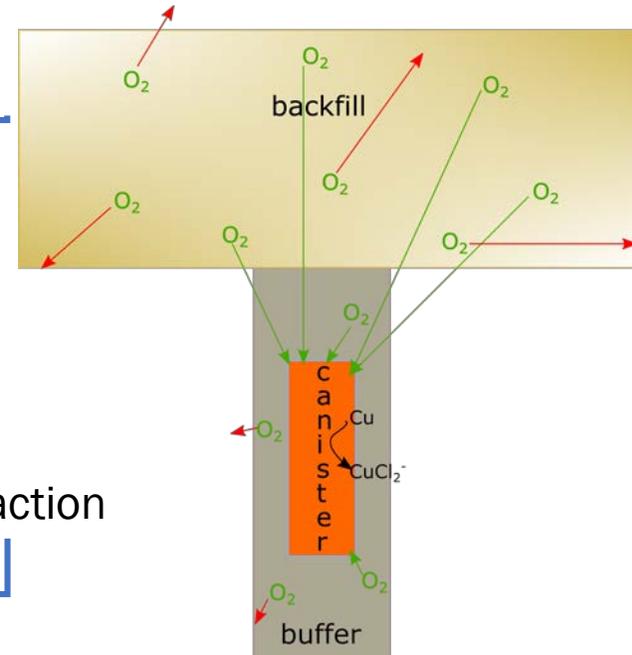
container diameter/deposition hole
assumption: O₂ consumed as it diffuses downwards by reaction with only lid & top 10 % of container height

GENERAL CORROSION

- All oxygen in voids reaches container → highly conservative



KBS-3 design: 50 % reaches surface → corrosion loss of 17 μm (max. 36 μm)



> O₂ but smaller fraction reach container

container diameter/deposition hole
assumption: O₂ consumed as it diffuses downwards by reaction with only lid & top 10 % of container height

Corrosion loss 106 μm = 123 μm total loss

GENERAL CORROSION

- Swiss concept

Host rock	Repository depth (m)	Repository Temp (°C)	Hydrostatic pressure	Lithostatic pressure	Bentonite saturation time	Bentonite swelling pressure	Salinity Cl (mol/l)
Opalinus Clay	450-850	Ambient 30-45 Max. ~ 160	4.5-8.5 MPa	15-22 MPa + glacial: 5 MPa	>100 years	2-4 MPa	Typ. 0.1 Max. 0.3

GENERAL CORROSION

- Swiss concept

Host rock	Repository depth (m)	Repository Temp (°C)	Hydrostatic pressure	Lithostatic pressure	Bentonite saturation time	Bentonite swelling pressure	Salinity Cl (mol/l)
Opalinus Clay	450-850	Ambient 30-45 Max. ~ 160	4.5-8.5 MPa	15-22 MPa + glacial: 5 MPa	>100 years	2-4 MPa	Typ. 0.1 Max. 0.3

- Conservative calculation for corrosion from trapped O₂ : 70 μm

GENERAL CORROSION

- Swiss concept

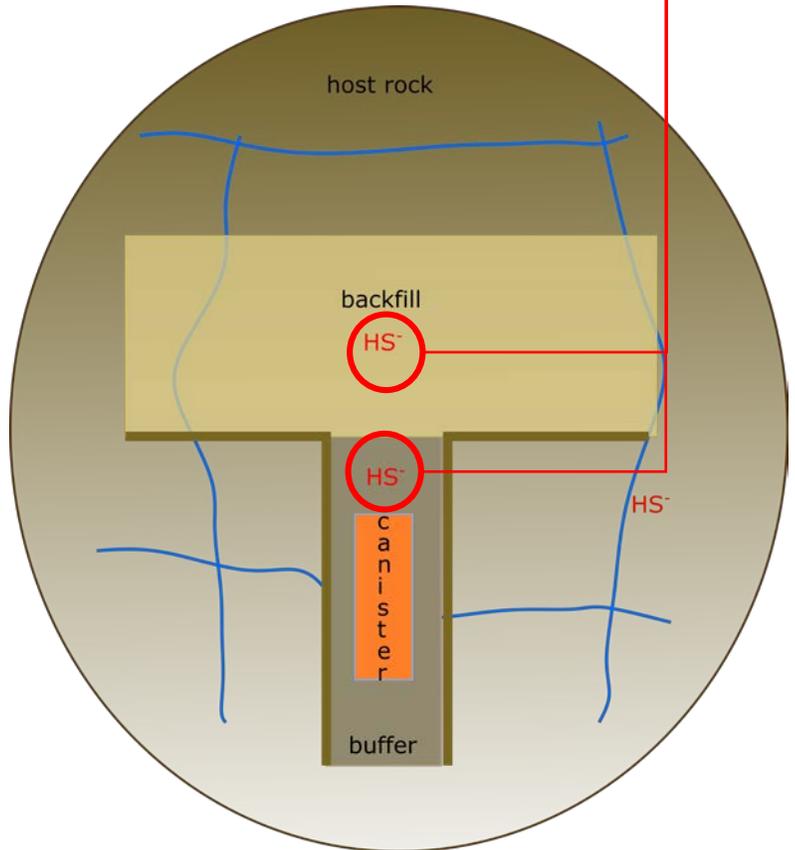
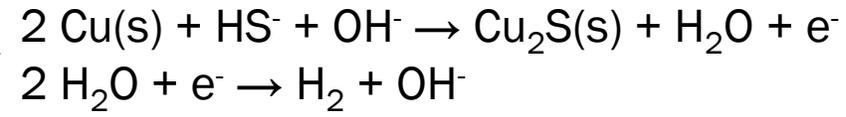
Host rock	Repository depth (m)	Repository Temp (°C)	Hydrostatic pressure	Lithostatic pressure	Bentonite saturation time	Bentonite swelling pressure	Salinity Cl (mol/l)
Opalinus Clay	450-850	Ambient 30-45 Max. ~ 160	4.5-8.5 MPa	15-22 MPa + glacial: 5 MPa	>100 years	2-4 MPa	Typ. 0.1 Max. 0.3

- Conservative calculation for corrosion from trapped O₂ : 70 µm
- Mass transport approach for trapped O₂
 - Cautious and sufficient (conservative)
 - Can be used in relevant scenarios including:
 - Deliberately or inadvertently unsealed tunnels during the GDF operational period
 - Access of glacial-melt water

GENERAL CORROSION

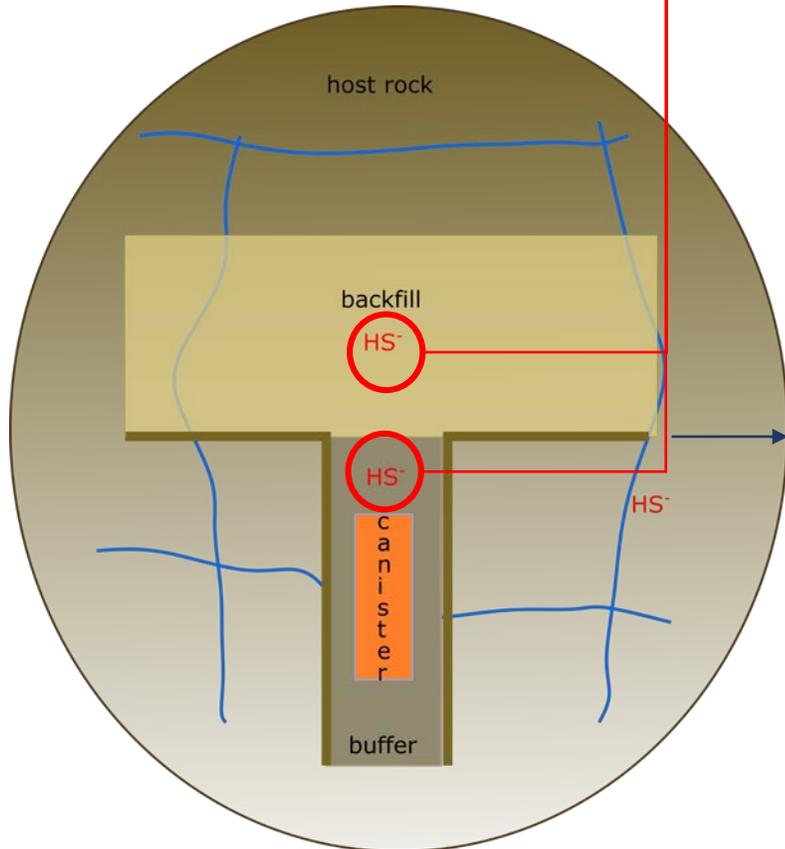
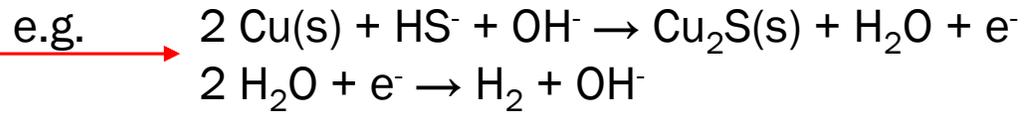
- - O₂
- Reactive transport modelling

e.g.



GENERAL CORROSION

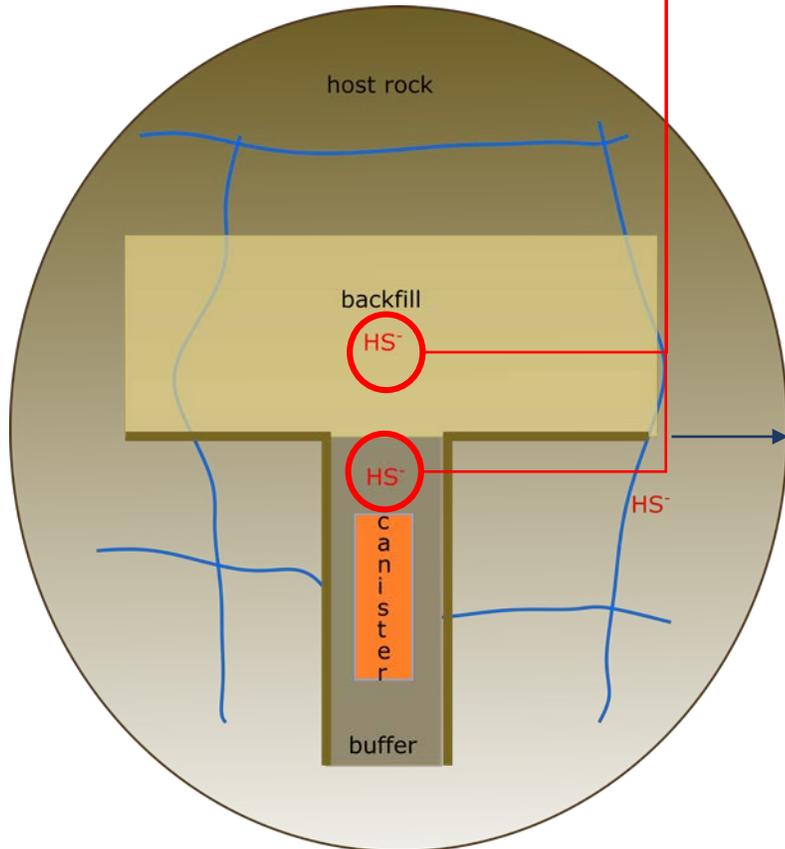
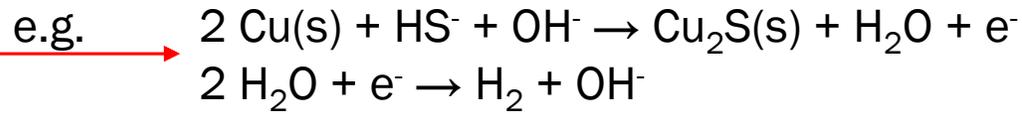
- - O₂
- Reactive transport modelling



- Assumptions for corrosion rate due to diffusion:
- react immediately upon contact with container surface
 - Future reaction is unhindered by formation of corrosion products

GENERAL CORROSION

- - O₂
- Reactive transport modelling



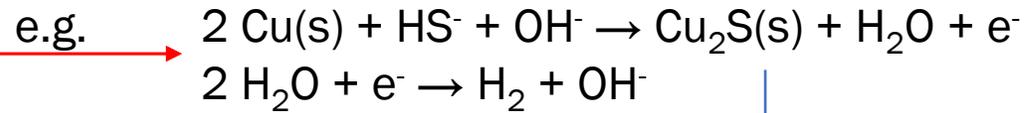
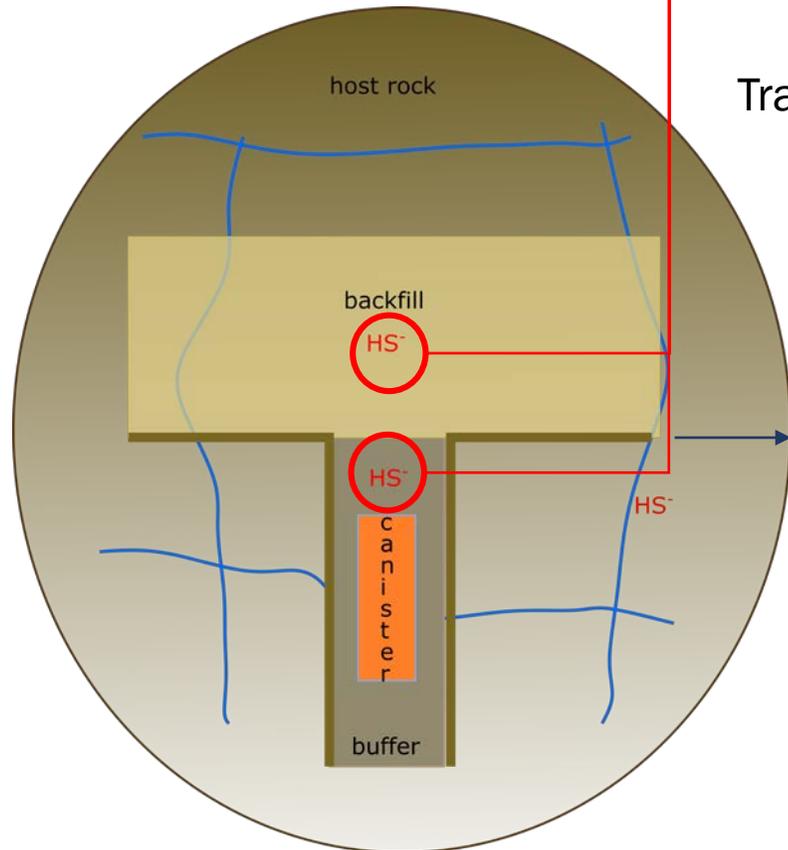
Justified by slow transport rate of HS⁻ ↔ inherent reaction rate of Cu with HS⁻

Assumptions for corrosion rate due to diffusion:

- react immediately upon contact with container surface
- Future reaction is unhindered by formation of corrosion products

GENERAL CORROSION

- $-O_2$
- Reactive transport modelling



Transport-limited: corrosion rate \sim flux of species reaching surface

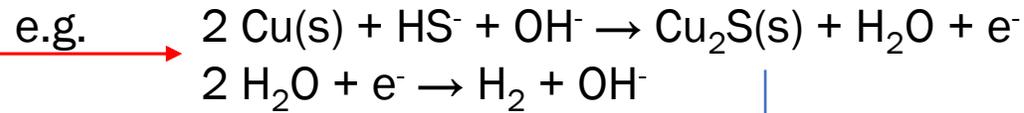
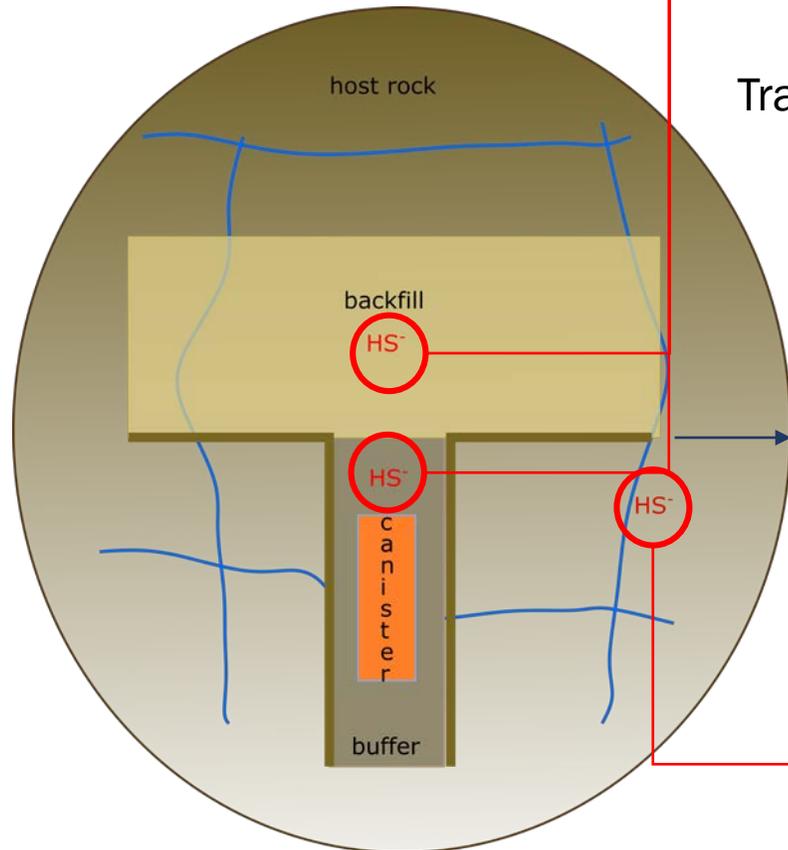
Justified by slow transport rate of $HS^- \leftrightarrow$ inherent reaction rate of Cu with HS^-

Assumptions for corrosion rate due to diffusion:

- react immediately upon contact with container surface
- Future reaction is unhindered by formation of corrosion products

GENERAL CORROSION

- $-O_2$
- Reactive transport modelling



Transport-limited: corrosion rate \sim flux of species reaching surface

Justified by slow transport rate of $\text{HS}^- \leftrightarrow$ inherent reaction rate of Cu with HS^-

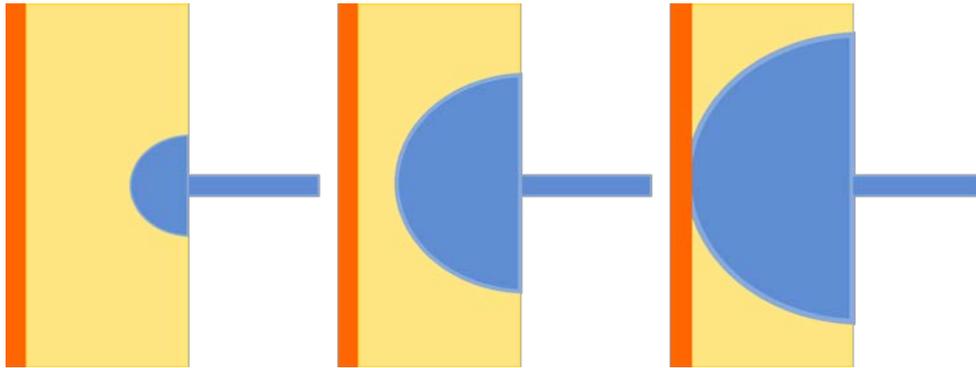
Assumptions for corrosion rate due to diffusion:

- react immediately upon contact with container surface
- Future reaction is unhindered by formation of corrosion products

Corrosion of copper by HS^- transport in groundwater evaluated by mass transport limitation
 Equilibrium $[\text{HS}^-]$ determined by source & sink

GENERAL CORROSION

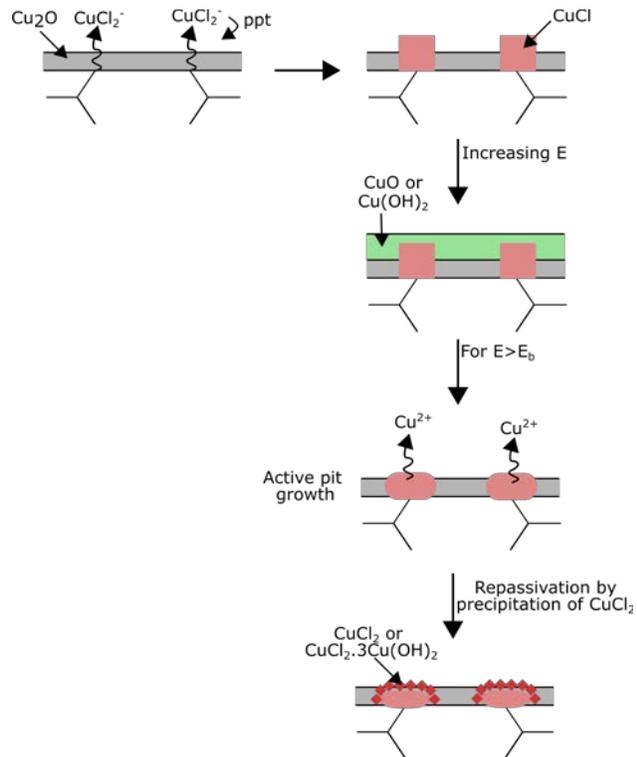
- Effect of buffer erosion from rock fracture on HS^- transport → mass transport modelling



Intact buffer	Partially eroded buffer
	Most pessimistic assumptions: <ul style="list-style-type: none"> • $[\text{HS}^-]$ 0.12 mM • flow rate ≥ 0.161 m/s → Failure (> 47 mm) could occur in 10^5 years
$[\text{HS}^-]$ 0.01 mM → < 0.001 $\mu\text{m}/\text{year}$	More realistic assumptions: <ul style="list-style-type: none"> • $[\text{HS}^-]$ 0.01 mM • High flow rate 0.251 m/s → Failure after 850 000 years

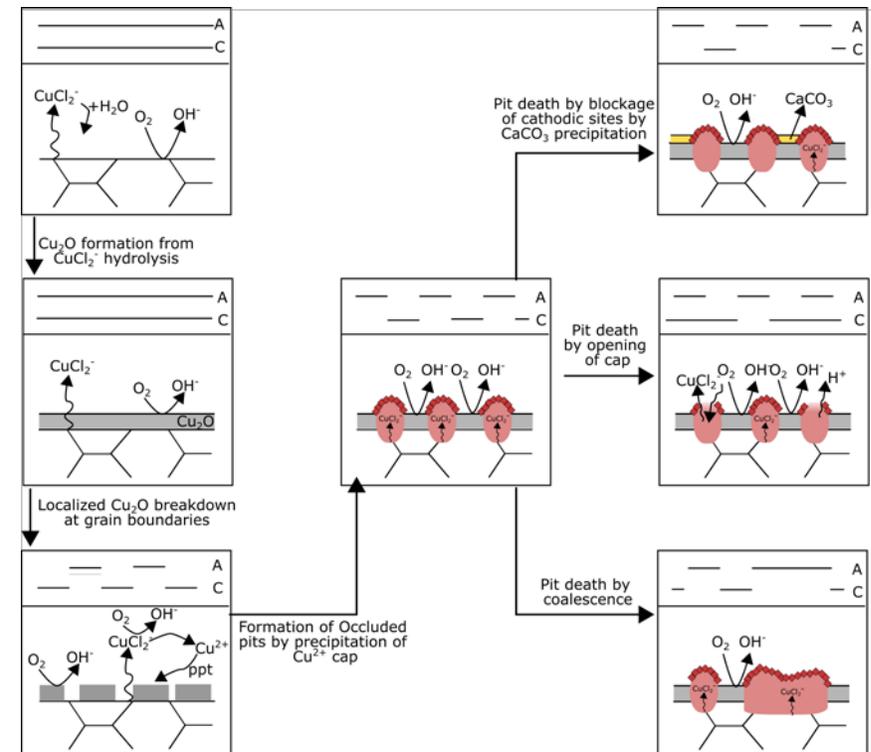
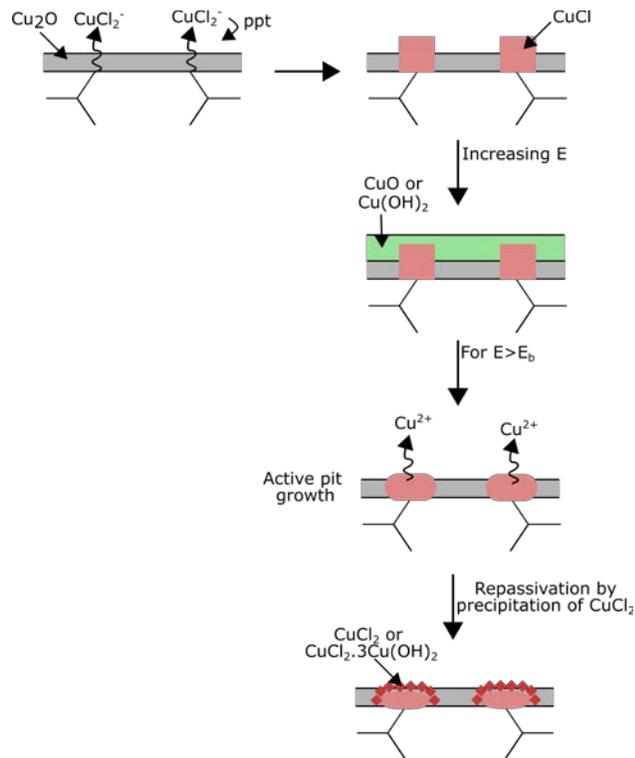
LOCALIZED CORROSION

- Pitting corrosion → non-uniform general corrosion
 - Only in aerobic early post closure phase



LOCALIZED CORROSION

- Pitting corrosion → non-uniform general corrosion
 - Only in aerobic early post closure phase
- Under-deposit corrosion → form of crevice corrosion
 - underneath precipitated surface film that acts as selective ion exchange membrane to create permanent anodic region



CALCULATION METHODS OF LOCALIZED CORROSION IN PA

- Empirical pitting factor

- Pitting factors from bronze-age artifacts i.e. 3000 years: 2-5
- Pitting factors from 50-80 year buried lightning conductor plates: 0-5

➔ Pessimistic pitting factor of 5 for buried copper containers

↳ Overly conservative due to shift to more general corrosion → expected to decrease in time

CALCULATION METHODS OF LOCALIZED CORROSION IN PA

- Empirical pitting factor

- Pitting factors from bronze-age artifacts i.e. 3000 years: 2-5
- Pitting factors from 50-80 year buried lightning conductor plates: 0-5



Pessimistic pitting factor of 5 for buried copper containers



Overly conservative due to shift to more general corrosion → expected to decrease in time

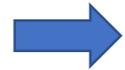
- Empirical amount of surface roughening

- Depending on concept:
 - KBS-3 → $\pm 50 \mu\text{m}$
 - Canadian → $100 \mu\text{m}$
- Needed when calculating under-deposit corrosion

CALCULATION METHODS OF LOCALIZED CORROSION IN PA

- Empirical pitting factor

- Pitting factors from bronze-age artifacts i.e. 3000 years: 2-5
- Pitting factors from 50-80 year buried lightning conductor plates: 0-5



Pessimistic pitting factor of 5 for buried copper containers



Overly conservative due to shift to more general corrosion → expected to decrease in time

- Empirical amount of surface roughening

- Depending on concept:
 - KBS-3 → ± 50 μm
 - Canadian → 100 μm
- Needed when calculating under-deposit corrosion

- Extreme-value statistical analysis

- $F(x) = \exp[-\exp(-ax + b)]$

KBS-3 design:



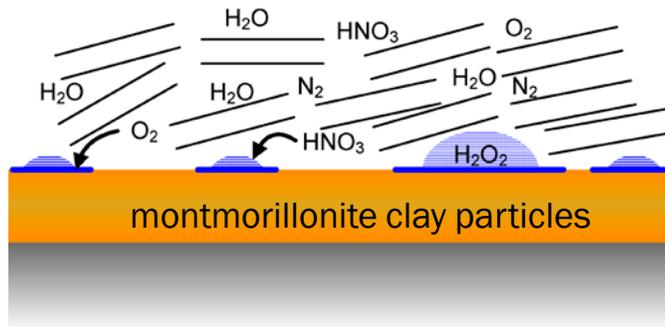
- 10^{-6} chance of a pit exceeding 7.5 mm after 10^6 years
- 10^{-6} chance of a pit exceeding 5 mm after just 10 years

- Copper will not passivate under repository conditions → not meaningful to use

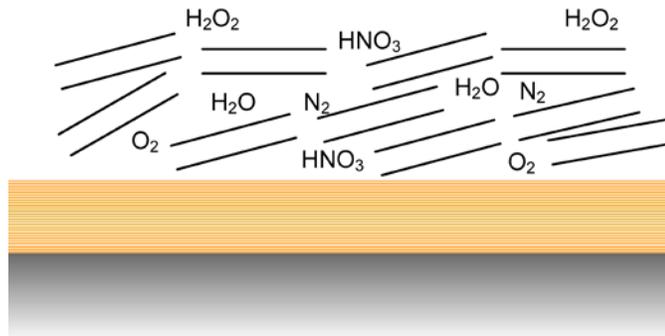
RADIATION ASSISTED CORROSION

- Radiolysis transients in the near-field

Absorption of HNO_3 formed by the radiolysis of humid air by liquid droplets on a non-uniformly wetted surface



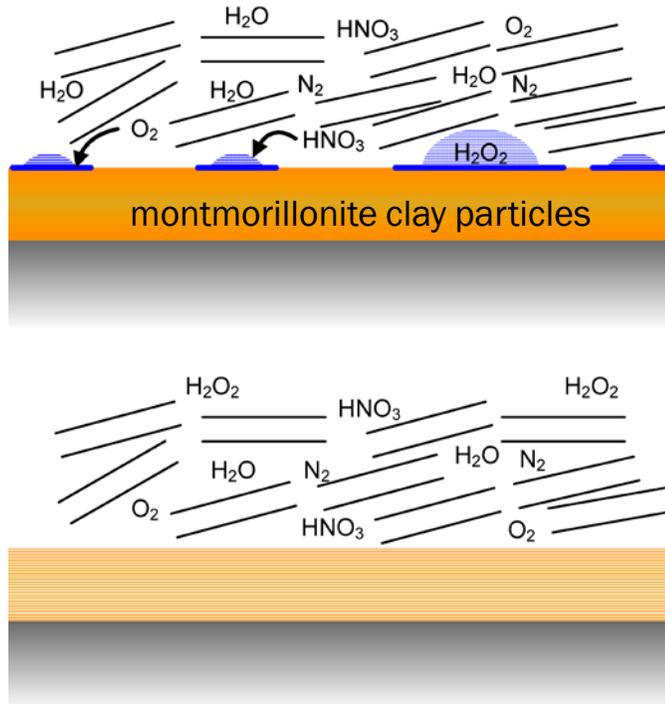
Radiolysis of humid air during a period when the container surface is dry



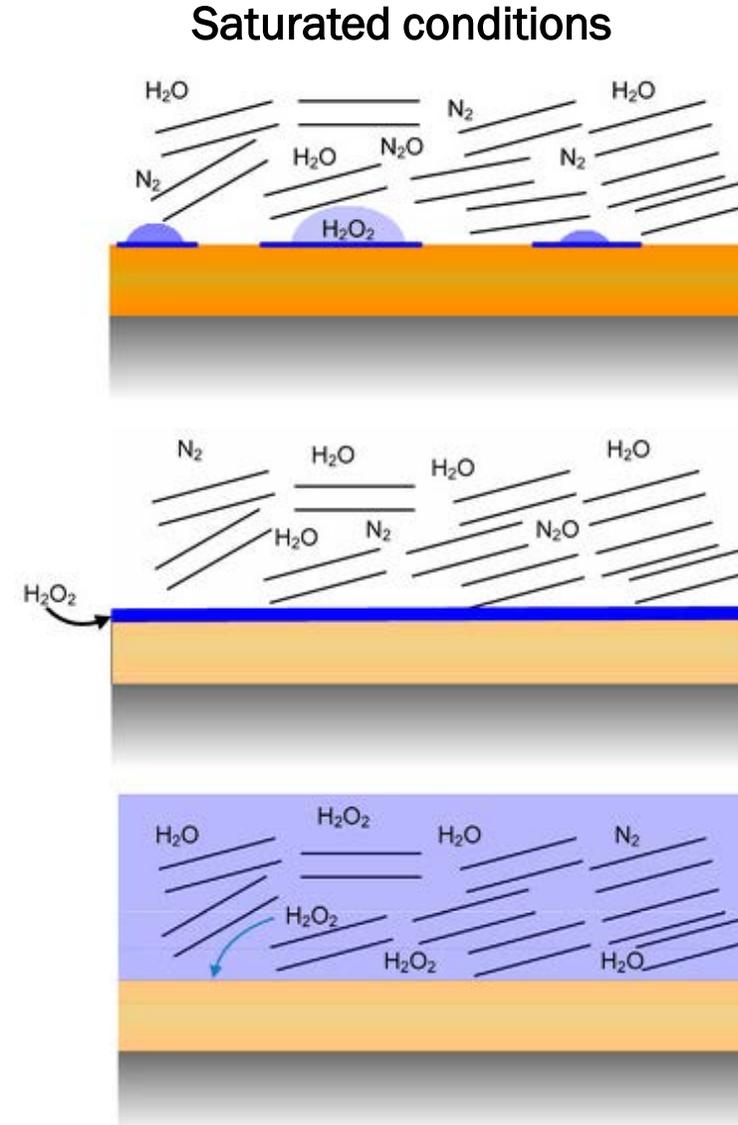
RADIATION ASSISTED CORROSION

- Radiolysis transients in the near-field

Absorption of HNO_3 formed by the radiolysis of humid air by liquid droplets on a non-uniformly wetted surface



Radiolysis of humid air during a period when the container surface is dry



Radiolysis of N_2 - H_2O following consumption of the initially trapped O_2 & radiolysis of liquid droplets following re-wetting of the container surface

Radiolysis of a thin surface water layer following complete wetting of the surface, with continued radiolysis of a humid N_2 - H_2O atmosphere

Radiolysis of a bulk aqueous phase following complete saturation of the buffer box

CALCULATION METHODS RADIATION ASSISTED CORROSION

- Mass balance of radiolytic produced oxidants

- Unsaturated conditions:

- calculation radiolytic yield/volume
 - assume oxidants produced will react

} → Bounding value

→ Used to calculate HNO_3 from γ -radiation in container buffer gap in KBS-3 concept

- $\text{HNO}_3 = (G \times V \times \rho \times D_0/A_v) \times (T/\ln 2) \times (1 - e^{-\ln 2 \cdot t/T})$
 - 0.015 mol HNO_3 & corrosion depth < 7 nm

- Saturated conditions:

- Radiolysis of $\text{H}_2\text{O} \rightarrow \text{H}_2 + \text{oxidants}$ that can cause corrosion → assumptions:
 - volume around container where all oxidants reach surface
 - Moles of oxidants produced/moles of metals corroded uniformly fixed
 - KBS-3 concept: volume 5 mm and Cu is oxidized as efficiently as dissolved $\text{Fe}^{2+} \rightarrow 14 \mu\text{m}$

RADIATION ASSISTED CORROSION

- Reasoned argument for exclusion
 - < 10 Gy/h \rightarrow no or inhibiting effect
 - > 10 Gy/h \rightarrow no consensus. No consistent effect of increasing cumulative dose
 - Mechanistic impact \rightarrow dose rate is key factor influencing corrosion rate
 - Surface dose rate 0.055 Gy/h (KBS-3) – 1 Gy/h (Canadian design)

RADIATION ASSISTED CORROSION

- Reasoned argument for exclusion

- < 10 Gy/h \rightarrow no or inhibiting effect
- > 10 Gy/h \rightarrow no consensus. No consistent effect of increasing cumulative dose
- Mechanistic impact \rightarrow dose rate is key factor influencing corrosion rate
- Surface dose rate 0.055 Gy/h (KBS-3) – 1 Gy/h (Canadian design)
- No corrosion enhancement

MICROBIOLOGICALLY INFLUENCED CORROSION

- Mass transport

- Pessimistically bounded by the supply of nutrients, i.e. organic matter

- Assumptions 1D diffusion calculation for HS⁻ transport

- [HS⁻] in backfill maintained at 0.1 mM
- Diffusivity set as that for uncharged species
- Corrosion on lid & topmost 10% of the container height

Corrosion depth of 2 mm

- Canadian system corrosion allowance of 1 mm if buffer remains intact

MICROBIOLOGICALLY INFLUENCED CORROSION

- Mass transport

- Pessimistically bounded by the supply of nutrients, i.e. organic matter

- Assumptions 1D diffusion calculation for HS^- transport

- $[\text{HS}^-]$ in backfill maintained at 0.1 mM
- Diffusivity set as that for uncharged species
- Corrosion on lid & topmost 10% of the container height

Corrosion depth of 2 mm

- Canadian system corrosion allowance of 1 mm if buffer remains intact

- Contribution of H_2 to HS^- production

- Based on amounts of steel with assumption that all produced HS^- reacts → corrosion loss of 300 μm

MICROBIOLOGICALLY INFLUENCED CORROSION

- Mass transport

- Pessimistically bounded by the supply of nutrients, i.e. organic matter

- Assumptions 1D diffusion calculation for HS⁻ transport

- [HS⁻] in backfill maintained at 0.1 mM
- Diffusivity set as that for uncharged species
- Corrosion on lid & topmost 10% of the container height

Corrosion depth of 2 mm

- Canadian system corrosion allowance of 1 mm if buffer remains intact

- Contribution of H₂ to HS⁻ production

- Based on amounts of steel with assumption that all produced HS⁻ reacts → corrosion loss of 300 μm

- Empirical rates of HS⁻ formation

- Experiments in favorable conditions → converted in corrosion rate → pessimistic thickness loss of 3 mm after 10⁶ years

MICROBIOLOGICALLY INFLUENCED CORROSION

- **Mass transport**

- Pessimistically bounded by the supply of nutrients, i.e. organic matter

- Assumptions 1D diffusion calculation for HS^- transport

- $[\text{HS}^-]$ in backfill maintained at 0.1 mM
- Diffusivity set as that for uncharged species
- Corrosion on lid & topmost 10% of the container height

Corrosion depth of 2 mm

- Canadian system corrosion allowance of 1 mm if buffer remains intact

- Contribution of H_2 to HS^- production

- Based on amounts of steel with assumption that all produced HS^- reacts → corrosion loss of 300 μm

- **Empirical rates of HS^- formation**

- Experiments in favorable conditions → converted in corrosion rate → pessimistic thickness loss of 3 mm after 10^6 years

- **Reasoned arguments for exclusion**

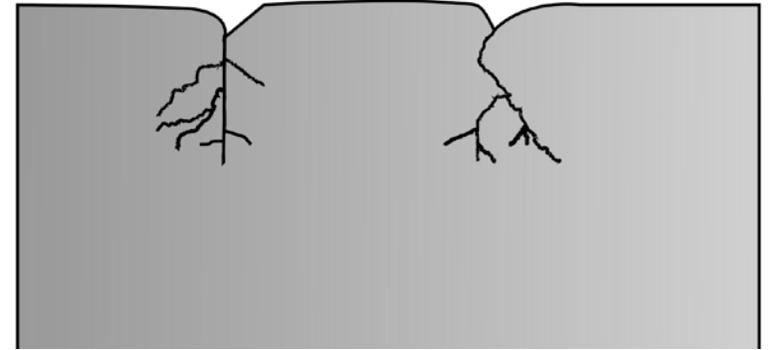
- Swedish SR-Site & Finish safety case

- High density of compacted bentonite

- Low water activity
- High swelling pressure
- Lack of physical space

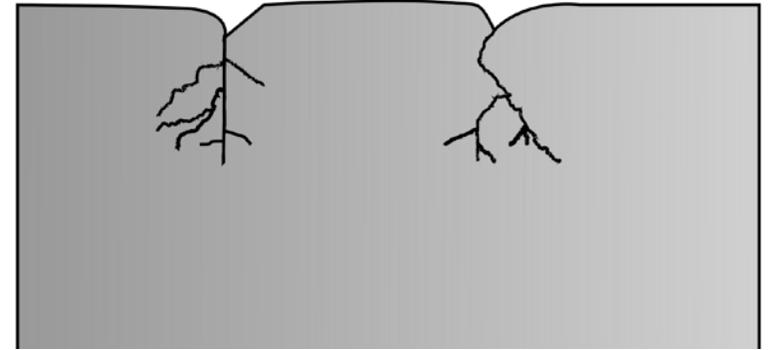
ENVIRONMENTAL - ASSISTED CRACKING

- Stress corrosion cracking
 - Stress + aggressive ions + oxidizing ions → unlikely
 - No mechanistic arguments
 - Experimentally validated by mixed-potential modelling of E_{corr} of copper
 - E_{corr} & surface pH → CuO_2/CuO surface film not thermodynamically stable
 - Not considered in Canadian concept
 - pH & corrosion potential far from range in which SCC is feasible



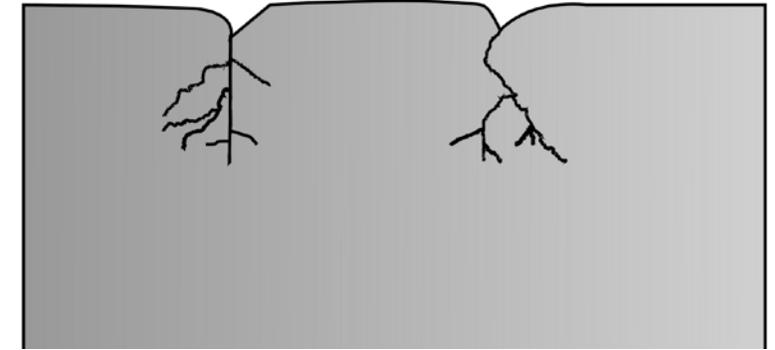
ENVIRONMENTAL - ASSISTED CRACKING

- Stress corrosion cracking
 - Stress + aggressive ions + oxidizing ions → unlikely
 - No mechanistic arguments
 - Experimentally validated by mixed-potential modelling of E_{corr} of copper
 - E_{corr} & surface pH → CuO_2/CuO surface film not thermodynamically stable
 - Not considered in Canadian concept
 - pH & corrosion potential far from range in which SCC is feasible
 - Crack-like defects observed in experiments in HS^- solution
 - HS^- transport sufficiently slow → corrosion transport-limited
 - HS^- fluxes at the surface too low to give the experimentally observed effects



ENVIRONMENTAL - ASSISTED CRACKING

- Stress corrosion cracking
 - Stress + aggressive ions + oxidizing ions → unlikely
 - No mechanistic arguments
 - Experimentally validated by mixed-potential modelling of E_{corr} of copper
 - E_{corr} & surface pH → CuO_2/CuO surface film not thermodynamically stable
 - Not considered in Canadian concept
 - pH & corrosion potential far from range in which SCC is feasible
 - Crack-like defects observed in experiments in HS^- solution
 - HS^- transport sufficiently slow → corrosion transport-limited
 - HS^- fluxes at the surface too low to give the experimentally observed effects



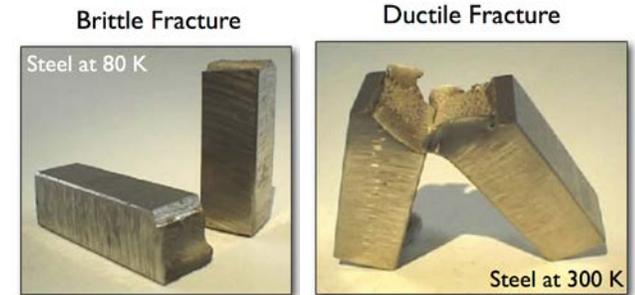
➔ Reasoned arguments for non-susceptibility

MECHANICAL DEGRADATION & COMBINED CORROSION - MECHANICAL EFFECTS

- Modes of mechanical degradation

- Fracture

- brittle fracture → caused by some form of embrittlement
 - ductile fracture → cup & cone dimpled fracture structure



- Plastic deformation

- metal overloaded past its yield strength
 - avoided by container design i.e. wall thickness

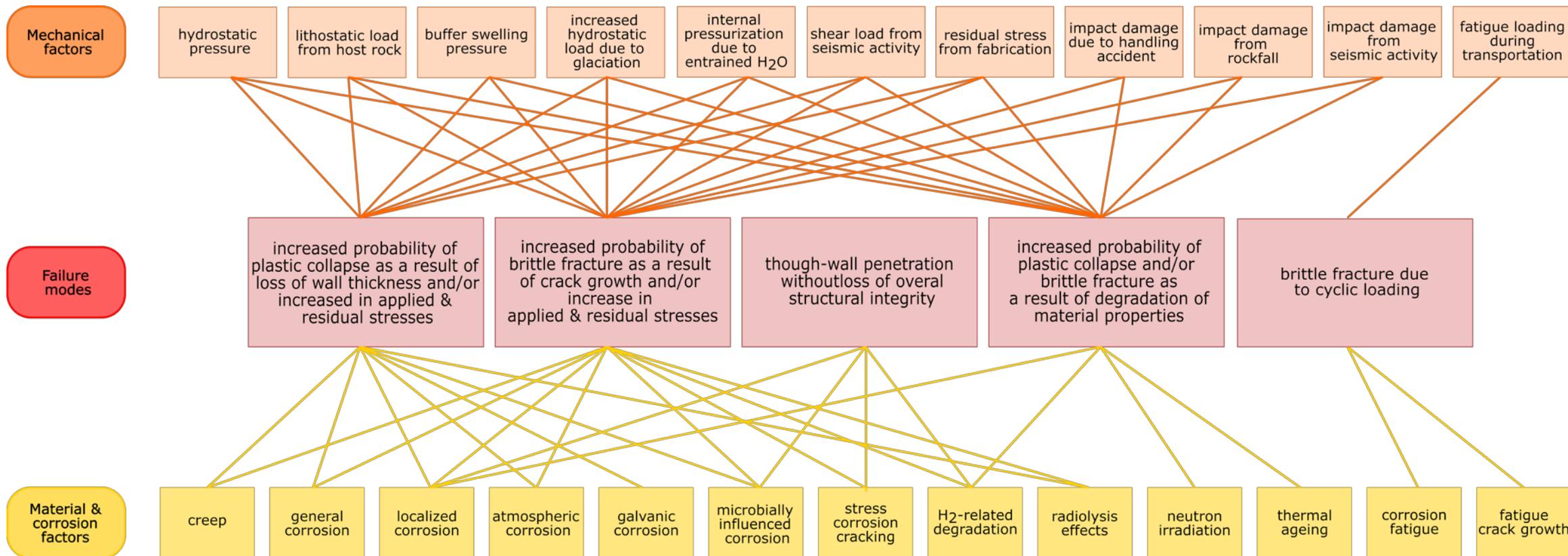


- Creep

- Slow deformation under influence of an applied static load below the yield stress
 - O₂-free P-doped copper → higher creep ductility

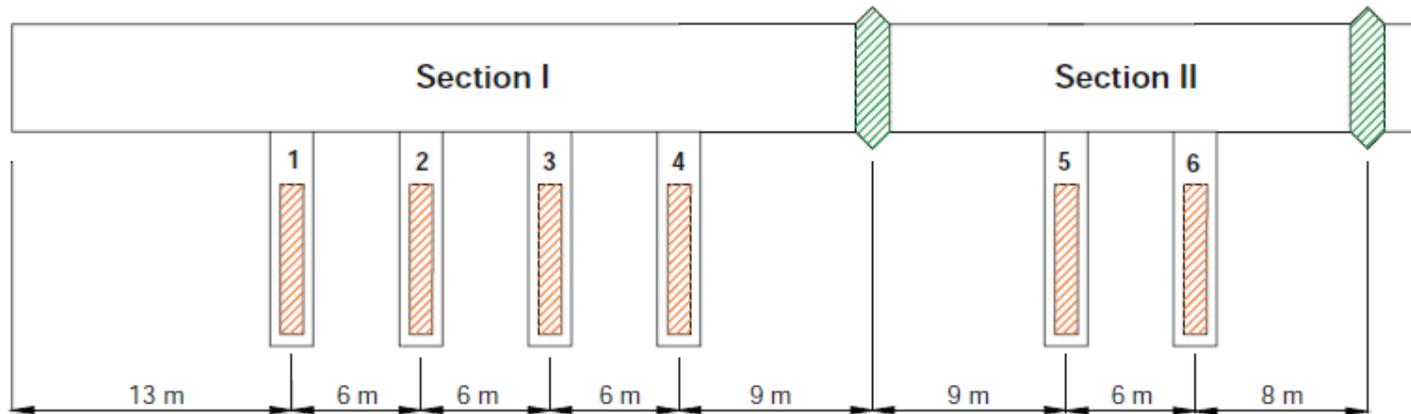


MECHANICAL & MATERIAL-RELATED FACTORS LEADING TO CONTAINER FAILURE & THEIR RELATIONSHIP TO VARIOUS FAILURE MODES



IN-SITU TESTING OF COPPER SPENT FUEL CONTAINERS

- Prototype Repository Experiment
 - Simulate conditions in KBS-3 repository
 - 6 full-sized dual-shell copper containers within vertical deposition holes in contact with bentonite
 - containers heated

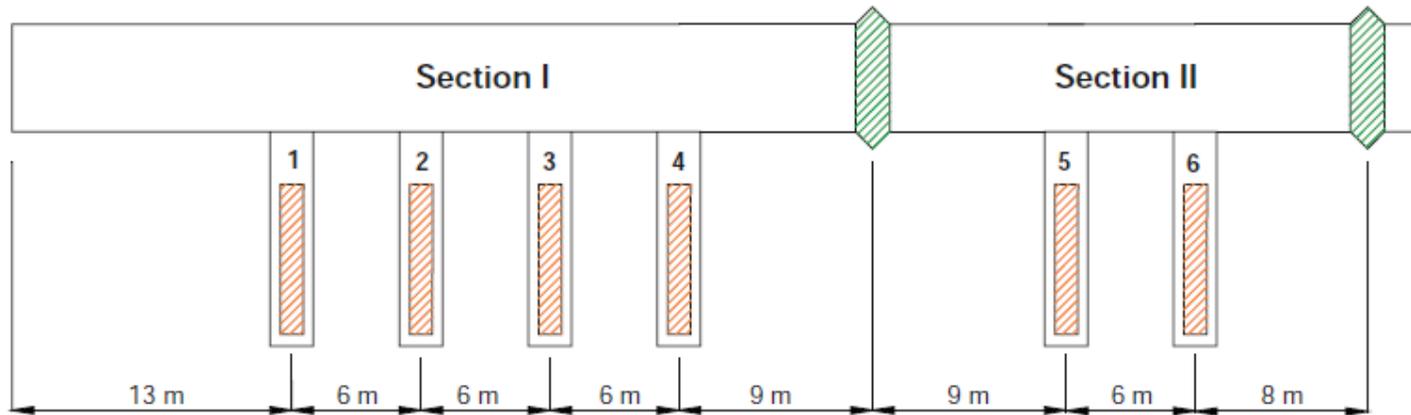


IN-SITU TESTING OF COPPER SPENT FUEL CONTAINERS

- Prototype Repository Experiment

- Simulate conditions in KBS-3 repository

- 6 full-sized dual-shell copper containers within vertical deposition holes in contact with bentonite
 - containers heated



- Shift to anaerobic conditions
 - Low level of corrosion
 - No microbial activity in bentonite buffer, low amount in backfill

PREDICTION OF CONTAINER LIFETIMES & IMPLICATIONS FOR PA

- KBS-3 concept
 - Max. corrosion loss by each mechanism over period of 10^6 year
 - Absence erosion/corrosion scenarios → no process > few mm
 - Sum is expected to be overestimate of the true expected corrosion loss
 - Even most conservative: total loss over 10^6 year < 5 mm

PREDICTION OF CONTAINER LIFETIMES & IMPLICATIONS FOR PA

- KBS-3 concept
 - Max. corrosion loss by each mechanism over period of 10^6 year
 - Absence erosion/corrosion scenarios → no process > few mm
 - Sum is expected to be overestimate of the true expected corrosion loss
 - Even most conservative: total loss over 10^6 year < 5 mm
 - Erosion → >> but extreme high rates only in least favorable conditions
 - Statistical analysis → 0-2 containers would fail within 10^6 year once uncertainties are taken into account

PREDICTION OF CONTAINER LIFETIMES & IMPLICATIONS FOR PA

- **KBS-3 concept**
 - Max. corrosion loss by each mechanism over period of 10^6 year
 - Absence erosion/corrosion scenarios → no process > few mm
 - Sum is expected to be overestimate of the true expected corrosion loss
 - Even most conservative: total loss over 10^6 year < 5 mm
 - Erosion → >> but extreme high rates only in least favorable conditions
 - Statistical analysis → 0-2 containers would fail within 10^6 year once uncertainties are taken into account
- **Canadian system**
 - Expected corrosion 0.27 mm over 10^6 year (conservative max. of 1.02 mm)
 - Assuming fixed $[HS^-]$ of 0.1 ppm at bentonite-rock interface for “expected value” and 1 ppm for “max value”

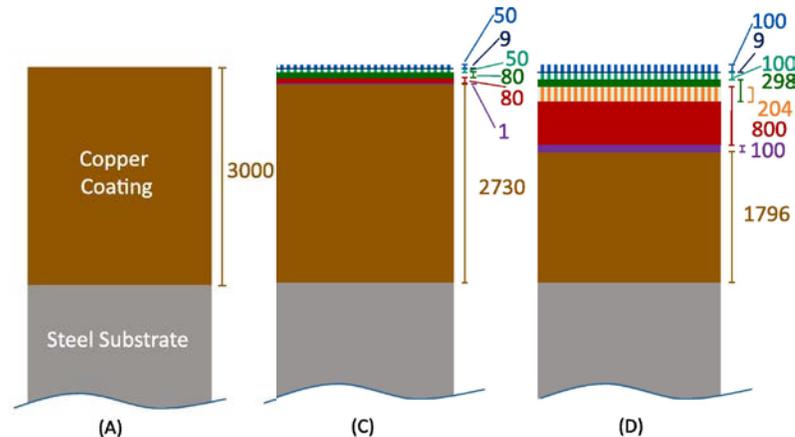


Illustration of cross sections for the Canadian used fuel container with relevant dimensions in μm for (A) the as-manufactured container; Maximum corrosion damage from non-uniform radiation-induced (light blue), radiation-induced (blue), non-uniform oxic (light green), oxic corrosion (green), sulphide corrosion (red), anoxic (purple), (C) current analysis, and (D) extreme upper bound.

SUMMARY OF APPROACHES FOR CORROSION IN PA FOR COPPER CONTAINERS

Mode of corrosion	Canada	Finland	Sweden	Switzerland	UK
Oxidic general corrosion	Mass balance within corrosion allowance				
Radiolysis-induced corrosion	Excluded or Mass balance within corrosion allowance				
Sulfide-induced anaerobic corrosion	Mass transport controlled – key factor driving corrosion allowance				
MIC before saturation		Excluded by reasoned argument			
SCC	Excluded by reasoned argument				
Pitting	Fixed corrosion allowance to account for surface roughening		Fixed corrosion allowance to account for surface roughening		

CONTENT

- Introduction
- Copper container corrosion
- Steel-bentonite models
- Integration of corrosion phenomena in performance assessments
- Performance assessments for copper-based canister corrosion
- **Performance assessments for iron-based alloy canister corrosion**
 - Atmospheric corrosion
 - General corrosion
 - Localised corrosion
 - Radiation assisted corrosion
 - Microbially influenced corrosion
 - Environmental-assisted cracking
 - Weld corrosion
 - Prediction of canister lifetimes and implications for PA

PA FOR IRON-BASED ALLOY CONTAINER CORROSION

- Low strength, low carbon alloys but \neq among countries
- Belgium, France, Japan, Switzerland and UK



PA FOR IRON-BASED ALLOY CONTAINER CORROSION

- Low strength, low carbon alloys but \neq among countries
- Belgium, France, Japan, Switzerland and UK
- Carbon steel
 - Corrosion mechanisms well characterized & predictable
 - Readily available & cheap



PA FOR IRON-BASED ALLOY CONTAINER CORROSION

- Low strength, low carbon alloys but \neq among countries
- Belgium, France, Japan, Switzerland and UK
- Carbon steel
 - Corrosion mechanisms well characterized & predictable
 - Readily available & cheap
 - Bentonite
 - Cementitious buffer
 - Crushed rock
 - Lifetime requirement of 1000 years



PA FOR IRON-BASED ALLOY CONTAINER CORROSION

- Low strength, low carbon alloys but \neq among countries
- Belgium, France, Japan, Switzerland and UK
- Carbon steel
 - Corrosion mechanisms well characterized & predictable
 - Readily available & cheap
 - Bentonite
 - Cementitious buffer \rightarrow stable passivating magnetite film
 - Crushed rock
 - Lifetime requirement of 1000 years



PA FOR IRON-BASED ALLOY CONTAINER CORROSION

- Low strength, low carbon alloys but \neq among countries
- Belgium, France, Japan, Switzerland and UK
- Carbon steel
 - Corrosion mechanisms well characterized & predictable
 - Readily available & cheap
 - Bentonite
 - Cementitious buffer \rightarrow stable passivating magnetite film
 - Crushed rock
 - Lifetime requirement of 1000 years

$\rightarrow H_2$

buffer destabilization

French design



PA FOR IRON-BASED ALLOY CONTAINER CORROSION

- Low strength, low carbon alloys but ≠ among countries
- Belgium, France, Japan, Switzerland and UK
- Carbon steel

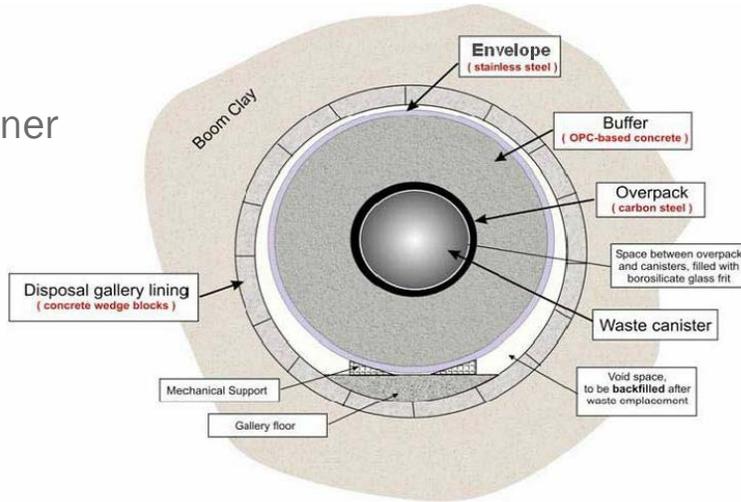
- Corrosion mechanisms well characterized & predictable
 - Readily available & cheap
 - Bentonite
 - Cementitious buffer → stable passivating magnetite film
 - Crushed rock
 - Lifetime requirement of 1000 years
- alter characteristics
- H₂ Fe²⁺
- buffer destabilization



LIFETIME CONTAINERS IN DIFFERENT CONCEPTS

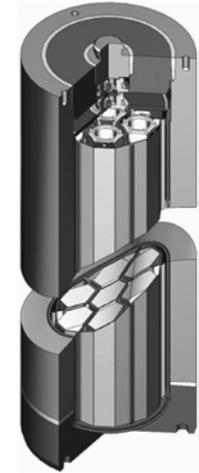
- Belgium:

- Supercontainer
- 5000 years



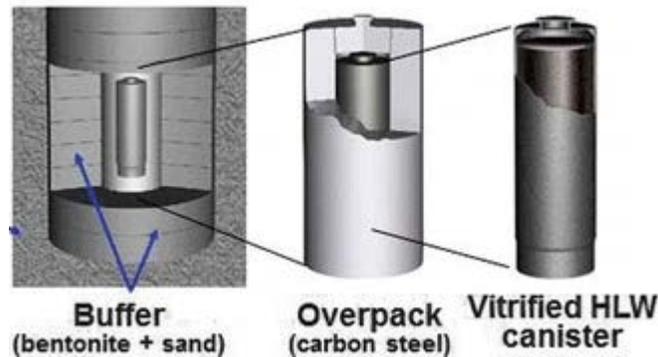
- Czech Republic

- Double walled:
 - inner stainless steel layer
 - outer carbon steel layer
- 10000 years



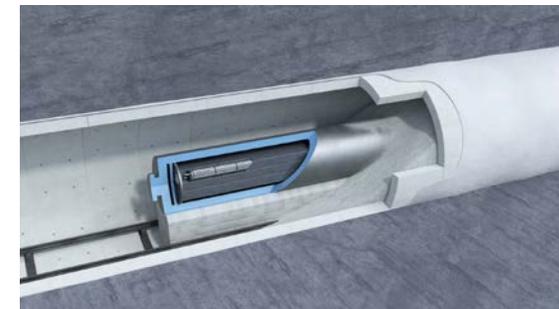
- Japan

- Double walled
- 1000 year



- Switzerland

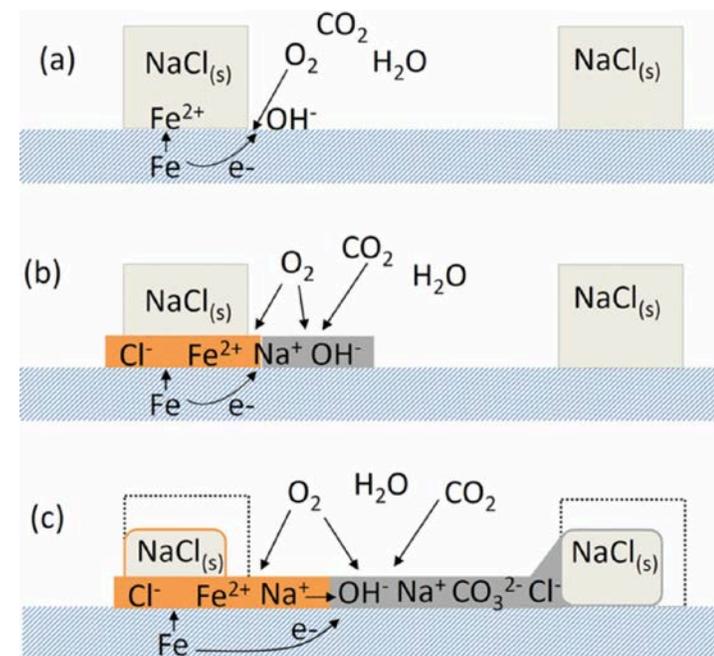
- 10000 year



ATMOSPHERIC CORROSION

- Dependent on the relative humidity
 - < 60 % RH → extremely slow
 - salts deposits

Schematic interpretation of the development of corrosion chemistry associated with NaCl crystals on a mild steel substrate below 76% RH



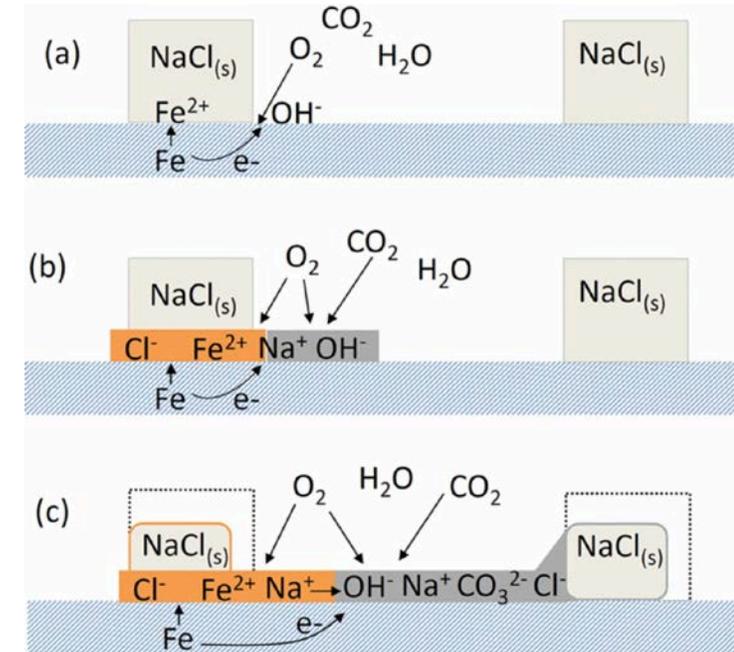
Upon initiation of corrosion (a), discrete chemistries develop at the anodic (orange) and cathodic (gray) sites (b), the extent to which is dependent on time and humidity level. At higher RH and longer times (c), puddles of catholyte develop on the surface that can substantially dissolve the NaCl crystals.

ATMOSPHERIC CORROSION

- Dependent on the relative humidity
 - < 60 % RH → extremely slow
 - salts deposits
- Initial dry period → corrosion < 100 μm

➔ Corrosion allowance < 1 mm

Schematic interpretation of the development of corrosion chemistry associated with NaCl crystals on a mild steel substrate below 76% RH

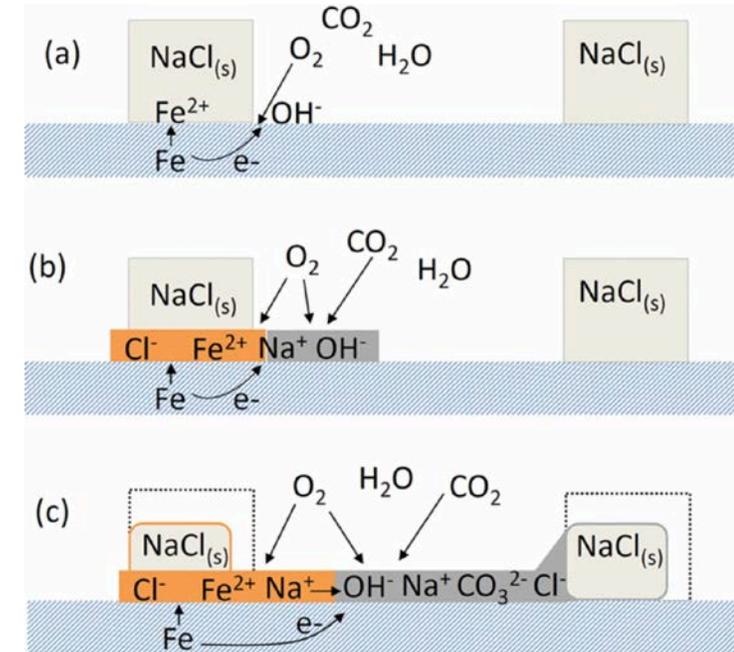


Upon initiation of corrosion (a), discrete chemistries develop at the anodic (orange) and cathodic (gray) sites (b), the extent to which is dependent on time and humidity level. At higher RH and longer times (c), puddles of catholyte develop on the surface that can substantially dissolve the NaCl crystals.

ATMOSPHERIC CORROSION

- Dependent on the relative humidity
 - < 60 % RH → extremely slow
 - salts deposits
 - Initial dry period → corrosion < 100 μm
- ➔ Corrosion allowance < 1 mm
- ~ embedded iron in subterranean environments: few μm/year

Schematic interpretation of the development of corrosion chemistry associated with NaCl crystals on a mild steel substrate below 76% RH

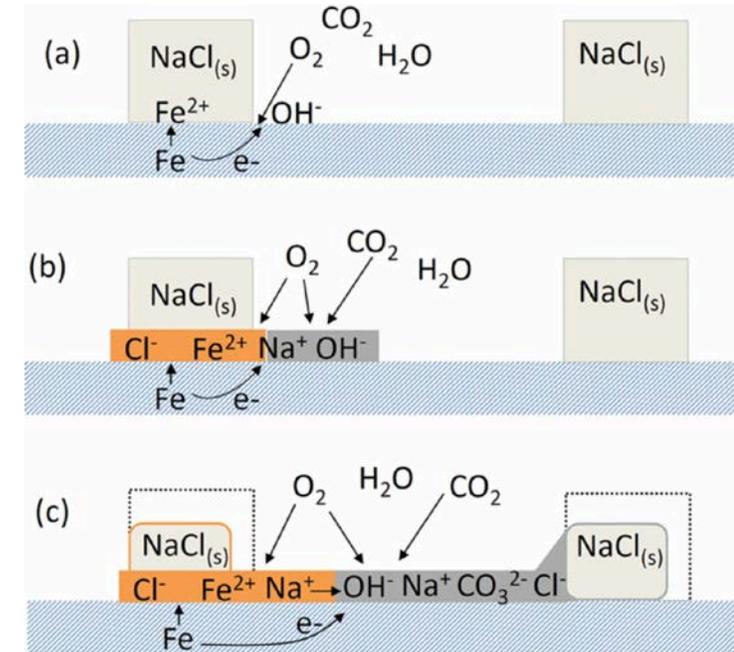


Upon initiation of corrosion (a), discrete chemistries develop at the anodic (orange) and cathodic (gray) sites (b), the extent to which is dependent on time and humidity level. At higher RH and longer times (c), puddles of catholyte develop on the surface that can substantially dissolve the NaCl crystals.

ATMOSPHERIC CORROSION

- Dependent on the relative humidity
 - < 60 % RH → extremely slow
 - salts deposits
 - Initial dry period → corrosion < 100 μm
- ➔ Corrosion allowance < 1 mm
- ~ embedded iron in subterranean environments: few μm/year
 - Fe (hydr)oxides → not expected to directly significantly undermine the integrity of the containers in environments of limited corrosivity
 - Impact of layer of rust?

Schematic interpretation of the development of corrosion chemistry associated with NaCl crystals on a mild steel substrate below 76% RH



Upon initiation of corrosion (a), discrete chemistries develop at the anodic (orange) and cathodic (gray) sites (b), the extent to which is dependent on time and humidity level. At higher RH and longer times (c), puddles of catholyte develop on the surface that can substantially dissolve the NaCl crystals.

UNIFORM GENERAL CORROSION

- Long-term anoxic conditions
- $\pm 1 \mu\text{m}/\text{year}$ ~ natural analogues $0.1 \mu\text{m}/\text{year}$

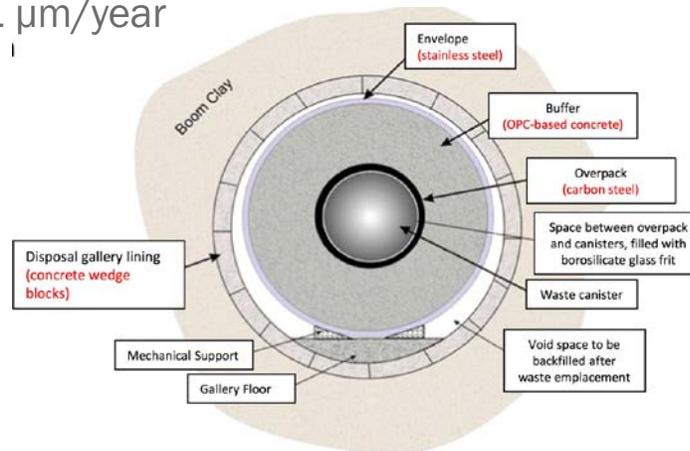
UNIFORM GENERAL CORROSION

- Long-term anoxic conditions
- $\pm 1 \mu\text{m}/\text{year}$ ~ natural analogues $0.1 \mu\text{m}/\text{year}$
- Czech Republic
 - outer carbon steel container:
 - mass loss over 4-month period $\rightarrow 5 \mu\text{m}/\text{year}$
 - conservative



UNIFORM GENERAL CORROSION

- Long-term anoxic conditions
- $\pm 1 \mu\text{m}/\text{year} \sim$ natural analogues $0.1 \mu\text{m}/\text{year}$
- Czech Republic
 - outer carbon steel container:
 - mass loss over 4-month period $\rightarrow 5 \mu\text{m}/\text{year}$
 - conservative
- Belgium
 - stable magnetite film $\rightarrow 0.1 \mu\text{m}/\text{year}$



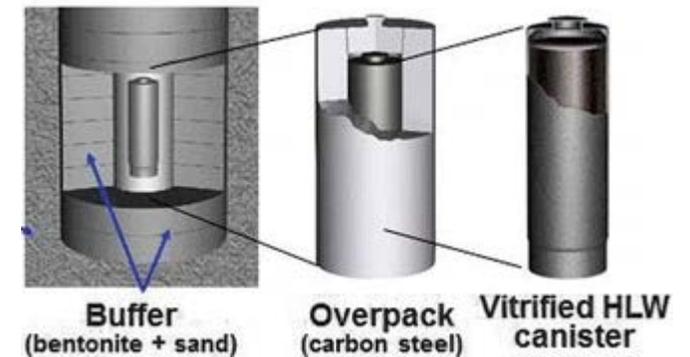
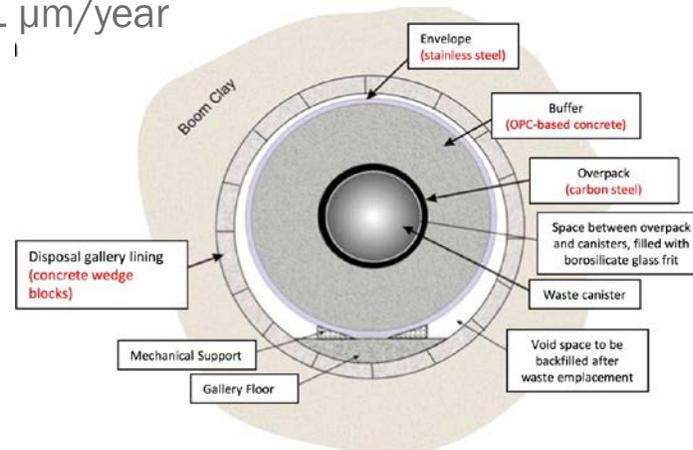
UNIFORM GENERAL CORROSION

- Long-term anoxic conditions
- $\pm 1 \mu\text{m}/\text{year} \sim$ natural analogues $0.1 \mu\text{m}/\text{year}$
- Czech Republic
 - outer carbon steel container:
 - mass loss over 4-month period $\rightarrow 5 \mu\text{m}/\text{year}$
 - conservative
- Belgium
 - stable magnetite film $\rightarrow 0.1 \mu\text{m}/\text{year}$

- Japan

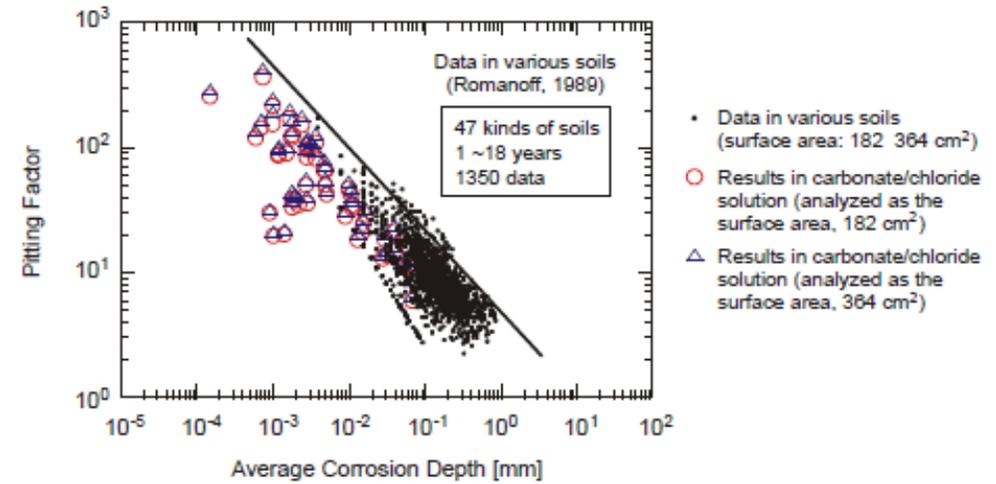
- Lab tests:

- corrosion rates dropped after 1 year
 - linear for several years at $2 \mu\text{m}/\text{year}$
 - 2 mm over 1000 year but pitting factor of 3 \rightarrow 6 mm corrosion allowance



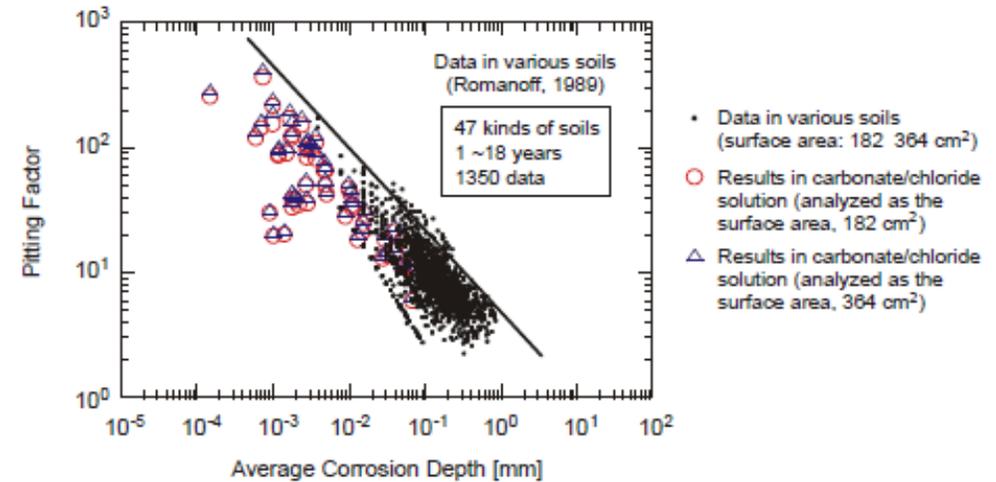
LOCALIZED CORROSION

- Only considered feasible in early oxic period
- Long-term field burial tests: pitting factors 100 → 10



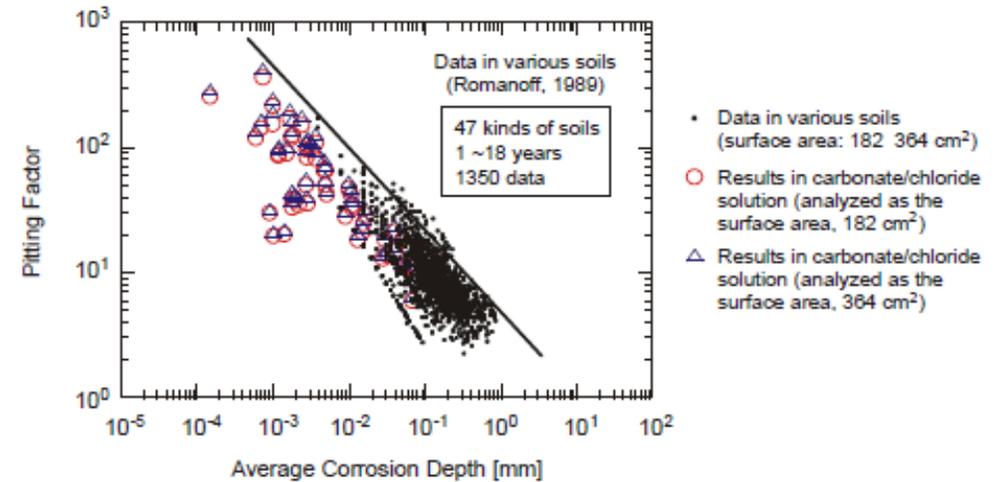
LOCALIZED CORROSION

- Only considered feasible in early oxic period
- Long-term field burial tests: pitting factors 100 → 10
- Swiss concept:
 - pitting corrosion allowance 10 mm in oxic phase



LOCALIZED CORROSION

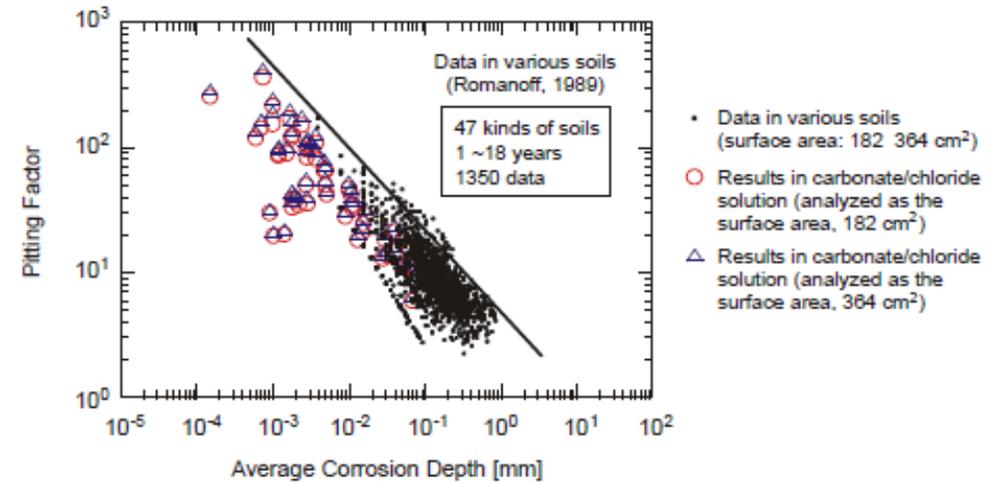
- Only considered feasible in early oxic period
- Long-term field burial tests: pitting factors 100 → 10
- Swiss concept:
 - pitting corrosion allowance 10 mm in oxic phase
- Japan:
 - Extreme value statistics with assumptions:
 - All O₂ in buffer & backfill consumed by pitting corrosion
 - No residual O₂ from tunnel reaches the container surface



LOCALIZED CORROSION

- Only considered feasible in early oxic period
- Long-term field burial tests: pitting factors 100 → 10
- Swiss concept:
 - pitting corrosion allowance 10 mm in oxic phase
- Japan:
 - Extreme value statistics with assumptions:
 - All O₂ in buffer & backfill consumed by pitting corrosion
 - No residual O₂ from tunnel reaches the container surface

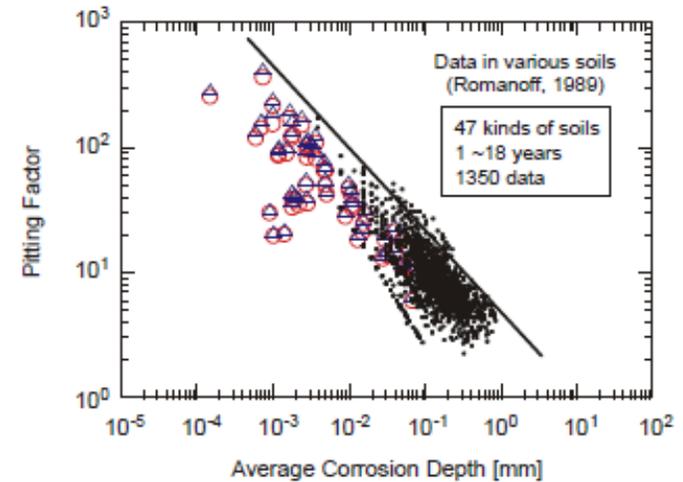
corrosion allowance 5-12 mm



LOCALIZED CORROSION

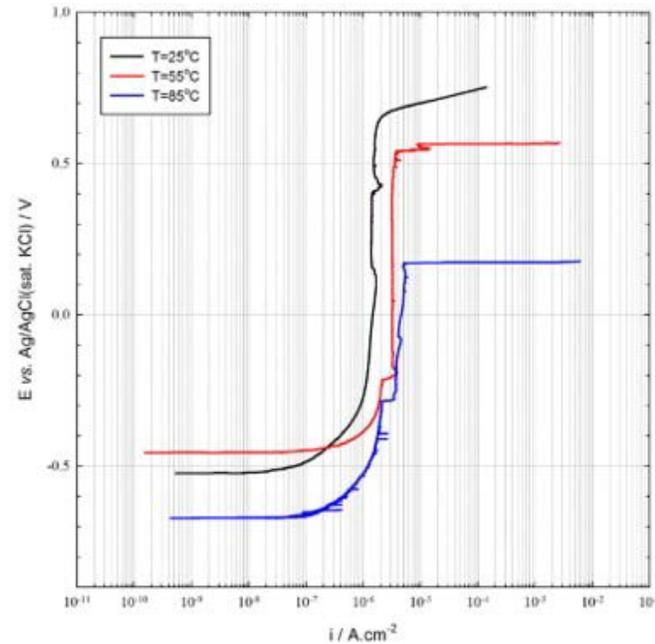
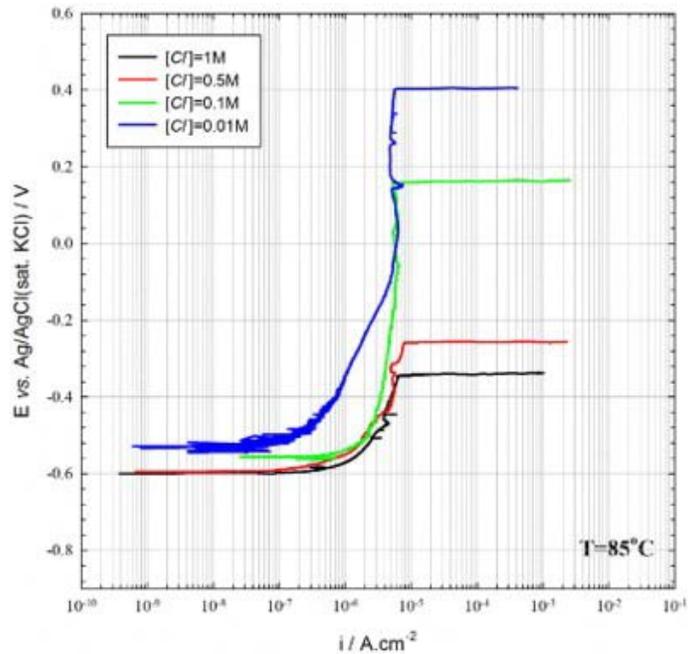
- Only considered feasible in early oxic period
- Long-term field burial tests: pitting factors 100 → 10
- Swiss concept:
 - pitting corrosion allowance 10 mm in oxic phase
- Japan:
 - Extreme value statistics with assumptions:
 - All O₂ in buffer & backfill consumed by pitting corrosion
 - No residual O₂ from tunnel reaches the container surface
 - Conservative

corrosion allowance 5-12 mm



LOCALIZED CORROSION

- Belgian supercontainer
 - Risk if magnetite film break down
 - Examined using electrochemical measurements
 - Dependency on $[Cl^-]$
 - Dependency on temp



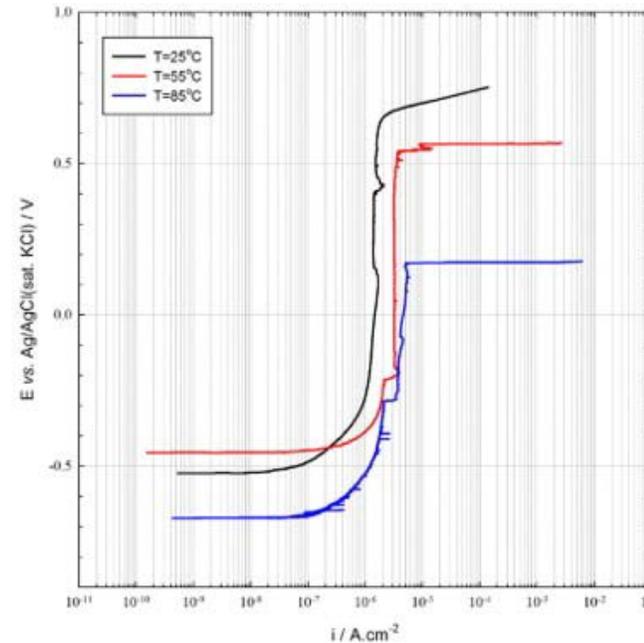
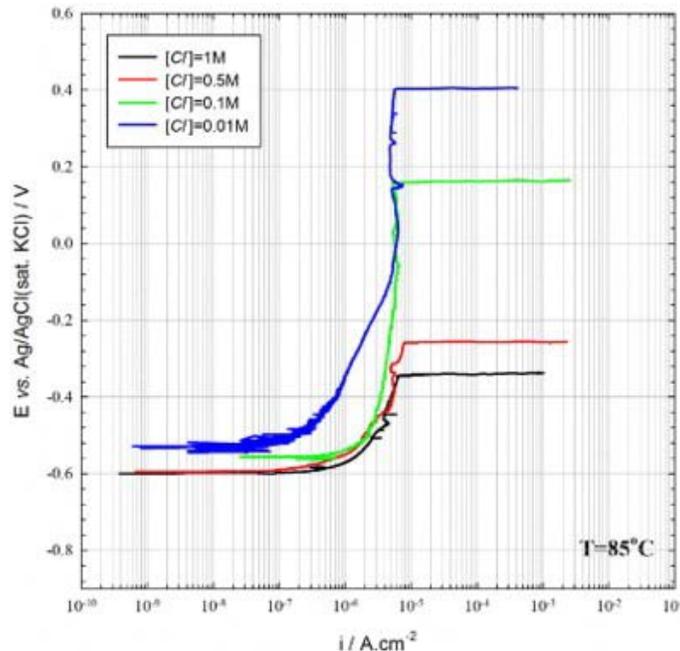
LOCALIZED CORROSION

- Belgian supercontainer

- Risk if magnetite film break down
- Examined using electrochemical measurements

- Dependency on $[Cl^-]$
- Dependency on temp

} Most aggressive conditions (1 M Cl, 85 °C): lowest potential \pm 200 mV



RADIATION-ASSISTED CORROSION

- Unsaturated ↔ saturated phase : $\text{HNO}_3 \leftrightarrow \text{H}_2\text{O}_2$
- Additional oxidation of steel by radiolysis products is small compared to general corrosion loss by H_2O oxidation

RADIATION-ASSISTED CORROSION

- Unsaturated ↔ saturated phase : $\text{HNO}_3 \leftrightarrow \text{H}_2\text{O}_2$
- Additional oxidation of steel by radiolysis products is small compared to general corrosion loss by H_2O oxidation
- Long-term corrosion tests Andra:
 - 80 Gy/h → increase corrosion rate
 - 20 Gy/h → no effect
- Swiss concept
 - Wall thickness container 14 cm → radiation shielding dose rate ± 0.2 Gy/h
- Czech concept
 - 0.3 Gy/h
- Japanese concept
 - 80 mm shielding allowance → surface dose rate $\ll 3$ Gy/h
- Belgian concept
 - No effect on anaerobic corrosion rate up to 25 Gy/h

} External surface dose rate < 10 Gy/h

RADIATION-ASSISTED CORROSION

- Unsaturated ↔ saturated phase : $\text{HNO}_3 \leftrightarrow \text{H}_2\text{O}_2$
 - Additional oxidation of steel by radiolysis products is small compared to general corrosion loss by H_2O oxidation
 - Long-term corrosion tests Andra:
 - 80 Gy/h → increase corrosion rate
 - 20 Gy/h → no effect
 - Swiss concept
 - Wall thickness container 14 cm → radiation shielding dose rate ± 0.2 Gy/h
 - Czech concept
 - 0.3 Gy/h
 - Japanese concept
 - 80 mm shielding allowance → surface dose rate $\ll 3$ Gy/h
 - Belgian concept
 - No effect on anaerobic corrosion rate up to 25 Gy/h
- External surface dose rate < 10 Gy/h
- NEGLIGIBLE EFFECT OF RADIOLYSIS
-
- ```
graph LR; A[80 Gy/h → increase corrosion rate] --- B[External surface dose rate < 10 Gy/h]; C[20 Gy/h → no effect] --- B; D[Wall thickness container 14 cm → radiation shielding dose rate ±0.2 Gy/h] --- B; E[0.3 Gy/h] --- B; F[80 mm shielding allowance → surface dose rate << 3 Gy/h] --- B; G[No effect on anaerobic corrosion rate up to 25 Gy/h] --- B; B --> H[NEGLIGIBLE EFFECT OF RADIOLYSIS]
```

## MICROBIOLOGICALLY INFLUENCED CORROSION

- High bentonite density/high pH expected to inhibit microbial activity → SRB only in far field
- Steel corrosion loss due to HS<sup>-</sup> flux << general anaerobic corrosion from H<sub>2</sub>O oxidation
  - Experiment in Opalinus Clay: 0.02 mm over 1000 years ↔ 1 mm

## MICROBIOLOGICALLY INFLUENCED CORROSION

- High bentonite density/high pH expected to inhibit microbial activity → SRB only in far field
- Steel corrosion loss due to  $\text{HS}^-$  flux  $\ll$  general anaerobic corrosion from  $\text{H}_2\text{O}$  oxidation
  - Experiment in Opalinus Clay: 0.02 mm over 1000 years  $\leftrightarrow$  1 mm

## WELD CORROSION

- Japanese concept
  - additional 3 mm corrosion allowance for welded regions → undetected welding defect up to 3 mm depth
  - preferential weld corrosion mitigated by Ni doping on weld material

## ENVIRONMENTAL ASSISTED CRACKING

- **Switzerland:**
  - SCC occurs in  $\text{HCO}_3^-/\text{CO}_3^{2-}$  at pH 6 and pH 10-11 ↔ pH bentonite porewater pH 7.3
  - Crack initiates → stifle due to absence of cyclic loading
- **Japan:**
  - Heat treatment on bulk material & welds eliminate or reduces tensile residual stresses
- **Belgium**
  - Slow strain testing at 140°C with  $[\text{HS}^-]$  up to 15.6 mM fraction properties of plain carbon steel ~ in argon

## ENVIRONMENTAL ASSISTED CRACKING

- **Switzerland:**
  - SCC occurs in  $\text{HCO}_3^-/\text{CO}_3^{2-}$  at pH 6 and pH 10-11 ↔ pH bentonite porewater pH 7.3
  - Crack initiates → stifle due to absence of cyclic loading
- **Japan:**
  - Heat treatment on bulk material & welds eliminate or reduces tensile residual stresses
- **Belgium**
  - Slow strain testing at 140°C with  $[\text{HS}^-]$  up to 15.6 mM fraction properties of plain carbon steel ~ in argon

**SCC UNLIKELY TO OCCUR**

## PREDICTION OF CONTAINER LIFETIMES & IMPLICATIONS FOR PA

- Conservative approaches:
  - expected lifetime 1000-10000 year ( $\ll$  copper)
  - $\gg$  corrosion:
    - 0.1  $\mu\text{m}/\text{year}$  cementitious alkaline conditions
    - 1-2  $\mu\text{m}/\text{year}$  in bentonite

## PREDICTION OF CONTAINER LIFETIMES & IMPLICATIONS FOR PA

- Conservative approaches:
  - expected lifetime 1000-10000 year (<< copper)
  - >> corrosion:
    - 0.1  $\mu\text{m}/\text{year}$  cementitious alkaline conditions
    - 1-2  $\mu\text{m}/\text{year}$  in bentonite

| Mode of corrosion            | France                                      | Belgium                                              | Switzerland                                  | Japan                                               | UK                       | Czech republic |
|------------------------------|---------------------------------------------|------------------------------------------------------|----------------------------------------------|-----------------------------------------------------|--------------------------|----------------|
| Anaerobic general corrosion  | Empirical corrosion rate                    |                                                      | Empirical corrosion rate and pitting factor  |                                                     | Empirical corrosion rate |                |
| Radiolysis-induced corrosion | Limit dose rate to 10 Gy hr <sup>-1</sup> . | No effect for dose rate of 25 Gy hr <sup>-1</sup> .  | Design requirement (<1 Gy hr <sup>-1</sup> ) | Limit dose rate to 3 Gy hr <sup>-1</sup>            |                          |                |
| Localised corrosion          |                                             | Reasoned argument based on passivity of surface film | Depth-dependent pitting factor               | Mass balance and extreme value statistical analysis |                          |                |
| SCC                          | Specify resistant material                  |                                                      | Exclude by reasoned argument                 |                                                     |                          |                |
| MIC                          |                                             |                                                      | Corrosion allowance based on mass transport  | Excluded by reasoned argument – negligible rate     |                          |                |

## FURTHER READING

- <https://www.ejp-eurad.eu/publications/eurad-d151-concord-initial-sota>
- King, F. (2014). "Predicting the Lifetimes of Nuclear Waste Containers." JOM 66(3).
- King, F. and M. Kolář (2018). "Lifetime Predictions for Nuclear Waste Disposal Containers." Corrosion 75(3).
- Svensk Kärnbränslehantering, A. (2010). Corrosion calculations report for the safety assessment SR-Site. SKB TR-10-66
- Nagra. (2002). Demonstration of disposal feasibility for spent fuel, vitrified high-level waste and long-lived intermediate-level waste. Nagra Report NTB 02-05.
- Performance Assessment for the Proposed High-Level Radioactive Waste Repository at Yucca Mountain, Nevada <https://www.sciencedirect.com/journal/reliability-engineering-and-system-safety/vol/122/suppl/C>